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(54) Alkaline earth metal hydrocarbyl phenates, their sulphurised derivatives, their production and use thereof

Erdalkalimetallalkylphenolate, ihre geschwefelten Derivate, ihre Herstellung und ihre Verwendung

Alkylphénates de métaux alcalino-terreux, leurs dérivés sulfurés, leur préparation et leur utilisation

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EP-A- 0 094 814	**EP-A- 0 095 322**
GB-A- 1 469 289	**GB-A- 1 470 338**
GB-A- 2 142 928	**US-A- 4 328 111**

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Description

[0001] The present invention relates in general to alkaline earth metal hydrocarbyl phenates and their sulphurised derivatives, their production and use thereof as lubricating oil additives. In particular the present invention relates to concentrate additive compositions comprising alkaline earth metal hydrocarbyl phenates and their sulphurised derivatives having both a high total base number (TBN) and an acceptable viscosity, to their production and to their use as lubricating oil additives.

[0002] In the internal combustion engine, by-products from the combustion chamber often blow by the piston and admix with the lubricating oil. Many of these by-products form acidic materials within the lubricating oil. This is particularly marked in diesel engines operating on low-grade fuels of high sulphur content wherein corrosive acids are produced by combustion. The acids thereby incorporated in the lubricating oil can include sulphur acids produced by oxidation of sulphur, hydrohalic acids derived from halogen lead scavengers in the fuel and nitrogen acids produced by the oxidation of atmospheric nitrogen within the combustion chamber. Such acids cause deposition of sludge and corrosion of the bearings and engine parts leading to rapid wear and early breakdown of the engine.

[0003] One class of compounds generally employed to neutralise the acidic materials and disperse sludge within the lubricating oil are the metal alkyl phenates and sulphurised metal alkyl phenates, wherein the metal is an alkaline earth metal such as calcium, magnesium or barium. Both "normal" and "overbased" alkaline earth metal alkyl phenates have been employed. The term "overbased" is used to describe those alkaline earth metal alkyl phenates in which the ratio of the number of equivalents of the alkaline earth metal moiety to the number of equivalents of the phenol moiety is greater than one, and is usually greater than 1.2 and may be as high as 4.5 or greater. In contrast, the equivalent ratio of alkaline earth metal moiety to phenol moiety in "normal" alkaline earth metal alkyl phenates is one. Thus, the "overbased" material contains greater than 20% in excess of the alkaline earth metal present in the corresponding "normal" material. For this reason "overbased" alkaline earth metal alkyl phenates have a greater capability for neutralising acidic matter than do the corresponding "normal" alkaline earth metal alkyl phenates.

[0004] The prior art teaches many methods for preparing both "normal" and "overbased" metal alkyl phenates. One such method for preparing "overbased" alkyl phenates generally referred to as the "single lime addition" process comprises reacting an alkyl phenol, in the presence or absence of sulphur, lubricating oil, a hydroxylic compound and excess alkaline earth metal hydroxide (above the stoichiometric proportion required to neutralise the alkyl phenol), to form an intermediate product, followed by carbonation, a heading distillation (to remove unreacted hydroxylic compound) and filtration. The production of intermediate product is accompanied by a marked increase in viscosity while the subsequent carbonation reduces the viscosity to a relatively low level. The increase in viscosity accompanying the formation of the intermediate product is undesirable because the reaction mixture becomes difficult to agitate to the detriment of subsequent reactions. Whilst this increase in viscosity may be controlled to an acceptable level by incorporation of less alkaline earth metal hydroxide in the reaction, the overbased alkyl phenate product necessarily possesses a reduced neutralisation capacity. In order to achieve a high neutralisation capacity product and at the same time control the viscosity of the intermediate product within acceptable limits, the alkaline earth metal hydroxide may be added in two, (generally referred to as the "double lime addition" process) or three separate reaction steps, with sequential carbonation steps. However, this method involves relatively long batch times. Another alternative is to use viscosity depressants, such as tridecanol, 2-ethylhexanol, or similar boiling range hydroxylic solvent, in the production of the intermediate product but such an expedient increases the raw material cost of the process. The highest total base number (TBN), expressed in mg KOH/g, consistent with an acceptable viscosity, generally achievable by prior art processes is about 300, though generally prior art TBNs are in the range from 200-300. It would clearly be a desirable objective to produce an additive concentrate comprising alkaline earth metal alkyl phenates or sulphurised derivatives thereof having a high TBN, that is a TBN greater than 300, and preferably greater than 350. To date it has not been found possible to achieve products of such high TBN because the use of larger concentrations of alkaline earth metal base leads to highly viscous products which, rather than being 'thinned' by subsequent carbonation attempts using excess carbon dioxide, are rendered insoluble. We have achieved this objective and thereby obtained products having a TBN in excess of 300, and in some cases greater than 350, whilst retaining an acceptable viscosity, that is a viscosity at 100°C of less than 1,000 cSt and avoiding insolubility by incorporating into the reaction mixture a defined amount of certain carboxylic acids having at least 10 carbon atoms in the molecule or acid derivatives.

[0005] The use of carboxylic acids either in the production of alkaline earth metal alkyl phenates and their sulphurised derivatives or in association therewith in lubricating oil compositions is not new, see for example US-A-3,372,116; GB-A-1440261; US-A-4049560 and EP-A-0094814.

[0006] US-A-3,372,116 discloses an improvement in the method for preparing a basic metal phenate by reacting at a temperature between about 25°C and the reflux temperature (A) a hydrocarbon-substituted phenol having at least 6 carbon atoms in the hydrocarbon substituent, a mixture of said phenol with up to an equivalent amount of a hydrocarbon-substituted succinic acid or anhydride having at least about 6 carbon atoms in the hydrocarbon substituent, or a substantially neutral alkali metal or alkaline earth metal salt or either of the foregoing, (B) about 1-10 equivalents, per equivalent of (A), of a calcium or strontium base, and (C) carbon dioxide, which improvement comprises carrying out the reaction in the presence of about 0.002-0.2 equivalent, per equivalent of said calcium or strontium base, of a carboxylic acid having up to about 100 carbon atoms or an alkali metal, alkaline earth metal, zinc or lead salt thereof. The preferred carboxylic acids are those containing up to about 10 carbon atoms, more preferred being monocarboxylic acids containing up to 10 carbon atoms and alkaline earth metal salts thereof. In many of the Examples water and a carboxylate salt are employed. Not only do we wish to avoid the presence of water but we also find that carboxylate salts can not be used in the process of the present invention because of their inherent insolubility in the system. The process of US-A-3,372,116 does not employ phenol to alkaline earth metal base ratios sufficient to produce phenates having TBNs in excess of 300.

