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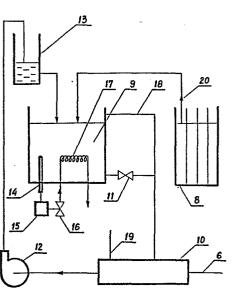
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 2 & 3
 D-8000 München 90(DE)
- [54] Method and device of conducting a closed cycle of the bath for plating of coatings.
- (57) The device for conducting a closed cycle of the electroplating bath, especially in the process of electroplating, comprising an electrolytic tank, an evaporation device connected with the electrolytic tank through a device feeding the electroplating bath, is characterized in that in the electrolytic tank or in the vicinity thereof heating devices (17) are comprised and in the evaporation chamber of the evaporation device (10) there are no heating devices, the evaporation chamber (2) of the evaporation device is horizontal and comprises a partition (3), the inlet (1) of the bath to the evaporation chamber is situated on the opposite side in relation to the partition (3), the evaporation chamber (2) comprises a perforated conduit (6) or conduits and/or conduits having porous walls, the evaporation chamber (2) is connected from the side of the partition (3) with a separator (4), the upper part of the separator (4) comprises a drop catcher (7), and the lower part of the separator (4) comprises a conduit (5) taking off the concentrated bath to the electrolytic tank (9), the heating device (17) in the tank being connected to a temperature-control system (14, 15, 16) for control of the temperature of the bath.



Instytut Mechaniki Precyzyjnej

EPAC-32047.8
July 12, 1984

Method and Device of conducting a closed cycle of the bath for plating of coatings

The subject of the invention is a method of conducting a closed cycle of the bath for plating 5 of coatings, especially in the process of electroplating, and devices for conducting a closed cycle of the bath for plating of coatings, especially in the process of electroplating.

The known methods of conducting a closed cyc10 le of the bath in the process of electroplating
consist usually in conducting the evaporative process. It is most often simed at evaporation of water used for rinsing and at obtaining a concentrated solution of the composition corresponding
15 to the composition of electroplating bath, after
which rinsing follows.

The known evaporative processes applied for this purpose are usually conducted at lowered pressure and indirect heating, most often at a rais20 ing film of the liquid. The application of vacuum

is simed at lowering the temperature of the process and at increasing the intensity thereof. This increases, however, the degree of difficulty of conducting the process and raises the cost of the process. Those skilled in the art know also vacuum processes with forced circulation, of still higher degree of complication and additionelly increased costs of conducting the process.

Another method of conducting the eveporative process is direct evaporation at atmospheric pressure. The feed is heated in an external heat exchanger, supplied upward to a column with a packing, wherein it evaporates, flowing down in the counter-current in relation to the flowing air.

It should be indicated that in all presently applied methods of evaporation the solution to be evaporated is heated in the evaporation zone.

20 le of beth in the process of electropleting comprise usually an evaporator. This is most often simed at evaporation of water used for rinsing and at obtaining a concentrated solution of the composition corresponding to the composition of electroplating bath, after which rinsing follows.

The known evaporators are, as a rule, vacuum devices, with an external heating chamber (indirect evaporators). Wost often they are the so-called evaporators with a raising film of the

liquid (of the compenies Pfaudler, Corning, Coe-mos). The application of vacuum is simed at lowering the temperature of the process and at increasing the intensity thereof. This raises, however, the cost of the device. Known also are vacuum circulating evaporators (of the Simex company).

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Another group of the applied evaporators are direct evaporators, in which evaporation proceeds at atmospheric pressure (evaporators of the Lancy company).

The feed is hested in the external hest exchanger, supplied upward to a column with a packing, wherein while flowing down in the counter-current in relation to the flowing air it evaporates.

In all presently applied methods of evaporation the heating chamber is an integral part of the evaporator.

The cost of hitherto applied methods and devices is considerable, especially in the case of chemically aggressive baths, e.g. the chromium plating bath. In the case of aggressive baths, heating elements of the evaporator should be made of special borosidicate glass (Simex company) or of special materials, e.g. titanium, tantalum.

Auxiliary equipment must be of special design (e.g. pumps) etc.

For example, the cost of the evaporator of Corning company, of the yield of Q=67 1 of evaporated liquid/hr is of the order of US \$ 20,000 (1977).

Such a considerable investment cost, in spite of economic management of the whole enterprise and obvious effects of environmental protection, sets back the progress of the new technique of utilization of wastes.

