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(54) LARGE PORE POLYMERIC MEMBRANE WITH DEFINED PORE DENSITY

POLYMERE MEMBRAN MIT GROSSEN POREN UND DEFINIERTER PORENDICHTE

MEMBRANE POLYMÈRE À PORES DE GRANDE DIMENSION ET À DENSITÉ DE PORES DÉFINIE

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Description

BACKGROUND OF THE INVENTION

[0001] Synthetic polymer membranes are used for filtration in a variety of applications. However, there is a need for membranes that provide sufficient strength and sufficient retention of undesirable material while providing good throughput. There is also a need for membranes for inkjet applications that minimize smearing.

[0002] The invention provides such membranes.

[0003] These and other advantages of the present invention will be apparent from the description as set forth below.

[0004] Polymeric membranes are known from EP 0 578 210 A2, CN 100402135 C, CA 1,313,736 C, US 2008/0061002 A1, EP 1 535 657 A1 and US 2002/0162792 A1 EP 0 578 210 A2 discloses the preparation of a membrane by preparing a solution of 90wt% polyethyleneglycol (PEG) and 10wt% polyethersulfone (no solvent). The solution is cast onto an aluminium plate, the plate being heated for 30 sees, such that the solution reaches a temperature of 90°C. Then the plate was immersed for 3 min in a water bath at 68°C. The membrane is intended for inkjet filtration.

[0005] US 2008/061002 A1 discloses the preparation of a polysulfone+PVP membrane (polysulfone + PVP in DMAc, 203 microm) with casting, exposure on hot plate of 100°C for 5 min, leading to solvent evaporation and subsequent quenching in water.

BRIEF SUMMARY OF THE INVENTION

[0006] The invention provides a porous polymeric membrane as set out in claim 1. The membrane comprises a first microporous skin surface; a second porous surface; and, a bulk between the first microporous skin surface and the second porous surface, wherein the bulk of the membrane has a pore density of at least 120 pores/mm². The first microporous skin surface comprises a pore density of at least 20 pores/50,000 micrometers² (μm²). In some embodiments, the first microporous skin surface comprises a mean pore size of at least 10 μm. The bulk of the membrane has a mean flow pore (MFP) size of at least 15 μm.

[0007] In some embodiments, the membrane comprises an isotropic membrane comprising a first microporous skin surface, the first microporous skin surface comprising a pore density of at least 20 pores/50,000 μm²; a second porous surface, wherein the second porous surface comprises a second microporous skin surface; and, a bulk between the first microporous skin surface and the second porous surface, wherein the bulk of the membrane has a pore density of at least 120 pores/mm². In other embodiments, the membrane comprises an asymmetric membrane comprising a first microporous skin surface, the first surface having a pore density of at least 20 pores/50,000 μm²; a second porous surface; and, a

bulk between the first microporous skin surface and the second porous surface, the bulk of the membrane having a pore density of at least 120 pores/mm², wherein the second porous surface comprises a second coarse porous surface, wherein the second coarse porous surface comprises pores having a mean pore size that is greater than the mean pore size of the pores in the first microporous skin surface. Typically, the second coarse porous surface comprises pores having a mean pore size that is at least 1.3 times the mean pore size of the pores in the first microporous skin surface.

[0008] The bulk of the asymmetric or the isotropic membrane has an MFP size of at least 15 μm. Additionally, in a typical embodiment, the first microporous skin surface of the asymmetric or the isotropic membrane has a mean pore size of at least 10 μm.

[0009] A method for making porous polymeric membranes is provided, the method comprising casting a polymer solution on a support, exposing the cast solution to a temperature of at least about 35 °C (95 °F) for at least about 40 seconds; inducing thermal phase inversion of the solution to form a pre-membrane; and, quenching the pre-membrane.

[0010] In other embodiments, methods of using the membranes and devices including the membranes are provided.

BRIEF DESCRIPTION OF THE SEVERAL VIEWS OF THE DRAWING(S)

[0011]

Figure 1A-1C show cross-sectional, microporous skin surface, and coarse porous surface views of several asymmetric membranes according to embodiments of the present invention.

Figure 2 shows cross-sectional, first microporous surface, and second microporous surface views of an isotropic membrane according to another embodiment of the present invention.

Figures 3A-3C show illustrative systems for preparing embodiments of membranes according to the present invention, the illustrated systems including heating belts to heat a stone having a cast solution thereon (Figure 3A), water baths to heat a stone having a cast solution thereon (Figure 3B), and a heating lamp to heat the side of the cast solution not contacting the stone (Figure 3C).

DETAILED DESCRIPTION OF THE INVENTION

[0012] The invention provides a porous polymeric membrane comprising a first microporous skin surface; a second porous surface; and, a bulk between the first microporous skin surface and the second porous surface, wherein the bulk has a pore density of at least 120 pores/mm². The first microporous skin surface comprises a pore density of at least 20 pores/50,000 μm². In a pre-

ferred embodiment, the first microporous skin surface comprises a mean pore size of at least 10 μm . Additionally, the bulk of the membrane has a mean flow pore (MFP) size of at least 15 μm .

[0013] In some embodiments, the membrane comprises an isotropic membrane comprising a first microporous skin surface, the first microporous skin surface comprising a pore density of at least 20 pores/50,000 μm^2 ; a second porous surface, wherein the second porous surface comprises a second microporous skin surface; and, a bulk between the first microporous skin surface and the second porous surface, wherein the bulk of the membrane has a pore density of at least 120 pores/ mm^2 . The bulk of the isotropic membrane has an MFP size of at least 15 μm , and in a preferred embodiment, the first microporous skin surface has a mean flow pore size of at least 10 μm .

[0014] In other embodiments, the membrane comprises an asymmetric membrane comprising a first microporous skin surface, the surface having a pore density of at least 20 pores/50,000 μm^2 ; a second porous surface; and, a bulk between the first microporous skin surface and the second porous surface, the bulk of the membrane having a pore density of at least 120 pores/ mm^2 , wherein the second porous surface comprises a second coarse porous surface, wherein the second coarse porous surface comprises pores having a mean pore size that is greater than the mean pore size of the pores in the first microporous skin surface. Typically, the second coarse porous surface comprises pores having a mean pore size that is at least 1.3 times the mean pore size of the pores in the first microporous skin surface. In some embodiments, the second coarse porous surface comprises pores having a mean pore size that is at least 1.5 times the mean pore size of the pores in the first microporous skin surface, for example, the second coarse porous surface can comprises pores having a mean pore size that is in the range of from about 5 times to 15 times the mean pore size of the pores in the first microporous skin surface. The bulk of the asymmetric membrane has an MFP size of at least 15 μm .

[0015] The polymeric membrane comprises a mixture of polysulfone and polyvinylpyrrolidone, the polysulfone is preferably a polyethersulfone.

[0016] Another embodiment of the invention comprises a method for processing a fluid, the method comprising passing the fluid through an embodiment of the membrane.

