

Title (en)

REDUCING THE TEMPERATURE IN A REGENERATION ZONE OF A FLUID CATALYTIC CRACKING PROCESS

Publication

**EP 0195129 B1 19880817 (EN)**

Application

**EP 85116235 A 19851219**

Priority

US 70362585 A 19850220

Abstract (en)

[origin: EP0195129A1] A method for operating a fluid catalytic cracking unit comprising a regeneration zone and a reaction zone with a relatively reduced temperature in the regeneration zone while processing a high-coke-making hydrocarbon feedstock having a 50 volume percent distillation temperature greater than about 500 DEG F (260 DEG C) which method comprises contacting at conversion conditions the feedstock in a reaction zone with a fluidizable mixture of regenerated cracking catalyst and low-coke-make non-catalytic solid particles, comprising a refractory inorganic oxide, in a ratio of low-coke-make solid particles to cracking catalyst from about 1:100 to about 10:1, the low-coke-make solid particles having a surface area of less than about 5 m<sup>2</sup>/g and a coke making capability of less than about 0.2 weight percent coke in the ASTM standard method for testing cracking catalyst by microactivity (MAT); separating the resulting hydrocarbon products from the mixture of deactivated cracking catalyst and low-coke-make solid particles; recovering the hydrocarbon products; passing the mixture of cracking catalyst and low-coke-make solid particles to the regeneration zone for generation by removal of coke; and passing the resulting regenerated mixture of cracking catalyst and low-coke-make solid particles from the regeneration zone to the reaction zone to contact the feedstock as described above whereby the regeneration zone temperature is maintained at a reduced temperature as compared to an equivalent operation without the use of the low-coke-make solid particles while simultaneously not reducing the coke burning capacity of the regeneration zone or affecting the operation of the reaction zone.

IPC 1-7

**C10G 11/14**

IPC 8 full level

**C10G 11/00** (2006.01); **C10G 11/14** (2006.01); **C10G 11/18** (2006.01)

CPC (source: EP KR)

**C10G 11/04** (2013.01 - KR); **C10G 11/18** (2013.01 - EP KR)

Designated contracting state (EPC)

AT BE CH DE FR IT LI NL SE

DOCDB simple family (publication)

**EP 0195129 A1 19860924; EP 0195129 B1 19880817**; AT E36553 T1 19880915; AU 5120985 A 19860828; AU 572370 B2 19880505; BR 8600707 A 19861029; CA 1264693 A 19900123; CN 1004141 B 19890510; CN 86100906 A 19860903; CS 112186 A2 19870917; CS 257282 B2 19880415; DD 253576 A5 19880127; DE 3564445 D1 19880922; ES 550983 A0 19871216; ES 8801359 A1 19871216; GR 860160 B 19860521; HU 202905 B 19910429; HU T44066 A 19880128; IN 163843 B 19881126; JP H0349316 B2 19910729; JP S61192793 A 19860827; KR 860006526 A 19860911; KR 900000891 B1 19900217; NO 166454 B 19910415; NO 166454 C 19910724; NO 855323 L 19860902; PL 145514 B1 19880930; PL 258018 A1 19870518; SU 1436885 A3 19881107; ZA 859538 B 19860827

DOCDB simple family (application)

**EP 85116235 A 19851219**; AT 85116235 T 19851219; AU 5120985 A 19851213; BR 8600707 A 19860219; CA 497345 A 19851211; CN 86100906 A 19860201; CS 112186 A 19860218; DD 28713286 A 19860218; DE 3564445 T 19851219; ES 550983 A 19860117; GR 860100160 A 19860121; HU 69586 A 19860219; IN 1083DE1985 A 19851218; JP 3368286 A 19860218; KR 860001187 A 19860220; NO 855323 A 19851227; PL 25801886 A 19860219; SU 4020678 A 19860219; ZA 859538 A 19851212