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(54) **Process and apparatus for nitrous oxide removal**

Verfahren und Vorrichtung zur Entfernung von Distickstoffmonoxid

Procédé et dispositif pour l'élimination de l'oxyde nitreux

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Description

[0001] The present invention relates to a process and an apparatus for the removal of nitrous oxide from a feed gas stream.

[0002] The cryogenic purification of air requires a pre-purification step for the removal of high-boiling and hazardous materials. Principal high-boiling air components include water and carbon dioxide. If removal of these impurities from ambient air is not achieved, then water and carbon dioxide will freeze out in cold sections of the separation apparatus (for example in heat exchangers and liquid oxygen sump) causing pressure drop and flow and operational problems. Various hazardous materials including acetylene and other hydrocarbons also need to be removed. High-boiling hydrocarbons are a problem because they concentrate in the liquid oxygen section of the separation apparatus, resulting in a potential explosive hazard.

[0003] A minor air component that has recently been recognised as important in the pre-purification of air is nitrous oxide. Nitrous oxide is present in ambient air at concentrations of about 0.3 ppm. Nitrous oxide has similar properties to carbon dioxide and therefore presents potential operation problems resulting from solids formation in the separation apparatus column and heat exchangers. In addition, nitrous oxide presents a safety hazard as it is known to enhance combustion of organic materials, and it is shock sensitive. Therefore, there is significant industrial interest in the removal of trace nitrous oxide from ambient air prior to cryogenic distillation.

[0004] The nitrous oxide concentration in the atmosphere is steadily increasing at about 0.2 to 0.3% a year as a result of exhaust-gases of sewage treatment plants and catalysts of combustion engines and thermal plants. In addition, attention to nitrous oxide has increased as the required purity of gaseous products (for example rare gases and oxygen) has increased. Many previous solids formation problems noted in air separation apparatus and attributed to carbon dioxide may have been due to nitrous oxide.

[0005] Current technology for the pre-purification of air consists of adsorptive treatment including thermal swing (TSA) adsorption processes (disclosed for example in US-A-4541851 and US-A-5137548) and pressure swing adsorption (PSA) processes (disclosed for example in US-A-5232474). In general such systems are designed for total water and carbon dioxide removal. A recent publication (Wenning, MUST meeting, 1996) highlighted the problem of nitrous oxide in air separation plants.

[0006] Wenning teaches that in conventional TSA processes using zeolites such as 5A, nitrous oxide is less strongly adsorbed than carbon dioxide. This leads to breakthrough of nitrous oxide before carbon dioxide. Nitrous oxide then enters the cold section of the apparatus. Similar results occur in alumina-based PSA processes. The applicants have shown that an all-alumina PSA process removes about 30% of the inlet nitrous oxide concentration in air. Mixed beds of alumina and zeolite used in TSA or PSA processes are known to result in more nitrous oxide breakthrough than non-mixed beds.

[0007] Catalysts are available which convert nitrous oxide to nitrogen and oxygen (Wenning), but these catalysts function at elevated temperatures which is undesirable.

[0008] US-A-5919286 teaches using a layer of zeolite at the product end of a PSA bed for nitrous oxide removal. US-A-6106593 teaches a 3 layer TSA adsorbent bed where the final adsorbent layer removes nitrous oxide. The adsorbent is defined by a minimum adsorption capacity for nitrous oxide (80 mmol/g/bar (79 mmol/g/atm)), and includes adsorbents such as CaX.

[0009] US 6273939 teaches the use of faujasite type zeolites, especially calcium-exchanged X or LSX, for the removal of nitrous oxide from air prior to cryogenic distillation. The adsorbent is defined by size only.

[0010] EP-A-1064978 teaches the use of barium-exchanged zeolite for removal of carbon dioxide, nitrous oxide and organic impurities from air prior to cryogenic distillation. 13X zeolite is used, which is stated to show a large amount of nitrous oxide breakthrough before carbon dioxide breakthrough.

[0011] EP-A-1092465 teaches the use of X-type zeolites with specified silicon to aluminium ratios for adsorptive removal of nitrous oxide and hydrocarbons from air prior to cryogenic distillation. Siliporite G586 from Ceca in 1.6 x 2.5 mm beads is used.

[0012] In these documents, adsorbents useful for nitrous oxide removal from air are identified by their composition or equilibrium selectivity.

[0013] In a first aspect, the present invention provides a process for removing water, carbon dioxide and nitrous oxide from a feed gas stream, comprising passing the feed gas stream through a first adsorbent to adsorb water, a second adsorbent to adsorb carbon dioxide and a third adsorbent to adsorb nitrous oxide and to form a purified feed gas stream, wherein the third adsorbent has a nitrogen diffusion parameter of 0.12 sec^{-1} or higher and a nitrous oxide capacity of 80 mmol/g/bar (79 mmol/g/atm) or higher at 30°C . The first, second and third adsorbents or any combination of them may optionally be the same material.