[0017] A method for making a porous membrane is provided, the method comprising casting a polymer solution on a support, exposing the cast solution to a temperature of at least about 35 $^{\circ}\text{C}$ (95 $^{\circ}\text{F}$) (preferably, at least about 37.8 $^{\circ}\text{C}$ (100 $^{\circ}\text{F}$)) for at least about 40 seconds; inducing thermal phase inversion of the solution to form a pre-membrane; and, quenching the pre-membrane, preferably in a water bath, more preferably a heated water bath, to provide a set membrane. The set membrane can be separated from the support and leached to remove the

solvent and other soluble ingredients (alternatively, the set membrane can be removed from the support before or during leaching). The separated membrane can be dried, or kept wet.

[0018] Advantageously, the inventive membranes are particularly suitable for inkjet applications, providing minimal smearing and/or gel line. An additional advantage is that they provide sufficient strength and sufficient retention of undesirable material while providing good throughput (flow rate).

[0019] Accordingly, in one embodiment of a method according to the invention, the method comprises filtering an ink-containing fluid by passing it through an embodiment of the membrane.

[0020] In other embodiments, devices including the membranes are provided. For example, in one embodiment, a device comprises a filter capsule for ink jet filtration, the capsule comprising a housing having an inlet and an outlet and defining a fluid flow path between the inlet and the outlet, and a filter comprising an embodiment of the membrane between the inlet and the outlet and across the fluid flow path. Optionally, the device comprises an opaque housing to protect against UV-light intrusion.

[0021] Membranes according to embodiments of the invention can be used in a variety of applications, including, for example, inkjet applications, diagnostic applications (including, for example, sample preparation and/or diagnostic lateral flow devices), filtering fluids for the pharmaceutical industry, filtering fluids for medical applications (including for home and/or for patient use, e.g., intravenous applications, also including, for example, filtering biological fluids such as blood (e.g., to remove leukocytes)), filtering fluids for the electronics industry, filtering fluids for the food and beverage industry, clarification, filtering antibody- and/or protein-containing fluids, cell detection (including *in situ*), cell harvesting, and/or filtering cell culture fluids. Alternatively, or additionally, membranes according to embodiments of the invention can be used to filter air and/or gas and/or can be used for venting applications (e.g., allowing air and/or gas, but not liquid, to pass therethrough). Membranes according to embodiments of the inventions can be used in a variety of devices, including surgical devices and products, such as, for example, ophthalmic surgical products.

[0022] As used herein, the term "skin" (in "microporous skin surface") does not indicate the relatively thick, nearly impervious layer of polymer that is present in some membranes. Here, the microporous skin is a relatively thin, porous surface that overlies a microporous region of variable thickness. The pores of the underlying microporous region may be the same size as, or somewhat smaller than, the skin pores. In asymmetric membranes according to the invention, the opposite face of the membrane (the second porous surface) can be referred to as the non-skin face, or the coarse pored surface.

[0023] The membranes can have any suitable pore structure, e.g., a pore size (for example, as evidenced

by bubble point, or by K_L as described in, for example, U.S. Patent 4,340,479, or evidenced by capillary condensation flow porometry), a mean flow pore (MFP) size (e.g., when characterized using a porometer, for example, a Porvair Porometer (Porvair plc, Norfolk, UK), or a porometer available under the trademark POROLUX (Porometer.com; Belgium)), a pore rating, a pore diameter (e.g., when characterized using the modified OSU F2 test as described in, for example, U.S. Patent 4,925,572), or removal rating that reduces or allows the passage therethrough of one or more materials of interest as the fluid is passed through the porous media. The pore structure used depends on the size of the particles to be utilized, the composition of the fluid to be treated, and the desired effluent level of the treated fluid.

[0024] The bulk of the asymmetric and isotropic membranes according to embodiments of the invention have an MFP size of at least 15 μm , in some embodiments, for example, 17 or 18 μm , and in some embodiments, at least about 20 μm , or greater.

[0025] Membranes according to embodiments of the invention have a high pore density in the bulk of the membranes. Pore density can be determined for a given membrane sample by, for example, viewing a scanning electron micrograph of the surface of the membrane of interest of a given square surface area and calculating the number of pores in the given area. The number of pores calculated to be in a given square area can be normalized to a particular reference area through a simple ratio. In contrast with commercially available membranes having pore densities in the bulk of about 8 pores/ mm^2 or even about 70 pores/ mm^2 , membranes (asymmetric and isotropic) produced in accordance with embodiments of the invention have pore densities in the bulk of at least 120 pores/ mm^2 , typically, pore densities of at least about 150 pores/ mm^2 , preferably, pore densities of at least about 160 pores/ mm^2 . In some embodiments, membranes according to the invention have pore densities in the bulk of about 200 pores/ mm^2 , or more.

[0026] Preferably, the microporous skin surface also has a high pore density (e.g., as determined by SEM surface pore analysis, for example, by calculating from an SEM micrograph at 800X magnification). In contrast with commercially available membranes having skin surface pore densities of about 13 pores/500 μm^2 , membranes produced in accordance with embodiments of the invention have skin surface pore densities of at least 20 pores/50,000 μm^2 , typically, skin surface pore densities of at least about 23 pores/50,000 μm^2 , preferably, skin surface pore densities of at least about 26 pores/50,000 μm^2 . In some embodiments wherein the second porous surface is a microporous surface, the second porous surface also has the high pore densities described above.

[0027] The porous surfaces of the membranes can have any suitable mean pore size, e.g., as determined by, for example, calculating the average surface pore size from an SEM micrograph at 800X magnification. Typically, at least the first microporous skin surface has

a mean pore size of at least 10 μm . In some embodiments, the first microporous skin surface has a mean pore size of at least about 15 μm , or at least about 20 μm .

[0028] Isotropic membranes according to the invention have first and second surfaces comprising microporous skin surfaces wherein the surfaces have mean pore sizes that are substantially the same. For example, the second microporous skin surface can have a mean pore size that is 1 to 1.2 times the mean pore size of the pores in the first microporous skin surface.

[0029] Asymmetric membranes have a pore structure (e.g., a mean flow pore size) varying throughout the bulk of the membrane. For example, the mean pore size decreases in size from one portion or surface to another portion or surface (e.g., the mean flow pore size decreases from the upstream portion or surface to the downstream portion or surface). However, other types of asymmetry are encompassed by embodiments of the invention, e.g., the pore size goes through a minimum pore

size at a position within the thickness of the asymmetric membrane. The asymmetric membrane can have any suitable pore size gradient or ratio. This asymmetry can be measured by, for example, comparing the mean pore size on major surface of a membrane with the mean pore size of the other major surface of the membrane.

