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54 **PROCESS FOR SIMULTANEOUSLY DIMERIZING ETHYLENE AND COPOLYMERIZING ETHYLENE WITH THE DIMERIZED PRODUCT.**

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EP-A- 0 004 647
US-A- 3 526 616
US-A- 4 329 255

Journal of Polymer Science: Polymer Chemistry Edition, vol. 22, November 1984, D.L. Beach et al.: "Dual functional catalysis for ethylene polymerization to branched polyethylene. I. Evaluation of catalytic systems", pp. 3027-3042

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Description

Field of the Invention

This invention relates to a process for producing copolymers of ethylene and butene-1 wherein the butene-1 comonomer is generated in situ within the polymerization reactor by a separately catalyzed ethylene dimerization reaction.

Background of the Invention

Recently a low cost fluidized bed process for producing ethylene polymers having a density of from 0.86 g/cm³ to 0.96 g/cm³ was introduced into the marketplace. This process, which met with immediate success and has now become the industry standard, comprises continuously copolymerizing ethylene with one or more higher alpha olefin monomers, usually butene, by means of a catalyst composition prepared by (1) forming a precursor composition from a magnesium compound, titanium compound and electron donor compound, (2) diluting said precursor composition with an inert carrier material, and (3) activating the precursor composition with an organoaluminum compound. Such process is more completely described in U.S. patents 4 302 565, 4 302 566 and 4 303 771, and European patent publication 0 120 503.

While this process has substantially reduced the cost of producing ethylene polymers, the cost still remains higher than desired because of the relatively high cost of the higher alpha olefin comonomer employed in the process vis-a-vis the cost of ethylene, particularly in those areas of the world where the disparity in price between such comonomer and ethylene is substantial. In view of this, it would be desirable to reduce the cost of producing such comonomer in order to further reduce the cost of the process and the polymers produced thereby.

One method suggested for producing higher alpha olefin comonomer comprises oligomerizing ethylene to higher alpha olefins, e.g., dimerizing ethylene to produce butene. Such dimerization has only infrequently been attempted in situ during the polymerization of ethylene, however, because of the difficulty of producing a compatible dimerization and polymerization system, i.e., one wherein the dimerization catalyst and polymerization catalyst operate under the same reaction conditions and do not interfere with each other chemically. Such in situ dimerization would be desirable, however, as a means of eliminating one of the comonomers employed, simplifying the polymerization process, and reducing the overall cost of the polymers produced.

One means of simultaneously dimerizing ethylene in situ and copolymerizing ethylene with the dimerized product has been suggested in U.S. patent 4 133 944. This method employs a transition metal catalyst, such as a Ziegler-type catalyst, together with a dimerization catalyst, such as a titanium alkoxide, and an alkylaluminum compound, for this purpose and requires temperatures of from 100°C to 350°C and pressures of from 300-1000 kgm/cm².

While U.S. patent 3 526 616 suggests that simultaneous in situ dimerization and copolymerization of

ethylene can be effected by means of a similar catalyst under milder temperature and pressure conditions, this patent requires that the transition metal compound employed be reacted with a bivalent metal hydroxychloride support in order to effect dimerization under such conditions.

The simultaneous in situ dimerization and copolymerization of ethylene with similar catalysts under mild temperature and pressure conditions has also been taught by David L. Beach and Yury V. Kissin [Dual Functional Catalysis for Ethylene Polymerization to Branched Polyethylene. I. Evaluation of Catalytic Systems, *Journal of Polymer Science: Polymer Chemistry Edition*, Vol. 22, 3027-3042 (1984)]. This reference further teaches that while solubilized titanium alkoxides produce fairly active dimerization catalysts, insolubilized compounds make ineffective catalysts. Thus, this system depends upon the presence of a solvent for its effectiveness, and suggests that such system is not effective in a gas phase fluid bed process.

Summary of the Invention

In accordance with the present invention it has now been discovered that ethylene can be simultaneously dimerized to produce butene-1 and copolymerized with the dimerized product in a gas phase fluidized bed process by means of a catalyst system comprising (a) a titanium tetraalkoxide, (b) a supported magnesium-titanium-based composition, and (c) a trialkylaluminum compound. Such process eliminates the use of comonomers other than ethylene, simplifies the polymerization process, and reduces the overall cost of the polymers produced.

Description of the Preferred Embodiment

Surprisingly, the simultaneous dimerization of ethylene and copolymerization of ethylene with the dimerized product has been found to proceed smoothly and efficiently under mild conditions of temperature and pressure in the absence of a solvent without mutual interference between the dimerization and polymerization catalysts employed in the process. As a result, polymerization activity remains high, and ethylene copolymer having excellent morphological properties required for successful operation in a fluidized bed is produced in high yield. One would not have expected such results in the absence of the various precautions followed by the prior art.

Although some cis and some trans butene-2, as well as other ethylene oligomers, are produced by the process, the dimerization reaction proceeds with high selectivity and results in the production of butene-1 at a selectivity in excess of 80 percent, usually in excess of 85 percent. Among the butene isomers produced by the process, butene-1 is produced at a selectivity in excess of 85 percent, usually in excess of 90 percent.

The titanium tetraalkoxide employed in the process serves as the dimerization catalyst for ethylene when activated with the trialkylaluminum compound. The titanium tetraalkoxides which are employed include those having the formula



wherein each R is a hydrocarbon radical free from aliphatic unsaturation, which radicals may be the same or different. Each R radical contains from 1 to 12 carbon atoms, usually from 1 to 6 carbon atoms. Such radicals may be aromatic, or cyclic, branched or straight chain aliphatic, and may be substituted with any substituent which is nonreactive with all the components of the catalyst composition and all other active components of the reaction system. Illustrative of such radicals are methyl, ethyl, *n*-propyl, isopropyl, *n*-butyl, isobutyl, tert-butyl, *n*-hexyl, cyclohexyl, 2-ethyl-hexyl, *n*-octyl, *n*-decyl, phenyl, tolyl, xylyl, and the like.

The titanium tetraalkoxide compounds can be used individually or in combination thereof, and include compounds such as titanium tetramethoxide, titanium tetraethoxide, titanium tetra-*n*-propoxide, titanium tetraisopropoxide, titanium tetra-*n*-butoxide, titanium tetraisobutoxide, titanium tetra-*n*-hexoxide, titanium tetracyclohexoxide, titanium tetra-2-ethylhexoxide, titanium tetra-*n*-octoxide, titanium tetra-*n*-decoxide, titanium tetraphenoxide, titanium tetratoloxide, and titanium tetraxyloxiide. Titanium tetraisobutoxide is particularly preferred.

The magnesium-titanium-based composition employed in the process serves as the polymerization catalyst for ethylene when activated with the trialkylaluminum compound. Such composition is formed by dissolving at least one titanium compound and at least one magnesium compound in at least one electron donor compound at a temperature of from about 20°C up to the boiling point of the electron donor compound. The titanium compound(s) can be added to the electron donor compound(s) before or after the addition of the magnesium compound(s), or concurrent therewith. The dissolution of the titanium compound(s) and the magnesium compound(s) can be facilitated by stirring, and in some instances by refluxing, these two compounds in the electron donor compound(s). After the titanium compound(s) and the magnesium compound(s) are dissolved, the resulting product may be isolated by crystallization or by precipitation with an aliphatic or aromatic hydrocarbon containing from 5 to 8 carbon atoms, such as hexane, isopentane or benzene. The crystallized or precipitated product may be recovered as fine, free-flowing particles having an average particle size of from about 10 microns to about 100 microns after drying at temperatures up to 60°C.