[0014] Preferably, the third adsorbent has a nitrogen diffusion parameter of 0.15 sec^{-1} or higher.

[0015] Optionally, the second and third adsorbents are the same material and are different from the first adsorbent.

[0016] Preferably, the feed gas is air.

[0017] Preferably, the process further comprises cryogenic distillation of the purified feed gas stream to separate a nitrogen rich stream and/or an oxygen rich stream.

[0018] Preferably, the adsorbents are regenerated by thermal swing adsorption. The adsorbents are preferably regenerated at a temperature of 50 to 400°C and/or at a pressure of 0.1 to 20 atm. Preferably, oxygen, nitrogen, methane, hydrogen, argon or a mixture of two or more thereof is passed over the adsorbents as they are regenerated

[0019] Preferably, the feed gas stream is at a temperature of 0 to 50°C, and/or at a pressure of 3 to 20 atm.

[0020] The first adsorbent may be selected from alumina, silica gel, impregnated alumina, zeolite A and zeolite X, and the second and third adsorbents may be selected from impregnated alumina, impregnated composite alumina/zeolite, zeolite A and zeolite X.

[0021] In a second aspect, the present invention relates to apparatus for removing water, carbon dioxide and nitrous oxide from a feed gas stream comprising in fluid series connection a first adsorbent to adsorb water, a second adsorbent to remove carbon dioxide and a third adsorbent to remove nitrous oxide, wherein the third adsorbent has a nitrogen diffusion parameter of 0.12 sec⁻¹ or higher and a nitrous oxide capacity of 79 mmol/g/atm or higher at 30°C and the first, second and third adsorbents are optionally the same material.

[0022] The apparatus preferably further comprises in fluid series connection a cryogenic air separation unit.

[0023] In a third aspect, the present invention relates to a process for removing nitrous oxide from a feed gas stream, comprising passing the feed gas stream over an adsorbent having a nitrogen diffusion parameter of 0.12 sec⁻¹ or higher and a nitrous oxide capacity of 80 mmol/g/bar (79 mmol/g/atm) or higher at 30°C.

[0024] The production of adsorbents having the required nitrogen diffusion parameter is within the skill of adsorbent manufacturers. Known chemical forms of the adsorbents can be produced having the required property by appropriate selection of manufacturing processes to produce suitable particle sizes and macropore diameter. Where there is significant variation in diffusion parameter during normal manufacture, suitable materials can be obtained by screening the product by a suitable diffusion parameter measurement to select the best batches.

[0025] The invention will be illustrated by the following examples, making reference to the accompanying drawings in which:-

Figure 1 shows a plot of nitrogen diffusion parameter vs. % nitrous oxide removal of 1 ppm carbon dioxide in the TSA outlet.

Figure 2 shows a schematic view of apparatus used in a preferred embodiment of the present invention.

Example 1

[0026] Carbon dioxide breakthrough curves were measured on samples of NaX and CaX at 25°C, 100 psig (690 kPag) with a feed gas of air with 400 ppm carbon dioxide. The feed cross-sectional flow rate was 30 lbmoles/hr/ft² (146 kg moles/hr/m²). The data were obtained in a 1 inch (2.5 cm) diameter column by 6 feet (1.8 m) long. Prior to the experiments, the zeolites were regenerated in flowing nitrogen at 200°C. The carbon dioxide capacity and mass transfer zone results are presented in the table below.

Adsorbent	Relative carbon dioxide capacity	Relative carbon dioxide mass transfer zone
NaX	1.00	1.0
CaX	1.29	1.8

[0027] The data in the table show a surprising result. Exchange of calcium for sodium in the X zeolite increases the carbon dioxide capacity as might be expected. However, the surprising result is that calcium exchange leads to a significant increase in the carbon dioxide mass transfer zone. In general, as the capacity of an adsorbent increases, the mass transfer zone for impurity removal decreases. This is because the higher driving force of the improved capacity shortens the mass transfer zone. The table results are surprising since the higher capacity CaX also shows a longer mass transfer zone despite an improved driving force.

[0028] If CaX is to be used to adsorb nitrous oxide and carbon dioxide, the relatively long mass transfer zone for carbon dioxide makes it important to use a form of the adsorbent which has a high capacity and short mass transfer zone for nitrous oxide, to prevent early breakthrough of the gases.

Example 2

[0029] Carbon dioxide and nitrous oxide breakthrough curves were measured on CaX materials with different gas uptake rates at 25°C, 100 psig (690 kPag) with a feed gas or air containing 400 ppm carbon dioxide and 5 ppm nitrous

oxide. The feed G-rate was 30 lbmoles/hr/ft² (146 kg moles/hr/m²). The data were obtained in a 1 inch (2.5 cm) diameter column by 6 feet (1.8 m) long. Prior to the experiments, the zeolites were regenerated in flowing nitrogen at 200°C.