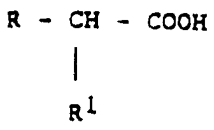
[0007] GB-A-1440261 discloses a lubricating oil composition comprising a lubricating oil, a detergent or dispersant additive and a mixture of at least two carboxylic acids, one acid having a melting point of at least 20°C and not more than 30 carbon atoms per molecule, and another acid having a melting point of below 20°C the weight proportion of low melting point acid to high melting point acid being between 1.5:1 and 8:1. The detergent may be an overbased phenate, those having a TBN of 50 to 100 being considered very suitable. In the lubricating oil composition the mixture of acids is present in an amount of 0.05 to 2.0 wt %.

[0008] US-A-4049560 describes the production of an overbased magnesium detergent by a process in which carbon dioxide is introduced into a reaction mixture which comprises:

(a) 15-40 wt % of a sulphurised phenol or thiophenol containing one or more hydrocarbyl substituents, or a phenol or thiophenol containing one or more hydrocarbyl substituents, or said phenol or thiophenol containing one or more hydrocarbyl substituents together with sulphur,
(b) 5-15 wt % of an organic sulphonic acid, an organic sulphonate or an organic sulphate,
(c) 5-15 wt % of a glycol, a C_1 to C_5 monohydric alkanol or C_2 to C_4 alkoxy alkanol,
(d) 2-15 wt % of a magnesium hydroxide or active magnesium oxide,
(e) at least 0.1 wt % of a C_1 to C_{18} carboxylic acid, an anhydride thereof, or an ammonium, an amine salt, a Group I metal or a Group II metal salt of said C_1 to C_{18} carboxylic acid, and
(f) at least 10% by weight of a diluent oil (including any present in components (a) and (b)).

[0009] The amount of carboxylic acid (component (e)) is preferably in the range 0.5 to 2.0% by weight. The product prepared by this reaction is said to have a TBN of about 200 to 250, e.g. about 225.

[0010] EP-A-0094814 discloses an additive concentrate for incorporation in a lubricating oil composition comprising lubricating oil, and from 10 to 90 wt % of an overbased alkaline earth metal hydrocarbyl sulphurised phenate which has been treated, either during or subsequent to the overbasing process, with from 0.1 to 10, preferably 2 to 6, wt % (based on the weight of additive concentrate) of an acid of the formula:



$$\underset{\displaystyle R^1}{\underset{|}{R - CH - COOH}} \qquad (I)$$

(wherein R is a C_{10} to C_{24} unbranched alkyl or alkenyl group, and R^1 is hydrogen, a C_1 to C_4 alkyl group or a $-CH_2-COOH$ group) or an anhydride or a salt thereof. The object of the invention of EP-A-0094814 is to overcome problems encountered with many additive concentrates containing overbased additives, namely lack of stability giving rise to sedimentation and foaming problems. The problem of EP-A-0094814 is not that of producing phenate additive concentrates having a TBN of greater than 300 and indeed the phenate additive concentrates produced by the process of the invention, although demonstrating overcoming the problems of stability and foaming, have TBN values of less than 300.

[0011] Our European Application Publication No. 0095322 discloses a process for the production of either an alkaline earth metal alkyl phenate or a sulphurised alkaline earth metal alkyl phenate which process comprises reacting at elevated temperature, in the presence or absence of sulphur, an alkyl phenol with an alkaline earth metal base in the presence as solvent of either an alkylene glycol alkyl ether or a polyalkylene glycol alkyl ether of formula:

$$R(OR^1)_xOR^2$$

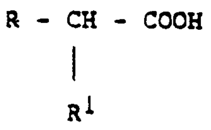
wherein R is a C_1 to C_6 alkyl group, R^1 is alkylene, R^2 is hydrogen or C_1 to C_6 alkyl and x is an integer in the range 1 to 6 and as catalyst an inorganic halide. It is said to be preferred to add a small amount, suitably up to 2% w/w of an acid, a suitable acid being stearic acid. The addition of stearic acid to the reactants can, it is said, enhance the ability of alkyl phenates to minimise emulsion formation in water.

[0012] It can be concluded that the prior art in which carboxylic acids are employed does not address the problem of producing additive concentrates comprising overbased alkaline earth metal hydrocarbyl phenates having a TBN of greater than 300 and an acceptable viscosity.

[0013] Our copending European Application Publication No. 0273588 of the same priority date as the present application claims a process for the production of an additive concentrate suitable for incorporation into a finished lubricating oil composition, the additive concentrate comprising:

(a) a lubricating oil,
(b) a lubricating oil soluble sulphurised alkaline earth metal hydrocarbyl phenate modified by incorporation of from greater than 2 to 35% by weight based on the weight of the concentrate of either:

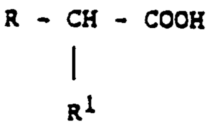
(i) at least one carboxylic acid having the formula:-



$$R - \underset{\displaystyle R^1}{\underset{|}{CH}} - COOH \qquad (I)$$

wherein R is a C_{10} to C_{24} alkyl or alkenyl group and R^1 is either hydrogen, a C_1 to C_4 alkyl group or a $-CH_2-COOH$ group, or an anhydride or ester thereof or (ii) a di-or polycarboxylic acid containing from 36 to 100 carbon atoms or an anhydride or ester thereof, the composition having a TBN greater than 300 and a viscosity at 100°C of less than 1000 cSt, which process comprises reacting at elevated temperature:

(A) a sulphurised alkaline earth metal hydrocarbyl phenate having a TBN less than that of the final additive concentrate,
(B) an alkaline earth metal base, either added in whole to the initial reactants, or in part to the initial reactants and the remainder in one or more portions at a subsequent stage or stages in the process,
(C) either a polyhydric alcohol having from 2 to 4 carbon atoms, a di- or tri- (C_2 to C_4) glycol, an alkylene glycol alkyl ether or a polyalkylene glycol alkyl ether,
(D) a lubricating oil,
(E) carbon dioxide added subsequent to the, or each, addition of component (B), and
(F) sufficient to provide from greater than 2 to 35% by weight based on the weight of the concentrate of either (i) at least one carboxylic acid having the formula:-



$$R - \underset{\displaystyle R^1}{\underset{|}{CH}} - COOH \qquad (I)$$

wherein R is a C_{10} to C_{24} alkyl or alkenyl group and R^1 is either hydrogen, a C_1 or C_4 alkyl group or a $-CH_2COOH$ group, or an anhydride or ester thereof or (ii) a di- or polycarboxylic acid containing from 36 to 100 carbon atoms or an anhydride or ester thereof,

the weight ratios of components (A) to (F) being such as to produce a concentrate having a TBN greater than 300.