About 0.5 mol to about 56 mols, and preferably about 1 mol to about 10 mols, of the magnesium compound(s) are used per mol of the titanium compound(s) in preparing this product.

The titanium compound(s) employed in preparing the magnesium-titanium-based composition has the structure



wherein R' is an aliphatic or aromatic hydrocarbon radical containing from 1 to 14 carbon atoms, or COR'' where R'' is an aliphatic or aromatic hydrocarbon radical containing from 1 to 14 carbon atoms,

X is selected from the group consisting of Cl, Br, I, and mixtures thereof,

a is 0, 1 or 2, b is 1 to 4 inclusive, and a + b = 3 or 4.

Suitable titanium compounds include TiCl₃, TiCl₄, Ti(OCH₃)Cl₃, Ti(OC₆H₅)Cl₃, Ti(OCOCH₃)Cl₃ and Ti(OCOC₆H₅)Cl₃. TiCl₃ is preferred because catalysts containing this material show particularly high activity at the temperatures employed in the process of the present invention.

The magnesium compound(s) employed in preparing the magnesium-titanium-based composition has the structure



wherein X is selected from the group consisting of Cl, Br, I, and mixtures thereof.

Suitable magnesium compounds include MgCl₂, MgBr₂ and MgI₂. Anhydrous MgCl₂ is particularly preferred.

The electron donor compound(s) employed in preparing the magnesium-titanium-based composition is an organic compound which is liquid at 25°C and in which the titanium and magnesium compounds are soluble. The electron donor compounds are known as such, or as Lewis bases.

The electron donor compounds are selected from the group consisting of alkyl esters of aliphatic and aromatic carboxylic acids, aliphatic ethers, cyclic ethers and aliphatic ketones. Among these electron donor compounds the preferable ones are alkyl esters of saturated aliphatic carboxylic acids containing from 1 to 4 carbon atoms; alkyl esters of aromatic carboxylic acids containing from 7 to 8 carbon atoms; aliphatic ethers containing from 2 to 8 carbon atoms, preferably from 4 to 5 carbon atoms; cyclic ethers containing from 4 to 5 carbon atoms, preferably mono- or di-ethers containing 4 carbon atoms; and aliphatic ketones containing from 3 to 6 carbon atoms, preferably from 3 to 4 carbon atoms. The most preferred of these electron donor compounds include methyl formate, ethyl acetate, butyl acetate, ethyl ether, tetrahydrofuran, dioxane, acetone and methyl ethyl ketone.

After the magnesium-titanium-based composition has been prepared it is diluted with an inert carrier material by (1) mechanically mixing or (2) impregnating such composition into the carrier material.

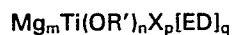
Mechanical mixing of the inert carrier and the magnesium-titanium-based composition is effected by blending these materials together using conventional techniques. The blended mixture suitably contains from about 3 percent by weight to about 50 percent by weight of the magnesium-titanium-based composition.

Impregnation of the inert carrier material with the magnesium-titanium-based composition may be accomplished by dissolving the magnesium-titanium-based composition in the electron donor compound, and then admixing the carrier with the dissolved composition. The solvent is then removed by drying at temperatures up to about 85°C.

The carrier may also be impregnated with the magnesium-titanium-based composition by adding the carrier to a solution of the chemical raw materials used to form said composition in the electron donor compound, without isolating said composition from

said solution. The excess electron donor compound is then removed by drying at temperatures up to about 85°C. Suitably, the impregnated carrier material contains from about 3 percent by weight to about 50 percent by weight, preferably from about 10 percent by weight to about 30 percent by weight, of the magnesium-titanium-based composition.

When prepared as disclosed above the blended or impregnated magnesium-titanium-based composition has the formula



wherein R' is an aliphatic or aromatic hydrocarbon radical containing from 1 to 14 carbon atoms, or COR'' wherein R'' is also an aliphatic or aromatic hydrocarbon radical containing from 1 to 14 carbon atoms,

X is selected from the group consisting of Cl, Br, I, and mixtures thereof,

ED is an electron donor compound,

m is 0.5 to 56, preferably 1.5 to 5,

n is 0, 1 or 2,

p is 2 to 116, preferably 6 to 14, and

q is 2 to 85, preferably 3 to 10.

The carrier materials employed to dilute the magnesium-titanium-based composition are solid, particulate, porous materials which are nonreactive with all the other components of the catalyst composition and all other active components of the reaction system. These carrier materials include inorganic materials, such as oxides of silicon and/or aluminum, and phosphates of aluminum. The carrier materials are used in the form of dry powders having an average particle size of from about 10 microns to about 250 microns, preferably from about 20 microns to about 150 microns. These materials are also porous and have a surface area of at least 3 square meters per gram, and preferably at least 50 square meters per gram. Polymerization activity of the catalyst, i.e., productivity, can be improved by employing a silica support having an average pore size of at least 80 Angstrom units, preferably at least 100 Angstrom units. The carrier material should be dry, that is, free of absorbed water. Drying of the carrier material can be effected by heating, e.g., at a temperature of at least 600°C when silica is employed as the support. Alternatively, when silica is employed, it may be dried at a temperature of at least 200°C and treated with about 1 weight percent to about 8 weight percent of one or more of the organoaluminum activator compounds described below. Modification of the support with an aluminum compound in this manner provides the catalyst composition with increased activity and also improves particle morphology of the resulting ethylene copolymers. Other organometallic compounds, such as diethylzinc, may also be used to modify the support.

In order for the titanium tetraalkoxide to be useful as a dimerization catalyst, and for the magnesium-titanium-based composition to be useful as a polymerization catalyst, they must be activated with a compound capable of transforming the titanium atoms of these materials to a state which will effect the desired dimerization and polymerization reac-

tions. Such activation is effected by means of a trialkylaluminum compound having the formula

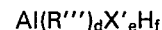


wherein each R''' is a saturated hydrocarbon radical containing from 1 to 14 carbon atoms, which radicals may be the same or different. Such radicals may be substituted with any substituent which is non-reactive with all the components of the catalyst composition and all other active components of the reaction system.

The activator compounds can be employed individually or in combination thereof, and include compounds such as $\text{Al}(\text{C}_2\text{H}_5)_3$, $\text{Al}(\text{i-C}_4\text{H}_9)_3$, $\text{Al}(\text{C}_6\text{H}_{13})_3$ and $\text{Al}(\text{C}_8\text{H}_{17})_3$. Triisobutylaluminum is particularly preferred because titanium tetraalkoxides activated with this material show particularly high dimerization activity.

If desired, the magnesium-titanium-based composition may be partially activated before it is introduced into the polymerization reactor. However, any activation undertaken outside of the polymerization reactor should be limited to the addition of an amount of activator compound which does not raise the molar ratio of activator compound:electron donor in the magnesium-titanium-based composition beyond 1.4:1. Preferably, when activation is effected outside the reactor in this manner, the activator compound is employed in an amount which will provide the magnesium-titanium-based composition with an activator compound:electron donor molar ratio of from about 0.1:1 to about 1.0:1. Such partial activation is carried out in a hydrocarbon solvent slurry followed by drying of the resulting mixture, to remove the solvent, at temperatures of from about 20°C to about 80°C, preferably from about 50°C to about 70°C. The resulting product is a free-flowing solid particulate material which can be readily fed to the polymerization reactor where activation is completed with additional activator compound.

Partial activation of the magnesium-titanium-based composition before it is introduced in the polymerization reactor may be effected by means of organoaluminum compounds having the formula



wherein X' is Cl or OR''',

R''' and R'''' are saturated hydrocarbon radicals containing from 1 to 14 carbon atoms, which radicals may be the same or different, and, if desired, substituted with any substituent which is nonreactive with all the components of the catalyst composition and all other active components of the reaction system,

e is 0 to 1.5,

f is 0 or 1, and

d + e + f = 3.

