

(19)



Europäisches Patentamt
European Patent Office
Office européen des brevets



(11)

EP 0 486 097 B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication and mention
of the grant of the patent:
28.02.1996 Bulletin 1996/09

(51) Int Cl.⁶: **C10L 1/22**

(21) Application number: **91202897.4**

(22) Date of filing: **08.11.1991**

(54) **Process for preparing detergent additive for fuels**

Verfahren zur Herstellung von Reinigungszusatz für Kraftstoffe

Procédé de preparation d'additif détergent pour combustibles

(84) Designated Contracting States:
AT BE CH DE DK ES FR GB GR LI LU NL SE

(30) Priority: **15.11.1990 IT 2207290**

(43) Date of publication of application:
20.05.1992 Bulletin 1992/21

(73) Proprietor: **EURON S.p.A.**
I-20097 San Donato Milanese (IT)

(72) Inventors:
• **Gatti, Emilio**
20157 Milan (IT)

• **Koch, Paolo**
20077 Melegnano (MILAN) (IT)
• **Tontodonati, Antonio**
20097 San Donato Milanese (MILAN) (IT)

(74) Representative: **Fusina, Gerolamo et al**
I-20121 Milano (IT)

(56) References cited:
WO-A-85/00620 **FR-A- 1 254 518**
US-A- 2 885 274 **US-A- 2 921 955**
US-A- 3 088 815 **US-A- 3 183 070**
US-A- 3 426 062 **US-A- 4 018 708**

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

EP 0 486 097 B1

Description

The present invention relates to a process for preparing an additive for liquid fuels, in particular gasolines, which additive is endowed with detergent properties.

To this additives, the task is committed, in internal combustion engines operating on the basis of either Otto or Diesel cycle, of keeping their feed systems clean and free from deposits and fouling, which otherways would reduce their internal boring and would hinder the movements of the parts to which their regulation is committed, with their functional effectiveness and energy efficiency being impaired.

From the prior art some classes of compounds are known, which are used either alone or as mixtures, as detergent additives for fuels. For example, from U.S. patent No. 3,676,089 the alkenylsuccinimides of polyamines; from U.S. patent No. 3,574,576, the polyamines substituted with polyisobutylene groups; from U.S. patent No. 3,649,229 the Mannich bases of polyisobutenylphenols; from U.S. patent No. 4,160,648 polyoxyalkylene aminocarbamates; from U.S. patent No. 4,198,306 polyoxyalkylene aminoesters; from U.S. patent No. 4,247,301 polyoxyalkylene polyamines; from U.S. patent No. 3,873,278 the ammonium salts of fatty polyoxyalkyleneamines and acids, are known.

Such compounds perform their task as detergents, but suffer -- to various extents -- from the drawback that they, inside the engine ignition or combustion chambers, create carbonaceous deposits, which result to be fouling for the hot engine parts, and do not meet the requirement of keeping clean also such parts.

Furthermore, their preparation requires multi-step synthesis processes and, oftentimes, the use of highly toxic and dangerous reactants, such as, e.g., chlorine (in U.S. No. 3,574,576); formaldehyde (in U.S. No. 3,649,229); phosgene (in U.S. No. 4,160,648); hydrochloric acid (in U.S. No. 4,247,301).

The subject-matter of the present invention is a process for preparing a class of detergent additives which fulfil such a function both in cold engine parts (i.e., the carburettor, conduits, injectors, intake valves, and so forth), and in hot engine parts (cylinders, pistons, exhaust valves, and so forth), said process being a single-step process easy to be practiced, by starting from reactants which are by far less toxic and dangerous.

In fact, the present Applicant found that the carbonic esters of higher alcohols containing a functional amino group display marked detergent properties in fuel compositions, without substantial phenomena of fouling in the hot engine parts.

In particular, the present invention concerns a Process for preparing a detergent fuel additive which comprises the step of transesterifying

(i) a tertiary amine having the formula



wherein

n is an integer comprised within the range of from 1 to 4, and

R' is a $-(CH_2)_n-OH$ group or an alkyl radical containing from 1 to 20 carbon atoms, with

(ii) an organic carbonate of formula



wherein

R'' is an alkyl group of from 1 to 4 carbon atoms or an aryl group, and with

(III) an alcohol of general formula



wherein

R₃ represents a straight or branched alkyl group (or a mixture of straight or branched alkyl groups) of from 6 to 30 carbon atoms optionally containing some ethereal oxygen atoms with a ratio of the ethereal oxygen atoms to carbon atoms of not more than 0.5.