The task of the invention is to work out a method and a device for pumping off the bath, comprising an appropriate evaporation device, so that it is possible to achieve the required evaporation of water from the system at the minimum costs.

The method of conducting a closed cycle of the beth for pleting of costings, especially in the process of electropleting, consists in feeding the both from the electrolytic mechining zo-15 ne to the evaporation zone, and from the evaporation zone - after concentration of the bath in the evaporation zone - back to the electrolytic mechining zone, and according to the essence of the invention it is characterized by that the 20 electroplating bath is heated in the electrolytic mechining zone and is introduced to the evaporation zone in which the bath is conducted in s flow in a thin layer horizontally, whereby in the whole eveporation zone or only in a part the-25 reof through the horizontally conducted bath air is conducted from below upwerds by berbotege, eventually, the conducted air is heated and afterwards wet air conducted through the beth is taken off outside from the circulation after pre-30 vious separation of entrained particles by the

inertia method, and the concentrated solution from the evaporation zone is fed back to the electrolytic machining zone, the electroplating bath being made up in a continuous way by washings from a water washer for rinsing of objects after the said electroplating bath.

According to the invention it is preferable that the electroplating bath is heated in the
electrolytic machining zone, supplying in the said
zone at least 25% of heat necessary for evaporation in the evaporation zone. In this case the remaining amount of necessary heat is supplied to
air which passes through the bath in the evaporation zone. by barbotage.

15 According to the invention it is advisable to introduce to the evaporation zone at least 55% of the volume of the electroplating bath.

It is preferable, according to the invention, to introduce to the electroplating bath at least 20 55% of the volume of washings after rinsing of objects treated in the said electroplating bath.

According to the invention it is advisable that the air taken off outside from the circulation is used for mixing the rinsing water in washers for washing the objects after the said electroplating bath.

It is preferable, according to the invention, that the air taken off outside from the circulation, after adding water vapour thereto, is used for washing the objects after the said electroplating bath.

According to the invention it is edvisable that from wet air conducted through the bath, taken off soutside from the circulation, water is condensed off and said condensed-off water is used as washing water in washers.

The device for conducting a closed cycle of the bath for plating of costings, especially in the process of electropleting, comprising an electrolytic tank, an evaporation device connected with the electrolytic tenk through a device feeding the electroplating both, preferably an air lift pump, according to the essence of the invention is characterized by that in the electrolytic tenk heeting devices are comprised, and in 15 the evaporation chamber of the evaporation device there are no heating devices, the evaporation chamber of the evaporation device is horizontal and comprises a partition whose height establishes the thickness of the layer of the liquid, the 20 both inlet to the evaporation chamber is at the opposite side in relation to the pertition, the evaporation chamber comprises a perforated conduit or conduits and/or conduits with porous walls, through which sir is supplied to the evaporated both, eventually heated sir, the evaporation chamber is from the side of the partition connected with a separator, the upper part of the separator comprises a drop catcher through which wet air is taken off, and the lower part of the separator comprises a conduit taking off the concentrated 30

beth to the electrolytic tenk, whereby the heeting device in the tenk is connected to the tempereture-control system to control the temperature of the bath.

It is preferable that the constructional material for building the evaporation device is polyvinyl chloride.

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It is edvisable that the drop cetcher is of a labyrinth type and comprises air-flow guide vanes.

According to the invention only the bath is evaporated, and heat necessary to heat the liquid is supplied, in principle, only to the both in the electrolytic tank or in the vicinity thereof, with the use of the heating element being the standard equipment of the said tank, or only the air introduced to the evaporation zone is heated. When the evaporator is assembled with the already operating electroplating equipment, we use the heating element elreedy existing in the electrolytic mechining zone. Due to this, in newly designed lines we avoid doubling the hesting elements. The method according to the invention reduces also the number of devices necessary for sutomatic control of the working parameters of the bath. If necessary for power reasons, additional heating is employed, with the supply of hest power being the complement between the hest power of the elreedy existing equipment and the heat power

necessary to conduct evaporation with the required yield.

According to the invention, evenoration is effected directly, by letting the air pass through the bath being evenorated flowing in a closed channel, being in the phase of dynamic foam.

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The solution sccording to the invention is described in the example of reclisation by means of the drawing of the exemplary device, which serves for realisation of the method. Fig.1 presents e schematic device together with a washer and a feeding tank, and fig.2 presents schematically a single evaporation module applied for realisation according to the invention and marked in fig.1 with number 10. The feed is supplied by a stub pipe 1, it flows by a flow pipe 2, overflows through e pertition 3, and from a separator 4 is taken off by a stub pipe 5. In the evaporated solution, parellel to the exis of the pipe 2, a supply pipe 6 of air is immersed, said air, passing through the solution, causes barbotege and evaporation thereof. The drop cetcher 7 errests perticles of the solution entrained by air. As materials for building the device polyvinyl chloride pipes are usually used.

