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(54) SPRAY DRYING APPARATUS AND METHODS OF USE

VORRICHTUNG UND VERFAHREN ZUR SPRÜHTROCKNUNG

APPAREIL DE SECHAGE PAR PULVERISATION ET SES PROCEDES D'UTILISATION

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US-B- 3 956 521

- **PATENT ABSTRACTS OF JAPAN** vol. 1995, no. 07, 31 August 1995 (1995-08-31) & JP 07 090307 A (HOKKAIDO SUMIDEN SEIMITSU KK; OTHERS: 01), 4 April 1995 (1995-04-04)
- **Spray Drying Handbook**, 5th edition, K.Masters, 1991, PartI, Chapters9,12,13,16

Remarks:

The file contains technical information submitted after the application was filed and not included in this specification

Description**Background of the Invention**

5 **[0001]** This invention generally relates to spray dryers and more particularly to methods and equipment for drying particles produced by spray drying.

10 **[0002]** Spray drying is commonly used in the production of particles for many applications, including food, cosmetics, fertilizers, dyes, and abrasives. Spray drying can be tailored to create a wide spectrum of particle sizes, including microparticles. Spray dried particles are useful in a variety of biomedical and pharmaceutical applications, such as the delivery of therapeutic and diagnostic agents, as described for example in U.S. Patent No. 5,853,698 to Straub et al., U.S. Patent No. 5,855,913 to Hanes et al., and U.S. Patent No. 5,622,657 to Takada et al.

15 **[0003]** In a typical process for making particles using a spray drying process, a solid forming material, such as a polymer, which is intended to form the bulk of the particle, is dissolved in an appropriate solvent to form a solution. Alternatively, the material can be suspended or emulsified in a non-solvent to form a suspension or emulsion. Other components, such as drugs, diagnostic agents, or pore forming agents, optionally are added at this stage. The solution then is atomized to form a fine mist of droplets. The droplets immediately enter a drying chamber where they contact a drying gas. The solvent is evaporated from the droplets into the drying gas to solidify the droplets, thereby forming particles. The particles then are separated from the drying gas and collected.

20 **[0004]** In scaling up such a spray drying process, for example from the laboratory or pilot plant scale to the commercial plant scale, certain disadvantages may be encountered. For example, if the drying efficiency is not adequately scaled, the solvent content of the product particles may increase undesirably. While increasing the drying capacity or drying rate should compensate for this insufficient drying, the increased drying rate may induce other problems. For example, it has been observed that increasing the drying rate results in unsuitable particle morphology and/or size distribution for some product particles, such as those having critically defined performance specifications. The change in drying rate may, for instance, alter the way in which the solid-forming material precipitates as the solvent is evaporated, thereby changing the structure (e.g., porosity) of the particle to be out of specification, rendering the particle unable to properly contain and deliver a diagnostic or therapeutic agent. Furthermore, changing the drying rate by reducing the flowrate (and consequently the velocity) of the drying gas may substantially reduce the product yield.

25 **[0005]** Even in cases where particle morphology and size distribution are less critical, scaling up the drying efficiency may require undesirably large increases in the size of process equipment, such as the drying chamber, drying gas source, and drying gas heater. The drying capacity generally is a function of the drying gas temperature, flowrate, pressure, and solvent composition. Moreover, larger capacity equipment generally requires more plant space. It is desirable to minimize the capital investment and space required to scale up a production process.

30 **[0006]** Inadequate product drying can also be a problem with known spray drying processes, particularly for some pharmaceutical products which must be dried at low temperatures in order to maintain the stability and/or activity of these materials. Further drying of these materials sensitive to high temperatures can be done using a fluidized bed; however, this process often results in undesirably variable process yields.

35 **[0007]** Known spray dryers typically are unsuitable for aseptic processing, as they may operate at negative pressure, for example, and may not be designed or constructed to comply with regulatory requirements. In particular, they do not provide a way to completely dry the material aseptically in a sanitizable, closed, and positive-pressure system.

40 **[0008]** It is therefore an object of the present invention to provide a method and apparatus for effectively drying particles made by spray drying.

45 **[0009]** It is another object of the present invention to provide a method and apparatus for spray drying that incorporates a drying process providing improved drying of the particles without detrimentally affecting product yield.

50 **[0010]** It is a further object of the present invention to provide an apparatus for drying spray dried particles that is relatively compact and inexpensive.

55 **[0011]** It is still another object of the present invention to provide a method and apparatus for spray-drying particles at low temperatures so as to preserve the stability or activity of labile materials.

50 **Summary of the Invention**

60 **[0012]** Improved spray drying methods and equipment are provided. In a preferred embodiment of the method, particles are formed by spraying a solution (or emulsion or solid-in-liquid suspension) of a material into a primary drying chamber and evaporating at least a portion of the solvent (or nonsolvent liquid) sufficient to solidify the particles. The solvent (or nonsolvent) is evaporated into the drying gas in which the particles are entrained. Then, the partially dried particles flow from the primary chamber into a secondary drying apparatus for additional drying. The secondary drying apparatus increases the drying efficiency of the spray dryer system without increasing the drying rate, while minimizing loss in yield.

65 **[0013]** The secondary drying apparatus includes tubing having a length sufficient to increase the contact time between

the drying gas and the particles (i.e. increase the residence time) to dry the particles to the extent desired, at a drying capacity or drying rate and temperature which would be too low to provide adequate drying using only the primary drying chamber. The ratio of the length of tubing to the length of the primary drying chamber is at least 2:1, and more preferably at least 3:1. The tubing cross-sectional area is substantially smaller than the cross-sectional area of the primary drying chamber, such that the particles move at higher velocity through the tubing to minimize product losses. The ratio of the cross-sectional area of the primary drying chamber to the cross-sectional area of the tubing preferably is between about 2:1 and 500:1, more preferably is between about 4:1 and 100:1, and most preferably is about 16:1.

[0014] In a preferred embodiment, the tubing is stainless steel, and electropolished to 20 RA or smoother, to provide a smooth surface for enhanced particle yield. The tubing preferably is in a compact coil design, for easier transporting and which has minimum space requirements. The tubing has a jacket to control the temperature of the secondary drying process. The primary drying chamber and secondary apparatus can be integrated into a single unit.

[0015] A preferred application for the spray drying process and equipment is in the production of particles between about 1 and 200 μm in diameter, which can be used in the delivery of a diagnostic or therapeutic agent.

15 Brief Description of the Drawings

[0016]

Figure 1 is a process equipment diagram of a preferred embodiment of the secondary drying apparatus integrated into a process for making and collecting spray dried particles.

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[0017] Improved spray drying methods and equipment have been developed. The improved process design enhances drying of spray dried particles prior to collection by increasing the time the particles contact the drying gas, preferably without increasing the drying rate or reducing the product yield. The increased residence time is accomplished by use of a secondary drying apparatus.

[0018] As used herein, the term "drying" in reference to droplets or particles means the removal of the solvent from the droplet or particle.

[0019] "Drying capacity" refers to the theoretical maximum quantity of liquid volatiles that can be evaporated into the drying gas. For example, if the drying capacity is met, the drying gas stream will be fully saturated with the volatiles. The drying capacity parameter is dependent on the drying gas flowrate, temperature, pressure, and volatile composition.