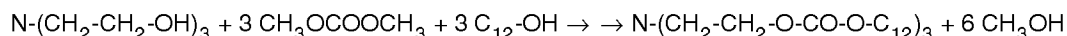
The presence in R₃ of possible ethereal oxygen atoms does not have any substantial effects on the characteristics of the resulting product, provided that such ethereal oxygen atoms are contained within a ratio of ethereal oxygen atoms to carbon atoms of 0.5 max. According to a preferred form of practical embodiment of the present invention, the compound with general formula (I) is triethanolamine or N-butyl-diethanolamine (in which $n = 2$ and R' is hydroxyethyl or

butyl), the compound with general formula (II) is dimethyl carbonate or diphenyl carbonate, the compound with general formula (III) is a mixture of linear or branched, primary aliphatic alcohols of from 7 to 26 carbon atoms -- obtained, e.g., by oxo-synthesis from either linear or branched olefines and carbon oxide and by means of the dimerization of such alcohols --, or a mixture of primary alcohols containing one or more ethereal groups on their alkyl chain -- obtained, e.g., as byproducts of condensation of alcohols in the processes of oxo-synthesis of alcohols from olefines and CO --, or a polyoxypropylene monoether, such as, e.g., polyoxypropylene monobutylether, with a molecular weight of not more than 1,000.

In the process for preparing said oil-soluble amino-carbonates the reaction is preferably carried out by bringing (I)/(II)/(III) reactants into contact with one another, in a mutual molar ratio comprised within the range of from 1:3:3 to 1:10:5, preferably in ratios of round 1:5:3.5. According to an alternative form of practical embodiment of the process of the present invention, the latter is subdivided into two steps: i.e., a first reaction of (I) with the excess of (II), and a subsequent reaction of the intermediate obtained in that way, with alcohol (III). The reaction leading to the product of the present invention can be catalysed by the usual trans-esterification catalysts (sodium hydroxide, potassium hydroxide, titanium alkoxides or tin derivatives), preferably dibutyltin dilaurate.

The reaction temperature is comprised within the range of from 80 to 200°C, preferably of from 100 to 180°C. The reaction is complete when the stoichiometric amount of R"-OH (in the case of dimethyl carbonate or diphenyl carbonate, R"-OH is methanol, or phenol, respectively) was formed from the reactants. The reaction development towards its completion is favoured by subtracting from the reaction mixture the alcohol R"-OH which is formed. For that purpose, the reaction can be favoured by azeotropically distilling off R"-OH, or with reduced pressures, and so forth, according to modalities well known in the art. The same reaction can be advantageously carried out as well in the presence of inert solvents, such as hydrocarbons, chlorinated compounds, and so forth.

The raw reaction product results to be practically free from functional -OH groups, and is prevalingly constituted by the compound of general formula (IV). With reference to the case of use of a C₁₂ alcohol, dimethyl carbonate and triethanolamine, the reaction scheme is as follows:



(IV)

The reaction is accompanied by the appearance of minor amounts of reaction byproducts, e.g., of condensation products of two molecules of triethanolamine with one molecule of dimethyl carbonate, and so on.

The additive according to the present invention results to be effective as a detergent already in very small amounts; the addition of from 0.005 to 0.1% by weight, preferably of from 0.02 to 0.06% by weight, results to be sufficient.

The product obtained from the trans-esterification according to the present invention is an oil-like liquid, having a considerably high viscosity, and difficult to be handled. Due to this reason, the addition thereof to the fuels can be made easier if it is used as a solution, e.g., as a concentrate containing from 25 to 95% by weight, and preferably from 50 to 70%, of the additive, dissolved in a solvent. The solvent can be selected from among alcohols, esters, ethers, hydrocarbons acting as good solvents for the product.

The same type of fuel can be used as the solvent, to which the additive will be subsequently added, such as, e.g., gasoline, gas oil, kerosene. For example, at the end of the synthesis reaction the product is diluted, inside the same reactor, by adding to it the diluent, in the desired amount, and using the same stirring means.

The additive obtained according to the process of present invention, both in concentrate form, and in its state as it is, is compatible with the other additives which are commonly used for combustibles or fuels for internal combustion engines, such as, e.g., antiknock, de-emulsifier, dispersant, antifoaming, rust-preventing additives, as normally used.

The following examples are reported for the purpose of illustrating the present invention without limiting it.