[0030] In those embodiments wherein the inventive membrane comprises an asymmetric membrane, the second porous surface comprises pores having a mean pore size that is greater than the mean pore size of the pores in the first microporous skin surface. Typically, the second surface has a mean pore size that is at least 1.3 times the mean pore size of the first surface. In some embodiments, the mean pore size of the second surface is at least about 1.5 times, or at least 2 times, the mean pore size of the first surface, for example, in the range of from about 3 to 15 times the mean pore size of the first surface, or from about 2 to about 10 times the mean pore size of the first surface.

[0031] Advantageously, membranes according to the invention provide good throughput (flow rate), typically, at least about 1500 ml/min@ 10 cm (1500 ml/min@4 inches) water pressure, preferably, at least about 2000 ml/min@ 10 cm (2000 ml/min@4 inches) water pressure.

[0032] Alternatively, or additionally, membranes according to the invention have a delta P transmembrane pressure (TMP) of about 150 Pascal (Pa) or less, preferably, about 125 Pa or less. For example, in some embodiments, the TMP is in the range of about 30 to about 100 Pa.

[0033] Membranes according to the invention can have a water bubble point of at least about 50.8 cm (20 inches) of water.

[0034] Membranes according to the invention are typically unsupported.

[0035] Typically, membranes according to the invention have a thickness in the range of from about 70 μm to about 300 μm , preferably in the range of from about 80 μm to about 150 μm .

[0036] Typically, the voids volume of the membrane is at least about 50%, e.g., in the range of from about 60% to about 90%, preferably, in the range of from about 70% to about 85%.

[0037] The membrane is prepared by a thermally induced phase inversion process. Typically, the phase inversion process involves casting or extruding polymer solution(s) into thin films, and precipitating the polymers through one or more of the following: (a) evaporation of the solvent and nonsolvent, (b) exposure to a non-solvent vapor, such as water vapor, which absorbs on the exposed surface, (c) quenching in a non-solvent liquid (e.g., a phase immersion bath containing water, and/or another non-solvent), and (d) thermally quenching a hot film so that the solubility of the polymer is suddenly greatly reduced. Phase inversion can be induced by the wet process (immersion precipitation), vapor induced phase separation (VIPS), thermally induced phase separation (TIPS), quenching, dry-wet casting, and solvent evaporation (dry casting). Dry phase inversion differs from the wet or dry-wet procedure by the absence of immersion coagulation. In these techniques, an initially homogeneous polymer solution becomes thermodynamically unstable due to different external effects, and induces phase separation into a polymer lean phase and a polymer rich phase. The polymer rich phase forms the matrix of the membrane, and the polymer lean phase, having increased levels of solvents and non-solvents, forms the pores.

[0038] Thermal phase inversion can be carried out using a variety of techniques and systems. For example, a casting bed, belt, or stone (or moving carrier or support thereon) can be heated using, illustratively, a heating pad, heating lamp, another heated object, a heated fluid circulation system, or a water bath. Typically, thermal phase inversion is carried out using a temperature of at least about 35 °C (95 °F), preferably, at least about 37.8 °C (100 °F), and in some embodiments, at least about 43.3 °C (110 °F), for at least about 40 seconds (preferably, at least about 45 seconds), so that phase inversion is completed before quenching.

[0039] Typically, a temperature gradient is initially produced in the thickness of the cast solution, such that the side or surface of the cast solution contacting (or facing) the heating lamp or heated casting bed, belt, stone, carrier or support will have a temperature that is different than the opposite side or surface positioned away from the lamp, bed, belt, stone, carrier or support.

[0040] Illustratively, using the exemplary systems 1000 shown in Figures 3A-3C for reference, a polymer solution is cast (using knife 110), typically on a moving belt, that moves over a stone 100 (in the casting direction shown by the single arrow on the stone) and into a quenching bath 150 (that may also provide a heating bath for heating the stone). The stone can be heated, e.g., by using at least one heating belt 175 (for example, as shown in Figure 3A, showing heating belts 175A, 175B, and 175C) or by using a heated water bath (for example,

as shown in Figure 3B), or heat can be applied to the side of the cast solution not contacting the belt or stone (for example, by using a heating lamp 160 as shown in Figure 3C).

[0041] If air velocity is desired, the system can include one or more fans to provide air velocity. Figures 3A-3C show six fans 200.

[0042] The membranes can be cast manually (e.g., poured, cast, or spread by hand onto a casting surface) or automatically (e.g., poured or otherwise cast onto a moving bed). Examples of suitable supports include, for example, polyethylene coated paper, or polyester (such as MYLAR).

[0043] A variety of casting techniques are known in the art and are suitable. A variety of devices known in the art can be used for casting. Suitable devices include, for example, mechanical spreaders, that comprise spreading knives, doctor blades, or spray/pressurized systems. One example of a spreading device is an extrusion die or slot coater, comprising a casting chamber into which the casting formulation (solution comprising a polymer) can be introduced and forced out under pressure through a narrow slot. Illustratively, the solutions comprising polymers can be cast by means of a doctor blade with knife gaps in the range from about 120 micrometers to about 500 micrometers, more typically in the range from about 180 micrometers to about 400 micrometers.

[0044] A variety of air gaps are suitable for use in the invention, and the air gaps can be the same for the same for the knives/doctor blades, or different. Typically, the air gaps are in the range of from about 76 cm (30 inches) to about 203 cm (80 inches), more typically, in the range of from about 89 cm (35 inches) to about 152 cm (60 inches).

[0045] A variety of casting speeds are suitable as is known in the art. Typically, the casting speed is at least about 52 cm (2 feet) per minute (fpm), e.g., with knife air gaps of at least about 7.6 cm (3 inches).

[0046] The polymer solution according to the invention comprises a mixture of polysulfone as a hydrophobic polymer and polyvinylpyrrolidone as a hydrophilic polymer. Suitable polymers are polysulfones, including aromatic polysulfones such as, for example, polyethersulfone, polycarbonate sulfone, bisphenol A polysulfone, polyarylsulfone, and polyphenylsulfone. In addition the typical polymer solutions comprise at least one solvent, and may further comprise at least one non-solvent. Suitable solvents include, for example, dimethyl formamide (DMF); N,N-dimethylacetamide (DMAC); N-methyl pyrrolidone (NMP); tetramethylurea; dioxane; diethyl succinate; dimethylsulfoxide; chloroform; and tetrachloroethane; and mixtures thereof. Suitable nonsolvents include, for example, water; various polyethylene glycols (PEGs; e.g., PEG-400, PEG-1000); various polypropylene glycols; various alcohols, e.g., methanol, ethanol, isopropyl alcohol (IPA), amyl alcohols, hexanols, heptanols, and octanols; alkanes, such as hexane, propane, nitropropane, heptanes, and octane; and ketone, ethers and es-

ters such as acetone, butyl ether, ethyl acetate, and amyl acetate; and various salts, such as calcium chloride, magnesium chloride, and lithium chloride; and mixtures thereof.