[0020] "Drying efficiency" refers to the quantity of evaporated liquid volatiles divided by the drying capacity for a given set of process parameters. The drying efficiency parameter depends on the solution flowrate, drying gas flowrate, temperature, pressure, and volatile composition, as well as the geometry of the drying chamber and the residence time of the material being dried.

[0021] "Drying rate" refers to the quantity of liquid volatiles evaporating from the surface of atomized droplets as a function of time. The drying rate is a function of particle size, composition, and morphology; drying gas temperature, pressure, and flowrate; solution flowrate; drying gas humidity; and particle position along the drying path length.

[0022] As used herein, the term "solvent" refers to the liquid in which the material forming the bulk of the spray dried particle is dissolved, suspended, or emulsified for delivery to the atomizer of a spray dryer and which is evaporated into the drying gas, whether or not the liquid is a solvent or nonsolvent for the material. Other volatilizable components, such as a volatile salt, may be included in the bulk material/liquid, and also volatilized into the drying gas. Examples of volatile salts, which are useful pore-forming agents, include ammonium bicarbonate, ammonium acetate, ammonium chloride, and ammonium benzoate.

[0023] The particles made by spray drying processes can be of any size. As used herein, the term "particle" includes micro-, submicro-, and macro-particles. Generally, the particles are between about 100 nm and 5 mm in diameter or longest dimension. The particles can be spheres, capsules, irregular shapes, crystals, powders, agglomerates, or aggregates. The particles can be hollow, that is they can have an outer shell surrounding a core of gas, such as a diagnostic agent, or they can be formed having pores through the solid material, yielding a honeycombed or sponged structure. The particles can be generally solid, that is they can be homogeneous throughout or they can include smaller solid particulates of diagnostic or therapeutic agent dispersed throughout the solid material of each particle.

Apparatus

[0024] A preferred embodiment of the secondary drying apparatus **10** is shown in Figure 1, as part of a spray dryer system. The secondary drying apparatus **10** includes a coil of tubing which forms the drying coil **11**, having drying coil inlet **12** and drying coil outlet **13**. The drying coil **11** is surrounded by a drying coil jacket **16**. The jacket **16** includes a

jacket inlet **14** and a jacket drain **15**. The jacket inlet **14** and jacket drain **15** provide a means for a heat exchange medium, such as cooling water, to flow respectively into and out of the drying coil jacket **16**. The drying coil jacket **16** is based on standard designs known in the heat exchanger art.

[0025] As used herein, the "primary drying chamber" is defined to be the vessel into which the atomized material and solvent is sprayed from the atomizer. The primary drying chamber has an internal flow space terminating in a discharge outlet. As used herein, the "discharge outlet" of the primary drying chamber is defined to be the area in which flowing drying gas/particles initially encounter a reduction in the flow cross-sectional area of at least 25% (i.e. the point at which the ratio of the cross-sectional area of the primary drying chamber to the cross-sectional area of the tubing is at least 4:3).

[0026] As used herein, the "length of the primary drying chamber" is defined to be the approximate minimum distance a droplet/particle must travel from the atomizer to reach the discharge outlet.

[0027] As used herein, the term "atomizer" refers to any atomization device. Representative atomizers include pressure nozzles, pneumatic nozzles, sonic nozzles, and rotary atomizers. Examples of suitable rotary atomizers include bushing wheels, vaned wheels, and vaneless discs. Pressure nozzles include swirled chamber and grooved core types. Pneumatic nozzles include two fluid (internal and external mixing) and three fluid types. Sonic nozzles include siren and whistle types.

[0028] As used herein, the terms "tubing" or "tube" refer to a pipe or other conduit having at least one inlet and at least one outlet. The cross-section of the tubing can be of any shape; circular is preferred. The tubing can be formed into any configuration. For example, it can be straight, serpentine, or coiled. Portions of the tubing can be stacked in connected layers, as commonly found in heat exchanger applications. The coil can be polygonal, circular, or a combination thereof. In a preferred embodiment, a circular coiled design is used, since it provides a compact design and is generally free of sharp bends in the flow path, which can provide unwanted points of particle impact and accumulation.

Tubing Dimensions

[0029] The tubing must have a pathway length long enough to provide sufficient contact time (i.e. residence time) between the drying gas and the particles as the particles travel from the discharge of the primary drying chamber to the product collection point, to dry the particles to the desired level using the specified drying rates, drying gas velocity, and temperatures. As used herein, the term "length" used in reference to the tubing refers to the approximate minimum distance a droplet/particle must travel from the inlet to reach the outlet. At a given velocity, the minimum length required to provide the necessary residence time for a given set of process conditions and materials may have to be obtained empirically. In a preferred method for empirically determining the minimum required length, a series of tubes of increasing length can be used in a series of spray drying tests run at constant flow rate and temperature, followed by measuring the moisture (i.e. the solvent residue) remaining in the product particles. One can then plot the moisture versus tube length to obtain a length-moisture curve. From this curve, one can extrapolate to obtain the minimum length required to obtain a particular moisture level for the set drying rate and drying gas velocity.

[0030] While the methods described above for selecting a residence time and tubing length can be adapted for use with a wide range of drying gas velocities, the velocity of the drying gas has been found to be critical to the production yield of the particles. For example, too low a velocity can cause particles to settle out of the gas stream. Too low of a velocity also can increase aggregation of material along the vessel wall due to (1) cohesion if particles are inadequately dry and have a tacky surface, (2) electrostatic forces due to static build up on well-dried particles, and/or (3) mechanical entrapment, for example, in cracks at piping joints or in microcracks in inadequately polished piping surfaces. The effect of a change in drying gas velocity depends on several factors, such as the particle's size, density, and aerodynamic properties. Typically, the drying gas velocity in the primary drying chamber is between about 0.1 and 100 m/s. In a preferred embodiment, the drying gas velocity in the primary drying chamber is between about 0.5 and 5 m/s.

[0031] In a preferred embodiment, the length of the tubing is at least twice the length of the primary drying chamber. More preferably, this tubing length to primary drying chamber ratio is greater than 3:1.

[0032] For some spray drying applications, the diameter of the tubing of the second drying apparatus is only slightly less than the diameter of the primary drying chamber, for example, having a reduction ratio (primary drying chamber cross-sectional area:tubing cross-sectional area) between 4:3 and 2:1. In a preferred embodiment, however, the diameter of the tubing is significantly smaller than the diameter of the primary drying chamber, thereby increasing the particle and gas velocity in the tubing compared to their velocity in the primary drying chamber in order to maximize product yield. The reduction ratio is preferably between 2:1 and 500:1, more preferably between about 4:1 and 100:1, and most preferably about 16:1. One of skill in the art can readily optimize this ratio for a given product, based on various process parameters, including the mass flow rates of drying gas and particle material and gas transfer equipment specifications.

[0033] The cross-sectional area of the tubing can be constant over, or can vary along, the length of the tubing. For example, one or more reducers (or expanders) can be used to connect sections of tubing to one another or to the primary drying chamber. In a preferred embodiment, the cross-sectional area is substantially uniform along the length of the tubing.

Other Tubing Specifications

[0034] The tubing can be formed of, or lined with, any material of sufficient structural integrity that is compatible with the spray dried particles. The tubing should be resistant to corrosion and crack damage. The tubing material should be compatible with the heat exchange medium selected. Representative materials include glasses, polymers, metals, and composites thereof. Examples of suitable metals include copper, aluminum, iron, brass, nickel, and steel. Polymeric materials generally should be properly grounded to prevent static charge build-up, which can cause particle accumulation and can otherwise be hazardous. Examples of suitable polymeric materials include polyvinylchloride and polytetrafluoroethylene (TEFLON™). The materials of construction are particularly important for particles intended for use in biomedical applications, where purity is essential. In a preferred embodiment, the tubing is medical grade stainless steel.