[0014] In one aspect the present invention provides Claim 1 from p. 18

[0015] Component (D) of the composition is a lubricating oil. The lubricating oil may suitably be either an animal oil, a vegetable oil or a mineral oil. Suitably the lubricating oil may be a petroleum-derived lubricating oil, such as a naphthenic base, paraffin base or mixed base oil. Solvent neutral oils are particularly suitable. Alternatively, the lubricating oil may be a synthetic lubricating oil. Suitable synthetic lubricating oils include synthetic ester lubricating oils, which oils include diesters such as di-octyl adipate, di-octyl sebacate and tridecyladipate, or polymeric hydrocarbon lubricating oils, for example liquid polyisobutenes and poly-alpha olefins. The lubricating oil may suitably comprise from 10 to

90%, preferably from 10 to 70%, by weight of the composition.

[0016] The concentrate comprises a lubricating oil soluble sulphurised or non-sulphurised, preferably sulphurised, calcium, magnesium or barium, preferably calcium, hydrocarbyl phenate modified by incorporation of from greater than 10 to less than 40% by weight based on the weight of the composition of (i). The hydrocarbyl phenate moiety of the phenate is preferably derived from at least one alkyl phenol. The alkyl groups of the alkyl phenol may be branched or unbranched. Suitable alkyl groups contain from 4 to 50, preferably from 9 to 28 carbon atoms. A particularly suitable alkyl phenol is the C_{12}-alkyl phenol obtained by alkylating phenol with propylene tetramer.

[0017] The hydrocarbyl phenate is modified by incorporation of (i). As regards (i), this is at least one carboxylic acid having the formula (I) or an acid anhydride or ester thereof. Acids of formula (I) are those wherein R is a C_{10} to C_{24}, more preferably C_{18} to C_{24} straight chain alkyl group and R^1 is hydrogen. Examples of suitable saturated carboxylic acids of formula (I) include capric acid, lauric acid, myristic acid, palmitic acid, stearic acid, arachidic acid, behenic acid and lignoceric acid. Mixtures of acids may also be employed, for example rape top fatty acids. Particularly suitable mixtures of acids are those commercial grades containing a range of acids, including both saturated and unsaturated acids. Such mixtures may be obtained synthetically or may be derived from natural products, for example cotton oil, ground nut oil, coconut oil, linseed oil, palm kernel oil, olive oil, corn oil, palm oil, castor oil, soyabean oil, sunflower oil, herring oil, sardine oil and tallow. Sulphurised acids and acid mixtures may also be employed. Instead of, or in addition to, the carboxylic acid there may be used either the acid anhydride or the ester derivatives of the acid, preferably the acid anhydride. It is preferred however to use a carboxylic acid or a mixture of carboxylic acids. A preferred carboxylic acid of formula (I) is stearic acid.

[0018] Preferably the carboxylic acid(s) having the formula (I), the di- or polycarboxylic acid, or the acid anhydride or ester thereof is incorporated in an amount from greater than 10% to 35%, more preferably from 12 to 20%, for example about 16% by weight based on the weight of the concentrate. An advantage of incorporating greater than 10% of the carboxylic acid or derivative thereof is generally a relativelylower concentrate viscosity.

[0019] Suitably the calcium, magnesium or barium may be present in the concentrate in an amount in the range from 10 to 20% by weight based on the weight of the concentrate.

[0020] The hydrocarbyl phenate may be either sulphurised or non-sulphurised, preferably sulphurised. Suitably sulphur may be present in the concentrate in an amount in the range from 1 to 6, preferably from 1.5 to 3% by weight based on the weight of the concentrate.

[0021] Suitably carbon dioxide may be present in the concentrate in an amount in the range from 5 to 20, preferably from 9 to 15% by weight based on the weight of the concentrate.

[0022] Preferably the TBN of the concentrate is greater than 350, more preferably greater than 400.

[0023] Preferably the concentrate may have a viscosity measured at 100°C of less than 750 cSt, more preferably less than 500 cSt.

[0024] In another aspect the present invention provides a process for the production of an additive concentrate for incorporation into a finished lubricating oil which process comprises reacting in the presence of a catalyst at elevated temperature components (A) to (F) as hereinbefore described, the weight ratios of components (A) to (F) being such as to produce a concentrate having a TBN greater than 300.

[0025] Component (A) of the reaction mixture is either (i) a hydrocarbyl phenol or (ii) a hydrocarbyl phenol and sulphur. Using component (A) (i) the product is a calcium, magnesium or barium hydrocarbyl phenate and using component (A) (ii) the product is a sulphurised calcium, magnesium or barium hydrocarbyl phenate. The hydrocarbyl phenol employed is that alkyl phenol from which is derived the desired hydrocarbyl phenate moiety as hereinbefore described.

[0026] The base (component B) may suitably be an oxide or hydroxide, preferably the hydroxide. Calcium hydroxide may be added for example in the form of slaked lime. Of calcium, magnesium and barium, calcium is preferred. The base must be added in an amount relative to component (A) sufficient to produce a product having a TBN in excess of 300, preferably in excess of 350. This amount will depend on a number of factors including the nature of the sulphurised alkyl phenol and will be higher than the amounts generally employed in prior art processes. Typically, the weight ratio of component (B) to component (A) may suitably be in the range from 0.2 to 50, preferably from 0.4 to 10. The base (B) is added in part to the initial reactants and the remainder in one or more portions at a subsequent stage or stages in the process. In order to produce an additive concentrate having a TNB greater than 350 and a viscosity at 100°C of less than 1000 cSt it is particularly desirable to add component (B) in at least two, and preferably more additions and to add component (F) in an amount greater than 10% by weight based on the weight of the additive concentrate product.

[0027] Component (C) is either a polyhydric alcohol having from 2 to 4 carbon atoms, a di- or tri- (C_2 to C_4) glycol alkyl ether. The polyhydric alcohol may suitably be either a dihydric alcohol, for example ethylene glycol or propylene glycol, or a trihydric alcohol, for example glycerol. The di- or tri- (C_2 to C_4) glycol may suitably be either diethylene glycol or triethylene glycol. The alkylene glycol alkyl ether or polyalkylene glycol alkyl ether may suitably be of the formula:-

$$R\,(OR^1)_xOR^2 \qquad (II)$$

wherein R is a C_1 to C_6 alkyl group, R^1 is an alkylene group, R^2 is hydrogen or C_1 to C_6 alkyl and x is an integer in the range from 1 to 6. Suitable solvents having the formula (II) include the monomethyl or dimethyl ethers of ethylene glycol, diethylene glycol, triethylene glycol or tetraethylene glycol. A particularly suitable solvent is methyl digol ($CH_3OCH_2CH_2OCH_2CH_2OH$). Mixtures of glycols and glycol ethers of formula (II) may also be employed. Using a glycol or glycol ether of formula (II) as solvent it is preferred to use in combination therewith an inorganic halide, for example ammonium chloride, and a lower, i.e. C_1 to C_4, carboxylic acid, for example acetic acid. Preferably the component (C) is either ethylene glycol or methyl digol, the latter in combination with ammonium chloride and acetic acid.