[0047] If desired, a solution comprising a polymer can further comprise, for example, one or more polymerization initiators (e.g., any one or more of peroxides, ammonium persulfate, aliphatic azo compounds (e.g., 2,2'-azobis(2-amidinopropane) dihydrochloride (V50)), and combinations thereof), and/or minor ingredients such as surfactants and/or release agents.

[0048] The membrane is hydrophilic, having a CWST of 72 dynes/cm (72×10^{-5} N/cm) or more. In some embodiments, the element has a CWST of 75 dynes/cm (about 75×10^{-5} N/cm) or more.

[0049] The surface characteristics of the membrane can be modified (e.g., to affect the CWST, to include a surface charge, e.g., a positive or negative charge, and/or to alter the polarity or hydrophilicity of the surface) by wet or dry oxidation, by coating or depositing a polymer on the surface, or by a grafting reaction. Modifications include, e.g., irradiation, a polar or charged monomer, coating and/or curing the surface with a charged polymer, and carrying out chemical modification to attach functional groups on the surface. Grafting reactions may be activated by exposure to an energy source such as gas plasma, vapor plasma, corona discharge, heat, a Van der Graff generator, ultraviolet light, electron beam, or to various other forms of radiation, or by surface etching or deposition using a plasma treatment.

[0050] A device comprising at least one membrane according to an embodiment of the invention can include additional elements, layers, or components, that can have different structures and/or functions, e.g., at least one of prefiltration, support, drainage, spacing and cushioning. Illustratively, an embodiment of the device can also include at least one additional element such as a mesh and/or a screen.

[0051] The filter, in some embodiments comprising a plurality of filter elements is typically disposed in a housing comprising at least one inlet and at least one outlet and defining at least one fluid flow path between the inlet and the outlet, wherein the filter is across the fluid flow path, to provide a filter device. Preferably, the filter device is sterilizable. Any housing of suitable shape and providing at least one inlet and at least one outlet may be employed.

[0052] The housing can be fabricated from any suitable rigid impervious material, including any impervious thermoplastic material, which is compatible with the fluid being processed. For example, the housing can be fabricated from a metal, such as stainless steel, or from a polymer.

[0053] The following examples further illustrate the invention but, of course, should not be construed as in any way limiting its scope.

[0054] In the following examples, a system is set up as generally shown in Figure 3B, including knife 110. Six

fans are used to provide air velocity. Solutions are cast on a moving MYLAR belt.

EXAMPLE 1

[0055] This example demonstrates the preparation of membranes according to embodiments of the invention.

[0056] Solutions are cast on a moving MYLAR belt (at a casting speed of 0.91 m/min (3.5 fpm), using a casting knife having a knife gap of 368 μm (14.5 mils). The fan speed is 60 watts.

[0057] A solution consisting of 11.0% PSF (P-3500), 2.0% DI water, 5.25% PVP (k-90), 19.5% PEG200, and 62.25% NMP is cast. Another solution consisting of 10.9% PSF (P-3500), 2.0% DI water, 5.5% PVP (k-90), 19.3% PEG200, and 62.25% NMP is cast.

[0058] Another solution consisting of 10.7% PSF (P-3500), 1.95% DI water, 5.1% PVP (k-90), 21.3% PEG200, and 60.95% NMP is cast.

[0059] Following each casting, the belt having the cast solution thereon is passed over a heated stone (heated to a temperature between 37.8 °C - 43.3 °C (100-110 °F)) for 55 seconds and then the solution is quenched in a water bath having a temperature of about 54.4 °C (130 °F).

[0060] SEM views (skin surface, coarse surface, and cross-section) of the membranes are shown in Figure 1A-1C.

[0061] The MFPs of the bulks of the membranes, as determined by the Xonics POROMETER, average 20 μm . The membranes exhibit a water flow averaging over 1980 ml/min@ 10 cm (1980 ml/min@4 inches) water pressure. The thickness of the membranes averages about 89 μm . The pore density of the membranes, as determined using a Xonics POROMETER, averages over 150 pores/mm², and the pore density of the microporous skin surfaces as determined by SEM surface pore analysis averages over 25 pores/50,000 μm^2 . The CWSTs of the membranes averages over 76 dynes/cm (76×10^{-5} N/cm).

[0062] In order to show the importance of heat, an asymmetric membrane is also prepared as generally described above (using a solution consisting of 11.0% PSF (P-3500), 2.0% DI water, 5.25% PVP (k-90), 19.5% PEG200, and 62.25% NMP), with the exception that the stone is at ambient temperature, rather than heated. The MFP of the bulk of the membrane, as determined by the Xonics POROMETER, is 8.9 μm . The membrane exhibits a water flow of 792 ml/min@ 10 cm (792 ml/min@4 inches) water pressure. The thickness of the membrane is about 110 μm . The pore density of the membrane, as determined using a Xonics POROMETER, is over 150 pores/mm², and the pore density of the microporous skin surface as determined by SEM surface pore analysis is over 25 pores/50,000 μm^2 .

EXAMPLE 2

[0063] This example demonstrates the preparation of an isotropic membrane according to another embodiment of the invention.

[0064] A solution consisting of 11.0% PSF (P-3500), 2.0% DI water, 5.25% PVP (k-90), 19.5% PEG200, and 62.25% NMP is cast on a moving MYLAR belt (at a casting speed of 0.91 m/min (3.5 fpm)), using a casting knife having a knife gap of 368 μm (14.5 mils). The fan speed is 70 watts (19.5 m/min (64 feet per minute (fpm)).

[0065] Following casting, the belt having the cast solution thereon is passed over a heated stone (between 37.8 $^{\circ}\text{C}$ - 43.3 $^{\circ}\text{C}$ (100-110 $^{\circ}\text{F}$)) for 65 seconds and then the solution is quenched in a water bath having a temperature of about 54.4 $^{\circ}\text{C}$ (130 $^{\circ}\text{F}$).

[0066] SEM views (first skin surface, second skin surface, and cross-section) of the membrane are shown in Figure 2. The mean pore size of the pores of the skin surfaces are each 19.5 μm .

[0067] The MFP of the bulk of the membrane is 19.8 μm . The water flow is over 1980 ml/min@ 10 cm (1980 ml/min@4 inches) water pressure. The pore density of the bulk is over 130 pores/mm², the membrane has a thickness of 90 μm , a tensile strength of 311 gram force (gF), and a break strength of 28%.

[0068] For comparison, an isotropic membrane is prepared as generally described in U.S. Patent Application Publication 2002/0162792 using a solution consisting of 9.0% PSF (P-3500), 2.0% DI water, 4.3% PVP (k-90), 19.5% PEG200, and 65.2% NMP. The MFP of the bulk of the membrane is 15 μm , the water flow is about 800 ml/min@ 10 cm (800 ml/min@4 inches) water pressure, the pore density of the bulk is in the range of about 70-92 pores/mm², the pore density of the microporous skin surface as determined by SEM surface pore analysis is 13 pores/50,000 μm^2 , the membrane has a thickness of 112 μm , a tensile strength of 125 gF, and a break strength of 7%.