[0030] All CaX materials tested had similar equilibrium nitrous oxide capacities, but their mass transfer rates were modified by changing particle size and particle form. The nitrogen uptake rate of each sample was determined by performing a volumetric uptake test and fitting the uptake rate curve (fractional approach to equilibrium vs. time) to Fick's Law. This technique is described in "Principles of Adsorption and Adsorption Processes", 1984, Chapter 6, D. Ruthven, John Wiley & Sons.

[0031] The results of the breakthrough testing are given in the following table.

[0032] The results of the breakthrough testing are given in the table below

Adsorbent	Form and Size	Relative carbon dioxide capacity	Absolute nitrous oxide capacity (mmol/g/atm) [mmol/g/bar]	Relative nitrous oxide capacity	% nitrous oxide removal at 1 ppm carbon dioxide out	D/r ² (sec ⁻¹)
CaX 1	1/16 inch (0.16 cm) pellets	1.0	(237) [240]	1.0	97.4%	0.25
CaX 2 Ceca Grade G586	8x12 mesh beads	1.06	(251) [254]	1.03	96.2%	0.14
CaX 3	6x8 mesh beads	1.10	(261) [264]	1.05	88.8%	0.062
CaX 4 UOP Grade VSA 2	8x12 mesh beads	0.94	(223) [226]	0.93	93.5%	0.11

[0033] The results show that, although all four CaX samples have essentially the same equilibrium properties, CaX materials with higher mass transfer rates show improved nitrous oxide capability.

[0034] The nitrogen diffusion parameters of adsorbents used in the known processes discussed above were also determined. The D/r² value for UOP APGB 8x12 (EP-1064978) was 0.19 sec⁻¹. The D/r² value for 1/16 inch (0.16 cm) UOP 13X (US-A-5919286) was 1.1 sec⁻¹. However, these similar materials do not have the desired equilibrium nitrous oxide adsorption properties: the nitrous oxide adsorption capacity of UOP 13X is 71 mmol/g/atm (72 mmol/g/bar). The D/r² value for Siliporite G586 from Ceca in 1.6 x 2.5 mm beads (EP-1092465) ranged from 0.10 to 0.14 sec⁻¹.

[0035] The adsorbents disclosed in US-A-6273939, US-A-4933158 and US-A-6106593 are defined by material and size only. As is shown by comparing the results for CaX2 and CaX4 in the table above, adsorbents of the same material and size may have different nitrogen diffusion parameters, and therefore the adsorbents used in these processes are not sufficiently well-defined to determine their nitrogen diffusion parameters. It is expected that CaX4 has a smaller macropore diameter than CaX2.

[0036] Figure 1 shows a plot of nitrogen diffusion parameter vs. % nitrous oxide removal at 1 ppm carbon dioxide in the TSA outlet. The results show that once D/r² values of 0.15 sec⁻¹ or higher are obtained, CaX of suitable capacity can remove essentially all nitrous oxide in the feed air.

Example 3

[0037] As shown in Figure 2, air to be purified is supplied to a main air compressor system 10 at an inlet 12 in which it is compressed by a multi-stage compressor with inter and after cooling by heat exchange with water. Optionally, the compressed air feed is sub-cooled in a cooler 8. The cooled compressed air is supplied to an inlet manifold 14 containing inlet control valves 16 and 18 to which is connected a pair of adsorbent bed containing vessels 20 and 22. The inlet manifold is bridged downstream of the control valves 16 and 18 by a venting manifold 24 containing venting valves 26, 28 which serve to close and open connections between the upstream end of respective adsorbent vessels 20 and 22 and a vent 30 via a silencer 32. Each of the two adsorbent beds 20 and 22 contains two adsorbents. A lower portion of the adsorbent bed is designated by the numerals 34, 34' in respective beds and upper portion by the numeral 36, 36'. Portion 34, 34' contains a first adsorbent to adsorb water (for example alumina) and portion 36, 36' contains a second adsorbent to adsorb carbon dioxide and nitrous oxide (for example CaX2, Example 2).

[0038] In alternative embodiments, each adsorbent bed 20, 22 may contain a single adsorbent, or may contain three separate adsorbents. Adsorbents may be arranged in layers, for example adsorbents may be radially layered. It should be understood that the vessels 20 and 22 can each if desired be separated into smaller vessels arranged in series and

references to "layers" of adsorbent above include arrangements in which the separate adsorbents are placed in separate vessels arranged in series.