[0035] The surface roughness of the inside of the tubing generally is a design consideration. A rough surface may reduce the yield and create problems with product purity in some applications, especially pharmaceutical grade products. The tubing preferably has a Roughness Average (RA) of 50 or smoother, and more preferably 20 or smoother. Standard electropolishing techniques can be used, for example, on stainless steel tubing to achieve these roughness levels.

[0036] In a preferred embodiment, the spray drying apparatus and system is designed and constructed to operate in a sterile or aseptic manner in order to produce sterile particles, particularly particles for medical or pharmaceutical products. It is preferred that the sterility can be certified or validated using known techniques. The apparatus can be made using techniques, equipment, and materials known in the art, and should be, for example, resistant to steam, heat, ionizing radiation, and/or sterilizing chemical vapors such as ethylene oxide, volatile peroxides and ozone. Couplings between sections of the apparatus should be selected to maintain the sterile conditions. Examples include TRICLOVER™ or equivalent flanges and gaskets.

[0037] The design and arrangement of the spray drying apparatus also should prevent, or at least minimize, powder accumulating within the apparatus or system except where intended (e.g., in a collector such as a cyclone). For example, the secondary dryer preferably is positioned to provide a constant downward slope from the primary chamber to the collection device. Additional gas feeds, preferably at a controlled temperature and sterile, can be provided at any point in the spray drying apparatus or system to facilitate particle transport and prevent unwanted accumulation throughout the entire apparatus to the collection point.

Method of Use

[0038] A preferred method of using the secondary drying apparatus is described with reference to Figure 1, wherein the secondary drying apparatus **10** is part of a spray drying process that includes a primary drying chamber **20**, a product cyclone **30**, and a product collection container **31**. While Figure 1 shows a co-current vertical downward flow spray dryer having a conical bottom, the methods and apparatus described herein are adaptable to essentially any type of spray dryer, including cross-current, mixed, or spiral flow dryers, having horizontal, vertical-up, or vertical-down flows. The primary drying chamber generally can be of any shape, including cylindrical, conical, or parallelepiped.

[0039] A product solution (C) is sprayed or atomized into primary drying chamber **20** through a nozzle **26**. The drying gas (A) enters through the drying gas feed inlet **23**, passes through drying gas heater **27**, and then flows through drying gas filter **24** to remove dust and other fine particulate matter. The drying gas then enters the primary drying chamber **20** through drying gas inlet **25**. Atomization gas (B) is supplied to nozzle **26** through atomization gas line **28** and fed through atomizer **26** into the primary drying chamber **20**.

[0040] The drying gas flow to drying gas feed inlet **23** can be induced by a variety of gas generating and/or transfer devices, such as a fan, blower, compressor, or liquefied gas evaporator. The gas source can be atmospheric air or a dedicated source of compressed gas or liquefied gas, stored for example in pressurized tanks. In a preferred embodiment, the drying gas is nitrogen, which is generated from a liquid nitrogen vaporizer, wherein the tank or vaporizer pressure provides the driving force.

[0041] The atomized droplets solidify into particles as they contact and are entrained in the cocurrent drying gas flow: Oversized particles are collected in collection jar **22**. The remaining particles exit through primary drying chamber discharge outlet **29** and flow to secondary drying apparatus **10**, where the particles pass through drying coil **11** via inlet **12** and outlet **13**.

The sufficiently dried particles then enter product cyclone **30** through product cyclone inlet **32**. In product cyclone **30**, the particles are separated from the drying gas (D), which is exhausted through product cyclone outlet **33**. The dried particles are collected in product collection container **31**.

[0042] One can finely control the drying process by controlling the circulation of a heat exchange medium through the drying coil jacket **16** during the spray drying process. Representative heat exchange media include water (liquid and steam), acetone, air, brine, d'limonene, ethanol, ethylene glycol, freons, isopropanol, nitrogen (gaseous and liquid), methanol, propylene glycol, silicon oil, and sulfur hexafluoride. Temperature control may be particularly important for maintaining the stability of product particles which are formed or contain highly temperature sensitive substances, such

as thermally labile drugs (including but not limited to proteins, peptides, vaccines, and nucleic acids) while simultaneously maximizing the drying efficiency.

[0043] The spray drying methods and equipment can be adapted for use in either a continuous or batch process.

[0044] In a preferred embodiment, the temperature of the inlet and outlet ports can be controlled to produce the desired products, and may be varied depending on the gas, solvent, and solid material used. For polymeric particles, the size of the particles of polymer solution is a function of the atomizer used to spray the polymer solution, the atomizer pressure, the flow rate, the polymer used, the polymer concentration, the type of solvent, the viscosity, the temperature of spraying (both inlet and outlet temperature), and the molecular weight of the polymer. Generally, the higher the molecular weight, the larger the particle size, assuming the concentration is the same.

[0045] In a typical spray drying process for making particles formed of polymeric materials, therapeutic agents such as drugs, or combinations thereof using the apparatus and methods described herein, the following process parameters are used: inlet temperature = 30 to 400 °C; outlet temperature = 6 to 100 °C; emulsion/solution/suspension flow rate = 5 to 5000 ml/min; and nozzle diameter = 0.2 to 4 mm ID. For polymeric particles, the polymer concentration in the emulsion/solution/suspension typically is 0.001 to 0.75 g/ml, and for drug particles, the drug concentration in the emulsion/solution/suspension also typically is 0.001 to 0.75 g/ml. The particle morphology depends on the several factors, including the selection of polymer and/or therapeutic agent, as well as the concentration, molecular weight, and flow rates of materials. In typical industrial spray drying processes for products that are less temperature sensitive, typical outlet temperatures are between about 70 and 400 °C. Masters, "Spray Drying Handbook" pp. 498-511 (5th ed., John Wiley & Sons 1991) describes typical plant design and spray drying conditions for a variety of materials. These designs and conditions can be adapted for use with the methods described herein.

[0046] Low inlet and outlet temperatures can be important for preserving the stability and activity of many pharmaceutical materials, particularly proteins, vaccines, peptides, nucleic acids, and chemically unstable drugs. Using the spray drying apparatus described herein to dry these materials, the inlet temperature can be less than 100 °C, preferably less than 60 °C, and more preferably less than 40 °C. The outlet temperature typically is equal to or less than the inlet temperature and thus can be less than 100 °C, preferably less than 60 °C, and more preferably less than 40 °C. In many embodiments, temperatures cooler than 40 °C are possible and preferable. For example, outlet temperatures of 25 °C or less, preferably 12 °C or less (See Example 3 below), are desirable, for example, for materials with low melting or degradation points.

