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(54) **COMPOSITIONS COMPRISING ENZYMES WITH ENDO-1, 4-BETA-XYLANASE ACTIVITY AND ENZYMES WITH ENDO-1,3(4)-BETA GLUCANASE ACTIVITY**

ZUSAMMENSETZUNGEN ENTHALTEND ENZYME MIT ENDO-1, 4-BETA-XYLANASE ACTIVITÄT UND ENZYME MIT ENDO-1,3(4)-BETA GLUCANASE AKTIVITÄT

COMPOSITIONS COMPRENANT DES ENZYMES AVEC L'ACTIVITÉ ENDO-1, 4-BETA-XYLANASE ET DES ENZYMES AVEC L'ACTIVITÉ ENDO-1,3(4)-BETA GLUCANASE

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**Description**

## FIELD OF THE INVENTION

5     **[0001]** The present invention relates to enzymes with improved properties and to compositions comprising these enzymes suitable for use in the production of a food, beverage (e.g. beer), feed, or biofuel, such as in a brewing process.

## BACKGROUND OF THE INVENTION

10    **[0002]** The use of enzymes in beer production is well known. Application of enzymes to the mashing step to improve mash filterability and increase extract yield is described in WO 97/42302.

**[0003]** WO2005118769 and WO2005059084 relates to a mashing and filtration step in a process for the production of beer, and to enzymatic compositions for use in such a process.

15    **[0004]** WO1999057325 relates to strains of *Penicillium funiculosum*, to new enzyme mixtures obtained from it and nucleic sequences thereto.

**[0005]** WO 2010/128140 relates to an enzyme composition comprising an expression product from *Trichoderma* in combination with one or more enzymes from a different fungal species.

**[0006]** WO 97/13853 relates to a method of identifying DNA sequences of proteins of interest.

**[0007]** WO 2009/108941 relates to enzymes useful for degrading plant biomass material.

20    **[0008]** Banergee et al. (2010) *Biochnol Biofuels* 3, 22 relates to a study on enzyme cocktails for specific pretreatment/biomass combinations.

**[0009]** Kvesitadze et al. (1994) *Microbios* 80,115-23 relates to endo- $\beta$ -1,4-glucanase and endo- $\beta$ -1,4-xylanase from the thermophilic fungus *Allescheria terrestris*.

25    **[0010]** Ito et al. (1992) *Biosci Biotechnol Biochem* 56, 906-12 relates to the cloning of the xynA gene coding for xylanase A from *Aspergillus kawachii*.

**[0011]** Wang et al. (2011) *Biotechnol Lett* 33, 1029-38 relates to the cloning of a endo-1,4- $\beta$ -D-xylanase of *Aspergillus usamii*.

30    **[0012]** However, there is a need for improved enzymes as well as combination of enzymes useful in the productions of food and beverage products, such as in the mashing, cooking and filtration steps in the production of an alcoholic beverage, such as beer or whiskey.

## OBJECT OF THE INVENTION

35    **[0013]** It is an object of embodiments of the invention to provide enzymes suitable for the production of food and beverage products, such as in the production of an alcoholic or non-alcoholic beverage, such as a cereal- or malt-based beverage like beer or whiskey. The enzymes provided may have improved properties in relation to the use in brewing. These wide varieties of improved properties comprise e.g. improved temperature optimums, improved ratio in activity on soluble (WE-AX) to insoluble (WU-AX) arabinoxylan substrates, reduced total pressure built up during lautering and/or filtration steps of a brewing process, as well as increased filterability of enzyme treated material.

## SUMMARY OF THE INVENTION

45    **[0014]** It has been found by the present inventor(s) that one or more enzyme as well as certain combinations of enzymes have improved properties relative to known enzymes and enzyme combinations, particularly in relation to the use in a process of brewing, wherein starch containing material is treated with the one or more enzyme to produce a brewing mash.

50    **[0015]** In one aspect, the present invention relates to a composition comprising an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity, which enzyme comprises an amino acid sequence having at least 90 % identity with SEQ ID NO: 1; in combination with an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity which enzyme comprises an amino acid sequence having at least 90% identity with SEQ ID NO:7.

55    **[0016]** In a further aspect, the present invention relates to the use of a composition according to the invention in the production of a food, feed, or malt beverage product, in the production of dough or baked products, in the preparation of pulp or paper, for the preparation of cereal components, such as in which the cereal is rye, wheat, or barley, in the production of beer or modification of by-products from a brewing process, in the production of wine or juice, or in the production of a first- or second-generation biofuel, such as bioethanol.