[0039] The apparatus has an outlet 38 connected to the downstream ends of the two adsorbent vessels 20, 22 by an outlet manifold 40 containing outlet control valves 42, 44. The outlet is connected to an air separation unit (ASU). The outlet manifold 40 is bridged by a regenerating gas manifold 46 containing regenerating gas control valves 48 and 50. Upstream from the regenerating gas manifold 46, a line 52 containing a control valve 54 also bridges across the outlet manifold 40.

[0040] An outlet for regenerating gas is provided at 56 which through control valve 58 is connected to pass through a heater 62 to the regenerating gas manifold 46. The operation of the valves may be controlled by suitable programmable timing and valve opening means as known in the art, not illustrated.

[0041] In operation air is compressed in the main compressor system 10 and is fed to the inlet manifold 14 and passes through one of the two vessels containing adsorbent. Starting from a position in which air is passing through open valve 16 to adsorbent vessel 20, and through open valve 42 to the outlet 38 and air separation unit, valve 18 in the inlet manifold will just have been closed to cut-off vessel 22 from the feed of air for purification. Valve 44 will just have closed also. At this stage valves 46, 50, 54, 26 and 28 are all closed. Bed 20 is thus on-line and bed 22 is to be regenerated.

[0042] To commence depressurisation of bed 22, valve 28 is opened and once the pressure in the vessel 22 has fallen to a desired level, valve 28 is kept open whilst valve 50 is opened to commence a flow of regenerating gas. The regenerating gas will typically be a flow of dry, CO₂-free nitrogen obtained from the air separation unit cold box, possibly containing small amounts of argon, oxygen and other gases, to which the air purified in the apparatus shown is passed. Valve 58 is opened so that the regenerating gas is heated to a temperature of for instance 100°C before passing into the vessel 22. The exit purge gas emerges from the vent outlet 30 in a cooled state.

[0043] At the end of the allotted regeneration period, valve 58 may be closed to end the flow of regenerating gas and valve 54 may be opened to displace nitrogen from the adsorbent and, after the closing of valve 28, to repressurise the vessel 22 with purified air. Thereafter, valve 54 may be closed and valves 18 and 44 may be opened to put the vessel 22 back on-line. The vessel 20 may then be regenerated in a similar manner and the whole sequence continued with the vessels being on-line, depressurising, regenerating, repressurising, and going back on-line in phase cycles of operation.

[0044] It will be appreciated that although the invention has been described with reference to preferred embodiments, many variations and modifications thereof are possible within the scope of the invention.

Claims

1. A process for removing water, carbon dioxide and nitrous oxide from a feed gas stream, comprising passing the feed gas stream through a first adsorbent to adsorb water, a second adsorbent to adsorb carbon dioxide and a third adsorbent to adsorb nitrous oxide and to form a purified feed gas stream, wherein the third adsorbent has a nitrogen diffusion parameter of 0.12 sec⁻¹ or higher and a nitrous oxide capacity of 80 mmol/g/bar (79 mmol/g/atm) or higher at 30°C.
2. A process as claimed in Claim 1, wherein the first, second and third adsorbents or any combination of them are the same material.
3. A process as claimed in Claim 1 or Claim 2, wherein the third adsorbent has a nitrogen diffusion parameter of 0.15 sec⁻¹ or higher.
4. A process as claimed in Claim 2, wherein the second and third adsorbents are the same material, and are different from the first adsorbent.
5. A process as claimed in any preceding claim, wherein the feed gas is air.
6. A process as claimed in Claim 5, further comprising cryogenic distillation of the purified feed gas stream to separate a nitrogen rich stream and/or an oxygen rich stream.
7. A process as claimed in any preceding claim, wherein the adsorbents are regenerated by thermal swing adsorption.
8. A process as claimed in Claim 7, wherein the adsorbents are regenerated at a temperature of 50 to 400°C.
9. A process as claimed in any preceding claim, wherein the feed gas stream is at a temperature of 0 to 50°C.