Applications

[0047] The secondary drying apparatus and methods described herein can be used in, or adapted to, a variety of spray drying processes to make particles in various industries, including abrasives, agricultural products, biochemical products, chemicals, cosmetics, dyes, foods, metals (e.g. abrasives), pigments, and pharmaceuticals. Representative pharmaceutical and biochemical products and product classes include proteins, peptides, and nucleic acids, as well as antibiotics, enzymes, vitamins, yeasts, sera, vaccines, plasma-derived products, hormones, mycelia, and amino acids. Representative chemicals and metals include acrylonitrile butadiene styrene (ABS), acrylic resin, alumina, aluminum sulfate, zinc and nickel catalysts, graphite, iron oxide, polyvinyl acetate, polyvinyl chloride, silica gel, sodium aluminate, titanium dioxide, and zinc phosphate. See Masters, "Spray Drying Handbook" pp. 499-511 (5th ed., John Wiley & Sons 1991), which describes these and other applications. The selection of the bulk material of the spray dried particle depends on the intended end use of the particle.

[0048] In one preferred embodiment, the spray drying apparatus is used to form particles of a therapeutic agent, which optionally can include one or more excipients. The therapeutic agent can be a small molecule drug or a larger molecule drug (e.g., peptide or protein), such as insulin, growth hormones, erythropoietin, or interferon. In an alternative preferred embodiment, the particles are formed of a bulk or matrix material having the therapeutic agent dispersed throughout the material, for use in controlled drug delivery.

[0049] The secondary drying apparatus preferably is used in a process to make particles having a diameter between about 100 nm and 5 mm, more preferably between about 1 and 200 μm. In a particularly preferred embodiment, the spray drying methods and equipment are adapted to make the microparticles as described in U.S. Patent No. 5,853,698 to Straub et al..

[0050] The polymers that can be used in the methods and equipment described herein include synthetic and natural polymers, non-biodegradable and biodegradable polymers, and water-soluble and water-insoluble polymers. Representative synthetic polymers include poly(hydroxy acids) such as poly(lactic acid), poly(glycolic acid), and poly(lactic acid-co-glycolic acid), polyglycolides, polylactides, polylactide co-glycolide copolymers and blends, polyanhydrides, polyorthoesters, polyamides, polycarbonates, polyalkylenes such as polyethylene and polypropylene, polyalkylene glycols such as poly(ethylene glycol), polyalkylene oxides such as poly(ethylene oxide), polyalkylene terephthalates such as poly(ethylene terephthalate), polyvinyl alcohols, polyvinyl ethers, polyvinyl esters, polyvinyl halides such as poly(vinyl chloride), polyvinylpyrrolidone, polysiloxanes, poly(vinyl alcohols), poly(vinyl acetate), polystyrene, polyurethanes and

co-polymers thereof, derivatized celluloses such as alkyl cellulose, hydroxyalkyl celluloses, cellulose ethers, cellulose esters, nitro celluloses, methyl cellulose, ethyl cellulose, hydroxypropyl cellulose, hydroxy-propyl methyl cellulose, hydroxybutyl methyl cellulose, cellulose acetate, cellulose propionate, cellulose acetate butyrate, cellulose acetate phthalate, carboxylethyl cellulose, cellulose triacetate, and cellulose sulfate sodium salt (jointly referred to herein as "synthetic celluloses"), polymers of acrylic acid, methacrylic acid or copolymers or derivatives thereof including esters, poly(methyl methacrylate), poly(ethyl methacrylate), poly(butylmethacrylate), poly(isobutyl methacrylate), poly(hexylmethacrylate), poly(isodecyl methacrylate), poly(lauryl methacrylate), poly(phenyl methacrylate), poly(methyl acrylate), poly(isopropyl acrylate), poly(isobutyl acrylate), and poly(octadecyl acrylate) (jointly referred to herein as "polyacrylic acids"), poly(butyric acid), poly(valeric acid), and poly(lactide-co-caprolactone), copolymers and blends thereof. As used herein, "derivatives" include polymers having substitutions, additions of chemical groups, for example, alkyl, alkylene, hydroxylations, oxidations, and other modifications routinely made by those skilled in the art. Examples of preferred non-biodegradable polymers include ethylene vinyl acetate, poly(meth)acrylic acid, polyamides, copolymers and mixtures thereof. Examples of preferred biodegradable polymers include polymers of hydroxy acids such as lactic acid and glycolic acid, polylactide, polyglycolide, polylactide co glycolide, and copolymers with PEG, polyanhydrides, poly(ortho)esters, polyurethanes, poly(butyric acid), poly(valeric acid), and poly(lactide-co-caprolactone). Representative natural polymers include proteins and polysaccharides.

[0051] The choice of solvent depends on the bulk material and the form of the material fed to the atomizer, e.g., whether the material is to be dissolved, suspended, or emulsified in the solvent. In a preferred embodiment for use with a polymeric material, the solvent is an organic solvent that is volatile or has a relatively low boiling point or can be removed under vacuum and which is acceptable for administration to humans in trace amounts. Representative solvents include acetic acid, acetaldehyde dimethyl acetal, acetone, acetonitrile, butynol, chloroform, chlorofluorocarbons, dichloromethane, dipropyl ether, diisopropyl ether, N,N-dimethylformamide (DMF), demethyl sulfoxide (DMSO), dioxane, ethanol, ethyl acetate, ethyl formate, ethyl vinyl ether, glycerol, heptane, hexane, isopropanol, methanol, methylene chloride, nitromethane, octane, pentane, tetrahydrofuran (THF), toluene, 1,1,1-trichloroethane, 1,1,2-trichloroethylene, water, xylene, and combinations thereof. In general, the polymer is dissolved in the solvent to form a polymer solution having a concentration of between 0.1 and 75% weight to volume (w/v), more preferably between 0.5 and 30% (w/v).

[0052] The present invention will be further understood with reference to the following non-limiting examples.

Example 1: Comparison of Secondary Drying Apparati

[0053] Three identical polymer emulsions were prepared, each composed of droplets of an aqueous phase suspended in a continuous polymer/organic solvent phase. The polymer was poly(lactide-co-glycolide) (PLGA) (50:50, MW approximately 35,000 Da) and the organic solvent was methylene chloride. The emulsions were sprayed through identical nozzles under identical process conditions of emulsion flow rate, atomization rate, drying gas rate, drying gas inlet temperature, and drying gas outlet temperature. Each emulsion was sprayed into a 6" (15.24 cm) diameter primary drying chamber ("PDC").

[0054] Three different secondary drying apparatus ("SDA") were evaluated: a 4" (10.16 cm) diameter drying chamber, a 6" (15.24 cm) diameter drying chamber, and a 1.5" (3.81 cm) diameter coil 100' (30.5 m) in length. The total drying chamber volume and estimated residence times for each design combination is provided in Table 1.

Table 1:

Drying Chamber Dimensions and Particle Residence Time Factor						
Length of PDC (in.) [cm]	Volume of PDC (in ³) [cm ³]	Diameter of SDA (in.) [cm]	Length of SDA (in.) [cm]	Volume of SDA (in ³) [cm ³]	Total Volume (in ³) [cm ³]	Residence Time Factor
14.0 [35.6]	396 [6487]	4.0 [10.16]	40.0 [101.6]	503 [8237]	898 [14724]	1x
14.0 [35.6]	396 [6487]	6.00 [15.24]	40.0 [101.6]	1131 [18533]	1527 [25020]	1.7x
14.0 [35.6]	396 [6487]	1.50 [3.81]	1200.0 [3048]	2121 [34750]	2516 [41237]	2.8x

[0055] The reduction ratio of the cross-sectional flow area is shown in Table 2.