[0028] Component (E) is carbon dioxide, which may be added in the form of a gas or a solid, preferably in the form of a gas. In gaseous form it may suitably be blown through the reaction mixture. We have found that generally the amount of carbon dioxide incorporated increases with increasing concentrations of component (F). In order to produce a concentrate having a TBN greater than about 350 the carbon dioxide is preferably added subsequent to each of two or preferably more additions of component (B).

[0029] Component (F) is a carboxylic acid of formula (I) or an acid anhydride or ester thereof as hereinbefore described. The amount of the aforesaid required to provide from greater than 10 to less than 40% by weight based on the weight of the concentrate will be to a first approximation the amount desired in the concentrate. In calculating this amount allowance should be made for loss of water from carboxylic acids, for example.

[0030] The reaction may be performed in the presence of a diluent. Suitable diluents are liquids having a volatility consistent with operation of the process, i.e. having a volatility such that they are readily strippable from the reaction mixture at the conclusion of the reaction. Examples of suitable diluents include 2-ethyl hexanol, iso-octanol, iso-heptanol and tri-decannol.

[0031] The reaction is carried out in the presence of a catalyst for the reaction. As catalyst there may be used an inorganic halide which may suitably be either a hydrogen halide, an ammonium halide or a metal halide. Suitably the metal moiety of the metal halide may be zinc, aluminium or an alkaline earth metal, preferably calcium. Of the halides, the chloride is preferred. Suitable catalysts include hydrogen chloride, calcium chloride, ammonium chloride, aluminium chloride and zinc chloride, preferably calcium chloride. Suitably the amount of catalyst employed may be up to 2.0% wt/wt.

[0032] Suitably the reaction of components (A) - (F) and also the carbonation reaction may be carried out at elevated temperatures in the range from 120 to 200, preferably from about 130 to 165°C, though the actual temperatures chosen for the reaction of components (A) - (F) and the carbonation may differ if desired. The pressure may be atmospheric, subatmospheric or superatmospheric.

[0033] The concentrate may be recovered by conventional means, for example by distillative stripping of component (C) and diluent (if any).

[0034] Finally, it is preferred to filter the concentrate so-obtained. Generally, the process of the invention will produce a concentrate having an acceptable viscosity, that is a viscosity of less than 1000 cSt at 100°C, and can produce concentrates having a viscosity less than 750 or 500 cSt at 100°C. Moreover, the concentrates generally have desirable viscosity index properties. Such viscometric properties are advantageous because they facilitate processing (including filtration) of the concentrate. However, it is also possible to produce concentrates having a higher viscosity than 1000 cSt at 100°C, generally at higher TBN levels. Filtration of such concentrates presents a problem, which may be overcome by adding a diluent prior to filtration and stripping the diluent off after filtration. Alternatively, high viscosity concentrates, for example concentrates having a viscosity at 100°C greater than 1000 cSt. and also having a high TBN, for example greater than 350, may be diluted by addition of further lubricating oil whilst maintaining a TBN greater than 300, thereby facilitating filtration.

[0035] A finished lubricating oil composition comprises a lubricating oil and sufficient of the additive concentrate as hereinbefore described to provide a TBN in the range from 0.5 to 120.

[0036] Preferably the finished lubricating oil composition contains sufficient of the additive concentrate to provide a TBN in the range from 0.5 to 100.

[0037] The amount of additive concentrate present in the finished lubricating oil will depend on the nature of the final use. Thus, for marine lubricating oils the amount of additive concentrate present may suitably be sufficient to provide a TBN in the range from 9 to 100 and for automobile engine lubricating oils the amount may suitably be sufficient to provide a TBN in the range from 4 to 20.

[0038] The finished lubricating oil may also contain effective amounts of one or more other types of conventional lubricating oil additives, for example viscosity index improvers, anti-wear agents, antioxidants, dispersants, rust inhibitors, pour-point depressants, or the like, which may be incorporated into the finished lubricating oil composition either directly or through the intermediacy of the concentrate.

[0039] In addition to their use as additives for incorporation into lubricating oil compositions, the additive concentrate of the present invention may also find application as fuels additives.

[0040] The invention will now be further illustrated by reference to the following Examples.

[0041] In all the Examples the term "TBN" is used. The TBN is the Total Base Number in mg KOH/g as measured by the method of ASTM D2896.

[0042] The viscosity was measured by the method of ASTM D445.

[0043] In all the Examples, except otherwise expressly stated, a commercially available C_{12}-alkyl phenol obtained by alkylating phenol with propylene tetramer was employed.

Example 1

[0044]

C_{12}alkyl phenol	75 g
Lubricating oil (100 SN)	131 g
Ume	82 g
Sulphur	23 g
Stearic acid	70 g
Calcium chloride	4 g
2-Ethyl hexanol	112 g

Method

[0045]

(a) The charge was heated to 145-165° C/700 mm Hg whilst adding ethylene glycol (36 g),
(b) The mixture was heated at 165°C/700 mm Hg for one hour,
(c) Carbon dioxide (40 g) was added at 165°C/l bar,
(d) The mixture was cooled to 125°C/700 mm Hg,
(e) Lime (35 g) was added at 125°C/700 mm Hg,
(f) The mixture was heated at 165°C/700 mm Hg for one hour,
(g) Carbon dioxide (20 g) was added at 165°C/l bar.
(h) The product was then stripped of solvent at 200°C/10 mm Hg, and
(i) The product was filtered. The filtration rate was fast.

Product Weight

[0046]

Crude Product	436 g
Distillate	169 g

Product Composition After Filtration

[0047]

Calcium	14.1 % w/w
Sulphur	2.9% w/w
CO_2	12.4% w/w
TBN	396
V_{100}	308 cSt
BPHV 150	1
Stearic acid	16.1% w/w

[0048] This Example demonstrates that a high TBN additive concentrate of acceptable viscosity can be produced in a "double lime addition" process according to the present invention.