Such activator compounds can be employed individually or in combination thereof and include compounds such as $\text{Al}(\text{C}_2\text{H}_5)_3$, $\text{Al}(\text{C}_2\text{H}_5)_2\text{Cl}$, $\text{Al}_2(\text{C}_2\text{H}_5)_3\text{Cl}_3$, $\text{Al}(\text{C}_2\text{H}_5)_2\text{H}$, $\text{Al}(\text{C}_2\text{H}_5)_2(\text{OC}_2\text{H}_5)$, $\text{Al}(\text{i-C}_4\text{H}_9)_3$, $\text{Al}(\text{i-C}_4\text{H}_9)_2\text{H}$, $\text{Al}(\text{C}_6\text{H}_{13})_3$ and $\text{Al}(\text{C}_8\text{H}_{17})_3$.

Alternatively, when the magnesium-titanium-based

composition is impregnated in the inert carrier, it may, if desired, be completely activated in the polymerization reactor without any prior activation outside of the reactor, in the manner described in U.S. patent 4 383 095.

The titanium tetraalkoxide, the partially activated or totally unactivated magnesium-titanium-based composition, and the required amount of activator compound necessary to complete activation of both titanium materials are usually introduced into the reactor through separate feed lines in order to more effectively control the amount of each of these materials in the reactor. However, if desired, any two or all three materials can be added together. If desired, the titanium tetraalkoxide may even be impregnated upon the same inert carrier as the magnesium-titanium-based composition. However, if the magnesium-titanium-based composition is to be partially activated with an organoaluminum compound before it is introduced into the reactor, it should be partially activated before the titanium tetraalkoxide is impregnated over it.

Both the titanium tetraalkoxide and activator compound employed are conveniently and preferably sprayed into the reactor dissolved in an inert liquid solvent, i.e., a solvent which is nonreactive with all the components of the catalyst composition and all other active components of the reaction system. Hydrocarbons such as isopentane, hexane, heptane, toluene, xylene, naphtha and mineral oil are preferred for this purpose. Generally, the titanium tetraalkoxide solution employed contains from 0.1 weight percent to 75 weight percent of such compound, usually from 5 weight percent to 40 weight percent of such compound, while the solution containing the activator compound generally contains from 5 weight percent to 75 weight percent of such compound. If desired, less concentrated or more concentrated solutions can be employed, or, alternatively, the titanium tetraalkoxide and activator compound can be added in the absence of solvent.

Any solvent employed to introduce the titanium tetraalkoxide and activator compound into the reactor is, of course, immediately vaporized in the reactor so that gaseous conditions are maintained in the reactor at all times. The amount of solvent employed should, of course, be carefully controlled so as to avoid the use of excessive quantities of liquid which would prevent the rapid vaporization thereof.

The activator compound is added to the reactor in such amounts as to provide a total aluminum:titanium atomic ratio of from about 5:1 to about 500:1. While high ratios result in good copolymer production rates, such ratios also cause significant deactivation of the dimerization catalyst as well as a high degree of ethylene hydrogeneration. For this reason, it is preferred to maintain an aluminum:titanium atomic ratio of from about 5:1 about 150:1.

The amount of titanium tetraalkoxide employed in the process depends upon the amount of butene-1 desired for copolymerization with ethylene. The greater the amount of butene-1 desired for copolymerization with ethylene, the greater the amount of titanium tetraalkoxide that must be employed. By the addition of progressively larger

amounts of titanium tetraalkoxide to the reactor, copolymers having progressively lower densities are obtained at any given melt index. However, since the polymerization activity of the magnesium-titanium-based catalyst component decreases as the concentration of titanium tetraalkoxide increases, excessive amounts of titanium tetraalkoxide should be avoided. Of course, if desired, in order to avoid this problem, or for any other reason, it is possible to add butene to the reactor from an external source rather than generating it completely in situ. If desired, this butene may be produced by the dimerization of ethylene employing the dimerization catalyst and procedure described herein, but in the absence of the ethylene polymerization catalyst. Although the dimerization reaction and polymerization reaction proceed side by side in the presence of both the dimerization catalyst and the polymerization catalyst, the two reactions are entirely independent of each other, and each is capable of proceeding independently of the other in the absence of the catalyst for the complementary reaction. Hence, it is possible to independently dimerize ethylene outside the reactor using only a dimerization catalyst and employ the dimerized product together with dimer generated in situ in the reactor in the presence of both the dimerization catalyst and the polymerization catalyst. As long as the total concentration of butene in the reactor remains constant, the copolymer product is not influenced by the source of the butene. The reaction conditions employed for the dimerization of ethylene in the absence of the ethylene polymerization catalyst are the same as those employed in its presence, except that in the absence of the polymerization catalyst, the activator compound may be employed in a somewhat lesser amount. The amount used must provide an aluminum:titanium ratio of as little as about 4:1 to 500:1.

The titanium tetraalkoxide is employed in the process in an amount which will provide an atomic ratio of titanium in the titanium tetraalkoxide to titanium in the magnesium-titanium-based composition of from about 0.01:1 to about 50:1. In order to produce copolymers having a density of greater than about 0.94 g/cm³ up to about 0.96 g/cm³, a ratio of from about 0.01:1 up to about 2:1 is normally required. Ratios of greater than about 2:1 to about 20:1 usually result in copolymers having a density of from about 0.91 g/cm³ up to about 0.94 g/cm³. Densities of less than about 0.91 g/cm³ generally require a ratio greater than about 20:1 up to about 50:1 for densities as low as about 0.86 g/cm³. In order to produce copolymers having a density of less than about 0.91 g/cm³, however, it is necessary to follow the precautions set forth in European patent publication 0 120 503, by Frederick John Karol et al., entitled «Preparation of Low Density, Low Modulus Ethylene copolymers In A Fluidized Bed».

The simultaneous dimerization of ethylene and copolymerization of ethylene with the dimerized product is effected, according to the present invention, in a continuous, fluidized bed process by continuously contacting ethylene gas with a catalytically effective amount of the catalyst system of the present invention in a fluidized bed reactor. In

accordance with the process, discrete portions of the catalyst components are continually fed to the reactor together with ethylene gas while polymer product is continually removed during the continuing process. Fluid bed reactors suitable for continuously preparing ethylene copolymers have been previously described and are well known in the art. Fluid bed reactors useful for this purpose are described, e.g., in U.S. patents 4 302 565, 4 302 566 and 4 303 771.

If desired, the ethylene gas feed may be diluted with an inert gas, i.e., a gas which is nonreactive with all the components of the catalyst composition and all other active components of the reaction system. The gaseous reaction mixture should, of course, be substantially free of catalyst poisons, such as moisture, oxygen, carbon monoxide, carbon dioxide, acetylene and the like.

Hydrogen may also be added to the reaction mixture as a chain transfer agent to regulate molecular weight. Generally, hydrogen is added to the reaction mixture in an amount sufficient to produce a hydrogen:ethylene mol ratio of from about 0.01:1 to about 5:1. In addition to hydrogen, other chain transfer agents may be employed to regulate the molecular weight of the copolymers.

