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(71) Applicant: **BP p.l.c.**

London SW1Y 4PD (GB)

(72) Inventor: **The designation of the inventor has not yet been filed**

(74) Representative: **Perkins, Nicholas David**

**BP International Limited
Patents and Agreements Division,
Chertsey Road
Sunbury-on-Thames,
Middlesex TW16 7LN (GB)**

(54) **Compositions and methods**

(57) A liquid lubricant base oil composition comprising (i) a base stock comprising at least 95 % by weight saturated hydrocarbons such as for example a Group II base stock, a Group III base stock and/or a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material and (ii) 0.2 to 30 % by weight

of an aromatic extract may be made by blending the components together and may be used with one or more additives in a lubricant composition which may be used in applications such as marine engine lubricants.

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Description

[0001] This invention relates to compositions and methods and in particular to lubricant base oil and lubricant compositions and to methods for making them.

[0002] Lubricant compositions generally comprise a base oil and one or more additives. According to API standard 1509, "ENGINE OIL LICENSING AND CERTIFICATION SYSTEM", November 2004 version 15th edition Appendix E, base stocks which are used for base oils are defined as belonging to one of five Groups as set out in Table I below.

Table I

Group	Saturated hydrocarbon content (wt%)		Sulphur content (wt%)		Viscosity Index
I	< 90	and/or	> 0.03	and	≥ 80 and < 120
II	≥ 90	and	≤ 0.03	and	≥ 80 and < 120
III	≥ 90	and	≤ 0.03	and	≥ 120
IV	polyalpha olefins				
V	all base stocks not in Groups I, II, III or IV				

[0003] Group I base stocks are generally preferred to Group II base stocks for the manufacture of lubricant compositions for marine 2-stroke and 4-stroke engines, particularly for engines operating on heavy fuel oil. However, Group II base stocks are becoming increasingly more readily available because older manufacturing capacity for Group I basestock is being closed and new manufacturing capacity tends to manufacture Group II base stock.

[0004] Group II base stocks may have some performance disadvantages compared to Group I base stocks when used in some lubricant compositions, for example in marine lubricants. These disadvantages may include poorer dispersancy, poorer seal swell performance, poorer solubility of additives, lower compatibility with fuel oil in marine engine applications (which can lead to deposit formation, for example in cool parts of the engine) and/or in some aspects, poorer oxidative stability.

[0005] Hydroprocessed base stocks may have advantages and disadvantages (Deckman, D.E. et al., Hart's Lubricants World, July 1997, pages 46 - 50) when used in industrial lubricant applications (Deckman D. E. et al., Hart's Lubricants World, Sept 1997, pages 20-26) and in commercial, personal vehicle and marine engine oils (Deckman D. E. et al., Hart's Lubricants World, Sept 1997, pages 27 - 28).

[0006] According to Deckman D. E. et al., in Hart's Lubricants World, Sept 1997, pages 27 - 28, "*Because hydrocracking results in a viscosity loss of the base stocks, marine oils cannot generally be formulated solely with hydrocracked base stocks, but require the use of significant amounts of bright stock. However, the use of bright stock is not desirable because of the presence of oxidatively unstable aromatics*".

[0007] Base stocks which are made by hydroprocessing, including Group II and Group III base stocks, have lower aromatics content and lower sulphur content than Group I base stocks.

[0008] Base stocks derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon materials also have a low aromatics content and so may also exhibit at least some of the poorer performance of Group II and Group III base stocks compared to Group I base stocks. WO 00/14187 and WO 2005/066314 relate to lubricant compositions comprising Fischer Tropsch derived base stock.

[0009] There remains a need for a base oil composition which overcomes, or at least mitigates these problems.

[0010] It has now been found that the use of 0.2 to 30 % by weight of an aromatic extract in a base oil comprising base stock, which base stock comprises at least 95 % by weight saturated hydrocarbons, can overcome or at least mitigate these problems.

[0011] Thus, according to one aspect of the present invention, there is provided a liquid lubricant base oil composition comprising (i) a base stock comprising at least 95 % by weight saturated hydrocarbons and (ii) 0.2 to 30 % by weight, preferably 0.2 to 18 % or 1 to 30 % by weight, more preferably 1.0 to 18 % by weight, of an aromatic extract.