Example 2 (Comparison)

[0049]

Charge: As for Example 1, except that the amount of lime in the charge was increased from 82 g to 117 g corresponding to the total amount of lime added in Example 1 in two additions.

Method

[0050] As for Example 1 except that the amount of carbon dioxide added in step (c) was increased from 40 g to 60 g and steps (d), (e), (f) and (g) were omitted. The filtration rate in the final step was slow.

Product Weight

[0051]

Crude Product	514 g

Product Composition After Filtration

[0052]

Calcium	14.1% w/w
Sulphur	3.0% w/w
CO_2	12.3% w/w
TBN	390
V_{100}	7600 cSt
Stearic acid	13.6% w/w

[0053] This Example demonstrates that an additive concentrate phenate having a high TBN can be produce in a single lime addition process but under the conditions of the Example the viscosity of the product is unacceptable for commercial operation without dilution with lubricating oil.

Example 3

[0054]

Charge: As for Example 1.

Method

[0055] As for Example 1, except that in step (g) the amount of carbon dioxide was increased from 20 g to 40 g and the following steps were added after step (g) and before steps (h) and (i):

(j) The mixture was cooled to 120°C,
(k) Lime (35 g) was added at 120°C,
(I) The mixture was heated at 165°C/700 mm Hg, and
(m) Carbon dioxide (50 g) was added to the mixture.

Product Weights

[0056]

Crude Product	484 g

(continued)

Distillate	169 g

Product Composition After Filtration

[0057]

Calcium	15.8% w/w
Sulphur	2.6% w/w
CO_2	15.0% w/w
TBN	439
V_{100}	506 cSt
Stearic acid	14.5% w/w

[0058] This Example demonstrates that high TBN additive concentrates can be produced by the process of the invention by a triple lime addition.

Example 4 (Comparison)

[0059]

Charge: As for Example 1 except that the amount of lubricating oil was reduced from 131 g to 158 g and the amount of stearic acid was reduced from 70 g to 43 g.

Method

[0060] As for Example 1 except that in step (d) the mixture was cooled to 135°C instead of 125°C.

Product Weights

[0061]

Crude Product	442 g
Distillate	155 g

Product Composition After Filtration

[0062]

Calcium	14.1% w/w
Sulphur	2.9% w/w
CO_2	11.9% w/w
TBN	393
V_{100}	3440 cSt
Stearic acid	9.8% w/w

[0063] This Example demonstrates by comparison with Example 1 that although a high TBN product can be produced at an acid level less than 10% w/w the viscosity of the product is high.

Example 5

[0064]

Charge:	C_{12}-alkylphenol	35.3 g
	Lubricating oil (SN 100)	131 g
	Sulphur	14.7 g
	Calcium chloride	4.0 g
	Stearic acid	109.1 g
	2-Ethyl hexanol	224 g

Method

[0065]

(a) The mixture was heated to 120°C,
(b) Lime (82 g) was added at 120°C/2" Hg vacuum,
(c) Ethylene glycol (36 g) was added at 145 - 165°C/2" Hg,
(d) The mixture was held at 165°C/2" Hg for 1 hour.
(e) Carbon dioxide (40 g) was added,
(f) The mixture was cooled to 130°C and lime (35 g) added at 130°C/2" Hg,
(g) The mixture was held at 165°C/2" Hg for 1 hour,
(h) Carbon dioxide (20 g) was added at 165°C,
(I) Solvent was stripped from the product at 200°C/30" Hg, and
(j) The product was filtered.

Product Weights

[0066]

Crude Product	397 g
Distillate	245 g

Product Composition After Filtration

[0067]

Calcium	13.6% w/w
Sulphur	1.2% w/w
CO_2	13.9% w/w
TBN	376
V_{100}	142 cSt
V_{100}	1881 cSt
VI	180
Carboxylic acid	27.5% w/w

[0068] This Example demonstrates that a high TBN product having an acceptable viscosity can be obtained using a stearic acid addition of 27.5% w/w based on the weight of the final product.

Example 6

[0069]

Charge: As for Example 5 except that the amount of C_{12}-alkylphenol was reduced from 35.3 g to 15.6 g and the amount of stearic acid was increased from 109.1 g to 128.7 g.

Method

[0070] As for Example 5.

Product Weights

[0071]

Crude Product	416 g
Distillate	242 g

Product Composition After Filtration

[0072]

Calcium	14.5% w/w
Sulphur	1.0% w/w
CO_2	13.6% w/w
TBN (mg KOH/g)	395
V_{100}	255 cSt
V_{40}	3100 cSt
VI	221
Stearic acid	30.9% w/w

[0073] This Example demonstrates that a high TBN product can be obtained at a stearic acid content of 30.9% w/w.

Examples 7

[0074]

Charge	C_{12}-alkyl phenol	64 g
	Lubricating oil (SN 100)	111 g
	Sulphur	20 g
	Stearic acid	59 g
	Calcium chloride	4 g
	2-Ethyl hexanol	190 g

Method

[0075]

(a) The charge was heated to 120°C/700 mm Hg,
(b) Lime (70 g) was added,
(c) The mixture was heated from 145°C to 165°C/700 mm Hg whilst adding ethylene glycol (32 g),
(d) The mixture was held at 165°C/700 mm Hg for 5 minutes.
(e) Carbon dioxide (44 g) was added at 165°C/l bar,
(f) The mixture was cooled to 120°C and lime (60 g) was added,
(g) The mixture was held at 165°C/700 mm Hg for 5 minutes,
(h) Carbon dioxide (44 g) was added at 165°C/l bar,
(i) Solvent was recovered from the product by stripping at 200°C/10 mm Hg, and
(j) The product was filtered.

Product Weights

[0076]

Crude Product	408 g
Distillate	245 g

Product Composition After Filtration

[0077]

Calcium	16.0% w/w
Sulphur	2.6% w/w
CO_2	14.6% w/w
TBN	450
V_{100}	488 cSt
Stearic acid	14.5% w/w

[0078] This Example demonstrates that an additive concentrate having a TBN as high as 450 and an acceptable viscosity can be produced by the process of the invention.

Example 8

[0079]

Charge	C_{12}-alkyl phenol	64 g
	Lubricating oil (SN 100)	111 g
	Sulphur	20 g
	Stearic acid	59 g
	Acetic acid	2 g
	Ammonium chloride	3 g
	Methyl diglycol	40 g

Method

[0080]

(a) The charge was heated to 120°C/100 mm Hg,
(b) Lime (70 g) was added,
(c) The mixture was heated from 145°C to 165°C/700 mm Hg whilst adding methyl diglycol (90 g),
(d) The mixture was held at 165°C/700 mm Hg for 1 hour,
(e) Carbon dioxide (34 g) was added,
(f) The mixture was cooled to 120°C and lime (30 g) was added,
(g) The mixture was held at 165°C/700 mm Hg for 1 hour,
(h) Carbon dioxide (17 g) was added,
(i) Solvent was recovered by stripping at 200°C/10 mm Hg, and
(j) The product was filtered.