**[0017]** Described herein is an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity, which enzyme comprises an amino acid sequence having at least 80% identity with any one selected from SEQ ID NO:1, SEQ ID NO:2, SEQ ID NO:3, SEQ ID NO:4, SEQ ID NO:5, SEQ ID NO:6, SEQ ID NO:17, and SEQ ID NO:18, or any functional fragment thereof.

**[0018]** As used herein "functional fragment" refers to a truncated version of an enzyme with essentially the same or at least a significant degree of enzyme activity as the non-truncated reference enzyme.

**[0019]** Described herein is an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity, which enzyme comprises an amino acid sequence having at least 80% identity with any one selected from SEQ ID NO:7, SEQ ID NO:8, SEQ ID NO:9, SEQ ID NO:10, and SEQ ID NO:11, SEQ ID NO:12, SEQ ID NO:13, SEQ ID NO:14, SEQ ID NO:15, SEQ ID NO:16, or any functional fragment thereof.

**[0020]** Described herein is a DNA construct comprising a DNA sequence encoding an enzyme as disclosed herein.

**[0021]** Described herein is a recombinant expression vector comprising a DNA construct comprising a DNA sequence encoding an enzyme as disclosed herein.

**[0022]** Described herein is a cell that has been transformed with a DNA construct comprising a DNA sequence encoding an enzyme as disclosed herein.

**[0023]** Described herein is a preparation comprising an enzyme, or a DNA construct, or a vector, or a cell as disclosed herein.

**[0024]** Described herein is composition comprising an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity as disclosed herein in combination with any one or more  $\beta$ -glucanase.

**[0025]** Described herein is a composition comprising an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity as disclosed herein in combination with any one or more xylanase.

**[0026]** In a further aspect the present invention relates to the use of a composition according to the invention in the production of a food, feed, or malt beverage product, such as beer or whiskey.

**[0027]** In a further aspect the present invention relates to the use of a composition according to the invention, in the production of dough or baked products.

**[0028]** In a further aspect the present invention relates to the use of a composition according to the invention, in the preparation of pulp or paper.

**[0029]** In a further aspect the present invention relates to the use of a composition according to the invention, for the preparation of cereal components. In some embodiments the cereal is rye, wheat, or barley.

**[0030]** In a further aspect the present invention relates to the use of a composition according to the invention, in the production of beer or modification of by-products from a brewing process.

**[0031]** In a further aspect the present invention relates to the use of a composition according to the invention, in the production of wine or juice.

**[0032]** In a further aspect the present invention relates to the use of a composition according to the invention, in the production of a first - or second-generation biofuel, such as bioethanol.

**[0033]** In a further aspect the present invention relates to a method of altering filterability of a starch comprising material, said method comprising the step of treating said starch comprising material with a composition according to the invention.

**[0034]** In a further aspect the present invention relates to a method of reducing pressure built up during lautering in a brewing application, said method comprising the step of treating a brewing mash with a composition according to the invention.

**[0035]** In a further aspect the present invention relates to a method for the production of a food, feed, or beverage product, such as an alcoholic or non-alcoholic beverage, such as a cereal or malt-based beverage like beer or whiskey, said method comprising the step of treating a starch comprising material with a composition according to the invention.

**[0036]** In a further aspect the present invention relates to a method for the production of a brewing mash, said method comprising the step of treating a starch comprising material with a composition according to the invention.

**[0037]** In a further aspect the present invention relates to a method for the production of a first - or second-generation biofuel, such as bioethanol, said method comprising the step of treating a starch comprising material with a composition according to the invention.

**[0038]** Described herein are products obtained by a method according to the invention.

**[0039]** Described herein is a composition comprising the product obtained by a method according to the invention, such as wherein the product is in a range of 0.1%-99.9%.

## LEGENDS TO THE FIGURE

**[0040]**

Fig. 1: Mashing profile used in lab scale and pilot scale brewing. Mashing was initiated by a 10 min mashing-in period after which the enzyme was added.

Fig. 2: Pilot scale Brewing application results from verification of the glucanase and xylanases screening. The B. sub glucanase S combined with the A. tub xylanases was tested against a blank and UltraFlo max. Data collected was the average flow (L/h), the total pressure build up over the lautering (mm WC, where 1 mm WC = 9.80665 Pa)

and the max pressure recorded during the lautering (mm WC).

Fig 3: Xylanase functionality in brewing

Fig. 4: Flow - lautering applying various xylanase candidates

Fig. 5: Beer filtration - average of repeated filtrations

Fig. 6: Beer filtration - average of repeated filtrations

Fig. 7: Mashing diagram of example 3.