Table 2:

Reduction Ratios of the Secondary Drying Apparati					
	Diameter of PDC (in.) [cm]	x-Area of PDC (in ²) [cm ²]	Diameter of SDA (in.) [cm]	x-Area of SDA (in ²) [cm ²]	Reduction Ratio
5	6.00 [15.24]	28.27 [182.4]	4.00 [10.16]	12.57 [81.1]	2.25:1
10	6.00 [15.24]	28.27 [182.4]	6.00 [15.24]	28.27 [182.4]	1:1
15	6.00 [15.24]	28.27 [182.4]	1.50 [3.81]	1.77 [11.4]	16:1

[0056] Yield was determined by dividing the collected product mass by the starting solid mass. Particle size of the spray dried product was measured using a Coulter MultiSizer. Moisture content of the spray dried product was determined by Karl Fischer titration. The results of the experiment are shown in Table 3.

Table 3:

Performance Results of Drying Study				
Drying Chamber Design	Batch Size (L)	Yield (% initial solids)	Size-Number Mean (μm)	Moisture Content (%)
6" + 4"	1.5	65.9	2.002	17.63
6" + 6"	1.5	54.2	1.856	11.72
6" + 1.5"	1.5	72.0	2.040	6.86

[0057] The coil system produced the highest yield (72%) and the lowest moisture (6.86%) of the three systems evaluated. As shown in Table 1, the residence times and drying capacities of the three systems are not identical, which probably accounts for at least some of the variation in measured moisture content. The variation in yield, however, is more striking, since if one were to increase the lengths of the 4" (10.16 cm) and 6" (15.24 cm) secondary chambers to provide a volume identical to that of the coils, the yield for the 4" (10.16 cm) and 6" (15.24 cm) secondary chamber systems would be even less than that of the coil system. The yield difference is most likely due to the comparatively lower drying gas velocity in the 4" (10.16 cm) and 6" (15.24 cm) secondary chambers.

Example 2: Comparison of Secondary Drying Apparati

[0058] Four identical polymer emulsions were prepared, each composed of an aqueous phase suspended in a continuous phase of polymer dissolved in an organic solvent. The emulsions were spray dried through identical nozzles under identical process conditions of emulsion flow rate, atomization rate, drying gas rate, drying gas inlet temperature, and drying gas outlet temperature. Each emulsion was sprayed into the same primary drying chamber, which had a diameter of 6" (15.24 cm) and a length of 18" (45.72 cm), for a total volume of 509 in³ (8340 cm³).

[0059] One emulsion was sprayed only into the primary drying chamber, while the three other emulsions were sprayed into the primary drying chamber and a secondary drying apparatus. Three different secondary drying apparatus having the same volume were evaluated: a 6" (15.24 cm) diameter tube, a 4" (10.16 cm) diameter tube, and a 1.5" (3.81 cm) diameter tube. Additional adaptors and tubing (1.5" (3.81 cm) diameter) were used to connect the primary drying chamber to the secondary drying apparatus and to connect the secondary drying apparatus to the cyclone. Since the volume of the connecting pieces was approximately the same for all PDC/SDA configurations, the total drying chamber volume remained approximately the same. The dimensions and volumes are shown below in Table 4.

Table 4:

Drying Chamber Dimensions and Volumes																																											
	Vol. PDC (in ³) [cm]	Dia. SDA (in.) [cm]	Length SDA (in.) [cm]	Vol. SDA (in ³) [cm ³]	Connecting Vol. (in ³) [cm ³]	Total Vol. (in ³) [cm ³]	Ratio of Cross- Sectional Area (PDC: SDA)																																				
5	509 [8340]	N/A	N/A	0 [0]	10 [164]	519 [8504]	N/A																																				
10	509 [8340]	6.00 [15.24]	37.0 [94.0]	1046 [17143]	320 [5244]	1875 [30727]	1:1																																				
15	509 [8340]	4 [10.16]	85.0 [215.9]	1068 [17504]	260 [4261]	1837 [30104]	2.25:1																																				
20	509 [8340]	1.50 [3.81]	600.0 [1524.0]	1060 [17375]	280 [4588]	1849 [30303]	16:1																																				
25	[0060] Samples of each product were lyophilized to determine the dry weight fraction of the product. The dry yield then was calculated as a percentage of the total polymer mass sprayed, using the following equation:																																										
30	$\text{Yield} = \frac{(\text{collected product mass}) \times (\text{dry weight fraction})}{(\text{total polymer mass sprayed})} \quad (\text{EQ. 1})$																																										
35	[0061] Particle size of the spray dried product was measured using a Coulter Multisizer. Moisture content of the spray dried product was determined by Karl Fischer titration. The results of these analyses are provided in Table 5.																																										
40	Table 5:																																										
45	<table border="1"> <thead> <tr> <th colspan="6">Performance Results of Drying Study</th> </tr> <tr> <th>Diameter of SDA (in.) [cm]</th> <th>Ratio of Cross-Sectional Area (PDC:SDA)</th> <th>Batch Size (L)</th> <th>Size-Number Mean (μm)</th> <th>Moisture Content (%)</th> <th>Dry Yield (%)</th> </tr> </thead> <tbody> <tr> <td>No SDA</td> <td>N/A</td> <td>6.0</td> <td>2.201</td> <td>28.6</td> <td>92.7</td> </tr> <tr> <td>6 [15.24]</td> <td>1:1</td> <td>6.0</td> <td>1.892</td> <td>13.0</td> <td>64.8</td> </tr> <tr> <td>4 [10.16]</td> <td>2.25:1</td> <td>6.0</td> <td>1.967</td> <td>13.3</td> <td>72.7</td> </tr> <tr> <td>1.5 [3.81]</td> <td>16:1</td> <td>6.0</td> <td>1.956</td> <td>12.2</td> <td>75.0</td> </tr> </tbody> </table>							Performance Results of Drying Study						Diameter of SDA (in.) [cm]	Ratio of Cross-Sectional Area (PDC:SDA)	Batch Size (L)	Size-Number Mean (μm)	Moisture Content (%)	Dry Yield (%)	No SDA	N/A	6.0	2.201	28.6	92.7	6 [15.24]	1:1	6.0	1.892	13.0	64.8	4 [10.16]	2.25:1	6.0	1.967	13.3	72.7	1.5 [3.81]	16:1	6.0	1.956	12.2	75.0
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1.5 [3.81]	16:1	6.0	1.956	12.2	75.0																																						
50	[0062] The moisture content of 28.6% obtained when the primary drying chamber was used without the secondary drying apparatus was undesirably high. The results show that the use of a secondary drying apparatus reduced the moisture content by approximately 55% and also reduced the mean particle size slightly. The size and moisture content obtained with the secondary drying apparatus were approximately the same for all configurations, which is expected since the emulsions were sprayed under identical process conditions and since each secondary drying apparatus had essentially the same total volume and residence time.																																										
55	[0063] The results indicate that the use of a secondary drying apparatus reduced the dry yield, presumably since some product was deposited onto the walls of the secondary drying apparatus, but that the yield increased as the ratio of the cross-sectional area of the primary drying chamber to the secondary drying apparatus increased. The yield difference was most likely due to the comparatively lower drying gas velocity in the 6" and 4" diameter secondary drying apparatus. By using a long length of smaller diameter tubing, it is possible to maximize the drying capacity while minimizing product loss. The experiment indicates that the drying capacity of the spray dryer can be increased by using a secondary drying apparatus and that the decrease in product yield can be minimized by using the secondary drying apparatus																																										

described herein.