Product Weights

[0081]

Crude Product	361 g

(continued)

Distillate	146 g

Product Composition After Filtration

[0082]

Calcium	14.1% w/w
Sulphur	2.7% w/w
CO_2	12.4% w/w
TBN	394
V_{100}	164 cSt
Stearic acid	16.3% w/w

[0083] This Example demonstrates that methyl diglycol can be used as component (C) and that ammonium chloride can be used as the catalyst in the process of the invention.

Example 9

[0084]

Charge	C_{12}-alkyl phenol	64 g
	Lubricating oil (SN 100)	73 g
	C_{18}-linear alpha-olefin	38 g
	Sulphur	23 g
	Stearic acid	59 g
	Calcium chloride	3 g
	2-Ethyl hexanol	190 g

Method

[0085] As for Example 8 except that in step (c) instead of methyl diglycol (90 g) there was used ethylene glycol (31 g) and in steps (d) and (g) the mixture was held at 165°C/700 mm Hg for 10 minutes instead of 1 hour.

Product Weights

[0086]

Crude Product	373 g
Distillate	239 g

Product Composition After Filtration

[0087]

Calcium	14.4% w/w
Sulphur	2.3% w/w
CO_2	13.3% w/w
TBN	405
V_{100}	460 cSt
Stearic acid	15.8% w/w

[0088] This Example demonstrates that a long carbon-chain alpha-olefin can be incorporated in the reaction.

Example 10

[0089]

Charge: As for Example 9 except that instead of the C_{18}-alpha-olefin (38 g) there was used a polyisobutene having an M_n of 500 (38 g).

Method

[0090] As for Example 9.

Product Weights

[0091]

Crude Product	363 g
Distillate	246 g

Product Composition After Filtration

[0092]

Calcium	14.3% w/w
Sulphur	2.8% w/w
CO_2	13.8% w/w
TBN	406
V_{100}	697 cSt
V_{100}	26,600 cSt
VI	175
Stearic acid	16.3% w/w

[0093] This Example demonstrates that a polyisobutene can be incorporated in the reaction.

Comparison Test

[0094]

Charge	C_{12}-alkyl phenol	75 g
	Lubricating oil (SN 100)	131 g
	Sulphur	23 g
	Calcium chloride	4 g
	Acetic acid	15 g
	2-Ethyl hexanol	112 g

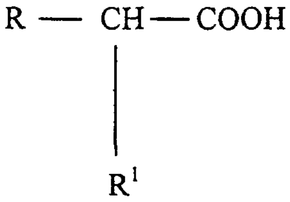
Method

[0095] As for Example 5 (a) - (d). Thereafter the mixture became a thick heterogeneous mass. Stirring was ineffective and the mixture gelled on cooling. The reaction was discontinued.

[0096] This Test demonstrates that acetic acid can not be used as the carboxylic acid in the process of the invention.

Claims

1. An additive concentrate suitable for incorporation into a finished lubricating oil which concentrate is obtainable by reacting in the presence of a catalyst at elevated temperature (A) either (i) a hydrocarbyl phenol or (ii) a hydrocarbyl phenol and sulphur, (B) a calcium, magnesium or barium base added in part to the initial reactants and the remainder in one or more portions at a subsequent stage or stages in the reaction, (C) either a polyhydric alcohol having from 2 to 4 carbon atoms, a di- or tri- (C_2 to C_4) glycol, an alkylene glycol alkyl either or a polyalkylene glycol alkyl ether, (D) a lubricating oil, (E) carbon dioxide added subsequent to each addition of component (B), and (F) sufficient to provide from greater than 10 to less than 40% by weight based on the weight of the concentrate of a carboxylic acid having the formula (I)



$$R-\underset{\displaystyle R^1}{\underset{|}{CH}}-COOH \qquad (I)$$

wherein R is a C_{10} to C_{24} straight chain alkyl group and R_1 is hydrogen, or an acid anhydride or ester thereof, the weight ratio of components (A) and (F) being such as to produce a concentrate having a TBN greater than 300 and a viscosity at 100°C of less than 1,000 $mm^2.s^{-1}$ (cSt).

2. An additive concentrate according to claim 1 wherein the lubricating oil content is from 10 to 90% by weight of the composition.

3. An additive concentrate according to either claim 1 or claim 2 comprising a calcium hydrocarbyl phenate.

4. An additive concentrate according to any one of the previous claims comprising a sulphurised hydrocarbyl phenate.

5. An additive concentrate according to any one of the preceding claims wherein the hydrocarbyl phenol is at least one alkyl phenol, the alkyl group or groups of the alkyl phenol or phenols containing from 9 to 28 carbon atoms.

6. An additive concentrate according to claim 5 wherein the hydrocarbyl phenol is a C_{12}-alkyl phenol obtained by alkylating phenol with propylene tetramer.

7. An additive concentrate according to any one of the preceding claims wherein component (F) is stearic acid.

8. An additive concentrate according to any one of claims 1 to 6 wherein component (F) is a mixture of carboxylic acids of formula (I), which mixture is a commercial grade containing a range of acids, including both saturated and unsaturated acids.

9. An additive concentrate according to any one of the preceding claims wherein component (F) is incorporated in an amount in the range from 12 to 20% by weight based on the weight of the concentrate.

10. An additive concentrate according to any one of the preceding claims wherein the TBN of the concentrate is greater than 350.

11. An additive concentrate according to claim 10 wherein the TBN of the concentrate is greater than 400.

12. An additive concentrate according to any one of the preceding claims wherein the viscosity at 100°C is less than 500 $mm^2.s^{-1}$ (cSt).

13. A process for the production of the additive concentrate as claimed in claims 1 to 12 which process comprises reacting at elevated temperature in the presence of a catalyst (A) either (i) a hydrocarbyl phenol or (ii) a hydrocarbyl phenol and sulphur, (B) a calcium, magnesium or barium base added in part to the initial reactants and the remainder in one or more portions at a subsequent stage or stages in the reaction, (C) either a polyhydric alcohol

having from 2 to 4 carbon atoms, a di- or tri (C_2 to C_4) glycol, an alkylene glycol alkyl ether or a polyalkylene glycol alkyl ether, (D) a lubricating oil, (E) carbon dioxide added subsequent to each addition of component (B), and (F) sufficient to provide from greater than 10 to less than 40% by weight based on the weight of the concentrate of a carboxylic acid having the formula (I) or an acid anhydride or ester thereof the weight ratios of components (A) to (F) being such as to produce a concentrate having a TBN greater than 300 and a viscosity at 100°C of less than 1000 $mm^2.s^{-1}$ (cSt).