[0012] According to a second aspect of the present invention, there is provided a method of making a liquid lubricant base oil composition as hereinafter defined which method comprises blending a base stock comprising at least 95 % by weight saturated hydrocarbons with sufficient aromatic extract to make a liquid lubricant base oil composition as hereinafter defined.

[0013] According to a third aspect of the present invention there is provided a liquid lubricant composition comprising a lubricant base oil composition as hereinafter defined and one or more additives, preferably selected from the group consisting of detergents, dispersants, anti-wear additives, anti-oxidants, anti-foams, corrosion inhibitors, pour point depressants, friction modifiers, tackifiers and viscosity index improvers.

[0014] The present invention solves the problem defined above by the use of 0.2 to 30 % by weight of an aromatic extract in a liquid lubricant base oil composition which base oil comprises a base stock comprising at least 95 % by weight saturated hydrocarbons. This provides a lubricant base oil which overcomes or at least mitigates, at least some of the deficiencies which may be associated with such base stocks.

[0015] The lubricant base oil composition of the present invention comprises 0.2 to 30 % by weight of an aromatic extract. Preferably, the lubricant base oil composition of the present invention comprises 0.2 to 18 % or 1.0 to 30 % by weight of the aromatic extract. More preferably, the lubricant base oil composition of the present invention comprises 1.0 to 18 % by weight aromatic extract.

[0016] Preferably, the base stock comprising at least 95 % by weight saturated hydrocarbons comprises a hydroprocessed base stock and/or a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material. The present invention provides a lubricant base oil which overcomes or at least mitigates, at least one of the deficiencies which may be associated with such base stocks, for example those deficiencies selected from the group consisting of poor dispersancy (for example, of soot and/or deposits), poor seal swell performance, poor solubility of additives and low compatibility with fuel oil in marine engine applications (which can lead to deposit formation, for example in cool parts of the engine), and also in some aspects, poor oxidative stability.

[0017] Thus, according to a further aspect of the present invention there is provided the use of 0.2 to 30 % by weight of an aromatic extract in a liquid lubricant base oil composition which base oil comprises a base stock comprising at least 95 % by weight saturated hydrocarbons, to mitigate at least one of the deficiencies of the base stock selected from the group consisting of poor dispersancy, poor seal swell performance, poor solubility of additives and low compatibility with fuel oil in marine engine applications.

[0018] In particular, the present invention provides a method which uses a defined amount of aromatic extract, to make a base oil using a hydroprocessed base stock which may comprise for example, a Group II base stock, a Group III base stock and/or a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material. This base oil can be used in applications where a Group I base stock has conventionally been used, such as for example, in marine engine applications, for example in 2-stroke marine diesel engine cylinder oils, 2-stroke marine diesel engine system oils and 4-stroke marine diesel engine crankcase lubricant compositions.

[0019] The aromatic extract is preferably made by the treatment of at least one refinery process stream in a solvent extraction process. Suitable solvent extraction process include contacting the at least one refinery process stream with a solvent such as furfural, n-methylpyrrolidone, sulphur dioxide, Duo-Sol™ or phenol to selectively extract from the refinery stream, aromatic and heterocyclic materials and to form a solution of these materials in the solvent. The solvent is then recovered from the solution for recycle to the extraction process; the resultant product being the aromatic extract.

[0020] The manufacture of aromatic extracts is known in the art and is described for example in "Lubricant base oil and wax processing" A. Sequeira, pages 81-118, pub. Marcel Dekker Inc. New York, 1994.

[0021] The aromatic extract may be a residual aromatic extract, which may be made by treatment in an extraction process, of solvent deasphalted vacuum residue (also known as DAO) made using Duo-Sol™, propane, butane or mixtures thereof as the solvent for the deasphalting.

[0022] The aromatic extract may be a distillate aromatic extract (DAE) which is an aromatic extract made by treatment in an extraction process, of a distillate stream from a vacuum distillation process. Preferably, the distillate aromatic extract is a treated distillate aromatic extract which is a distillate aromatic extract which has been subjected to at least one further treatment. Suitably, the at least one further treatment is selected from the group consisting of hydrotreatment, hydrogenation, hydrodesulphurisation, clay treatment, acid treatment and further solvent extraction.