10. A process as claimed in any preceding claim, wherein the feed gas stream is at a pressure of 3 to 20 atm.
11. A process as claimed in any preceding claim, wherein the adsorbents are regenerated at a pressure of 0.1 to 20 atm.
- 5 12. A process as claimed in any preceding claim, wherein oxygen, nitrogen, methane, hydrogen, argon or a mixture of two or more thereof is passed over the adsorbents as they are regenerated.
13. A process as claimed in any preceding claim, wherein the first adsorbent is selected from alumina, silica gel, impregnated alumina, zeolite A and zeolite X.
- 10 14. A process as claimed in any preceding claim, wherein the second adsorbent is selected from impregnated alumina, impregnated composite alumina/zeolite, zeolite A and zeolite X.
- 15 15. A process as claimed in any preceding claim, wherein the third adsorbent is selected from impregnated alumina, impregnated composite alumina/zeolite, zeolite A and zeolite X.
16. A process as claimed in any preceding claim, wherein the third adsorbent is CaX zeolite.
17. Apparatus for removing water, carbon dioxide and nitrous oxide from a feed gas stream comprising in fluid series connection a first adsorbent to adsorb water, a second adsorbent to remove carbon dioxide and a third adsorbent to remove nitrous oxide, wherein the third adsorbent has a nitrogen diffusion parameter of 0.12 sec^{-1} or higher and a nitrous oxide capacity of 80 mmol/g/bar (79 mmol/g/atm) or higher at 30°C and the first, second and third adsorbents may optionally be the same material.
- 25 18. Apparatus as claimed in Claim 17, further comprising in fluid series connection a cryogenic air separation unit.
19. A process for removing nitrous oxide from a feed gas stream, comprising passing the feed gas stream over an adsorbent having a nitrogen diffusion parameter of 0.12 sec^{-1} or higher and a nitrous oxide capacity of 80 mmol/g/bar (79 mmol/g/atm) or higher at 30°C
- 30 20. The use of an adsorbent having a nitrogen diffusion parameter of 0.12 sec^{-1} or higher and a nitrous oxide capacity of 80 mmol/g/bar (79 mmol/g/atm) for removing nitrous oxide from a feed gas stream.

Patentansprüche

1. Verfahren zur Entfernung von Wasser, Kohlendioxid und Distickstoffmonoxid aus einem Speisegasstrom mit Durchführen des Speisegasstroms durch ein erstes Adsorptionsmittel, um Wasser zu adsorbieren, ein zweites Adsorptionsmittel, um Kohlendioxid zu adsorbieren, und ein drittes Adsorptionsmittel, um Distickstoffmonoxid zu adsorbieren und einen gereinigten Speisegasstrom zu bilden, wobei das dritte Adsorptionsmittel einen Stickstoff-Diffusionsparameter von $0,12 \text{ sec}^{-1}$ oder höher und eine Distickstoffmonoxid-Kapazität von 80 mmol/g/bar (79 mmol/g/atm) oder höher bei 30°C hat.
2. Verfahren nach Anspruch 1, wobei das erste, zweite und dritte Adsorptionsmittel oder irgendeine Kombination von ihnen das gleiche Material sind.
3. Verfahren nach Anspruch 1 oder 2, wobei das dritte Adsorptionsmittel einen Stickstoff-Diffusionsparameter von $0,15 \text{ sec}^{-1}$ oder höher hat.
4. Verfahren nach Anspruch 2, wobei das zweite und dritte Adsorptionsmittel das gleiche Material sind und sich vom ersten Adsorptionsmittel unterscheiden.
5. Verfahren nach einem der vorhergehenden Ansprüche, wobei das Speisegas Luft ist.
6. Verfahren nach Anspruch 5, weiterhin mit kryogener bzw. Tieftemperaturdestillation des gereinigten Speisegasstroms, um einen stickstoffreichen Strom und/oder einen sauerstoffreichen Strom abzutrennen.
7. Verfahren nach einem der vorhergehenden Ansprüche, wobei die Adsorptionsmittel durch Wärme- bzw. Tempera-

turwechseladsorption regeneriert werden.

8. Verfahren nach Anspruch 7, wobei die Adsorptionsmittel bei einer Temperatur von 50 bis 400°C regeneriert werden.

9. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Speisegasstrom sich bei einer Temperatur von 0 bis 50°C befindet.

10. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Speisegasstrom sich auf einem Druck von 3 bis 20 atm befindet.

11. Verfahren nach einem der vorhergehenden Ansprüche, wobei die Adsorptionsmittel bei einem Druck von 0,1 bis 20 atm regeneriert werden.

12. Verfahren nach einem der vorhergehenden Ansprüche, wobei Sauerstoff, Stickstoff, Methan, Wasserstoff, Argon oder Gemische von zwei oder mehr dieser Substanzen über die Adsorptionsmittel geführt werden, wenn sie regeneriert werden.

13. Verfahren nach einem der vorhergehenden Ansprüche, wobei das erste Adsorptionsmittel ausgewählt wird aus Aluminiumoxid, Kieselgel, imprägniertes Aluminiumoxid, Zeolit A und Zeolit X.

14. Verfahren nach einem der vorhergehenden Ansprüche, wobei das zweite Adsorptionsmittel ausgewählt wird aus imprägniertem Aluminiumoxid, imprägniertem Aluminiumoxid/Zeolit-Verbundwerkstoff, Zeolit A und Zeolit X.

15. Verfahren nach einem der vorhergehenden Ansprüche, wobei das dritte Adsorptionsmittel ausgewählt wird aus imprägniertem Aluminiumoxid, imprägniertem Aluminiumoxid/Zeolit-Verbundwerkstoff, Zeolit A und Zeolit X.