Example 3: Making PLGA Microparticles at Low Temperatures

5 [0064] The spray drying apparatus described in Example 1 was used to make and dry particles of poly(lactide-co-glycolide) (PLGA) (50:50, MW approximately 35,000 Da) using low processing temperatures. The primary drying chamber had a length of 19 inches (48.26 cm) and a diameter of 6 inches (15.24 cm), and the secondary drying apparatus had a diameter of 1.5 inches (3.81 cm) and a length of 100 feet (30.5 m).

10 [0065] The PLGA was dissolved in methylene chloride to form approximately 29 L (liters) of a 3% (w/w) PLGA solution. The polymer solution then was emulsified with 2 L of an aqueous solution of 18% ammonium bicarbonate in a 75 liter mixing tank fitted with an Admix Rotosolver homogenizer (Model 100RS88SS) by homogenizing for 6.5 minutes at 3450 RPM.

15 [0066] The emulsion was sprayed at a flow rate of 150 ml/min. and aerosolized with nitrogen at a flow rate of 115 liter/min. in an internal-mixing air-atomizing nozzle. Drying gas (nitrogen) was heated to an inlet temperature of 55 °C and introduced into the drying chamber at a flow rate of 105 kg/hr. The drying gas outlet temperature was found to be 12 °C. The partially dried particles (exiting the primary drying chamber) were passed through the secondary drying apparatus, which was jacketed with water at 18 °C, and then collected.

20 [0067] The overall yield of particles collected was 91%. The particles had a size distribution characterized by a number-average (X_n) diameter of 2.0 μm and a volume-average diameter (X_v) of 5.3 μm , as determined in a Coulter counter. The moisture content was 5.18% (w/w). The low moisture content was achieved using drying gas temperatures significantly lower than standard practice in current spray drying systems.

Example 4: Making PEG Microparticles at Low Temperatures

25 [0068] The process described in Example 3 was repeated, except for the following parameters: (1) polyethylene glycol (PEG) (MW 8000) was used in place of PLGA; (2) the primary chamber length was 25 inches (63.5 cm); (3) the homogenization time was 10 minutes; (4) the drying gas flow rate was 150 kg/hr; and (5) the flow rate of polymer emulsion to the spray nozzle was 200 ml/min.

30 [0069] The overall yield of free-flowing particles collected was 96%. The low temperature processing allowed the preparation of particles of PEG, which might otherwise melt or fuse together during processing, as the melting temperature of PEG (MW 8000) is typically between about 55 and 65 °C. Examples 3 and 4 thus demonstrate that both the inlet and outlet drying gas temperatures can be lowered using the spray drying devices and methods described herein as compared to those temperatures typically used in conventional spray drying.

35 [0070] Modifications and variations of the present invention will be obvious to those of skill in the art from the foregoing detailed description. Such modifications and variations are intended to come within the scope of the following claims.

Claims

40 1. A spray drying apparatus comprising
a primary drying chamber having an internal flow space terminating in a discharge outlet, and
a secondary drying chamber comprising tubing having an inlet in fluid communication with the discharge outlet of the primary drying chamber,
wherein the ratio of the cross-sectional area of the primary drying chamber to the cross-sectional area of the tubing is at least 413, and
wherein the ratio of the length of the tubing to the length of the primary drying chamber is at least 2:1, and wherein
the tubing has a jacket through which a heat exchange medium may be circulated to control the temperature in the tubing.

45 2. The apparatus of claim 1 wherein the ratio of the length of the tubing to the length of the primary drying chamber is at least 3:1.

3. The apparatus of claim 1 wherein the ratio of the cross-sectional areas of the primary drying chamber to the cross sectional area of the tubing is between about 2:1 and 500:1, preferably between about 4:1 and 100:1, more preferably about 16:1.

55 4. The apparatus of claim 1 wherein the tubing is in a coil.

5. The apparatus of claim 1 wherein the tubing further comprises an outlet in fluid communication with a particle collection device.

6. The apparatus of claim 1 wherein the tubing comprises 50 RA or smoother stainless steel.

7. The apparatus of claim 1 adapted to be operable under sterile or aseptic conditions, thereby forming spray dried particles that are sterile.

8. A method of making particles comprising

10 (a) spraying an emulsion, solution or suspension which comprises a solvent and a bulk material through an atomizer, in a primary drying chamber having a discharge outlet and containing a drying gas, to form droplets of the solvent and bulk material dispersed in the drying gas;

15 (b) evaporating a portion of the solvent into the drying gas to solidify the droplets and form particles;

(c) flowing the particle and drying gas through a secondary drying chamber comprising tubing having an inlet in fluid communication with the discharge outlet of the primary drying chamber, to evaporate a second portion of the solvent into the drying gas,

20 wherein the ratio of the cross-sectional area of the primary drying chamber to the cross-sectional area of the tubing is at least 4:3, and

wherein the ratio of the length of the tubing to the length of the primary drying chamber is at least 2:1, and wherein the tubing is jacketed and the jacketing contains a heat exchange medium for controlling the temperature in the tubing.

9. The method of claim 8 wherein the apparatus is as defined in any of claims 2 to 7.

25 10. The method of claim 9 wherein the jacketing contains cooling water.

11. The method of claim 8 wherein the bulk material is a polymer and the particles are microparticles.

30 12. The method of claim 11 wherein the microparticles are between about 1 and 10 μ m in diameter.

13. The method of claim 11 wherein the microparticles contain a therapeutic or diagnostic agent.

35 14. The method of claim 8 wherein the bulk material is a therapeutic or diagnostic agent.

15. The method of claim 8 solution or suspension further comprises a volatile salt that is volatilized in step (b), step (c), or a combination thereof.

40 16. The method of claim 8 wherein the drying gas entering the primary drying chamber in step (a) has an inlet temperature less than 100 °C, preferably less than 60 °C, more preferably less than 40 °C.

17. The method of claim 8 wherein the drying gas exiting the secondary drying apparatus has an outlet temperature less than 100 °C preferably less than 60°C, more preferably less than 40 °C, even more preferably less than 25 °C.

45 18. A secondary drying chamber adaptable to the particle/gas discharge outlet of a primary drying chamber of a spray dryer comprising

tubing having an inlet that can be connected in fluid engagement to the discharge outlet of the primary drying chamber, wherein the ratio of the cross-sectional area of the primary drying chamber to the cross-sectional area of the tubing is at least 4:3, and and

50 wherein the ratio of the length of the tubing to the length of the primary drying chamber is at least 2:1, and wherein the tubing has a jacket through which a heat exchange medium may be circulated to control the temperature in the tubing.

19. The secondary drying chamber of claim 18 wherein the tubing comprises 50 RA or another stainless steel.

55 20. The secondary drying chamber of claim 18 wherein the tubing in a coiled configuration.