[0023] The aromatic extract may have an aromatics content of 60 to 85 weight %, which may be measured by ASTM D 2007.

[0024] The aromatic extract may have properties such as those described in Concawe Product Dossier 92/101 "Aromatic Extracts".

[0025] The distillate aromatic extract may have a boiling point in the range 250 - 680 °C, which may be measured according to ASTM D 2887. The distillate aromatic extract may have a kinematic viscosity at 40°C in the range 5 - 18000 mm²/s, which may be measured according to ASTM D 445. The distillate aromatic extract may have a kinematic viscosity at 100 °C in the range 3 - 60 mm²/s, which may be measured according to ASTM D 445. The distillate aromatic extract may have an average molecular mass in the range 300 - 580, which may be measured according to ASTM D 2887. The distillate, aromatic extract may have a carbon number range in the range C₁₅ - C₅₄, which may be measured according to ASTM D 2887. The distillate aromatic extract may have an aromatic content in the range 65 - 85 weight %, which may be measured according to ASTM D 2007.

[0026] The residual aromatic extract may have a boiling point of greater than 380°C, which may be measured according to ASTM D 2887. The residual aromatic extract may have a kinematic viscosity at 40 °C of greater than 4000 mm²/s, which may be measured according to ASTM D 445. The residual aromatic extract may have a kinematic viscosity at 100 °C in the range 60 - 330 mm²/s, which may be measured according to ASTM D 445. The residual aromatic extract may have an average molecular mass of greater than 400, which may be measured according to ASTM D 2887. The

residual aromatic extract may have a carbon number range of greater than C₂₅, which may be measured according to ASTM D 2887. The residual aromatic extract may have an aromatic content in the range 60 - 85 weight %, which may be measured according to ASTM D 2007.

[0027] Aromatic extracts may comprise polycyclic aromatic compounds (PAC's) some of which are carcinogens. The amount of material (weight %) which can be extracted into dimethyl sulphoxide (DMSO) is used as an indication of the amount of unacceptable material (including polycyclic aromatic compounds) in the aromatic extracts. IP 346 (Institute of Petroleum Test Method 346) is a method used for determining weight % DMSO extract. The aromatic extract may be an untreated distillate aromatic extract having a dimethyl sulphoxide extractable polycyclic aromatics content in the range 10 - 30 weight %, which may be measured according to IP 346. Aromatic extracts with greater than 3 weight % dimethyl sulphoxide extractable polycyclic aromatics content are classed as carcinogenic and give rise to requirements in several jurisdictions that the material be labelled with certain symbols and risk phrases to identify health, safety and environmental hazards. For this reason at least, it is preferred that the aromatic extract has less than 3 weight % dimethyl sulphoxide extractable polycyclic aromatics content (low PCA extract). More preferably, the aromatic extract is a residual aromatic extract or a treated distillate aromatic extract, with less than 3 weight % dimethyl sulphoxide extractable polycyclic aromatics content.

[0028] Preferably, the aromatic extract does not contain any significant amount of wax, because if present, wax may deposit in use.

[0029] The base stock of the present invention comprising at least 95 % by weight saturated hydrocarbons may comprise both a hydroprocessed base stock and a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material. Suitably, base stock of the present invention comprising at least 95 % by weight saturated hydrocarbons may comprise a hydroprocessed base stock or a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material.

[0030] The hydroprocessed base stock is preferably a Group II and/or Group III base stock, such as defined according to API standard 1509, "ENGINE OIL LICENSING AND CERTIFICATION SYSTEM", November 2004 version 15th edition Appendix E.

[0031] The base stock comprising at least 95 % by weight saturated hydrocarbons preferably comprises a Group II and/or Group III base stock, such as defined according to API standard 1509, "ENGINE OIL LICENSING AND CERTIFICATION SYSTEM", November 2004 version 15th edition Appendix E, comprising at least 95% by weight saturated hydrocarbons.