16. Verfahren nach einem der vorhergehenden Ansprüche, wobei das dritte Adsorptionsmittel CAX Zeolit ist.

17. Vorrichtung zur Entfernung von Wasser, Kohlendioxid und Distickstoffmonoxid aus einem Speisegasstrom mit einer Strömungsreihen-Verbindung aus einem ersten Adsorptionsmittel zur Adsorption von Wasser, einem zweiten Adsorptionsmittel zur Entfernung von Kohlendioxid und einem dritten Adsorptionsmittel zur Entfernung von Distickstoffmonoxid, wobei das dritte Adsorptionsmittel einen Stickstoff-Diffusionsparameter von $0,12 \text{ sec}^{-1}$ oder höher und eine Distickstoffmonoxid-Kapazität von 80 mmol/g/bar (79 mmol/g/atm) oder höher als 30°C hat und das erste, zweite und dritte Adsorptionsmittel optional der gleiche Werkstoff sein können.

18. Vorrichtung nach Anspruch 17, weiterhin mit einer Strömungsreihen-Verbindung mit einer Tieftemperatur-Luftzerlegungseinheit.

19. Verfahren zur Entfernung von Distickstoffmonoxid aus einem Speisegasstrom mit der Leitung des Speisegasstrom über ein Adsorptionsmittel mit einem Stickstoff-Diffusionsparameter von $0,12 \text{ sec}^{-1}$ oder höher und einer Distickstoffmonoxid-Kapazität von 80 mmol/g/bar (79 mmol/g/atm) oder höher bei 30°C.

20. Verwendung eines Adsorptionsmittels mit einem Stickstoff-Diffusionsparameter von $0,12 \text{ sec}^{-1}$ oder höher und einer Distickstoffmonoxid-Kapazität von 80 mmol/g/bar (79 mmol/g/atm) zur Entfernung von Distickstoffmonoxid aus einem Speisegasstrom

Revendications

1. Procédé pour éliminer l'eau, le dioxyde de carbone et l'oxyde nitreux d'un courant de gaz d'alimentation, comprenant le passage du courant de gaz d'alimentation à travers un premier adsorbant pour adsorber l'eau, un deuxième adsorbant pour adsorber le dioxyde de carbone et un troisième adsorbant pour adsorber l'oxyde nitreux et pour former un courant de gaz d'alimentation purifié, dans lequel le troisième adsorbant a un paramètre de diffusion de l'azote de $0,12 \text{ sec}^{-1}$ ou supérieur et une capacité d'adsorption de l'oxyde nitreux de 80 mmoles/g/bar (79 mmoles/g/atm) ou supérieure, à 30°C.

2. Procédé tel que revendiqué dans la revendication 1, dans lequel les premier, deuxième et troisième adsorbants ou n'importe quelle combinaison de ceux-ci sont le même matériau.

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3. Procédé tel que revendiqué dans la revendication 1 ou la revendication 2, dans lequel le troisième adsorbant a un paramètre de diffusion de l'azote de $0,15 \text{ sec}^{-1}$ ou supérieur.
- 5 4. Procédé tel que revendiqué dans la revendication 2, dans lequel les deuxième et troisième adsorbants sont le même matériau, et sont différents du premier adsorbant.
5. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le gaz d'alimentation est l'air.
- 10 6. Procédé tel que revendiqué dans la revendication 5, comprenant en outre une distillation cryogénique du courant de gaz d'alimentation purifié pour séparer un courant riche en azote et/ou un courant riche en oxygène.
7. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel les adsorbants sont régénérés par une adsorption modulée en température.
- 15 8. Procédé tel que revendiqué dans la revendication 7, dans lequel les adsorbants sont régénérés à une température de 50 à 400°C .
- 20 9. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le courant de gaz d'alimentation est à une température de 0 à 50°C .
10. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le courant de gaz d'alimentation est à une pression de 3 à 20 atm.
- 25 11. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel les adsorbants sont régénérés à une pression de 0,1 à 20 atm.
- 30 12. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel l'oxygène, l'azote, le méthane, l'hydrogène, l'argon ou un mélange de deux ou plusieurs de ceux-ci est passé à travers les adsorbants à mesure qu'ils sont régénérés.
13. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le premier adsorbant est choisi parmi l'alumine, le gel de silice, l'alumine imprégnée, les zéolite A et zéolite X.
- 35 14. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le deuxième adsorbant est choisi parmi l'alumine imprégnée, un composite d'alumine/zéolite imprégné, les zéolite A et zéolite X.
- 40 15. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le troisième adsorbant est choisi parmi l'alumine imprégnée, un composite d'alumine/zéolite imprégné, les zéolite A et zéolite X.
- 50 16. Procédé tel que revendiqué dans l'une quelconque des revendications précédentes, dans lequel le troisième adsorbant est une zéolite CaX.
- 45 17. Appareil pour éliminer l'eau, l'oxyde de carbone et l'acide nitreux d'un courant de gaz d'alimentation comprenant dans un montage de fluides en série, un premier adsorbant pour adsorber l'eau, un deuxième adsorbant pour éliminer le dioxyde de carbone et un troisième adsorbant pour éliminer l'oxyde nitreux, dans lequel le troisième adsorbant a un paramètre de diffusion de l'azote de $0,12 \text{ sec}^{-1}$ ou supérieur et une capacité d'adsorption de l'oxyde nitreux de 80 mmoles/g/bar (79 mmoles/g/atm) ou supérieure, à 30°C et, les premier, deuxième et troisième adsorbants peuvent éventuellement être le même matériau.
- 55 18. Appareil tel que revendiqué dans la revendication 17, comprenant en outre dans un montage de fluides en série, une unité de séparation d'air cryogénique.
19. Procédé pour éliminer l'oxyde nitreux d'un courant de gaz d'alimentation, comprenant le passage du courant de gaz d'alimentation sur un adsorbant ayant un paramètre de diffusion de l'azote de $0,12 \text{ sec}^{-1}$ ou supérieur et une capacité d'adsorption de l'oxyde nitreux de 80 mmoles/g/bar (79 mmoles/g/atm) ou supérieure, à 30°C .
20. Utilisation d'un adsorbant ayant un paramètre de diffusion de l'azote de $0,12 \text{ sec}^{-1}$ ou supérieur, et une capacité