The simultaneous dimerization of ethylene and copolymerization of ethylene with the dimerized product is readily effected at a temperature of from about 30°C to about 115°C. The temperature employed, of course, must be maintained below the sintering temperature of the copolymers produced in order to prevent polymer agglomeration. When copolymers having a density of from 0.91 g/cm³ to 0.96 g/cm³ are desired, temperatures of from about 75°C to about 115°C, preferably from about 75°C to about 100°C, are usually employed. When producing copolymers having a density of less than 0.91 g/cm³, lower temperatures of from about 30°C to about 80°C, preferably from about 40°C to about 60°C, should be employed because of the lower sintering temperature of the product. In the latter case, it is also necessary to dilute the reaction mixture with a large quantity of a diluent gas to help prevent agglomeration and sustain polymerization on a continuous basis, as described in European patent publication 0 120 503, by Frederick John Karol et al, *supra*.

Pressures of up to about 7000 kPa can be employed in the process, although pressures of from about 70 kPa to about 2500 kPa are preferred. The ethylene partial pressure is preferably maintained between about 56 kPa to about 1900 kPa.

In order to maintain a viable fluidized bed, the superficial gas velocity of the gaseous reaction mixture through the bed must exceed the minimum flow required for fluidization, and preferably is at least 0.06 meter per second above the minimum flow. Ordinarily the superficial gas velocity does not exceed 1.5 meters per second, and most usually no more than 0.75 meters per second is sufficient.

The copolymers produced in accordance with the process of the present invention usually have a density of from 0.86 g/cm³ to 0.96 g/cm³. Such copolymers contain from about 50 mol percent to about 99 mol percent of polymerized ethylene, and

from about 1 mol percent to about 50 mol percent of polymerization butene-1.

The ethylene copolymers produced in accordance with the process of the present invention have a standard or normal load melt index of from 0 g/10 minutes to about 100 g/10 minutes, preferably of from about 0.2 g/10 minutes to about 80 g/10 minutes. Such polymers have a high load melt index (HLMI) of from greater than 0 g/10 minutes to about 2500 g/10 minutes. The melt index of a polymer varies inversely with its molecular weight and is a function of the polymerization temperature of the reaction, the density of the polymer, and the hydrogen/ethylene ratio in the reaction system. Thus, the melt index is raised by increasing the polymerization temperature and/or by increasing the hydrogen/ethylene ratio.

The ethylene copolymers produced in accordance with the process of the present invention have a melt flow ratio (MFR) of from about 22 to about 40, preferably of from about 25 to about 35. Melt flow ratio is another means of indicating the molecular weight distribution (M_w/M_n) of a polymer. An MFR in the range of from about 22 to about 40 corresponds to a M_w/M_n of from about 2.7 to about 6.5, and an MFR in the range of from about 25 to about 35 corresponds to a M_w/M_n of from about 2.8 to about 4.8.

The ethylene copolymers produced in accordance with the process of the present invention are granular materials having an average particle size of from about 0.02 to about 0.20 centimeters, usually of from about 0.05 to about 0.13 centimeters, in diameter. The particle size is important for the purpose of readily fluidizing the polymer particles in the fluid bed reactor. These granular materials also contain no more than 4.0 percent of fine particles having a diameter of less than 0.005 inches.

The ethylene polymers produced in accordance with the process of the present invention have a bulk density of from about 240 kilograms per cubic meter to about 513 kilograms per cubic meter,

The following Examples are designed to illustrate the process of the present invention and are not intended as a limitation upon the scope thereof.

The properties of the polymers produced in the Examples was determined by the following test methods:

Density

ASTM D-1505 procedure is followed for polymers having a density of less than 0.940 g/cm³, and a modified procedure is used for polymers having a density of 0.940 gr/cm³ or more. For the low density polymers, a plaque is made and conditioned for one hour at 100°C to approach equilibrium crystallinity. For the high density polymers, the plaque is conditioned for one hour at 120° to approach equilibrium crystallinity, and is then quickly cooled to room temperature. Measurement for density is then made in a density gradient column and density values are reported as grams/cm³.

Melt Index (MI)

ASTM D-1238, Condition E. Measured at 190°C and reported as grams per 10 minutes.

Flow Index (HLMI)

ASTM D-1238, Condition F. Measured at 10 times the weight used in the melt index test above.

Melt Flow Ratio (MFR)

Ratio of Flow Index:Melt Index.

Productivity

A sample of the resin product is ashed, and the weight percent of ash is determined. Since the ash is essentially composed of the catalyst, the productivity is thus the kilograms of polymer produced per kilogram of total catalyst consumed.

Bulk Density

ASTM D-1895, Method B. The resin is poured via 3/8" diameter funnel into a 400 ml graduated cylinder to the 400 ml line without shaking the cylinder, and weighed by difference.

Average Particle Size

Calculated from sieve analysis data measured according to ASTM D-1921, Method A, using a 500 g sample. Calculations are based on weight fractions retained on the screen.

*Example 1**Impregnation of Support with Mg-Ti-Based Composition*

In a 12 liter flask equipped with a mechanical stirrer were placed 41.8 g (0.439 mol) of anhydrous MgCl₂ and 2.5 liters of tetrahydrofuran (THF). To this mixture, 29.0 g (0.146 mol) of TiCl₃ · 0.33 AlCl₃ were added over a 1/2 hour period. The mixture was heated at 60°C for another 1/2 hour in order to completely dissolve the material.

Five hundred grams (500 g) of silica was dehydrated by heating at a temperature of 600°C and slurried in 3 liters of isopentane. The slurry was stirred while 186 ml of a 20 percent by weight solution of triethylaluminum in hexane was added thereto over a 1/4 hour period. The resulting mixture was then dried under a nitrogen purge at 60°C over a period of about 4 hours to provide a dry, free-flowing powder containing 5.5 percent by weight of the aluminum alkyl.

The treated silica was then added to the solution prepared as above. The resulting slurry was stirred for 1/4 hour and then dried under a nitrogen purge at 60°C over a period of about 4 hours to provide a dry, impregnated, free-flowing powder.

*Example 2**Partial Activation of Mg-Ti-Based Composition*

(a) The silica-impregnated magnesium-titanium-based composition prepared in accordance with Example 1 was slurried in 3 litres of anhydrous isopentane and stirred while a 20 percent by weight solution of tri-n-hexylaluminum in anhydrous hexane was added thereto over a 1/4 hour period. The tri-n-hexylaluminum solution was employed in an amount sufficient to provide 0.2 mols of this compound per mol of tetrahydrofuran in the magnesium-

titanium-based composition. After addition of the tri-n-hexylaluminum was completed, stirring was continued for an additional 1/4 hour. The mixture was then dried under a nitrogen purge at a temperature of 65 ± 10°C over a period of about 4 hours to provide a dry, free-flowing powder. This material was stored under dry nitrogen until it was needed.

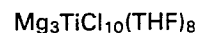
(b) The procedure was repeated employing the tri-n-hexylaluminum solution in an amount sufficient to provide 0.6 mols of this compound per mol of tetrahydrofuran in the magnesium-titanium-based composition.

(c) The silica-impregnated magnesium-titanium-based composition prepared in accordance with Example 1 was partially activated with diethylaluminum chloride and tri-n-hexylaluminum employing the same procedure as in 2(b) except that a 20 percent by weight solution of diethylaluminum chloride in anhydrous hexane was added to the silica-impregnated magnesium-titanium-based composition slurry prior to the addition of the tri-n-hexylaluminum solution. The diethylaluminum chloride solution was added over a 1/4 hour period in an amount sufficient to provide 0.4 mols of this compound per mol of tetrahydrofuran in the magnesium-titanium-based composition.

Examples 3 to 9

Ethylene was simultaneously dimerized to produce butene-1 and copolymerized with the dimerized product under varying reaction conditions in a fluid bed reactor system similar to that described and illustrated in U.S. patents 4 302 565, 4 302 566 and 4 303 771.