EXAMPLE 3

[0069] This example demonstrates the preparation of asymmetric membranes with different asymmetry ratios according to embodiments of the invention.

[0070] Solutions consisting of 11.0% PSF (P-3500), 2.0% DI water, 5.25% PVP (k-90), 19.5% PEG200, and 62.25% NMP are cast on a moving MYLAR belt (at a casting speed of 0.91 m/min (3.5 fpm)), using a casting knife having a knife gap of 368 μm (14.5 mils). The fan speeds are 70, 80 and 85 watts (19.5 m/min (64 fpm), 29 m/min (95 fpm), and 31.7 m/min (104 fpm), respectively). Following each casting, the belt having the cast solution thereon is passed over a heated stone (between 37.8 $^{\circ}\text{C}$ - 43.3 $^{\circ}\text{C}$ (100-110 $^{\circ}\text{F}$)) for 50 seconds and then the solution is quenched in a water bath having a temperature of about 54.4 $^{\circ}\text{C}$ (130 $^{\circ}\text{F}$).

[0071] The resultant asymmetric membranes have

asymmetry ratios of 1.8, 2.5, and 3.7, respectively. The MFPs of the bulks of the membranes are 18.2 μm , 16.6 μm , and 17.4 μm , respectively. The water flows are 1720, 1650, and 1633 ml/min@ 10 cm (1633 ml/min@4 inches) water pressure, respectively. The mean pore sizes of the first microporous surfaces are 15 μm , 12.1 μm , and 10 μm , respectively, and the mean pore sizes of the second porous (coarse) surfaces are 27.8 μm , 30 μm , and 37 μm , respectively.

EXAMPLE 4

[0072] This example demonstrates the preparation of asymmetric membranes, including asymmetric membranes prepared using temperatures greater than 23.9 $^{\circ}\text{C}$ (75 $^{\circ}\text{F}$) (Reference) according to embodiments of the invention.

[0073] Solutions consisting of 11.0% PSF (P-3500), 2.0% DI water, 5.25% PVP (k-90), 19.5% PEG200, and 62.25% NMP are cast on a moving MYLAR belt (at a casting speed of 0.91 m/min (3.5 fpm)), using a casting knife having a knife gap of 368 μm (14.5 mils). The fan speed is 70 watts. Following each casting, the belt having the cast solution thereon is passed over a heated stone (heated to 23.9 $^{\circ}\text{C}$, 35 $^{\circ}\text{C}$, and 40.5 $^{\circ}\text{C}$ (75 $^{\circ}\text{F}$, 95 $^{\circ}\text{F}$, and 105 $^{\circ}\text{F}$)) for 50 seconds and then the solution is quenched in a water bath have a temperature of about 54.4 $^{\circ}\text{C}$ (130 $^{\circ}\text{F}$).

[0074] The membranes prepared using stones heated to 23.9 $^{\circ}\text{C}$ (Reference), 35 $^{\circ}\text{C}$ (Reference), and 40.5 $^{\circ}\text{C}$ (75 $^{\circ}\text{F}$, 95 $^{\circ}\text{F}$, and 105 $^{\circ}\text{F}$) have water flows of 810 ml/min@ 10 cm (810 ml/min@4 inches) water pressure, 1630 ml/min@ 10 cm (1630 ml/min@4 inches) water pressure, and 2300 ml/min@ 10 cm (2300 ml/min@4 inches) water pressure, respectively. The bulks of the membranes have MFP sizes of 8.9 μm , 14 μm , and 20 μm , respectively.

Claims

1. A planar porous hydrophilic polymeric membrane having a CWST of $72 \cdot 10^{-5}$ N/cm (72 dynes/cm) or more comprising:

- (a) a first microporous skin surface, the microporous first skin surface comprising a pore density of at least 20 pores/50,000 μm^2 ;
- (b) a second porous surface; and,
- (c) a bulk between the first microporous skin surface and the second porous surface wherein the bulk has a pore density of at least 120 pores/mm²;

55 wherein the bulk of the membrane comprises a mean flow pore (MFP) size of at least 15 μm ; and wherein the polymeric membrane comprises a mixture of polysulfone and polyvinylpyrrolidone.

2. The membrane of claim 1, wherein the polymeric membrane has first and second surfaces comprising the microporous skin surfaces, wherein the second microporous skin surface has a mean pore size of 1 to 1.2 times the mean pore size of the pores in the first microporous skin surface. 5

3. The membrane of claim 1, wherein the polymeric membrane comprises an asymmetric membrane, wherein the second porous surface comprises pores having a mean pore size that is at least 1.3 times the mean pore size of the pores in the first microporous skin surface. 10

4. The asymmetric membrane of claim 3, wherein the second porous surface comprises pores having a mean pore size in the range of from 2 to 15 times the mean pore size of the pores in the first microporous skin surface. 15

5. The membrane of any one of claims 1 to 4, wherein the first microporous skin surface has a mean pore size of at least 10 μm . 20

6. The membrane of any one of claims 1 to 5, wherein the polymeric membrane comprises a polyethersulfone membrane. 25

7. A method for processing a fluid comprising: passing the fluid through the membrane of any one of claims 1 to 6. 30

weist, welche die mikroporösen Hautoberflächen umfassen, wobei die zweite mikroporöse Hautoberfläche eine mittlere Porengröße aufweist, welche das 1- bis 1,2-Fache der mittleren Porengröße der Poren in der ersten mikroporösen Hautoberfläche beträgt. 5

3. Membran nach Anspruch 1, wobei die polymere Membran eine asymmetrische Membran umfasst, wobei die zweite poröse Oberfläche Poren mit einer mittleren Porengröße umfasst, welche mindestens das 1,3-Fache der mittleren Porengröße der Poren in der ersten mikroporösen Hautoberfläche beträgt. 10

4. Asymmetrische Membran nach Anspruch 3, wobei die zweite poröse Oberfläche Poren mit einer mittleren Porengröße im Bereich des 2- bis 15-Fachen der mittleren Porengröße der Poren in der ersten mikroporösen Hautoberfläche umfasst. 15

5. Membran nach einem der Ansprüche 1 bis 4, wobei die erste mikroporöse Hautoberfläche eine mittlere Porengröße von mindestens 10 μm umfasst. 20

6. Membran nach einem der Ansprüche 1 bis 5, wobei die polymere Membran eine Polyethersulfonmembran umfasst. 25

7. Verfahren zum Verarbeiten eines Fluids, umfassend:
Hindurchleiten des Fluids durch die Membran nach einem der Ansprüche 1 bis 6. 30

Patentansprüche

1. Planare poröse hydrophile polymere Membran mit einem CWST-Wert von $72 \cdot 10^{-5}$ N/cm (72 dyn/cm) oder mehr, umfassend:

(a) eine erste mikroporöse Hautoberfläche, wobei die mikroporöse erste Hautoberfläche eine Poredichte von mindestens 20 Poren/50 000 μm^2 umfasst; 40

(b) eine zweite poröse Oberfläche; und

(c) ein Volumen zwischen der ersten mikroporösen Hautoberfläche und der zweiten porösen Oberfläche, wobei das Volumen eine Poredichte von mindestens 120 Poren/mm² aufweist; 45

wobei das Volumen der Membran eine mittlere Durchflusssporen-(MFP)-größe von mindestens 15 μm aufweist; und 50

wobei die polymere Membran eine Mischung von Polysulfon und Polyvinylpyrrolidon umfasst. 55

2. Membran nach Anspruch 1, wobei die polymere Membran eine erste und eine zweite Oberfläche auf-

Revendications

1. Membrane polymère hydrophile poreuse plane ayant un CWST de $72 \cdot 10^{-5}$ N/cm (72 dynes/cm) ou supérieur comprenant :

(a) une première surface de peau microporeuse, la première surface de peau microporeuse comprenant une densité de pores d'au moins 20 pores/50 000 μm^2 ;

(b) une seconde surface poreuse ; et,

(c) un volume entre la première surface de peau microporeuse et la seconde surface poreuse dans laquelle le volume présente une densité de pores d'au moins 120 pores/mm² ;

dans laquelle le volume de la membrane comprend une taille de pores d'écoulement moyenne (MFP) d'au moins 15 μm ; et

dans laquelle la membrane polymère comprend un mélange de polysulfone et polyvinylpyrrolidon. 50

2. Membrane selon la revendication 1, dans laquelle la membrane polymère présente des premières et se-

conde surfaces comprenant les surfaces de peaux microporeuses, dans laquelle la seconde surface de peau microporeuse présente une taille moyenne de pores de 1 à 1,2 fois la taille moyenne de pores des pores dans la première surface de peau microporeuse. 5

3. Membrane selon la revendication 1, dans laquelle la membrane polymère comprend une membrane asymétrique, dans laquelle la seconde surface poreuse comprend des pores ayant une taille moyenne de pores qui est au moins 1,3 fois la taille moyenne de pores des pores dans la première surface de peau microporeuse. 10
4. Membrane asymétrique selon la revendication 3, dans laquelle la seconde surface poreuse comprend des pores ayant une taille moyenne de pores dans l'intervalle de 2 à 15 fois la taille moyenne de pores des pores dans la première surface de peau microporeuse. 15
5. Membrane selon l'une quelconque des revendications 1 à 4, dans laquelle la première surface de peau microporeuse présente une taille moyenne de pores d'au moins 10 µm. 20
6. Membrane selon l'une quelconque des revendications 1 à 5, dans laquelle la membrane polymère comprend une membrane de polyéthersulfone. 25
7. Procédé pour le traitement d'un fluide comprenant : le passage du fluide à travers la membrane selon l'une quelconque des revendications 1 à 6. 30

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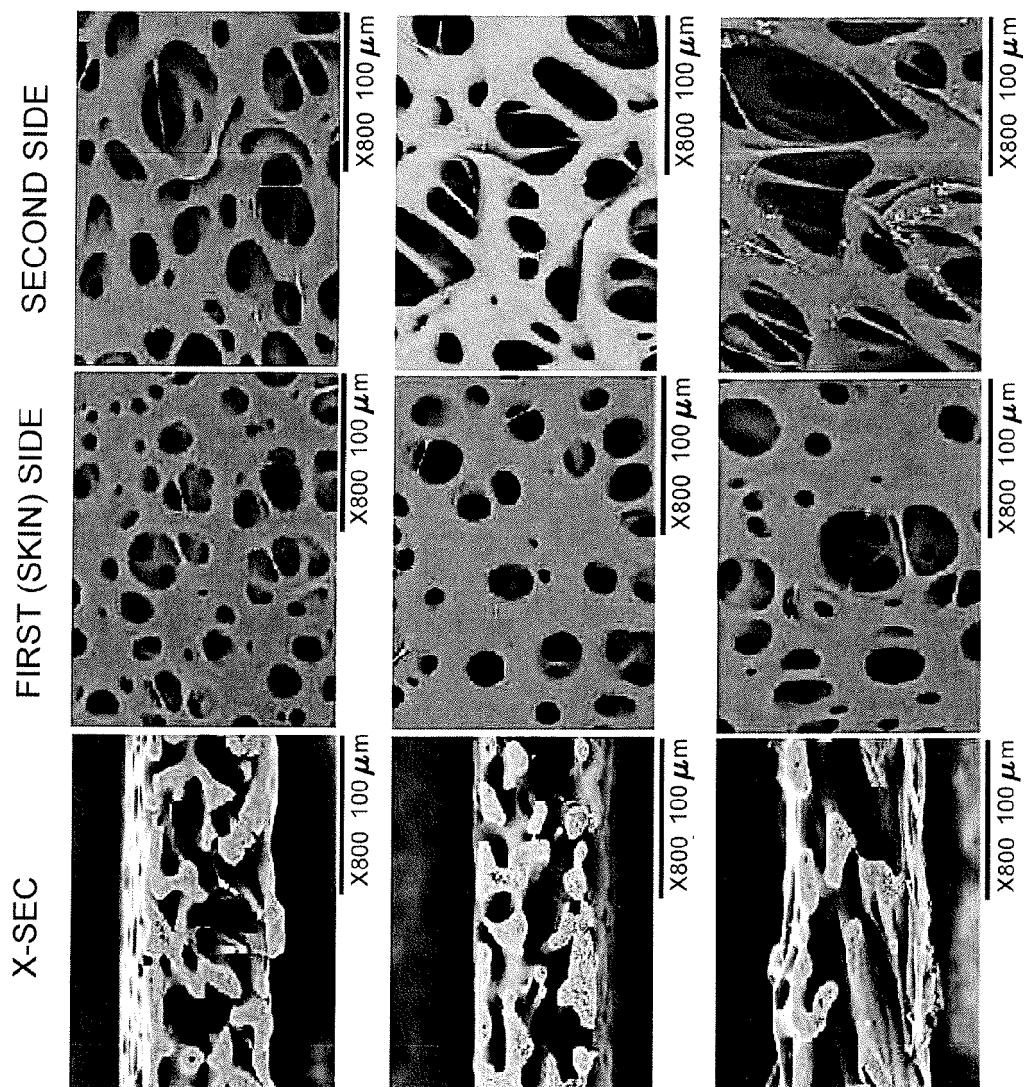