14. A process according to claim 13 wherein component (B) is lime.

15. A process according to either claim 13 or claim 14 wherein the weight ratio of component (B) to component (A) is in the range from 0.4 to 10.

16. A process according to any one of claims 13 to 15 wherein component (C) is ethylene glycol.

17. A process according to any one of claims 13 to 15 wherein component. (C) is methyl digol.

18. A process according to any one of claims 13 to 17 wherein a diluent is present.

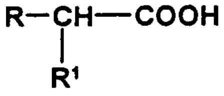
19. A process according to any one of claims 13 to 18 wherein the catalyst is an inorganic halide.

20. A process according to claim 19 wherein the halide moiety of the inorganic halide catalyst is chloride.

21. A process according to any one of claims 13 to 20 wherein the catalyst is calcium chloride.

Patentansprüche

1. Additivkonzentrat, geeignet zum Einbringen in ein fertiges Schmieröl, wobei das Konzentrat erhältlich ist durch Umsetzen in Gegenwart eines Katalysators bei erhöhter Temperatur (A) entweder (i) eines Hydrocarbylphenols oder (ii) eines Hydrocarbylphenols und Schwefels, (B) einer Calcium-, Magnesium- oder Bariumbase, die teilweise zu den ursprünglichen Reaktanten zugesetzt wird und deren Rest in einem oder mehreren Teilen in einer darauffolgenden Stufe oder in darauffolgenden Stufen der Reaktion zugegeben wird, (C) entweder eines mehrwertigen Alkohols mit 2 bis 4 Kohlenstoffatomen, eines Di- oder Tri-(C_2-C_4)Glykols, eines Alkylenglykolalkylethers oder eines Polyalkylenglykolalkylethers, (D) eines Schmieröls, (E) von Kohlendioxid, das nach jeder Zugabe von Komponente (B) zugegeben wird, und (F) genügend einer Carbonsäure mit der Formel (I)



$$R-\underset{\displaystyle R^1}{\underset{|}{CH}}-COOH \qquad (I)$$

worin R eine geradkettige (C_{10}-C_{24})Alkylgruppe darstellt und R^1 Wasserstoff bedeutet oder eines Säureanhydrids oder eines Esters davon, um von mehr als 10 bis weniger als 40 Gew.-%, bezogen auf das Gewicht des Konzentrats, zur Verfügung zu stellen, wobei das Gewichtsverhältnis der Komponenten (A) und (F) so ist, daß ein Konzentrat mit einer TBN von mehr als 300 und einer Viskosität bei 100°C von weniger als 1000 $mm2.s^{-1}$ (cSt) zur Verfügung gestellt wird.

2. Additivkonzentrat nach Anspruch 1, worin der Schmierölgehalt 10 bis 90 Gew.-% der Zusammensetzung beträgt.

3. Additivkonzentrat nach Anspruch 1 oder Anspruch 2, umfassend ein Calciumhydrocarbylphenat.

4. Additivkonzentrat nach einem der vorstehenden Ansprüche, umfassend ein sulfuriertes Hydrocarbylphenat.

5. Additivkonzentrat nach einem der vorstehenden Ansprüche, worin das Hydrocarbylphenol zumindest ein Alkylphenol ist, wobei die Alkylgruppe oder die Alkylgruppen des Alkylphenols oder der Alkylphenole 9 bis 28 Kohlenstoffatome enthält bzw. enthalten.

6. Additivkonzentrat nach Anspruch 5, worin das Hydrocarbylphenol ein C_{12}-Alkylphenol ist, welches durch Alkylieren von Phenol mit einem Propylentetramer erhalten wird.

7. Additivkonzentrat nach einem der vorstehenden Ansprüche, worin die Komponente (F) Stearinsäure ist.

8. Additivkonzentrat nach einem der Ansprüche 1 bis 6, worin die Komponente (F) ein Gemisch aus Carbonsäuren der Formel (I) ist, welches Gemisch eine handelsübliche Qualität ist, welche einen Bereich von Säuren, einschließlich sowohl gesättigter als auch ungesättigter Säuren, enthält.

9. Additivkonzentrat nach einem der vorstehenden Ansprüche, worin die Komponente (F) in einer Menge in einem Bereich von 12 bis 20 Gew.-%, bezogen auf das Gewicht des Konzentrats, eingebracht ist.

10. Additivkonzentrat nach einem der vorstehenden Ansprüche, worin die TBN des Konzentrats mehr als 350 beträgt.

11. Additivkonzentrat nach Anspruch 10, worin die TBN des Konzentrats mehr als 400 beträgt.

12. Additivkonzentrat nach einem der vorstehenden Ansprüche, worin die Viskosität bei 100°C weniger als 500 mm^2 s^{-1} (cSt) beträgt.

13. Verfahren zur Herstellung des Additivkonzentrats nach den Ansprüchen 1 bis 12, welches Verfahren das Umsetzen von (A) entweder (i) einem Hydrocarbylphenol oder (ii) einem Hydrocarbylphenol und Schwefel, (B) einer Calcium-, Magnesium- oder Bariumbase, welche teilweise zu den ursprünglichen Reaktanten zugesetzt wird und der Rest in einem oder mehreren Teilen in einer darauffolgenden Stufe oder in darauffolgenden Stufen in der Reaktion zugesetzt wird, (C) entweder einem mehrwertigen Alkohol mit 2 bis 4 Kohlenstoffatomen, einem Di- oder Tri(C_2-C_4) glykol, einem Alkylenglykolalkylether oder einem Polyalkylenglykolalkylether, (D) einem Schmieröl, (E) Kohlendioxid, welches nachfolgend zu jeder Zugabe der Komponente (B) hinzugefügt wird und (F) genügend einer Carbonsäure mit der Formel (I) oder eines Säureanhydrids oder Esters davon, um von mehr als 10 bis weniger als 40 Gew.-%, bezogen auf das Gewicht des Konzentrats zur Verfügung zu stellen, in Gegenwart eines Katalysators bei erhöhter Temperatur umfaßt, wobei das Gewichtsverhältnis der Komponenten (A) bis (F) derart ist, daß ein Konzentrat mit einer TBN von mehr als 300 und einer Viskosität bei 100°C von weniger als 1000 mm^2 s^{-1} (cSt) hergestellt wird.