In each polymerization, silica-impregnated magnesium-titanium-based composition prepared in accordance with Example 1 and partially activated in accordance with Example 2(a) was continually fed to the polymerization reactor along with titanium tetraalkoxide, as a solution in isopentane, and trialkylaluminum, also as a solution in isopentane. The magnesium-titanium-based composition had the empirical formula



wherein THF stands for tetrahydrofuran.

The ethylene gas employed, in each instance, was diluted with nitrogen, and hydrogen was added to the gaseous reaction mixture as a chain transfer agent to regulate the molecular weight of the copolymer produced. In examples 3 to 7, the butene was generated completely in situ by the dimerization of ethylene. In examples 8 and 9, additional butene was added to the gaseous reaction mixture in order to supplement that generated in the reactor.

Table 1 below sets forth the details of these polymerizations, as well as the properties of the polymers produced by such polymerizations and the productivity of each catalyst system.

Comparative Examples A and B

For comparative purposes, ethylene was homopolymerized in the absence of the titanium tetraalkoxide dimerization catalyst. Also for pur-

poses of comparison, ethylene was copolymerized with butene-1 in the absence of the titanium tetraalkoxide dimerization catalyst using butene-1 which was provided completely from a source external to the reactor. For the homopolymerization, silica-impregnated magnesium-titanium-based composition prepared in accordance with Example 1 and partially activated in accordance with Example 2(b) was employed. For the copolymerization, silica-impregnated magnesium-titanium-based composition prepared in accordance with Example 1 and partially activated in accordance with Example 2(c) was employed. The details of these polymerizations are set forth in Table 1 below along with the details of Example 3 to 9.

TABLE I

Example	Comparative Example A	Comparative Example B	3	4	5	6	7	8	9
Partial Activation of Mg-Ti Polym. Cat.									
Partial Activator	(C ₆ H ₁₃) ₃ Al	(C ₂ H ₅) ₂ AlCl/ (C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al	(C ₆ H ₁₃) ₃ Al
Mol Ratio Partial Activator: Tetrahydrofuran	0.6	0.4/0.6	0.2	0.2	0.2	0.2	0.2	0.2	0.2
Reaction Conditions									
Mg-Ti Polym. Cat. Feed Rate, g/hr	7	2	11	12	11	5	7	7	12
Titanium Tetraalkoxide, [(RO) ₄ Ti]	None	None	(n-C ₄ H ₉ O) ₄ Ti	(i-C ₄ H ₉ O) ₄ Ti	(i-C ₄ H ₉ O) ₄ Ti	(i-C ₄ H ₉ O) ₄ Ti	(i-C ₄ H ₉ O) ₄ Ti	(i-C ₄ H ₉ O) ₄ Ti	(i-C ₄ H ₉ O) ₄ Ti
Conc. (RO) ₄ Ti Soln., Wt. %	—	—	1	5	5	5	5	5	5

TABLE I (Continued)

Example	Comparative Example A	Comparative Example B	3	4	5	6	7	8	9
(RO) ₄ Ti Soln. Feed Rate, cc/hr	—	—	200	20	85	69	62	80	44
Conc. (RO) ₄ Ti in Fluid Bed, ppm	0	0	40	60	85	110	130	100	60
Activator (trialkylaluminum)	(C ₂ H ₅) ₃ Al	(i-C ₄ H ₉) ₃ Al	(C ₂ H ₅) ₃ Al	(i-C ₄ H ₉) ₃ Al	(i-C ₄ H ₉) ₃ Al	(i-C ₄ H ₉) ₃ Al	(i-C ₄ H ₉) ₃ Al	(i-C ₄ H ₉) ₃ Al	(i-C ₄ H ₉) ₃ Al
Conc. Activator Soln., Wt. %	5	10	5	10	10	10	10	10	10
Activator Soln. Feed Rate, cc/hr	110	90	130	220	225	183	152	220	240
Temperature, °C	90	80	90	90	85	80	80	80	80
Total Pressure, kPa	2069	2069	2069	2069	2069	2069	2069	2069	2069
Ethylene Partial Pressure, kPa	897	690	862	828	897	855	690	552	552
Nitrogen Partial Pressure, kPa	616	848	578	827	437	487	813	1075	1087
Hydrogen Partial Pressure, kPa	556	179	603	290	188	171	159	110	99
Butene/Ethylene Mol Ratio	—	0.51	0.03	0.15	0.61	0.65	0.59	0.6	0.6
Hydrogen/Ethylene Mol Ratio	0.62	0.26	0.70	0.35	0.21	0.20	0.23	0.20	0.18
Molar Ratio Al:Mg-Ti Polym. Cat.	40	40	70	70	70-100	90	115	90	60
Molar Ratio Al:(RO) ₄ Ti	—	—	2-4	8-12	10-20	9	11	7-9	10-15
Molar Ratio (RO) ₄ Ti:Mg-Ti Polym. Cat.	—	—	1.3	5.5	10.5	14	8	10	4.5
<i>Polymer Properties</i>									
Melt Index, g/10 Min.	7.4	1.1	9.5	2.9	1.5	0.8	1.1	0.7	0.9
Flow Index, g/10 Min.	178.0	22.4	256.0	70.0	48.0	23.4	29.2	18.9	22.5
Melt Flow Ratio	24	21	27	24	32	29	27	27	25
Density, g/cm ³	0.965	0.918	0.960	0.938	0.926	0.920	0.920	0.921	0.910
Bulk Density, kg/m ³	368	417	401	352	352	336	336	384	256
Average Particle Size, cm.	0.08	0.08	0.05	0.08	0.08	0.10	0.08	0.10	0.20
<i>Productivity</i>									
Ash, Wt. %	0.035	0.035	0.039	0.059	0.064	0.055	0.059	—	—
Kg Polymer/kg Ash	2857	2857	2564	1695	1563	1818	1695	—	—

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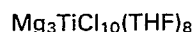
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Example 10

Ethylene was simultaneously dimerized to produce butene-1 and copolymerized with the dimerized product in a large fluid bed reactor.

Silica-impregnated magnesium-titanium-based composition prepared in accordance with Example 1 and partially activated in accordance with Example 2(a) was continually fed to the polymerization reactor along with titanium tetrakisobutoxide, as a solution in isopentane, and triisobutylaluminum, also as a solution in isopentane. The magnesium-titanium-based composition had the empirical formula



wherein THF stands for tetrahydrofuran.

The ethylene gas employed was diluted with nitrogen, and hydrogen was added to the gaseous reaction mixture as a chain transfer agent to regulate the molecular weight of the copolymer produced.

Table 2 below sets forth the details of the polymerization, as well as the properties of the polymer produced and the productivity of the catalyst system.