FIG. 1A

FIG. 1B

FIG. 1C

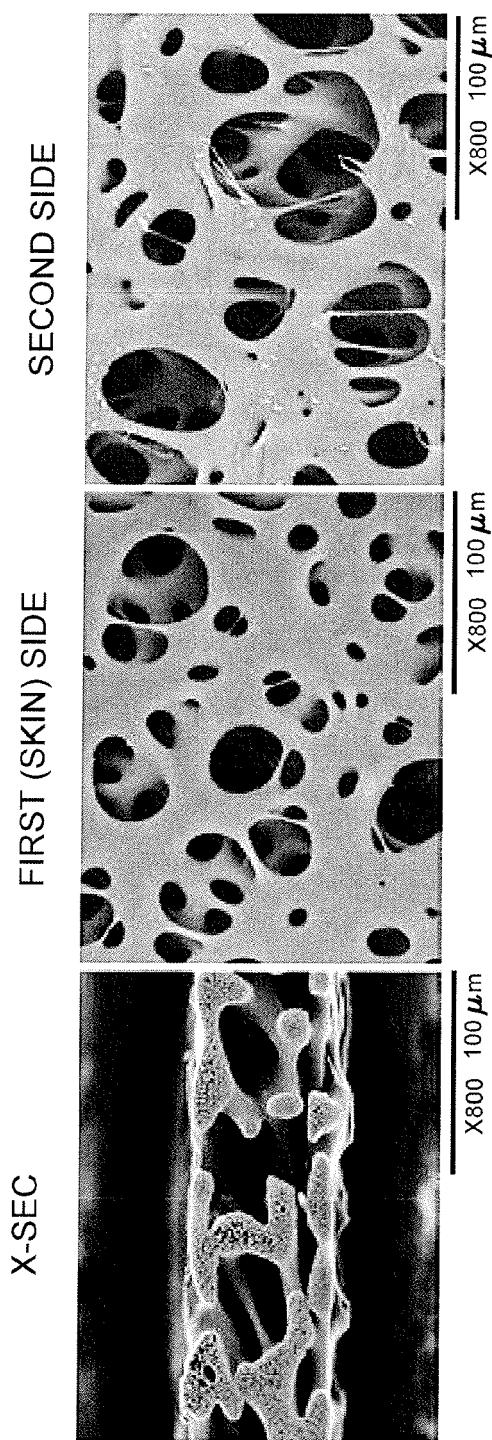


FIG. 2

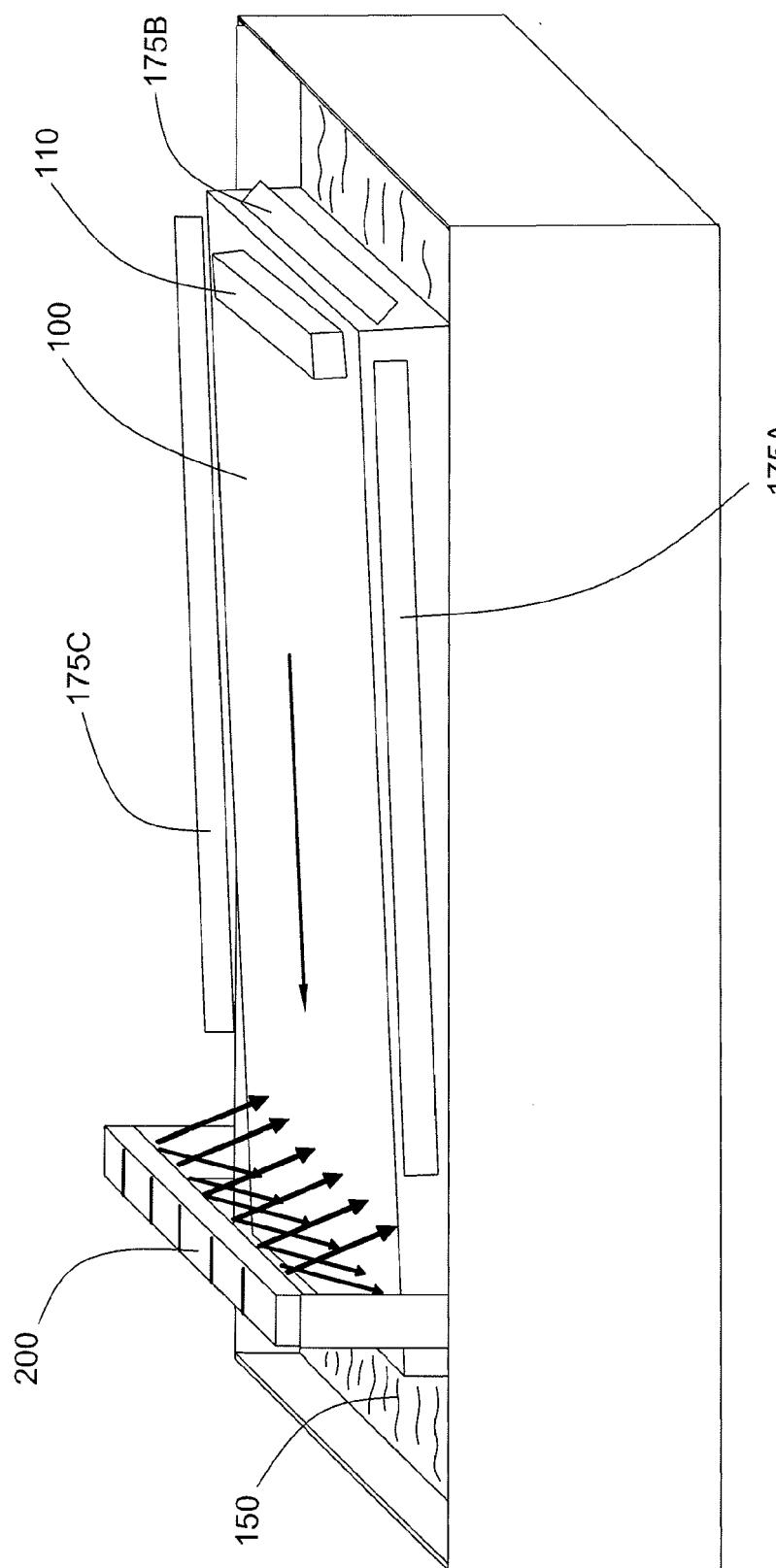


FIG. 3A

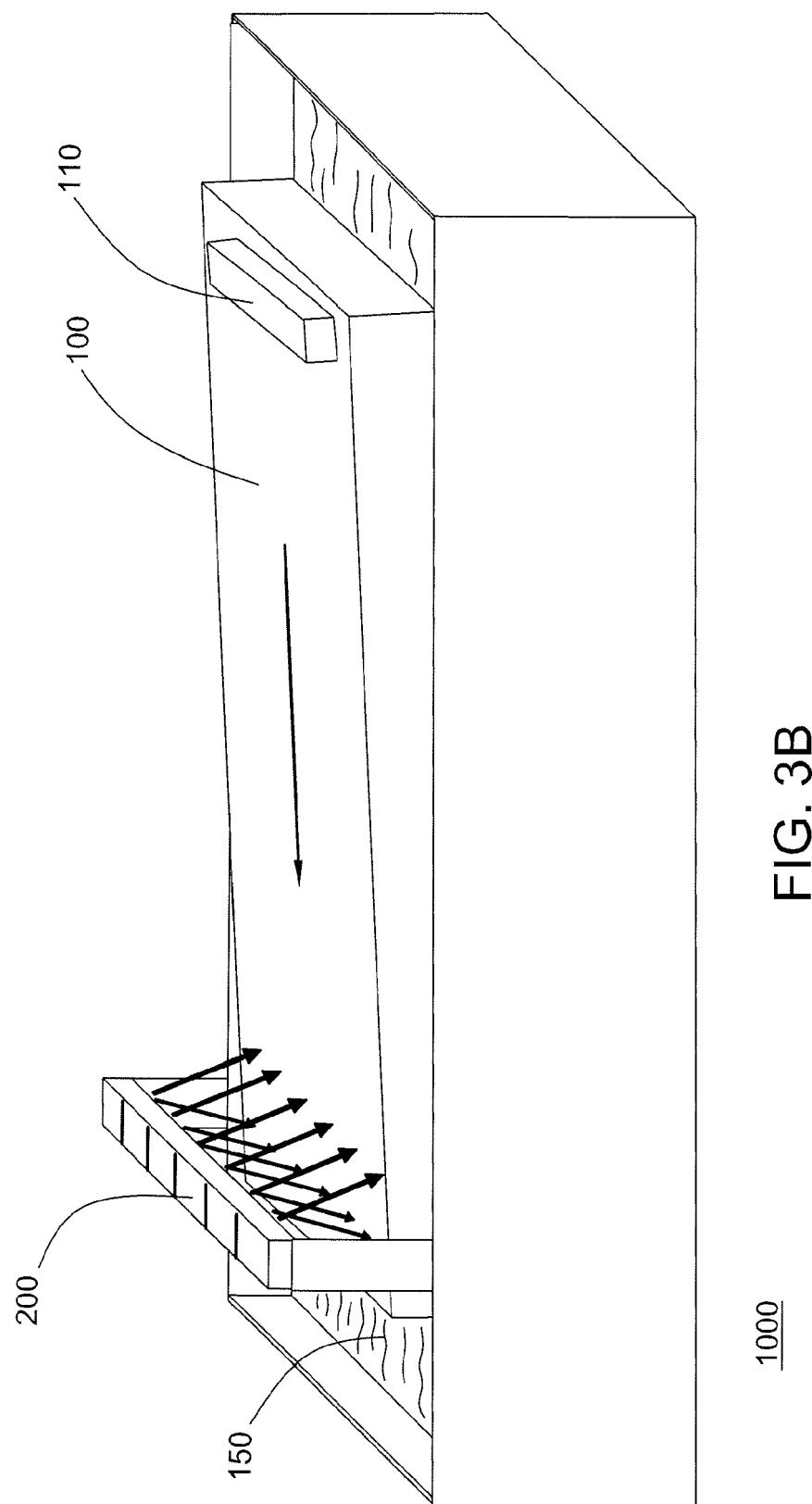


