

Title (en)
CIRCULAR ECONOMY FOR PLASTIC WASTE TO POLYETHYLENE AND CHEMICALS VIA REFINERY CRUDE UNIT

Title (de)
KREISLAUFWIRTSCHAFT FÜR KUNSTSTOFFABFÄLLE ZU POLYETHYLEN UND CHEMIKALIEN ÜBER RAFFINERIEROHSTOFFEINHEIT

Title (fr)
ÉCONOMIE CIRCULAIRE DE DÉCHETS PLASTIQUES EN POLYÉTHYLÈNE ET PRODUITS CHIMIQUES PAR L'INTERMÉDIAIRE D'UNE UNITÉ BRUTE DE RAFFINERIE

Publication
EP 4081616 A1 20221102 (EN)

Application
EP 20906532 A 20201223

Priority
• US 201962952655 P 20191223
• US 2020066792 W 20201223

Abstract (en)
[origin: US2021189250A1] Provided is a continuous process for converting waste plastic into recycle for polyethylene polymerization or for normal alpha olefins. The process comprises selecting waste plastics containing polyethylene and/or polypropylene and then passing the waste plastics through a pyrolysis reactor to thermally crack at least a portion of the polyolefin waste and produce a pyrolyzed effluent. The pyrolyzed effluent is separated into offgas, a naphtha/diesel fraction, a heavy fraction, and char. The naphtha/diesel fraction is passed to a crude unit in a refinery from which is recovered a straight run naphtha fraction (C5-C8) or a propane/butane (C3-C4) fraction. The straight run naphtha fraction, or propane and butane (C3-C4) fraction, is passed to a steam cracker for ethylene production. The ethylene is converted to normal alpha olefin and/or polyethylene. Also, a heavy fraction from the pyrolysis reactor can be combined with a heavy fraction of normal alpha olefin stream recovered from the steam cracker. The combined heavy fraction and heavy fraction of normal alpha olefin stream can be passed to a wax hydrogenation zone to produce wax.

IPC 8 full level
C10B 53/07 (2006.01); **C10B 57/06** (2006.01); **C10G 1/02** (2006.01)

CPC (source: EP KR US)
C07C 2/30 (2013.01 - US); **C07C 4/04** (2013.01 - EP KR US); **C08F 10/02** (2013.01 - US); **C10B 53/07** (2013.01 - US); **C10G 1/002** (2013.01 - EP KR US); **C10G 1/10** (2013.01 - EP KR US); **C10G 9/36** (2013.01 - EP KR); **C10G 50/00** (2013.01 - EP KR); **C10G 57/00** (2013.01 - EP KR); **C10G 73/02** (2013.01 - EP KR US); **C10G 73/44** (2013.01 - EP KR); **C10B 53/07** (2013.01 - EP KR); **C10G 2300/1003** (2013.01 - EP KR US); **C10G 2300/1044** (2013.01 - EP KR); **C10G 2300/1081** (2013.01 - EP KR); **C10G 2300/202** (2013.01 - US); **C10G 2300/205** (2013.01 - US); **C10G 2300/4006** (2013.01 - US); **C10G 2300/4012** (2013.01 - US); **C10G 2300/4018** (2013.01 - US); **C10G 2400/02** (2013.01 - EP KR US); **C10G 2400/04** (2013.01 - EP KR US); **C10G 2400/08** (2013.01 - US); **C10G 2400/20** (2013.01 - EP KR); **C10G 2400/22** (2013.01 - US); **Y02P 20/143** (2015.11 - KR); **Y02P 20/52** (2015.11 - EP KR); **Y02P 20/582** (2015.11 - EP KR); **Y02W 30/62** (2015.05 - KR)

C-Set (source: EP)
C07C 4/04 + **C07C 11/04**

Designated contracting state (EPC)
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Designated extension state (EPC)
BA ME

Designated validation state (EPC)
KH MA MD TN

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US 11518943 B2 20221206; US 2021189250 A1 20210624; BR 112022011773 A2 20220830; CA 3164217 A1 20210701; CA 3164217 C 20240423; CN 114867823 A 20220805; CN 114867823 B 20240213; EP 4081616 A1 20221102; EP 4081616 A4 20240228; JP 2023508355 A 20230302; KR 20220119410 A 20220829; MX 2022007306 A 20221021; US 11732197 B2 20230822; US 2023094207 A1 20230330; WO 2021133881 A1 20210701

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