Such a solution has a number of advantages in relation to the existing devices.

The device and the method are characterized by big design simplicity, essiness of execution, simple operation and failure-free work during use.

On the basis of one standard module, such as shown in the example in fig.1, it is possible to build to the device according to the invention multi-module evaporators of the required yield, usualby to about 100 l/hr of the evaporated liquid.
Such evaporators require little space and can be easily compiled with the already operating electroplating line. In laboratory conditions the operation of one module of the evaporator presented in fig.1, of the length of the pipe 2 of D=70 mm and the length of the evaporation zone l=0.5 m.

In the second experiment two modules of the eveporator were used for closing the material circulation after chromium plating in a small electroplating plant working in a semi-technical scale. Perameters of a single module: D=110 mm, 1=1200 mm.

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As shown in fig.2, washings from washers 8 are directed as a whole by a conduit 20 to an electrolytic tank 9. The rate of flow of the bath through the evaporator 10 is controlled by the valve 11. The device has an emergency overflow whose overflow conduit is marked in fig.2 with number 18. After evaporation, the bath is supplied by the pump 12 to the feeding tank 13 wherefrom it flows to 25 the tank 9. The temperature in the tank is controlled by a temperature-control system consisting of elements 14, 15, 16, 17. The outlet of air from the evaporation module is marked with number 19. Total evaporation from two modules connected parallely was 10 1/hr. It enables closing the material circulation of the electroplating plant.

Fig. 2 does not snow ion-exchange columns whrough which washings flow in order to eliminate impurities, mainly ions Cr^{34} , Fe^{3+} .

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1. A method of conducting a closed cycle of the bath for plating of coatings, especially in the process of electropleting, consisting in feeding the bath from the electrolytic machining zone to the eveporation zone, and from the evaporation zone efter concentration of the bath in the evaporation zone back to the electrolytic machining zone, characterized in that the electroplating both is hested in the electrolytic machining zone and is introduced to the evaporation zone in which the beth in conducted in the flow in a thin film horizontally, whereby in the whole evaporation zone or only in a part thereof through the horizontally conducted bath from below upwards air is conducted by berbotege, eventually, the air being conducted is hested, and afterwards wet air conducted through the bath is taken off outside from the circulation after previous separation of entreined perticles by the inertie method, and the concentrated solution from the evaporation zone is introduced back to the electrolytic mechining zone, and thereefter the electroplating bath is made up in a continuous way with weshings from the water washer for washing the objects after said electroplating bath.

7. / method according to claim 1, characterized in that the electroplating both is heated in the electrolytic machining zone, at least 25% of heat necessary for evaporation in the evaporation zone being supplied in the said zone.

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- 3. A method eccording to claim 1, characterized in that to the evaporation zone at least 55% of the volume of the electroplating both is fed.
- 4. A method according to claim 1, characterized in that
 to the electroplating bath at least 55% of the volume of washings after washing of objects treated
 in the said electroplating bath is fed.
 - 5. A method according to claim 1, characterized in that air taken off outside from the circulation is used for mixing of washing water in washers for washing the objects after the said electroplating bath.
 - 6. A method according to claim 1, characterized in that air taken off outside from the circulation is, after adding water vapour thereto, used for washing the objects after the said electroplating bath.
- 7. A method according to claim 1, characterized in that from wet air conducted through the bath, taken off outside from the circulation, water is condensed off and said condensed-off water is used as weshing water in washers.