TABLE 2

Example	10
<i>Partial Activation of Mg-Ti Polym. Cat.</i>	
Partial Activator	(C ₆ H ₁₃) ₃ Al
Mol Ratio Partial Activator:Tetrahydrofuran	0.2
<i>Reaction Conditions</i>	
Mg-Ti Polym. Cat. Feed Rate, g/hr	318
Titanium Tetraalkoxide, [(RO) ₄ Ti]	(i-C ₄ -H ₉ O) ₄ Ti
Conc. (RO) ₄ Ti Solution, Wt. %	5
(RO) ₄ Ti Solution Feed Rate, l/hr	6.4
Conc. (RO) ₄ Ti in Fluid Bed, ppm	56
Activator	(i-C ₄ H ₉) ₃ Al
Conc. Activator Solution, Wt. %	20
Activator Soln. Feed Rate, l/hr	16.5
Temperature, °C	80
Total Pressure, kPa	1862
Ethylene Partial Pressure, kPa	759-828
Nitrogen Partial Pressure, kPa	473
Hydrogen Partial Pressure, kPa	198
Gas velocity, m/sec	0.55
Space Time Yield, kg/hr/m ³	80
Butene/Ethylene Mol Ratio	0.5
Hydrogen/Ethylene Mol Ratio	0.25
Molar Ratio Al:Mg-Ti Polym. Cat.	77
Molar Ratio Al:(RO) ₄ Ti	18
Molar Ratio (RO) ₄ Ti:Mg-Ti Polym. Cat.	4.3
<i>Polymer Properties</i>	
Melt Index, g/10 Min.	1.0
Flow Index, g/10 Min.	26
Melt Flow Ratio	26
Density, g/cm ³	0.919
Bulk density, kg/m ³	336-352
Average Particle Size, cm.	0.10

TABLE 2 (Continued)

Example	10
<i>Productivity</i>	
Ash, Wt. %	0.028
Kg Polymer/kg Ash	3571

Gas analysis showed that butene-1 was generated by the dimerization at a selectivity in excess of 85 percent. Among the butene isomers produced, butene-1 was produced at a selectivity in excess of 93 percent.

Claims

1. A continuous process for simultaneously dimerizing ethylene to produce butene-1 and copolymerizing ethylene with the dimerized product in a fluidized bed which comprises continuously contacting ethylene in a fluid bed reactor, at a temperature of from 30°C up to 115°C and a pressure no greater than 7000 kPa, with a catalytically effective amount of a catalyst system comprising

(a) a titanium tetraalkoxide having the formula



wherein each R is a hydrocarbon radical free from aliphatic unsaturation containing from 1 to 12 carbon atoms,

(b) a magnesium-titanium-based composition having the formula



wherein R' is an aliphatic or aromatic hydrocarbon radical containing from 1 to 14 carbon atoms, or COR'' wherein R'' is an aliphatic or aromatic hydrocarbon radical containing from 1 to 14 carbon atoms,

X is selected from the group consisting of Cl, Br, I, and mixtures thereof,

Ed is an organic electron donor compound selected from the group consisting of alkyl esters of aliphatic and aromatic carboxylic acids, aliphatic ethers, cyclic ethers and aliphatic ketones,

m is 0.5 to 56,

n is 0, 1 or 2,

p is 2 to 116, and

q is 2 to 85

said magnesium-titanium-based composition being diluted with an inert carrier material, and

(c) a trialkylaluminum compound having the formula



wherein each R''' is a saturated hydrocarbon radical containing from 1 to 14 carbon atoms,

Said titanium tetraalkoxide and said magnesium-titanium-based composition being employed in such

amounts as to provide an atomic ratio of titanium in the titanium tetraalkoxide to titanium in the magnesium-titanium-based composition of from 0.01:1 to 50:1, and

said trialkylaluminum compound being employed in an amount such as to provide a total aluminum:titanium atomic ratio of from 5:1 to 500:1.

2. A process as in claim 1 wherein said magnesium-titanium-based composition is mechanically mixed with the inert carrier material and the blended mixture contains from 3 percent by weight to 50 percent by weight of the magnesium-titanium-based composition.

3. A process as in claim 1 wherein the inert carrier material is impregnated with the magnesium-titanium-based composition and the impregnated carrier contains from 3 percent by weight to 50 percent by weight of the magnesium-titanium-based composition.

4. A process as in claim 3 wherein the inert carrier material is impregnated with both the magnesium-titanium-based composition and the titanium tetraalkoxide.

5. A process as in any one of claims 1 to 4 wherein the inert carrier material is silica.

6. A process as in any one of claims 1 to 5 wherein R is an aliphatic radical containing from 1 to 6 carbon atoms, X is Cl, [ED] is tetrahydrofuran, m is 1.5 to 5, n is 0, p is 6 to 14, and q is 3 to 10.

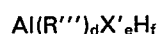
7. A process as in claim 6 wherein the titanium tetraalkoxide is titanium tetraisobutoxide; the magnesium-titanium-based composition is composed of magnesium dichloride, titanium trichloride, and tetrahydrofuran; and the trialkylaluminum compound is triisobutylaluminum.

8. A process as in any one of claims 1 to 7 wherein a portion of the butene-1 is added to the reactor from an external source.

9. A process as in any one of claims 1 to 8 wherein a temperature of from 75°C to 115°C is employed, the titanium tetraalkoxide and magnesium-titanium-based composition are employed in such amounts as to provide an atomic ratio of titanium in the titanium tetraalkoxide to titanium in the magnesium-titanium-based composition of greater than 2:1 to 20:1, and the trialkylaluminum compound is employed in an amount such as to provide a total aluminum:titanium atomic ratio of 5:1 to 150:1.

10. A process as in any one of claims 1 to 9 wherein the ethylene feed is diluted with an inert gas, the ethylene partial pressure is between 56 kPa and 1900 kPa, and hydrogen is added to the reaction mixture in an amount sufficient to produce a hydrogen:ethylene molar ratio of from 0.01:1 to 5:1.

11. A process as in any one of claims 1 to 10 wherein the magnesium-titanium-based composition is partially activated before it is introduced into the polymerization reactor by means of an organoaluminum activator compound, said activator compound being employed in an amount which does not raise the molar ratio of activator compound:electron donor in the magnesium-titanium-based composition beyond 1.4:1, and said activator compound having the formula



wherein X' is Cl or OR''',

R''' and R'''' are saturated hydrocarbon radicals containing from 1 to 14 carbon atoms,

e is 0 to 1.5,

f is 0 or 1, and

d + e + f = 3.

12. A process as in claim 11 wherein the organoaluminum activator compound employed to partially activate the magnesium-titanium-based composition is employed in an amount which will provide the magnesium-titanium-based composition with an activator compound:electron donor molar ratio of from 0.1:1 to 1.0:1.

13. A continuous process for dimerizing ethylene to produce butene-1 in a fluidized bed which comprises continuously contacting ethylene in a fluid bed reactor, at a temperature of from 30°C up to 115°C and a pressure no greater than 7000 kPa, with a catalytically effective amount of a catalyst system comprising

(a) a titanium tetraalkoxide having the formula



wherein each R is a hydrocarbon radical free from aliphatic unsaturation containing from 1 to 12 carbon atoms, and

(b) a trialkylaluminum compound having the formula



wherein each R''' is a saturated hydrocarbon radical containing from 1 to 14 carbon atoms,

said trialkylaluminum compound being employed in an amount such as to provide a total aluminum:titanium atomic ratio of from 4:1 to 500:1.

14. A process as in claim 13 wherein R is an aliphatic radical containing from 1 to 6 carbon atoms.

15. A process as in claim 14 wherein the titanium tetraalkoxide is titanium tetraisobutoxide and the trialkylaluminum compound is triisobutylaluminum.

16. A process as in any one of claims 13 to 15 wherein a temperature of from 75°C to 115°C is employed, and the trialkylaluminum compound is employed in an amount such as to provide a total aluminum:titanium atomic ratio of 5:1 to 150:1.