[0032] Preferably, the Group II base stock or Group III base stock is a hydroprocessed base stock which may be made by hydroprocessing, preferably of vacuum distillate or deasphalted vacuum residue, or by hydroisomerising the bottoms stream from a clean fuels hydrocracker. The manufacture of base stock by hydroprocessing is known in the art and is described for example in "Lubricant base oil and wax processing" A. Sequeira, pages 119 - 152, pub. Marcel Dekker Inc. New York, 1994.

[0033] The base stock derived from a Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material may be made by any suitable known process for the manufacture of base stock from Fischer Tropsch process. Processes for the manufacture of a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material which may be used, are described for example in US4943672, EP-A-0668342 and EP-A-0776959, the contents of which are hereby incorporated by reference. Thus, the base stock may be made by the steps of (i) producing Syngas, (ii) Fischer-Tropsch synthesis of hydrocarbons from the Syngas, (iii) hydrocracking of the hydrocarbons to produce naphtha and diesel/kerosene fuel process streams together with a waxy paraffinic residue and (iv) hydroisomerising the waxy residue to produce the base stock.

[0034] The liquid lubricant base oil composition according to the present invention may be made by blending a base stock comprising at least 95 % by weight saturated hydrocarbons with sufficient an aromatic extract to make the lubricant base oil composition. The blending may be performed in a batch blending process or in a continuous blending process. Batch blending may be performed by introducing the base stock and aromatic extract into a blend kettle whilst stirring and/or agitating the blending components. Continuous blending may be performed using an in-line mixer to blend the base stock and aromatic extract. Heating may be necessary during the blending to facilitate handling of the aromatics extracts.

[0035] Preferably, the liquid lubricant base oil composition of the present invention has a viscosity in the range 7 to 40 cSt at 100° C.

[0036] The liquid lubricant base oil composition of the present invention is particularly useful for the manufacture of 2-stroke marine diesel engine cylinder oils, 2-stroke marine diesel engine system oils or 4-stroke marine diesel engine crankcase lubricant compositions.

[0037] The liquid lubricant composition according to the present invention comprises a liquid lubricant base oil composition as hereinafter defined and one or more additives, preferably selected from the group consisting of detergents, dispersants, anti-wear additives, anti-oxidants, anti-foams, corrosion inhibitors, pour point depressants, friction modifiers, tackifiers and viscosity index improvers.

[0038] The concentrations of additives in the lubricant composition according to the present invention depend upon the use for which the lubricant composition is intended.

[0039] One or more anti-oxidants may be present in the lubricant composition at a total concentration by weight of 0 to 1 %, usually at a concentration by weight of not greater than 0.5%.

[0040] One or more anti-wear additives may be present in the lubricant composition at a total concentration by weight of 0 to 2 %, usually at a concentration by weight of not greater than 1 %.

[0041] One or more high over-based detergents may be present in the lubricant composition at a total concentration by weight of 0 to 40 %.

[0042] One or more low base detergents may be present in the lubricant composition at a total concentration by weight of 0 to 10 %.

[0043] One or more neutral detergents may be present in the lubricant composition at a total concentration by weight of 0 to 2 %.

[0044] One or more dispersants may be present in the lubricant composition at a total concentration by weight of 0 to 10%.

[0045] One or more anti-foams may be present in the lubricant composition at a total concentration by weight of 0 to 0.1 %.

[0046] One or more corrosion inhibitors may be present in the lubricant composition at a total concentration by weight of 0 to 1 %.

[0047] One or more pour point depressants may be present in the lubricant composition at a total concentration by weight of 0 to 1 %.

[0048] One or more friction modifiers may be present in the lubricant composition at a total concentration by weight of 0 to 5%.

[0049] One or more tackifiers may be present in the lubricant composition at a total concentration by weight of 0 to 15 %.

[0050] One or more viscosity index improvers may be present in the lubricant composition at a total concentration by weight of 0 to 20 %.

[0051] The concentration ranges for the additives may be independent of each other. Alternatively, combinations of such concentration ranges may be used for any particular lubricant composition.

[0052] The liquid lubricant compositions of the present invention may be used as a 2-stroke marine diesel engine cylinder oil, 2-stroke marine diesel engine system oil or 4-stroke marine diesel engine crankcase lubricant composition.