Example No. 1

49.5 grams (0.33 mol) of 98%-pure triethanolamine, 328 grams (1.33 mol) of "C21" alcohol-ether (alcohol-ether C₂₁H₄₄O₂ available from Exxon Chemicals under the designation MD-EA-21), 100 grams (1.1 mol) of dimethyl carbonate and 5 grams of dibutyltin dilaurate are charged to a reactor of 1.5 litres of capacity, equipped with heating jacket, rotary-blade stirrer, thermocouple connected with a temperature reader, dripping funnel and 10-cm-long fractionation column connected with a Claisen condenser with thermometer.

The temperature inside the reaction vessel is increased up to approximately 115°C, by causing a heating fluid coming from a temperature-controlled bath, to circulate inside the reactor jacket. Inside the reactor, an inert atmosphere of nitrogen is maintained. The reaction proceeds with development of methanol, which is distilled off as it is formed: in fact, an azeotropic mixture of dimethyl carbonate/methanol with a composition of about 1:1, is formed. Its development is controlled by maintaining the head temperature under 65°C. As the reaction proceeds, dimethyl carbonate lost through the azeotropic mixture is replenished by adding approximately 65 g thereof through the dripping funnel, with said dimethyl

carbonate being hence kept always in a slight excess in the reaction mixture.

Two hours later, the head temperature is gradually increased during 4 hours, until it reaches the value of 185°C. This temperature value is then maintained for a further 10 hours and, after collecting 110 g of azeotropic mixture, the course of the reaction is started to be checked by I.R. analysis for the hydroxy group. The operation is completed, after about 16 hours, when the hydroxy number decreases down to values of about 10 mg of KOH/g. The reaction mixture is then purged with a nitrogen stream, by operating at the temperature of about 185°C and with a nitrogen flow rate of 100 cc/minute, for one hour. The reaction product, hereinafter indicated to as "Additive A", is a pale yellow liquid having the following characteristics:

- Nitrogen content : 1.13 % by weight
- Hydroxy number (ASTM D 1957) : 7.3 mg of KOH/g
- T.B.N. (total base number) (ASTM D 664): 42.75 mg of KOH/g
- Pour point (ASTM D 97) : -45°C
- Viscosity at 100°C (ASTM D 445) : 11 cSt
- Viscosity at 40°C (ASTM D 445) : 90.8 cSt
- Thermogravimetric analysis (carried out on a Perkin Elmer TGA7 by weighing 1.2 mg of sample, which is heated from 50°C to 500°C at a temperature increase rate of 10°C/minute, with a nitrogen stream flowing at a flow rate of 25 cc/minute): a Loss of 100% at 350°C is evidenced.

Example N. 2

49.5 grams of triethanolamine (0.333 mol), 200 grams (1.0 mol) of isotridecyl alcohol (a prevalingly branched alcohol obtained by oxo-synthesis from propylene tetramers, manufactured by Henkel), 100 grams (1.1 mol) of dimethyl carbonate and 3.9 grams of dibutyltin dilaurate are charged to the previously described reactor.

The reaction mixture is heated up to 115°C, and through the dripping funnel, a further 65 grams of dimethyl carbonate is added. Two hours later, the temperature is gradually increased, within an 8-hour period, up to 180°C. This temperature is maintained for a further 6 hours and, after collecting 110 grams of azeotropic mixture, the reaction course begins to be checked by means of the I.R. analysis of the raw reaction mixture. The operation is ended, after about 16 hours, when the hydroxy number decreases down to values of about 8 mg of KOH/g. Then, a mild stripping, with nitrogen, of the raw reaction mixture is started (180°C for 1 hour, with a nitrogen flow rate of 100 cc/minute). The reaction product, hereinafter indicated to as "Additive B", is a pale yellow liquid, which has the following characteristics:

- Nitrogen content : 1.54 % by weight
- Hydroxy number (ASTM D 1957) : 7.7 mg of KOH/g
- T.B.N. (total base number) (ASTM D 664): 61 mg of KOH/g
- Pour point (ASTM D 97) : -51°C
- Viscosity at 100°C (ASTM D 445) : 6.62 cSt
- Viscosity at 40°C (ASTM D 445) : 40.35 cSt
- Thermogravimetric analysis (carried out as in Example N. 1 : loss of 100% at 335°C.

Example N. 3

The effectiveness of the compounds disclosed herein, and of their mixtures, in keeping clean the intake valves of an internal combustion engine was evaluated by means of the engine rig test, by using a Mercedes M102E engine.