Patentansprüche

1. Sprühtrocknungsapparatur, umfassend

5 eine primäre Trockenkammer mit einem internen Strömungsraum, der in einer Auslassöffnung endet, und eine sekundäre Trockenkammer, die eine Rohrleitung mit einem Einlass umfasst, der mit der Auslassöffnung der primären Trockenkammer in Fluidverbindung ist, wobei das Verhältnis der Querschnittsfläche der primären Trockenkammer zur Querschnittsfläche der Rohrleitung wenigstens 4:3 ist, und wobei das Verhältnis der Länge der Rohrleitung zur Länge der primären Trockenkammer wenigstens 2:1 ist, und 10 wobei die Rohrleitung eine Ummantelung aufweist, durch die ein Wärmeaustauschermedium zur Steuerung der Temperatur in der Rohrleitung zirkuliert werden kann.
2. Apparatur nach Anspruch 1, wobei das Verhältnis der Länge der Rohrleitung zur Länge der primären Trockenkammer wenigstens 3:1 ist. 15
3. Apparatur nach Anspruch 1, wobei das Verhältnis der Querschnittsfläche der primären Trockenkammer zur Querschnittsfläche der Rohrleitung zwischen ungefähr 2:1 und 500:1 liegt, vorzugsweise zwischen ungefähr 4:1 und 100:1, bevorzugter bei ungefähr 16:1.
4. Apparatur nach Anspruch 1, wobei die Rohrleitung in einer Rohrschlaufe vorliegt. 20
5. Apparatur nach Anspruch 1, wobei die Rohrleitung außerdem einen Auslass umfasst, der mit einer Vorrichtung zum Sammeln von Teilchen in Fluidverbindung ist.
6. Apparatur nach Anspruch 1, wobei die Rohrleitung 50-RA-Stahl oder glatteren rostfreien Stahl umfasst. 25
7. Apparatur nach Anspruch 1, die so angepasst ist, dass sie unter sterilen oder aseptischen Bedingungen betrieben werden kann, wodurch sprühgetrocknete Teilchen gebildet werden, die steril sind.
8. Verfahren zur Herstellung von Teilchen, umfassend das
 - (a) Sprühen einer Emulsion, Lösung oder Suspension, die ein Lösemittel und eine Masse eines Materials umfasst, durch einen Zerstäuber in eine primäre Trockenkammer, die eine Auslassöffnung aufweist und ein Trocknungsgas enthält, zur Erzeugung von Tröpfchen aus dem Lösemittel und der Masse des Materials, die im Trocknungsgas dispergiert sind; 35
 - (b) Verdampfen eines Teils des Lösemittels in das Trocknungsgas, um die Tröpfchen zu verfestigen und Teilchen zu bilden;
 - (c) Strömenlassen des Teilchens und des Trocknungsgases durch eine sekundäre Trockenkammer, die eine Rohrleitung umfasst, die einen Einlass in Fluidverbindung mit der Auslassöffnung der primären Trockenkammer aufweist, um einen zweiten Teil des Lösemittels in das Trocknungsgas zu verdampfen, 40

wobei das Verhältnis der Querschnittsfläche der primären Trockenkammer zur Querschnittsfläche der Rohrleitung wenigstens 4:3 ist, und

wobei das Verhältnis der Länge der Rohrleitung zur Länge der primären Trockenkammer wenigstens 2:1 ist, und 45 wobei die Rohrleitung eine Ummantelung aufweist und die Ummantelung ein Wärmeaustauschermedium zur Steuerung der Temperatur in der Rohrleitung enthält.
9. Verfahren nach Anspruch 8, wobei die Apparatur so ausgelegt ist, wie es in einem beliebigen der Ansprüche 2 bis 7 definiert ist. 50
10. Verfahren nach Anspruch 9, wobei die Ummantelung Kühlwasser enthält.
11. Verfahren nach Anspruch 8, wobei die Masse des Materials ein Polymer ist und die Teilchen Mikroteilchen sind.
- 55 12. Verfahren nach Anspruch 11, wobei die Mikroteilchen einen Durchmesser zwischen 1 und 10 µm haben.
13. Verfahren nach Anspruch 11, wobei die Mikroteilchen ein therapeutisches oder diagnostisches Mittel enthalten.

14. Verfahren nach Anspruch 8, wobei die Masse des Materials ein therapeutisches oder diagnostisches Mittel ist.

15. Verfahren nach Anspruch 8, wobei die Lösung oder Suspension außerdem ein flüchtiges Salz umfasst, das im Schritt (b), im Schritt (c) oder in einer Kombination von diesen verdampft wird.

5 16. Verfahren nach Anspruch 8, wobei das Trocknungsgas beim Eintreten in die primäre Trockenkammer im Schritt (a) eine Eintrittstemperatur von unter 100°C hat, vorzugsweise von unter 60°C, bevorzugter von unter 40°C.

10 17. Verfahren nach Anspruch 8, wobei das Trocknungsgas beim Verlassen der sekundären Trockenapparatur eine Austrittstemperatur von unter 100°C hat, vorzugsweise von unter 60°C, bevorzugter von unter 40°C, und noch bevorzugter von unter 25°C.

15 18. Sekundäre Trockenkammer, die an den Auslass für die Abgabe von Teilchen/Gas einer primären Trockenkammer eines Sprühtrockners angepasst werden kann, umfassend eine Rohrleitung mit einem Einlass, der in Fluidverbindung mit der Auslassöffnung der primären Trockenkammer verbunden werden kann, wobei das Verhältnis der Querschnittsfläche der primären Trockenkammer zur Querschnittsfläche der Rohrleitung wenigstens 4:3 ist, und wobei das Verhältnis der Länge der Rohrleitung zur Länge der primären Trockenkammer wenigstens 2:1 ist, und 20 wobei die Rohrleitung eine Ummantelung aufweist, durch die ein Wärmeaustauschermedium zur Steuerung der Temperatur in der Rohrleitung zirkuliert werden kann.

19. Sekundäre Trockenkammer nach Anspruch 18, wobei die Rohrleitung 50-RA-Stahl oder glatteren rostfreien Stahl umfasst.

25 20. Sekundäre Trockenkammer nach Anspruch 18, wobei die Rohrleitung in Form einer Rohrschlange vorliegt.

30 **Revendications**

1. Appareil de séchage par pulvérisation comprenant une première chambre de séchage ayant un espace d'écoulement interne se terminant par une sortie de refoulement, et une seconde chambre de séchage comprenant un tubage ayant une entrée en communication fluidique avec la sortie de refoulement de la première chambre de séchage, dans lequel le rapport de la zone de coupe transversale de la première chambre de séchage à la zone de coupe transversale du tubage est au moins 4:3, et dans lequel le rapport de la longueur du tubage à la longueur de la première chambre de séchage est au moins 2:1, et dans lequel le tubage possède une chemise à travers laquelle un milieu échangeur de chaleur peut être mis en circulation pour contrôler la température dans le tubage.

2. Appareil selon la revendication 1, dans lequel le rapport de la longueur du tubage à la longueur de la première chambre de séchage est au moins 3:1.

3. Appareil selon la revendication 1, dans lequel le rapport de la zone de coupe transversale de la première chambre de séchage à la zone de coupe transversale du tubage est entre 2:1 et 500:1 environ, préféablement entre 4:1 et 40 100:1 environ, de préférence 16:1 environ.

4. Appareil selon la revendication 1, dans lequel le tubage est dans un rouleau.

5. Appareil selon la revendication 1, dans lequel le tubage comprend en outre une sortie en communication fluidique avec un dispositif de récupération de particules.

6. Appareil selon la revendication 1, dans lequel le tubage comprend un acier inoxydable de 50 RA ou plus lisse.

55 7. Appareil selon la revendication 1, adapté pour pouvoir fonctionner dans des conditions stériles ou aseptiques, formant ainsi des particules séchées par pulvérisation qui sont stériles.