The concentration ranges for additives for such lubricant compositions according to the present invention are given in the Table II below. Such concentration ranges may be independent of each other. Alternatively, combinations of such concentration ranges may be used for any particular lubricant composition.

55 50 45 40 35 30 25 20 15 10 5

Table II.

Concentration ranges are expressed in % by weight of the liquid lubricant composition.										
Lubricant Composition	High overbased detergent	Low base detergent	Anti-wear additive	Neutral detergent	Dispersant	Anti-foam	Corrosion inhibitor	Pour Point Depressant	Viscosity Index Improver	Anti-oxidant
Cylinder oil lubricant	5-40	0-10	0-2	0-2	0 - 4, preferably 0.5 - 4	0-0.1	0-1	0-1	0-20	0-1
2-stroke crank case lubricant (System Oil)	0-5	0-5	0-1	0-2	0-1.5	0-0.1	0-0.2	0-1	0-20	0-1
4-stroke crankcase lubricant	3-30	0-10	0-2	0-2	0 - 10, preferably 0.3 - 10	0-0.1	0-0.2	0-1	0-20	0-1

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[0053] The invention will now be described by way of example only and with reference to Figure 1 which is a graph of the performance of base oil with various amounts of aromatic extract.

[0054] In these experiments a hydroprocessed base stock was a Group II base stock comprising at least 97 % by weight saturated hydrocarbons was used. The aromatic extract was a low PCA brightstock extract (less than 3 % polycyclic aromatics, brightstock furfural extract) provided by Shell. Properties of these components are given in Table III below.

Table III General properties of components

Components	Test Method	Jurong 500N Base stock	Aromatic Extract (AE)
Type		Group II	Aromatic Extract
KV40, mm ² /s (cSt)	IP71	91.58	-
KV100, mm ² /s (cSt)	IP71	10.64	71.47
VI	IP226	99	-
Density, g/cm ³ (15 °C)	IP365	0.8746	0.9897
Flash point (PMCC), °C	IP34	232.3	284.3
Flash point (COC), °C	IP36	266	308
Pour point, °C	IP15	-18	-12
Colour	ASTM D1500	0.1	>8
TAN, mg KOH/g	IP1A	<0.05	0.09
TBN, mg KOH/g	IP276	<0.05	2.14
Sulphur, %	ASTM D4951	0.0037	4.13
Nitrogen, %	ASTM D5762	0.0027	0.11
Demulsibility, secs	IP19	75	-
Dialysis, % wt	BAM72	<0.1	<0.1
Oxidation IP48	IP48		Rams bottom
Viscosity ratio		3.06	carbon - 4.3 %
Carbon before, wt. %		0.05	
Carbon after, wt. %		0.60	
Carbon, Δ		0.55	
Carbon types wt %	BAM76		Viscosity too high to permit determination
Carbon, aromatic C _A		1.2	
Carbon, naphthenic C _N		67.2	
Carbon, paraffinic C _P		31.6	
Hydrocarbon types wt %	D2007		
Saturates		97.9	11.3
Aromatics		2.1	80.2
Polars		<0.1	8.5

[0055] The base stock and aromatic extract were shown not to contain any significant amounts of waxy materials. Base oil compositions were prepared by blending the aromatic extract (AE) with various amounts of the Group II base stock. Properties of the base oil compositions are given in Table IV below.

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Table IV

Sample	Test Method	Example 1	Example 2
Base Oil Composition (weight %)		88% Group II 12% AE	76% Group II 24%AE
KV40, mm ² /s (cSt)	IP71		162.4
KV100, mm ² /s (cSt)	IP71	12.3	14.43
VI	IP226	92	85
Density, g/cm ³	IP365	0.8870	0.9005
Flash point (PMCC), °C	IP34	238.3	236.1
Flash point (COC), °C	IP36	254	264
Pour point, °C	IP15	-15	-12
Colour	ASTM D1500	6.1	>8
TAN, mg KOH/g	IP1A	<0.05	<0.05
TBN, mg KOH/g	IP276	0.22	0.47
Sulphur, wt. %	ASTM D4951	0.49	0.98
Nitrogen, wt. %	ASTM D5762	0.019	0.032
Demulsibility, secs	IP19	405	630
Dialysis, % wt	BAM72	<0.1	<0.1
Oxidation IP48	IP48		
Viscosity ratio		1.18	1.40
Carbon before, wt. %		0.31	0.69
Carbon after, wt. %		0.87	2.37
Carbon , Δ		0.56	1.68
Carbon types wt %	BAM76		
Carbon, aromatic C _A		4.4	7.1
Carbon, naphthenic C _N		63.7	63.0
Carbon, paraffinic C _P		31.9	29.9
Viscosity gravity constant	ASTM D2501	0.799	0.902