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d'adsorption de l'oxyde nitreux de 80 mmoles/g/bar (79 mmoles/g/atm) pour éliminer l'oxyde nitreux d'un courant de gaz d'alimentation.

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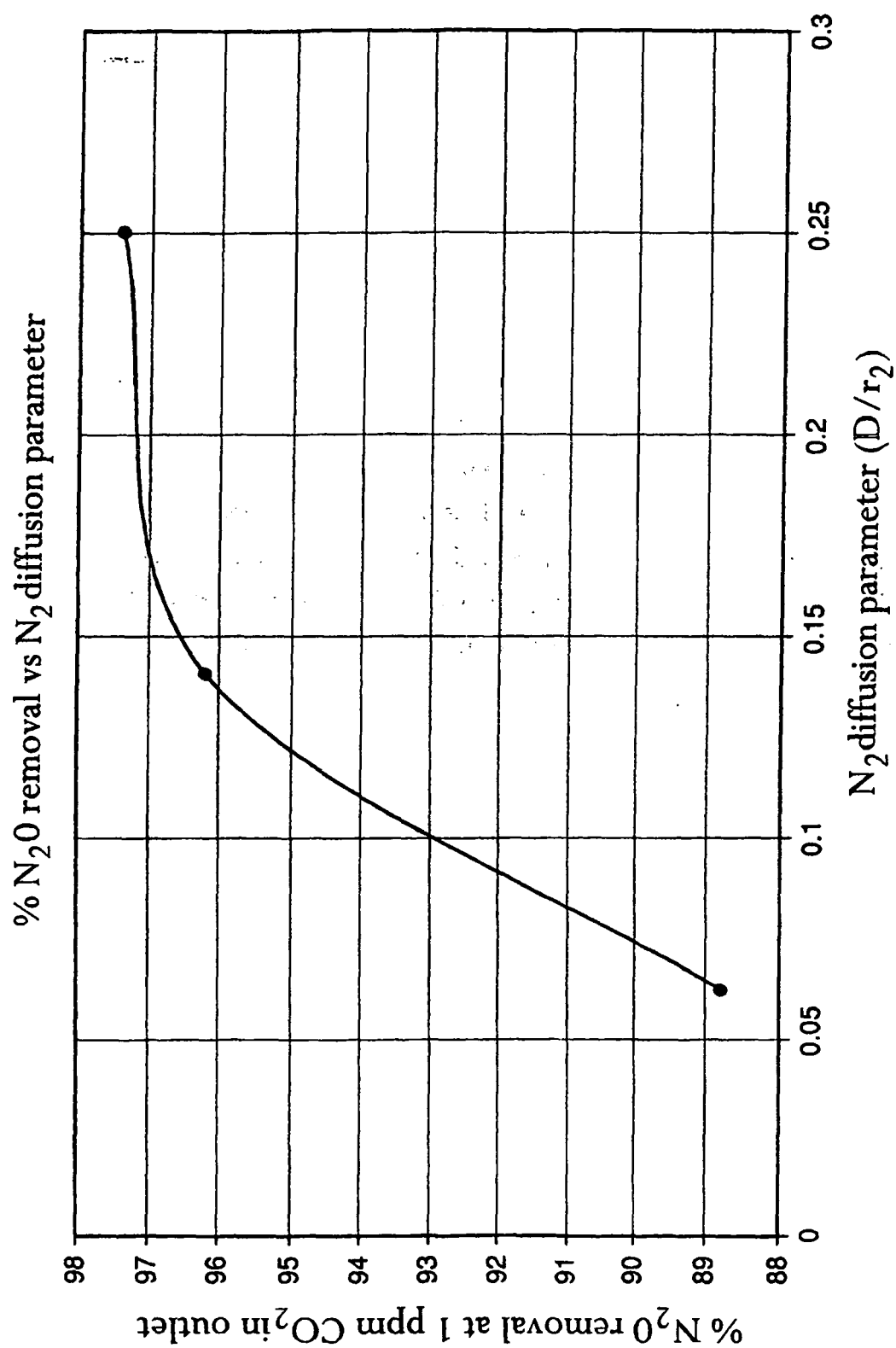