8. Procédé de fabrication de particules comprenant les étapes consistant à :

5 (a) pulvériser une émulsion, une solution ou une suspension qui comprend un solvant et un matériau en vrac à travers un pulvérisateur, dans une première chambre de séchage ayant une sortie de refoulement et contenant un gaz de séchage, pour former des gouttelettes du solvant et du matériau en vrac dispersées dans le gaz de séchage ;

10 (b) faire évaporer une partie du solvant dans le gaz de séchage pour solidifier les gouttelettes et former des particules ;

15 (c) faire couler la particule et le gaz de séchage à travers une seconde chambre de séchage comprenant un tubage ayant une entrée en communication fluidique avec la sortie de refoulement de la première chambre de séchage, pour faire évaporer une seconde partie du solvant dans le gaz de séchage,

dans lequel le rapport de la zone de coupe transversale de la première chambre de séchage à la zone de coupe transversale du tubage est au moins 4:3, et

15 dans lequel le rapport de la longueur du tubage à la longueur de la première chambre de séchage est au moins 2:1, et dans lequel le tubage est chemisé et la chemise contient un milieu échangeur de chaleur pour contrôler la température dans le tubage.

9. Procédé selon la revendication 8, dans lequel l'appareil est comme défini selon l'une quelconque des revendications 20 2 à 7.

10. Procédé selon la revendication 9, dans lequel la chemise contient de l'eau de refroidissement.

11. Procédé selon la revendication 8, dans lequel le matériau en vrac est un polymère et les particules sont des micro-particules.

25 12. Procédé selon la revendication 11, dans lequel les microparticules ont entre 1 et 10 μm environ de diamètre.

30 13. Procédé selon la revendication 11, dans lequel les microparticules contiennent un agent thérapeutique ou diagnostique.

35 14. Procédé selon la revendication 8, dans lequel le matériau en vrac est un agent thérapeutique ou diagnostique.

15. Procédé selon la revendication 8, dans lequel la solution ou la suspension comprend en outre un sel volatil qui est volatilisé à l'étape (b), l'étape (c), ou une combinaison de celles-ci.

40 16. Procédé selon la revendication 8, dans lequel le gaz de séchage entrant dans la première chambre de séchage dans l'étape (a) a une température d'entrée inférieure à 100° C, préféablement inférieure à 60° C, de préférence inférieure à 40° C.

45 17. Procédé selon la revendication 8, dans lequel le gaz de séchage sortant du second appareil de séchage a une température de sortie inférieure à 100° C, préféablement inférieure à 60° C, de préférence inférieure à 40° C, de préférence même inférieure à 25° C.

18. Seconde chambre de séchage adaptable à la sortie de refoulement de particule/gaz d'une première chambre de séchage d'un sécheur par pulvérisation comprenant :

50 un tubage ayant une entrée qui peut être raccordée en un engagement fluidique à la sortie de refoulement de la première chambre de séchage,

dans lequel le rapport de la zone de coupe transversale de la première chambre de séchage à la zone de coupe transversale du tubage est au moins 4:3, et

55 dans lequel le rapport de la longueur du tubage à la longueur de la première chambre de séchage est au moins 2:1, et dans lequel le tubage possède une chemise à travers laquelle un milieu échangeur de chaleur peut être mis en circulation pour contrôler la température dans le tubage.

19. Seconde chambre de séchage selon la revendication 18, dans laquelle le tubage comprend un acier inoxydable de 50 RA ou plus lisse.

20. Seconde chambre de séchage selon la revendication 18, dans laquelle le tubage est dans une configuration enroulée.

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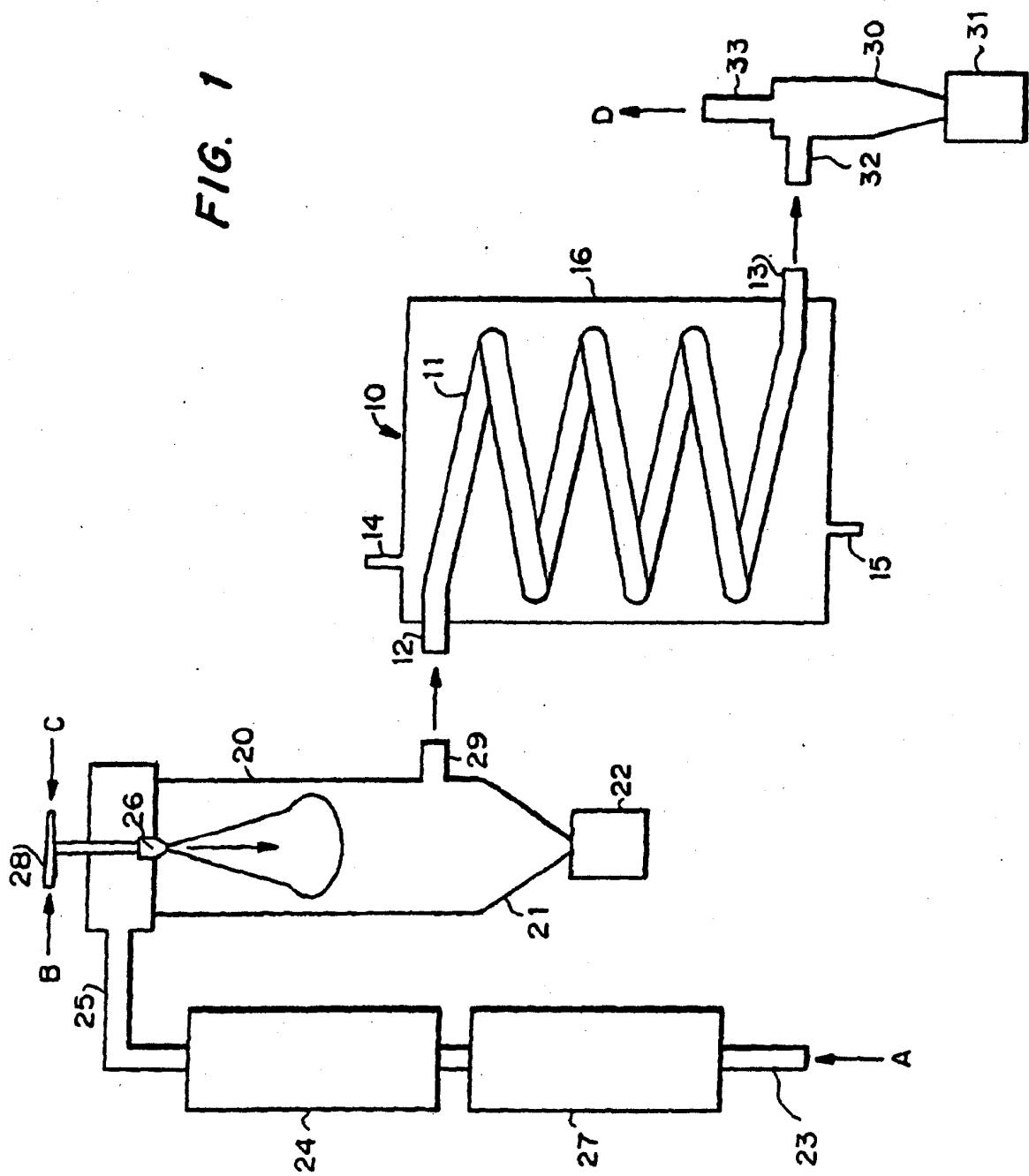
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FIG. 1



REFERENCES CITED IN THE DESCRIPTION

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