[0056] Further base oils were prepared using the Group II base stock and the aromatic extract in other amounts. Oxidation properties of the base oils were tested according to the Institute of Petroleum procedure IP48 and the results are given in Table V below :

Table V.

Wt. % aromatic extract in base oil	Sample	Δ viscosity Ratio	Carbon unoxidized %	Carbon oxidized %	Δ carbon %
0	Experiment A	3.06	0.05	0.60	0.55
3	Example 3	1.18	0.12	0.33	0.21
6	Example 4	1.11	0.20	0.37	0.17
12	Example 1	1.18	0.31	0.87	0.56
18	Example 5	1.30	0.52	1.35	0.83
24	Example 2	1.40	0.69	2.37	1.68

(continued)

Wt. % aromatic extract in base oil	Sample	Δ viscosity Ratio	Carbon unoxidized %	Carbon oxidized %	Δ carbon %
30	Example 6	1.60	0.87	2.76	1.89

[0057] Experiment A is not according to the present invention because it does not contain any aromatic extract.

[0058] The results of the change in carbon (Δ carbon) and viscosity ratio at the different concentrations of aromatic extract in the base oil are also shown in Figure 1.

[0059] The results of the Δ carbon and viscosity ratio show that the aromatic extract provides an improvement in Δ carbon at a concentration of aromatic extract up to about 12 % by weight and an improvement in viscosity ratio at a concentration of aromatics extract of up to 30 % by weight.

[0060] These results show the beneficial effect of the presence of 0.2 to 30 % by weight of aromatic extract in a base oil composition comprising a base stock comprising at least 95 weight % saturated hydrocarbons.

[0061] Lubricant compositions suitable for use in a marine 4-stroke engine using heavy fuel were prepared using a salicylate-rich additive package and base oils comprising different amounts of aromatic extract.

[0062] Properties of the formulated lubricant compositions are shown in Table VI below.

Table VI.

Base oil blend used in lubricant	Test Methods	100% Group II	88% Group II 12% AE	76% Group II 24% AE
Sample			Example 7	Example 8
KV40, mm ² /s (cSt)	IP71	99.28	124.2	160.4
KV100, mm ² /s(cSt)	IP71	11:63	13.12	15.04
VI	IP226	105	99	93
TBN, mg KOH/g	IP276	38.71	40.59	40.29
Pour Point, °C	IP15	-21	-18	-15
Flash point (PMCC), °C	IP34	218.8	220.2	226.2
Metals, ppm	ICP			
Ca		14996	13641	13667
P		565	481	483
Zn		518	505	503
Si		8	11	12
Na		54	50	50
Foam, ml/ml	IP146			
Sequence 1		0/0	0/0	0/0
Sequence 2		280/0	350/0	390/0
Sequence 3		0/0	10/0	10/0
Density, g/cm ³	IP365	0.9018	0.9123	0.9231
ARV, mins	IP313	20.6	25.1	31.7
Demulsibility, ml	ASTM D1401	1/0/79 (60 mins. 82 °C)	1/0/79 (60 mins. 82 °C)	1/0/79 (60 mins. 82 °C)

[0063] Oxidation properties of the lubricant compositions were measured. The results are shown in Table VII below.

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Table VII.