Characteristics of the engine:

- Displacement (litres) : 2.299
 - Bore (mm) : 95.5
 - Stroke (mm) : 80.25
 - Max. power at 5,100 rpm* (kW) : 100
 - Max. torque at 3,500 rpm (Nm) : 205
- * rpm = revolutions per minute

The test time is of 60 hours, and the engine operating conditions are provided for by the "Intake Valve Cleanliness Test" method (FEV- Procedure, September 1988). An unleaded Eurosuper gasoline was used, containing 3.86% of methyl-tert.butyl-ether (MTBE), as anti-knock additive, and to which 400 parts by volume per million parts by volume (ppm vol/vol) of Additive A, produced as disclosed in Example N. 1, had been added.

The gasoline has the following characteristics:

- Specific gravity at 15°C (ASTM D 1298) 0.749 kg/l
- RON (ASTM D 2699) 96.3
- MON (ASTM D 2700) 86.3
- FIA: aromatics (ASTM D 1319) 36 % by vol
- 5 : olefines (ASTM D 1319) 5 % by vol
- : saturated hydrocarbons (ASTM D 1319) 59 % by vol
- Actual gums (ASTM D 381) 2 mg/100cc
- Copper corrosion (ASTM D 130) 1a

10 The four intake valves of the engine were weighed before, and after the test. The difference in weight, expressed as milligrams, is indicative of the amount of deposits formed during the test. The appearance of the deposits is further-
more evaluated by means of a visual method, by comparison to standard valves. The evaluation is given as a merit
rating from 1 to 10, according to the method of CRC Manual N. 5 (a merit rating 10 indicates a completely clean engine).

15 The test results obtained by using gasoline with Additive A added, and taking into consideration the average value
from two test runs, were as follows:

- Average weight of the deposits: 108 mg
- Merit rating : 8.96

20 Example N. 4

 The detergent activity of Additive A, prepared as disclosed in Example N. 1, on the fouling of the feeding system in
general (intake valves and carburettor organs) was determined by means of the engine test on an Opel Kadett 1.2 S
engine. A procedure was followed, which is the one described in CEC -- Coordinating European Council -- F-04-A-87.
25 A reference gasoline, as well as the same gasoline with 400 ppm (v/v) added of Additive A prepared as disclosed in
Example N. 1, were used.

 The test is carried out by feeding, through a system of independent carburettors, two cylinders with the gasoline
without additive, and both residual cylinders with the same gasoline, containing the additive under test. The comparison
of the results (valve fouling, carburettor merit ratings), relevant to the pair of cylinders fed with additive-free gasoline
30 and to the pair of cylinders fed with gasoline with additive added, makes it possible the effectiveness of the tested additive
to be evaluated.

 The test results were the following:

	Gasoline in pristine state	Gasoline with additive added
35 - Intake valve fouling (mg)	413	214
- Cleanliness merit rating (intake valves)	6.70	7.90
- Cleanliness merit rating (throttle valve body)	9.22	9.96
- Cleanliness merit rating (intake manifold)	8.30	8.90
40 - Cleanliness merit rating (throttle valve)	9.26	9.46

 The use of the additive in question reduces by 48.2% the weight of deposits on the intake valves, relatively to the
additive-free gasoline. Furthermore, the cleanliness merit ratings on carburettor organs result to be higher in the case
of gasoline containing the tested additive.

Claims

1. Process for preparing a detergent fuel additive which comprises the step of transesterifying

50 (i) a tertiary amine having the formula



55 wherein

 n is an integer comprised within the range of from 1 to 4, and

R' is a $-(CH_2)_n-OH$ group or an alkyl radical containing from 1 to 20 carbon atoms, with

(ii) an organic carbonate of formula



wherein

R'' is an alkyl group of from 1 to 4 carbon atoms or an aryl group, and with

(III) an alcohol of general formula



wherein

R₃ represents a straight or branched alkyl group (or a mixture of straight or branched alkyl groups) of from 6 to 30 carbon atoms optionally containing some ethereal oxygen atoms with a ratio of the ethereal oxygen atoms to carbon atoms of not more than 0.5.

2. A process according to claim 1, characterized in that compound (I) is triethanolamine or N-butyl-diethanolamine ($n = 2$ and R' is hydroxyethyl or butyl), compound (II) is dimethyl carbonate or diphenyl carbonate, compound (III) is a mixture of linear or branched, primary aliphatic alcohols of from 7 to 26 carbon atoms, or a mixture of primary alcohols containing one or more ethereal groups on their alkyl chain, or a polyoxypropyleneglycol monobutylether.