- 8. A device for conducting a closed cycle of the bath for plating of coatings, especially in the process of electroplating, comprising an electrolytic tank, an evaporation device connected with the 5 electrolytic tank through a device feeding the electroplating bath, preferably an air lift pump, cheracterized in that . the electrolytic tenk comprises heating devices (17) and in the evaporation chamber of the evaporation device (10) there are no heating devices, the evaporation chamber 10 (2) of the eveporation device is horizontal and comprises a partition (3) whose height establishes the thickness of the horizontal layer of the bath, the inlet (1) of the bath to the evaporation chember is at the opposite side in relation 15 to the partition (3), the evaporation chamber (2) comprises a perforated conduit (6) or conduits and/or conduits having porous walls, through which to the evaporated bath air is fed, eventually heated sir, the eveporation chember (2) is connec-20 ted from the side of the pertition with a sepsrator (4), the upper part of the separator (4) comprises a drop catcher (7) through which wet eir is taken off, and the lower part of the seperator (4) comprises a conduit (5) taking off the concentrated bath to the tank (9), the heating device (17) being connected to the temperature--control system (14, 15, 16) for controlling the temperature of the bath.
- 30 9. A device according to claim 8, characterized in that the constructional material to build the evaporation device is polyvinyl chloride.
 - 10. A device according to claim 8, characterized in that the drop catcher (7) is of the labyrinth type and comprises air-flow guide vanes.

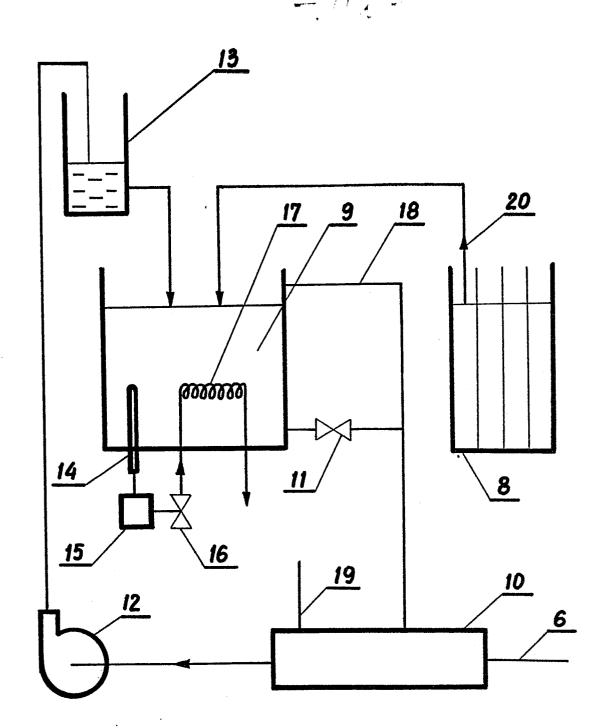
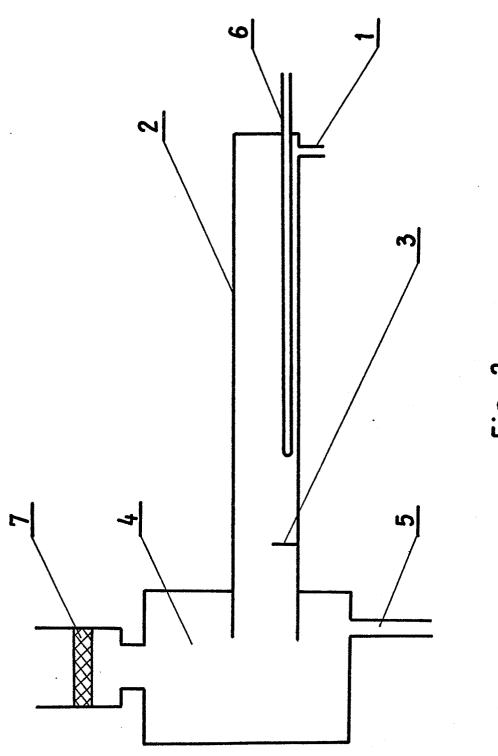


Fig. 1



r19. 2



EUROPEAN SEARCH REPORT

DOCUMENTS CONSIDERED TO BE RELEVANT				EP 84108238.1	
Category		indication, where appropriate, ant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.4)	
A			1,8	C 25 D 21/00 C 25 D 21/10 C 25 D 21/18	
A	DE - B2 - 2 729	 9 270 (H. STOLLE) g. *	1	C 25 D 17/00 C 25 D 19/00 C 23 G 1/36	
A	DE - B2 - 1 962 * Claims; f:	2 249 (NORDNERO AB)	1		
A	<u>US - A - 3 623</u> * Claims; f:	962 (L.C. BEALE)	1,8		
A	EP - A1 - O O79 KAISHA SANSHIN	 9 987 (KABUSHIKI SEISAKUSHO)	1,8	TECHNICAL FIELDS SEARCHED (Int. Cl.4)	
	* Claims; f:	ig. 2-4 *		C 25 D C 23 G	
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	The present search report has b	een drawn up for all claims			
Place of search		Date of completion of the search	<u> </u>	Examiner	
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