Base oil used in lubricant composition	Test Method	100% Group II	88% Group II 12% AE	76% Group II 24% AE
Sample			Example 7	Example 8
Isothermal oxidation test (ISOT) Δ BN, % Δ KV 40, % Δ KV100, %	ISOT 72hrs @ 165°C	-1.42 +3.02 +0.25	-2.60 +8.9 +0.70	-2.87 +22.8 +1.47
Panel Coker aluminium panels 22hrs 325°C	BEM144	68.1	121.4	137.1
Panel Coker Steel panels 2x4hrs 320°C Average	In-house method	107.4/147.7 127.6	33.3/28.9 31.1	10.2/9.4 9.8
Cu corrosion 3 hrs 120°C	ASTM D130	N/A	1a slight tarnish	1a slight tarnish
Cu corrosion 3hrs 150°C	ASTM D130	N/A	1a slight tarnish	1a slight tarnish
Rusting characteristics	IP135B	N/A	No rusting	No rusting

[0064] The results in Table VII show some improvement is observed within the Panel Coker Test using steel panels undertaken according to the in-house method at 12 and 24 % by weight aromatic extract indicating an improvement within the solvency of the lubricant composition when aromatic extract is used.

[0065] Wear properties of the lubricant compositions were measured using a Cameron Plint test. The results are shown in Table VIII below.

Table VIII.

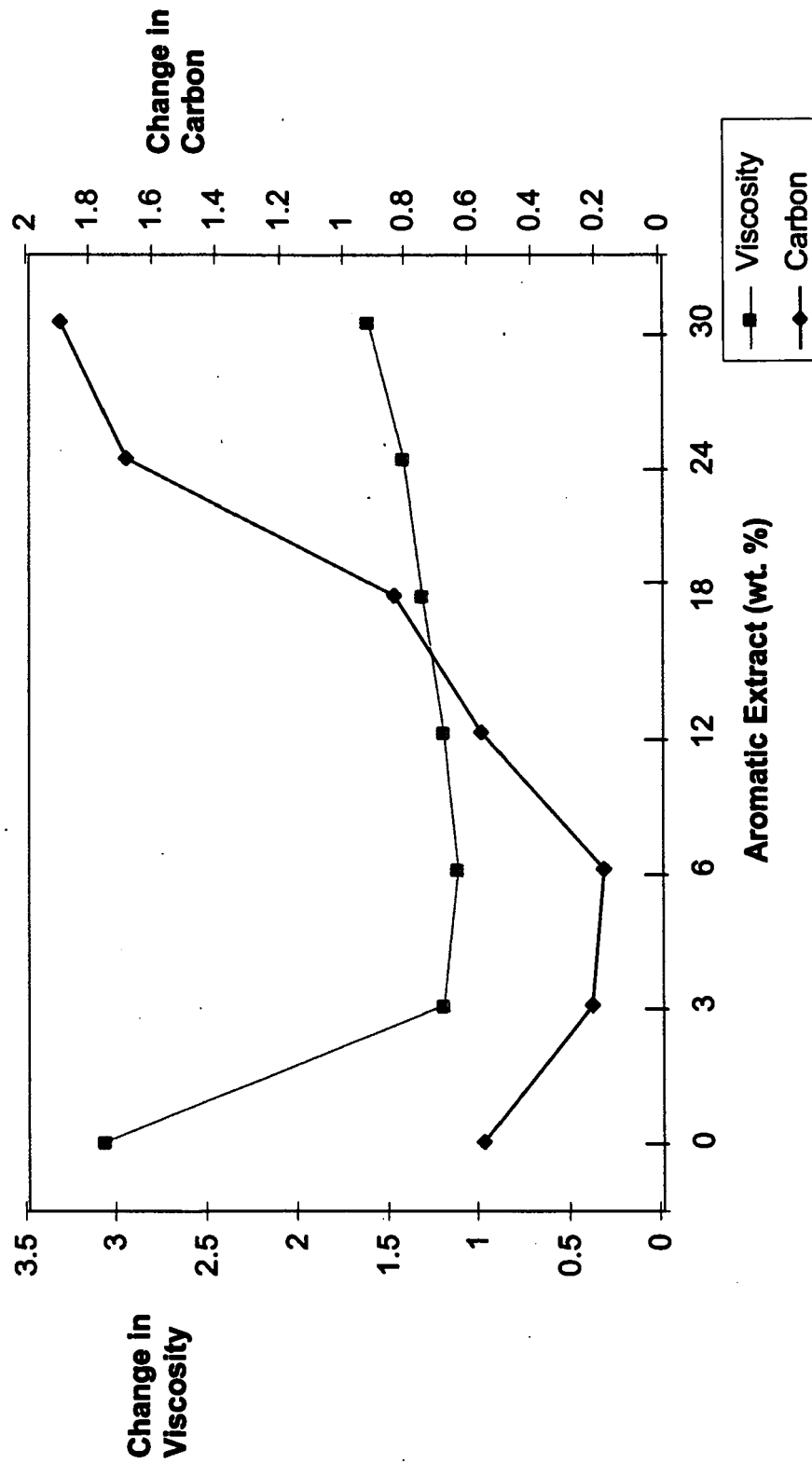
	Test	Wear vol. mm ³	Specific Wear Rate (SWR) m ³ /Nm	Mean Wear Scar Depth (MWSD) μ m	Pin wear mm
Bad reference	1074	0.0643	5.82 E-17	22.7	0.024
Good reference	1082	0.0119	7.35 E-18	12.1	0.006
100% Gp II	006A/02	0.00182	1.12 E-18	18.9	0.007
88% Group II 12% AE	010A/01	0	0.00 E+00	0	0.002
76% Group II 24% AE	011A/01	0.0254	1.57 E-17	18	0.009