Patentansprüche

1. Kontinuierliches Verfahren zum gleichzeitigen Dimerisieren von Ethylen zur Bildung von Buten-1 und Copolymerisieren von Ethylen mit dem dimerisierten Produkt in einem Wirbelbett, das das In-Berührung-bringen von Ethylen in einem Wirbelbettreaktor bei einer Temperatur von 30 bis 115°C und einem Druck nicht über 7000 kPa mit einer katalytisch wirksamen Menge eines Katalysatorsystems, das umfaßt:

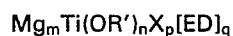
(a) Titantetraalkoxid der Formel



worin jedes R ein von aliphatisch ungesättigten

Bindungen freier Kohlenwasserstoffrest mit 1 bis 12 Kohlenstoffatomen ist,

(b) eine Zusammensetzung auf Magnesium/Titan-Basis mit der Formel



worin R' ein aliphatischer oder aromatischer Kohlenwasserstoffrest mit 1 bis 14 Kohlenstoffatomen oder OR'' ist,

worin R'' ein aliphatischer oder aromatischer Kohlenwasserstoffrest mit 1 bis 14 Kohlenstoffatomen ist,

X ausgewählt ist aus der aus Cl, Br, J und Mischungen derselben bestehenden Gruppe,

ED eine organische Elektronendonatorverbindung ist, ausgewählt aus der aus Alkylestern aliphatischer und aromatischer Carbonsäuren, aliphatischen Ether, cyclischen Ether und aliphatischen Ketonen bestehenden Gruppe,

m = 0,5 bis 56 ist,

n = 0, 1 oder 2 ist,

p = 2 bis 116 ist und

q = 2 bis 85 ist

wobei die Zusammensetzung auf Magnesium/Titan-Basis mit einem inerten Trägermaterial verdünnt ist, und

(c) eine Trialkylaluminiumverbindung der Formel



worin jedes R''' ein gesättigter Kohlenwasserstoffrest mit 1 bis 14 Kohlenstoffatomen ist, umfaßt,

wobei das Titantetraalkoxid und die Zusammensetzung auf Magnesium/Titan-Basis in solchen Mengen verwendet werden, daß sich ein Atom-Verhältnis von Titan im Titantetraalkoxid zum Titan in der Zusammensetzung auf Magnesium/Titan-Basis von 0,01:1 bis 50:1 ergibt, und die Trialkylaluminiumverbindung in einer solchen Menge verwendet wird, daß sich ein Atom-Gesamtverhältnis von Aluminium zu Titan von 5:1 bis 500:1 ergibt.

2. Verfahren nach Anspruch 1, worin die Zusammensetzung auf Magnesium/Titan-Basis mechanisch mit dem inerten Trägermaterial gemischt wird und die gemischte Mischung 3 bis 50 Gew.-% der Zusammensetzung auf Magnesium/Titan-Basis enthält.

3. Verfahren nach Anspruch 1, worin das inerte Trägermaterial mit der Zusammensetzung auf Magnesium/Titan-Basis imprägniert wird und der imprägnierte Träger 3 bis 50 Gew.-% der Zusammensetzung auf Magnesium/Titan-Basis enthält.

4. Verfahren nach Anspruch 3, worin das inerte Trägermaterial sowohl mit der Zusammensetzung auf Magnesium/Titan-Basis als auch dem Titantetraalkoxid imprägniert wird.

5. Verfahren nach irgendeinem der Ansprüche 1 bis 4, worin das inerte Trägermaterial Siliciumdioxid ist.

6. Verfahren nach irgendeinem der Ansprüche 1 bis 5, worin R ein aliphatischer Rest mit 1 bis 6 Kohlenstoffatomen ist, X = Cl ist, [ED] = Tetrahydrofuran ist, m = 1,5 bis 5 ist, n = 0 ist, p = 6 bis 14 ist und q = 3 bis 10 ist.

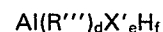
7. Verfahren nach Anspruch 6, worin das Titantetraalkoxid Titantetraisobutoxid ist, die Zusammensetzung auf Magnesium/Titan-Basis aus Magnesiumdichlorid, Titantrichlorid und Tetrahydrofuran besteht und die Trialkylaluminiumverbindung Triisobutylaluminium ist.

8. Verfahren nach irgendeinem der Ansprüche 1 bis 7, worin ein Teil des Butens-1 dem Reaktor aus einer äußeren Quelle zugegeben wird.

9. Verfahren nach irgendeinem der Ansprüche 1 bis 8, worin eine Temperatur von 75 bis 115°C angewendet wird, das Titantetraalkoxid und die Zusammensetzung auf Magnesium/Titan-Basis in solchen Mengen verwendet werden, daß sich ein Atom-Verhältnis von Titan im Titantetraalkoxid zum Titan in der Zusammensetzung auf Magnesium/Titan-Basis von mehr als 2:1 bis 20:1 ergibt, und die Trialkylaluminiumverbindung in einer Menge verwendet wird, daß sich ein Atom-Gesamtverhältnis von Aluminium zu Titan von 5:1 bis 150:1 ergibt.

10. Verfahren nach irgendeinem der Ansprüche 1 bis 9, worin die Ethylenbeschickung mit einem inerten Gas verdünnt wird, der Ethylenteildruck zwischen 56 kPa und 1900 kPa liegt und Wasserstoff zur Reaktionsmischung in ausreichender Menge zugefügt wird, um ein Mol-Verhältnis von Wasserstoff:Ethylen von 0,01:1 bis 5:1 zu erzielen.

11. Verfahren nach irgendeinem der Ansprüche 1 bis 10, worin die Zusammensetzung auf Magnesium/Titan-Basis vor ihrer Einführung in den Polymerisationsreaktor mittels einer Organoaluminium-Aktivatorverbindung teilweise aktiviert wird, wobei die Aktivatorverbindung in einer Menge verwendet wird, die das Mol-Verhältnis der Aktivatorverbindung zum Elektronendonator in der Zusammensetzung auf Magnesium/Titan-Basis nicht über 1,4:1 erhöht und die Aktivatorverbindung der Formel



hat, worin X' = Cl oder OR'''' ist, R''' und R'''' gesättigte Kohlenwasserstoffreste mit 1 bis 14 Kohlenstoffatomen sind,

e = 0 bis 1,5 ist,

f = 0 oder 1 ist und

d + e + f = 3 ist.

12. Verfahren nach Anspruch 11, worin die zum teilweise Aktivieren der Zusammensetzung auf Magnesium/Titan-Basis verwendete Organoaluminium-Aktivatorverbindung in einer Menge verwendet wird, daß bezüglich der Zusammensetzung auf Magnesium/Titan-Basis ein Mol-Verhältnis von Aktivatorverbindung zu Elektronendonator von 0,1:1 bis 1,0:1 erhalten wird.

13. Kontinuierliches Verfahren zum Dimerisieren von Ethylen unter Bildung von Buten-1 in einem Wirbelbett, das umfaßt: das kontinuierliche In-Berührung-bringen von Ethylen in einem Wirbelbettreaktor bei einer Temperatur von 30 bis 115°C und einem Druck nicht über 7000 kPa mit einer katalytisch wirksamen Menge eines Katalysatorsystems, das umfaßt

(a) ein Titantetraalkoxid der Formel



worin jedes R ein von aliphatisch ungesättigten Bindungen freier Kohlenwasserstoffrest mit 1 bis 12 Kohlenstoffatomen ist, und

(b) eine Trialkylaluminiumverbindung der Formel



worin jedes R''' ein gesättigter Kohlenwasserstoffrest mit 1 bis 14 Kohlenstoffatomen ist, wobei die Trialkylaluminiumverbindung in einer solchen Menge verwendet wird, daß sich ein Atom-Gesamtverhältnis von Aluminium zu Titan von 4:1 bis 500:1 ergibt.

14. Verfahren nach Anspruch 13, worin R ein aliphatischer Rest mit 1 bis 6 Kohlenstoffatomen ist.

15. Verfahren nach Anspruch 14, worin das Titan-tetraalkoxid Titan-tetraisobutoxid und die Trialkylaluminiumverbindung Triisobutylaluminium ist.