#### DETAILED DISCLOSURE OF THE INVENTION

**[0041]** Beer is traditionally referred to as an alcoholic beverage derived from malt, such as malt derived from barley grain, and optionally adjunct, such as starch containing plant material (e.g. cereal grains) and optionally flavoured, e.g. with hops.

**[0042]** In the context of the present invention, the term "beer" is meant to comprise any fermented wort, produced by fermentation/brewing of a starch-containing plant material, thus in particular also beer produced exclusively from adjunct, or any combination of malt and adjunct.

**[0043]** The term "fermentation" means in the present context production of a substance such as ethanol by growing microorganisms in a culture. Commonly, microorganisms such as yeast are used for fermentation.

**[0044]** As used herein the term "malt" is understood as any malted cereal grain, such as malted barley. "Adjunct" can be defined as any starch-containing plant material which is not malt or barley malt.

**[0045]** "Starch-containing plant material" can e.g. be one or more cereal, such as barley, wheat, maize, rye, sorghum, millet, or rice, and any combination thereof. The starch-containing plant material can be processed, e.g. milled, malted, partially malted or unmalted. Unmalted cereal is also called "raw grain". Examples of non-cereal starch-containing plant material comprise e.g. tubers, such as potatoes and cassava.

**[0046]** As used herein, the terms "beverage" and "beverage(s) product" includes such foam forming fermented beverages as full malted beer, beer brewed under the "Reinheitsgebot", ale, dry beer, near beer, light beer, low alcohol beer, low calorie beer, porter, bock beer, stout, malt liquor, non-alcoholic beer, non-alcoholic malt liquor and the like. The term "beverages" or "beverages product" also includes non-foaming beer and alternative malt beverages such as fruit flavoured malt beverages, e. g. , citrus flavoured, such as lemon-, orange-, lime-, or berry-flavoured malt beverages, liquor flavoured malt beverages, e. g. , vodka-, rum-, or tequila-flavoured malt liquor, or coffee flavoured malt beverages, such as caffeine-flavoured malt liquor, and the like.

**[0047]** Beer can be made from a variety of starch-containing plant material by essentially the same process, where the starch consists mainly of glucose homopolymers in which the glucose residues are linked by either alpha-1, 4- or alpha-1,6-bonds, with the former predominating.

**[0048]** The process of making fermented beverages such as beer is commonly referred to as brewing. The traditional raw materials used in making these beverages are water, hops and malt. In addition or instead of malt, adjuncts such as common corn grits, refined corn grits, brewer's milled yeast, rice, sorghum, refined corn starch, barley, barley starch, dehusked barley, wheat, wheat starch, torrefied cereal, cereal flakes, rye, oats, potato, tapioca, and syrups, such as corn syrup, sugar cane syrup, inverted sugar syrup, barley and/or wheat syrups, and the like may be used as a source of starch. The starch will eventually be converted enzymatically into fermentable sugars.

**[0049]** Concerning beers made predominantly from malt (e.g. up to 15-20% adjunct), for a number of reasons, the malt, which is produced principally from selected varieties of barley, has the greatest effect on the overall character and quality of the beer. First, the malt is the primary flavouring agent in beer. Second, the malt provides the major portion of the fermentable sugar. Third, the malt provides the proteins, which will contribute to the body and foam character of the beer. Fourth, the malt provides the necessary enzymatic activity during mashing.

**[0050]** Hops also contribute significantly to beer quality, including flavouring. In particular, hops (or hops constituents) add desirable bittering substances to the beer. In addition, the hops act as protein precipitants, establish preservative agents and aid in foam formation and stabilization. Not all beers are produced using hops. Other stabilizing agents, such as proteases (e.g. papain) may also be used.

**[0051]** Without wanting to be construed as limiting for the present invention, a conventional brewing process can be described as follows:

**[0052]** The process for making beer is well known in the art, but briefly, it involves five steps: (a) mashing and/or adjunct cooking (b) wort separation and extraction (c) boiling and hopping of wort (d) cooling, fermentation and storage, and (e) maturation, processing and packaging. Typically, in the first step, milled or crushed malt is mixed with water and

held for a period of time under controlled temperatures to permit the enzymes present in the malt to convert the starch present in the malt into fermentable sugars.

**[0053]** In the second step, the mash is transferred to a "lauter tun" or mash filter where the liquid is separated from the grain residue. This sweet liquid is called "wort" and the left over grain residue is called "spent grain". The mash is typically subjected to an extraction, which involves adding water to the mash in order to recover the residual soluble extract from the spent grain.