[0066] The wear properties were compared against reference lubricant formulations with good and bad wear performance. The results show an exceptionally good wear performance for a lubricant composition with a base oil comprising 12 % by weight aromatic extract. However, at the higher concentration of 24 % by weight aromatics extract in the base oil, there is no significant improvement in wear performance compared to the composition with 100% Group II base oil. This data implies that there is an optimum concentration of aromatic extract for wear performance.

Claims

1. A liquid lubricant base oil composition comprising (i) a base stock comprising at least 95 % by weight saturated hydrocarbons and (ii) 0.2 to 30 % by weight, preferably 0.2 to 18 % or 1 to 30 % by weight, more preferably 1.0 to 18 % by weight, of an aromatic extract.
2. A liquid lubricant base oil composition as claimed in claim 1 in which the base stock comprising at least 95 % by weight saturated hydrocarbons comprises a hydroprocessed base stock and/or a base stock derived from Fischer-Tropsch synthesised, waxy, paraffinic hydrocarbon material.
3. A liquid lubricant base oil composition as claimed in claim 2 in which the hydroprocessed base stock is a Group II base stock and/or a Group III base stock.
4. A liquid lubricant base oil composition as claimed in claim 1 in which the base stock comprises a Group II base stock and/or a Group III base stock.
5. A liquid lubricant base oil composition as claimed in any one of claims 1 to 4 in which the aromatic extract has a dimethyl sulphoxide extractable polycyclic aromatics content of less than 3 weight %.
6. A method of making a liquid lubricant base oil composition as claimed in any one of claims 1 to 5 which method comprises blending a base stock comprising at least 95 % by weight saturated hydrocarbons with sufficient aromatic extract to make a liquid lubricant base oil composition as claimed in any one of claims 1 to 5.
7. A liquid lubricant composition comprising a liquid lubricant base oil composition as claimed in any one of claims 1 to 5 and one or more additives, preferably selected from the group consisting of detergents, dispersants, anti-wear additives, anti-oxidants, anti-foams, corrosion inhibitors, pour point depressants, friction modifiers, tackifiers and viscosity index improvers.
8. A liquid lubricant composition as claimed in claim 7 when used as a 2-stroke marine diesel engine cylinder oil, 2-stroke marine diesel engine system oil or 4-stroke marine diesel engine crankcase lubricant composition.
9. The use of 0.2 to 30 % by weight of an aromatic extract in a liquid lubricant base oil composition which base oil comprises a base stock comprising at least 95 % by weight saturated hydrocarbons, to mitigate at least one of the deficiencies of the base stock selected from the group consisting of poor dispersancy, poor seal swell performance, poor solubility of additives and low compatibility with fuel oil in marine engine applications.

**Figure 1 Effect on IP48 Results of Aromatic Extract
in Base Oil**





European Patent
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EUROPEAN SEARCH REPORT

Application Number
EP 07 25 0739

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