FIG. 3B

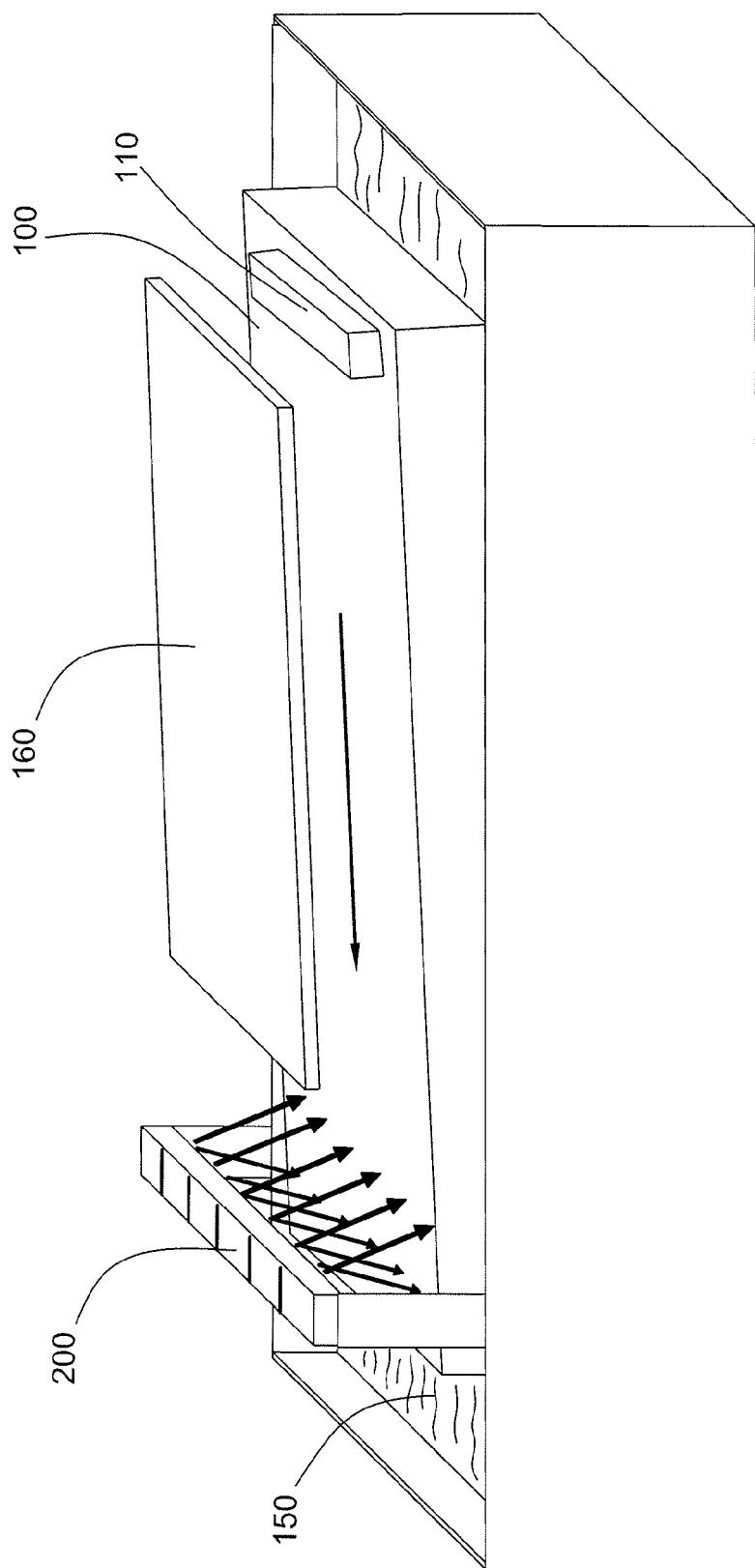


FIG. 3C

REFERENCES CITED IN THE DESCRIPTION

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