14. Verfahren nach Anspruch 13, worin die Komponente (B) Kalk ist.

15. Verfahren nach Anspruch 13 oder Anspruch 14, worin das Gewichtsverhältnis von der Komponente (B) zur Komponente (A) im Bereich von 0,4 bis 10 ist.

16. Verfahren nach einem der Ansprüche 13 bis 15, worin die Komponente (C) Ethylenglykol ist.

17. Verfahren nach einem der Ansprüche 13 bis 15, worin die Komponente (C) Methyldigol ist.

18. Verfahren nach einem der Ansprüche 13 bis 17, worin ein Verdünnungsmittel vorhanden ist.

19. Verfahren nach einem der Ansprüche 13 bis 18, worin der Katalysator ein anorganisches Halogenid ist.

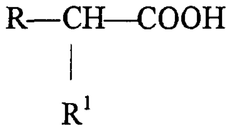
20. Verfahren nach Anspruch 19, worin der Halogenidrest des anorganischen Halogenidkatalysators Chlorid ist.

21. Verfahren nach einem der Ansprüche 13 bis 20, worin der Katalysator Calciumchlorid ist.

Revendications

1. Concentré d'additifs approprié à l'incorporation dans une huile lubrifiante finie, le concentré étant susceptible d'être obtenu par réaction en présence d'un catalyseur à température élevée de (A) soit (i) d'un hydrocarbyl phénol, soit (ii) d'un hydrocarbyl phénol et du soufre, (B) une base dérivée de calcium, magnésium ou baryum ajoutée en partie dans les réactifs de départ, le reste étant ajouté en une ou plusieurs parties à un ou plusieurs stade(s) ultérieur(s) de la réaction, (C) un polyol ayant 2 à 4 atomes de carbone, un di- ou un tri- glycol en C_2 à C_4 un alkyl éther d'alkylène glycol ou un alkyl éther de polyalkylène glycol, (D) une huile lubrifiante, (E) du dioxyde de carbone

ajouté après chaque addition de composé (B), et (F) un acide carboxylique de formule (I)



$$R{-}\underset{\substack{|\\ R^1}}{CH}{-}COOH \qquad (I)$$

dans laquelle R est un radical alkyl à chaîne linéaire en C_{10} à C_{24} et R^1 est l'hydrogène, ou un ester ou un anhydride dudit acide, en quantité suffisante pour représenter plus de 10% et moins de 40% en poids du poids du concentré, le rapport en poids des composants (A) et (F) étant tel que l'on obtienne un concentré ayant un IAT supérieur à 300 et une viscosité à 100°C inférieure à 1 000 $mm^2.s^{-1}$ (cSt).

2. Concentré d'additifs selon la revendication 1, dans lequel l'huile de lubrification constitue 10 à 90 % en poids de la composition.

3. Concentré d'additifs selon la revendication 1 ou 2, comprenant un hydrocarbyl phénolate de calcium.

4. Concentré d'additifs selon l'une quelconque des revendications précédentes, comprenant un hydrocarbyl phénolate sulfuré.

5. Concentré d'additifs selon l'une quelconque des revendications précédentes, dans lequel l'hydrocarbyl phénolate est au moins un alkyl phénol, le groupe alkyl ou les groupes alkyl du (ou des) phénol(s) contenant de 9 à 28 atomes de carbone.

6. Concentré d'additifs selon la revendication 5, dans lequel l'hydrocarbyl phénol est un alkyl (C_{12}) phénol obtenu par alkylation d'un phénol avec un propylène tétramère.

7. Concentré d'additifs selon l'une quelconque des revendications précédentes, dans lequel le composé (F) est l'acide stéarique.

8. Concentré d'additifs selon l'une des revendications 1 à 6, dans lequel le composé (F) est un mélange d'acides carboxyliques de formule (I), ce mélange étant un mélange commercial contenant une série d'acides, comprenant à la fois des acides saturés et des acides insaturés.

9. Concentré d'additifs selon l'une quelconque des revendications précédentes dans lequel le composé (F) est incorporé en quantité représentant 12 à 20 % en poids par rapport au poids du concentré.

10. Concentré d'additifs selon l'une quelconque des revendications précédentes dans lequel l'IAT du concentré est supérieur à 350.

11. Concentré d'additifs selon la revendication 10 dans lequel l'IAT du concentré est supérieur à 400.

12. Concentré d'additifs selon l'une quelconque des revendications précédentes dans lequel la viscosité à 100°C est inférieure à 500 $mm^2.s^{-1}$ (cSt).

13. Procédé de fabrication d'un concentré d'additifs tel que revendiqué dans les revendications 1 à 12, ledit procédé comprenant la réaction à température élevée en présence d'un catalyseur de (A) soit (i) un hydrocarbyl phénol, soit (ii) un hydrocarbyl phénol et du soufre, (B) une base dérivée de calcium, magnésium ou de baryum ajoutée en partie dans les réactifs de départ, le reste étant ajouté en une ou plusieurs parties à un ou plusieurs stade(s) ultérieur(s) de la réaction, (C) un polyol ayant 2 à 4 atomes de carbone, un di- ou tri-glycol en C_2 à C_4, un alkyl éther d'alkylène glycol ou un alkyl éther de polyalkylène glycol, (D) une huile lubrifiante, (E) du dioxyde de carbone ajouté après chaque addition de composant (B), et (F) un acide carboxylique de formule (I) ou un ester ou un anhydride dudit acide, en quantité suffisante pour représenter plus de 10 % et moins de 40 % en poids du poids du concentré, les rapports en poids des composants (A) à (F) étant tels que l'on obtienne un concentré ayant un IAT supérieur à 300 et une viscosité à 100°C inférieure à 1 000 $mm^2.s^{-1}$ (cSt).

14. Procédé selon la revendication 13 dans lequel le composant (B) est de la chaux.

15. Procédé selon l'une des revendications 13 ou 14 dans lequel le rapport en poids du composé (B) au composé (A) est compris entre 0,4 et 10.

16. Procédé selon l'une des revendications 13 à 15 dans lequel le composé (C) est l'éthylène glycol.

17. Procédé selon l'une des revendications 13 à 15 dans lequel le composé (C) est le méthyl digol.

18. Procédé selon l'une des revendications 13 à 17 dans lequel un diluant est présent.

19. Procédé selon l'une des revendications 13 à 18 dans lequel le catalyseur est un halogénure minéral.

20. Procédé selon la revendication 19 dans lequel l'ion halogénure de l'halogénure minéral utilisé comme catalyseur est un chlorure.

21. Procédé selon l'une des revendications 13 à 20 dans lequel le catalyseur est le chlorure de calcium.