3. A process according to one or more of claims from 1 to 2, characterized in that the reaction is carried out at 80-200°C, preferably at 100-180°C, using a molar ratio of (I)/(II)/(III) reactants comprised within the range of from 1:3:3 to 1:10:5, preferably of round 1:5:3.5, in the presence of a trans-esterification catalyst, preferably dibutyltin dilaurate.

Patentansprüche

1. Verfahren zur Herstellung eines Reinigungszusatzes für Kraftstoffe, das den Schritt der Umesterung

(i) eines tertiären Amins mit der Formel



worin

n eine im Bereich von 1 bis 4 enthaltene ganze Zahl ist und

R' eine $-(CH_2)_n-OH$ Gruppe oder ein 1 bis 20 Kohlenstoffatome enthaltender Alkylrest ist, mit

(ii) einem organischen Carbonat der Formel



worin

R'' eine Alkylgruppe mit 1 bis 4 Kohlenstoffatomen oder eine Arylgruppe ist und mit

(iii) einem Alkohol der allgemeinen Formel



worin

R₃ eine gerad- oder verzweigt-kettige Alkylgruppe (oder ein Gemisch von gerad- oder verzweigt-kettigen Alkylgruppen) mit von 6 bis 30 Kohlenstoffatomen darstellt, welche wahlweise einige Ethersauerstoffatome mit einem Verhältnis von Ethersauerstoffatomen zu Kohlenstoffatomen von nicht mehr als 0,5 enthält.

2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß die Verbindung (I) Triethanolamin oder N-Butyldiethanolamin ($n = 2$ und R' ein Hydroxyethyl- oder Butylrest ist) ist, Verbindung (II) Dimethylcarbonat oder Diphenylcarbonat ist, Verbindung (III) ein Gemisch aus linearen oder verzweigten, primären aliphatischen Alkoholen mit von 7 bis 26 Kohlenstoffatomen oder ein Gemisch aus primären Alkoholen, welche eine oder mehrere Ethergruppen in

ihre Alkylkette enthalten, oder ein Polyoxypropylenglycolmonobutylether ist.

3. Verfahren nach einem oder mehreren der Ansprüche 1 oder 2, dadurch gekennzeichnet, daß die Umsetzung bei 80 bis 200°C, bevorzugt bei 100 bis 180°C unter Verwendung eines molaren Verhältnisses von (I) / (II) / (III) -Reaktanten, das im Bereich von 1:3:3 bis 1:10:5 liegt, bevorzugt etwa 1:5:3,5, in Gegenwart eines Umesterungskatalysators, bevorzugt Dibutylzinndilaurat, durchgeführt wird.

Revendications

1. -Procédé de préparation d'additif détergent pour combustibles comprenant l'étape de trans-estérification

(i) d'une amine tertiaire de formule



dans laquelle

n est un entier compris dans le domaine allant de 1 à 4, et

R' est un groupe $-(CH_2)_n-OH$ ou un radical alkyle ayant 1 à 20 atomes de carbone, avec

(ii) un carbonate organique de formule



dans laquelle

R'' est un radical alkyle ayant 1 à 4 atomes de carbone ou aryle, et avec

(iii) un alcool de formule générale



dans laquelle

R₃ représente un radical alkyle linéaire ou ramifié (ou un mélange de radicaux alkyle linéaires ou ramifiés) ayant 6 à 30 atomes de carbone éventuellement entrecoupés d'atomes d'oxygène en fonction éther, avec un rapport des atomes d'oxygène en fonction éther aux atomes de carbone d'au plus 0,5.

2. Procédé selon la revendication 1, caractérisé en ce que le composé de formule (I) est le triéthanolamine ou le N-butyldiethanolamine (n = 2 et R' est le radical hydroxyéthyl ou butyl), le composé de formule (II) est le diméthyl carbonate ou le diphényl carbonate, le composé de formule (III) est un mélange d'alcool aliphatiques primaires, linéaires ou ramifiés, ayant de 7 à 26 atomes de carbone, ou un mélange d'alcools primaires contenant une ou plusieurs fonctions éther sur leur chaîne alkyle, ou un éther monobutylique de polyoxypropylèneglycol.

3. Procédé selon l'une quelconque des revendications 1 à 2, caractérisé en ce que la réaction est effectuée à 80-200°C, de préférence à 100-180°C, en utilisant un rapport molaire des réactifs (I)/(II)/(III) compris dans le domaine allant de 1:3:3 à 1:10:5, de préférence environ 1:5:3,5, en présence d'un catalyseur de trans-estérification de préférence le dilaurate de dibutyl-étain.