16. Verfahren nach irgendeinem der Ansprüche 13 bis 15, worin eine Temperatur von 75 bis 115°C angewendet wird und die Trialkylaluminiumverbindung in einer solchen Menge verwendet wird, daß sich ein Atom-Gesamtverhältnis von Aluminium zu Titan von 5:1 bis 150:1 ergibt.

Revendications

1. Procédé simultané continu de dimérisation d'éthylène pour produire du butène-1 et de copolymérisation d'éthylène avec le produit dimérisé dans un lit fluidisé, qui consiste à faire entrer de l'éthylène, dans un réacteur à lit fluide, à une température allant de 30°C jusqu'à 115°C et à une pression ne dépassant pas 7000 kPa, en contact continu avec une quantité catalytiquement efficace d'un système catalyseur comprenant:

(a) un tétraalkylate de titane de formule



dans laquelle chaque R désigne un radical hydrocarboné dépourvu de non-saturation aliphatique contenant 1 à 12 atomes de carbone,

(b) une composition à base de magnésium et de titane répondant à la formule



dans laquelle R' est un radical d'hydrocarbure aliphatique ou aromatique contenant 1 à 14 atomes de carbone, ou un groupe COR'' dans lequel R'' est un radical d'hydrocarbure aliphatique ou aromatique contenant 1 à 14 atomes de carbone,

X est choisi dans le groupe comprenant Cl, Br, I, et leurs mélanges,

ED désigne un composé organique donneur d'électrons choisi dans le groupe comprenant des esters alkyliques d'acides carboxyliques aliphatiques et aromatiques, des éthers aliphatiques, des éthers cycliques et des cétones aliphatiques,

m a une valeur de 0,5 à 56,

n a la valeur 0, 1 ou 2,

p a une valeur de 2 à 116, et

q a une valeur de 2 à 85,

ladite composition à base de magnésium et de titane étant diluée avec un support inerte, et

(c) un composé trialkylique d'aluminium répondant à la formule



dans laquelle chaque R''' est un radical hydrocarboné saturé contenant 1 à 14 atomes de carbone, ledit tétraalkylate de titane et ladite composition à base de magnésium et de titane étant utilisés en quantités choisies de manière qu'il y ait un rapport atomique du titane dans le tétraalkylate de titane au titane dans la composition à base de magnésium et de titane de 0,01:1 à 50:1, et

ledit composé trialkylique d'aluminium étant utilisé en une quantité choisie de manière qu'il y ait un rapport atomique total aluminium:titane de 5:1 à 500:1.

2. Procédé suivant la revendication 1, dans lequel la composition à base de magnésium et le titane est mélangée mécaniquement avec la matière de support inerte et le mélange obtenu contient 3 à 50 pourcent en poids de la composition à base de magnésium et de titane.

3. Procédé suivant la revendication 1, dans lequel la matière inerte de support est imprégnée de composition à base de magnésium et de titane et le support imprégné contient 3 à 50 pourcent en poids de la composition à base de magnésium et de titane.

4. Procédé suivant la revendication 3, dans lequel la matière inerte de support est imprégnée de la composition à base de magnésium et de titane et du tétraalkylate de titane.

5. Procédé suivant l'une quelconque des revendications 1 à 4, dans lequel la matière inerte de support est la silice.

6. Procédé suivant l'une quelconque des revendications 1 à 5, dans lequel R est un radical aliphatique contenant 1 à 6 atomes de carbone, X est le chlore, [ED] est le tétrahydrofurane, m a une valeur de 1,5 à 5, n a la valeur 0, p a une valeur de 6 à 14 et Q a une valeur de 3 à 10.

7. Procédé suivant la revendication 6, dans lequel le tétraalkylate de titane est le tétra-isobutylate de titane, la composition à base de magnésium et de titane est constituée de dichlorure de magnésium, de trichlorure de titane et de tétrahydrofurane; et le composé trialkylique d'aluminium est le triisobutylaluminium.

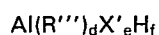
8. Procédé suivant l'une quelconque des revendications 1 à 7, dans lequel une portion du butène-1 est ajoutée au réacteur depuis une source extérieure.

9. Procédé suivant l'une quelconque des revendications 1 à 8, dans lequel on utilise une température de 75 à 115°C, le tétraalkylate de titane et la composition à base de magnésium et de titane sont utilisés en quantités donnant un rapport atomique du titane dans le tétraalkylate de titane au titane dans la composition à base de magnésium et de titane allant de plus de 2:1 à 20:1, et le composé trialkylique d'aluminium est utilisé en une quantité donnant un rapport atomique total aluminium:titane de 5:1 à 150:1.

10. Procédé suivant l'une quelconque des revendications 1 à 9, dans lequel la charge d'éthylène est diluée avec un gaz inerte, la pression partielle

d'éthylène se situe entre 56 kPa et 1900 kPa, et de l'hydrogène est ajouté au mélange réactionnel en une quantité suffisante pour qu'il y ait un rapport molaire hydrogène:éthylène de 0,01:1 à 5:1.

11. Procédé suivant l'une quelconque des revendications 1 à 10, dans lequel la composition à base de magnésium et de titane est partiellement activée avant d'être introduite dans le réacteur de polymérisation au moyen d'un composé organique d'aluminium activateur, ledit composé activateur étant utilisé en une quantité qui n'élève pas le rapport molaire composé activateur:donneur d'électrons dans la composition à base de magnésium et de titane au-delà de 1,4:1, et ledit composé activateur répond à la formule



dans laquelle X' représente Cl ou OR'''' ,

R''' et R'''' sont des radicaux hydrocarbonés saturés contenant 1 à 14 atomes de carbone,

e a une valeur de 0 à 1,5,

f a la valeur 0 ou 1, et

la somme d + e + f = 3.

12. Procédé suivant la revendication 11, dans lequel le composé organique d'aluminium activateur utilisé pour activer partiellement la composition à base de magnésium et de titane est utilisé en une quantité qui donne une composition à base de magnésium et de titane dans laquelle le rapport molaire du composé activateur au donneur d'électrons va de 0,1:1 à 1,0:1.

13. Procédé continu de dimérisation d'éthylène pour produire du butène-1 dans un lit fluidisé, qui

consiste à faire entrer en continu de l'éthylène, dans un réacteur à lit fluide à une température de 30°C jusqu'à 115°C et à une pression n'excédant pas 7000 kPa, en contact avec une quantité catalytiquement efficace d'un système catalyseur comprenant

(a) un tétraalkylate de titane de formule



dans laquelle chaque R représente un radical hydrocarboné dépourvu de non-saturation aliphatique contenant 1 à 12 atomes de carbone, et

(b) un composé trialkylique d'aluminium répondant à la formule



dans laquelle chaque R''' est un radical hydrocarboné saturé contenant 1 à 14 atomes de carbone, ledit composé trialkylique d'aluminium étant utilisé en une quantité telle qu'il y ait un rapport atomique total aluminium:titane de 4:1 à 500:1.

14. Procédé suivant la revendication 13, dans lequel R est un radical aliphatique contenant 1 à 6 atomes de carbone.

15. Procédé suivant la revendication 14, dans lequel le tétraalkylate de titane est le tétraisobutylate de titane et le composé trialkylique d'aluminium est le triisobutylaluminium.

16. Procédé suivant l'une quelconque des revendications 13 à 15, dans lequel on utilise une température de 75°C à 115°C et le trialkylaluminium est utilisé en une quantité telle qu'il y ait un rapport atomique total aluminium:titane de 5:1 à 150:1.

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