FIG. 1

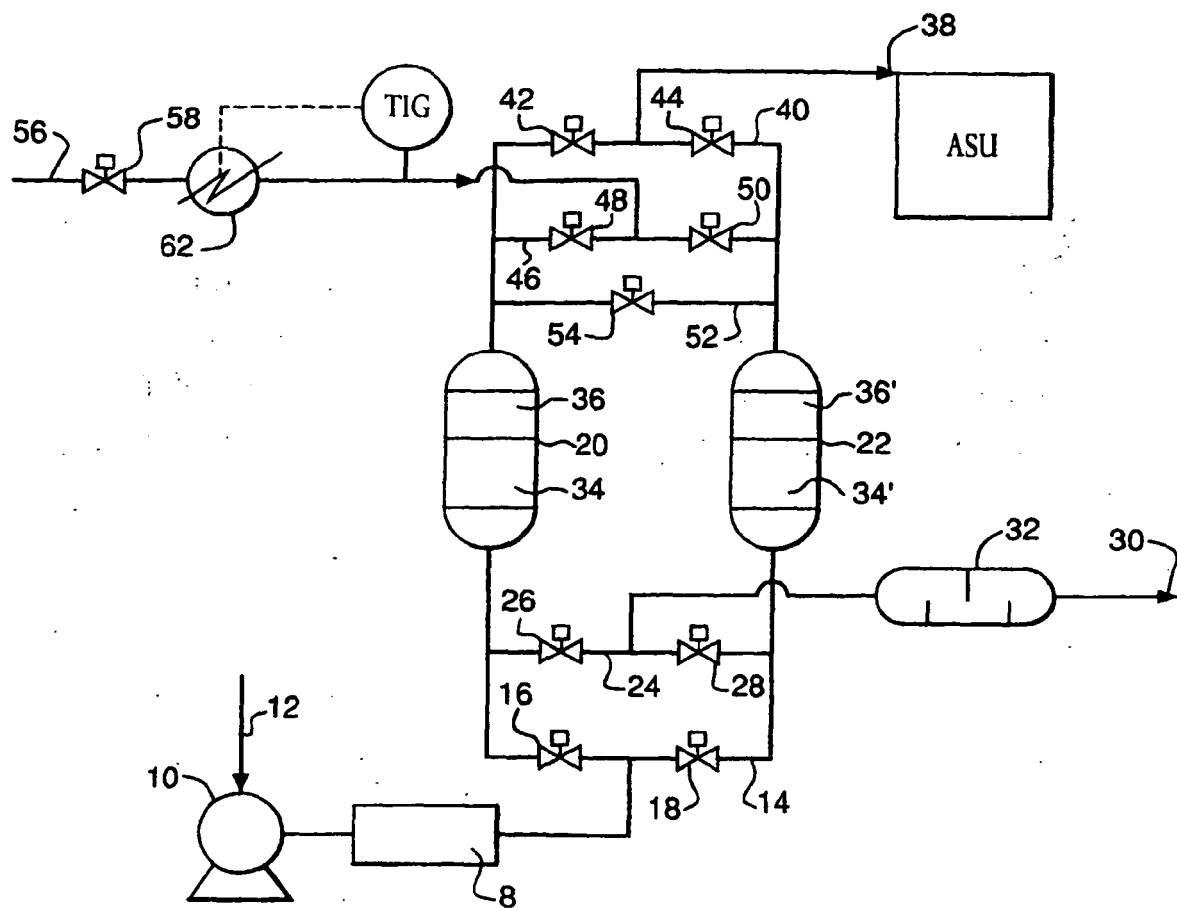


FIG. 2

REFERENCES CITED IN THE DESCRIPTION

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