**[0054]** In the third step, the wort is boiled vigorously. This sterilizes the wort and helps to develop the colour, flavour and odour. Hops are added at some point during the boiling.

**[0055]** In the fourth step, the wort is cooled and transferred to a fermentor, which either contains the yeast or to which yeast is added. The yeast converts the sugars by fermentation into alcohol and carbon dioxide gas; at the end of fermentation the fermentor is chilled or the fermentor may be chilled to stop fermentation. The yeast flocculates and is removed.

**[0056]** In the last step, the beer is cooled and stored for a period of time, during which the beer clarifies and its flavour develops, and any material that might impair the appearance, flavour and shelf life of the beer settles out. Prior to packaging, the beer is carbonated and, optionally, filtered and pasteurized.

**[0057]** After fermentation, a beverage is obtained which usually contains from about 2% to about 10% alcohol by weight. The non-fermentable carbohydrates are not converted during fermentation and form the majority of the dissolved solids in the final beer.

**[0058]** This residue remains because of the inability of malt amylases to hydrolyze the alpha-1,6-linkages of the starch. The non-fermentable carbohydrates contribute about 50 calories per 12 ounces of beer.

**[0059]** Recently, there has been a widespread popularization of brewed beverages called light beers, reduced calorie beers or low calorie beers, particularly in the U. S. market. As defined in the U. S., these beers have approximately 30% fewer calories than a manufacturer's "normal" beer.

**[0060]** Further information on conventional brewing processes, as well as definitions for terms used in the field of brewing technology to be applied for the present invention, may be found in "Technology Brewing and Malting" by Wolfgang Kunze of the Research and Teaching Institute of Brewing, Berlin (VLB), 2nd revised Edition 1999, ISBN 3-921690-39-0, 3rd edition (2004): ISBN 3-921690-49-8, 4th updated edition, 2010 (ISBN 978-3-921690-64-2).

**[0061]** Xylanases are classified in EC 3.2.1.8, EC 3.2.1.32, EC 3.2.1.136 and EC 3.2.1.156.; their activity may be measured e.g. as described in the examples. Suitable xylanases to be used in combination with an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity according to the invention includes any xylanase classified in EC 3.2.1.8, EC 3.2.1.32, EC 3.2.1.136 and EC 3.2.1.156, such as any one disclosed in WO 2010072226, WO 2010072225, WO 2010072224, WO 2005059084, WO2007056321, WO2008023060A, WO9421785, WO2006114095, WO2006066582, US 2008233175, and WO10059424.

**[0062]** Endo-1,4-beta xylanase is classified as EC 3.2.1.8. The enzyme causes endohydrolysis of 1,4-beta-D-xylosidic linkages in xylans.

**[0063]** The terms "family 11 xylanase", "Glycoside hydrolase (GH) family 11" or simply "GH 11 xylanase" as used herein refers to an endo-1,4-beta xylanase classified as EC 3.2.1.8, which causes endohydrolysis of 1,4-beta-D-xylosidic linkages in xylans and which is classified as a family 11 xylanase according to B. Henrissat, A classification of glycosyl hydrolases based on amino acid sequence similarities. Biochem. J. 280 (1991), pp. 309-316.

**[0064]** The terms "Family 10 xylanase", "Glycoside hydrolase (GH) family 10", or simply "GH 10 xylanase" comprises enzymes with a number of known activities, such as xylanase (EC:3.2.1.8); endo-1,3-beta-xylanase (EC:3.2.1.32); cellobiohydrolase (EC:3.2.1.91). These enzymes were formerly known as cellulase family F.

**[0065]** In some embodiments the enzyme exhibiting endo-1,4- $\beta$ -xylanase activity is a family 11 xylanase. In some embodiments the enzyme exhibiting endo-1,4- $\beta$ -xylanase activity is a family 10 xylanase.

**[0066]** In one aspect, the enzyme composition according to the invention has endo-1,4-beta xylanase activity as measured by the assay described in the examples.

**[0067]** An assay for measuring xylanase activity may be carried out at pH 3.5 or pH 5 and 50 °C using xylan as substrate, or it can be performed at different pH and temperature values for the additional characterisation and specification of enzymes. Enzyme activity is calculated from the increase in absorbance caused by xylose at 540 nm per unit time.

**[0068]** In some embodiments the enzyme composition according to the invention comprises a xylanase activity of at least about 5000 U/g, such as at least about 6000 U/g, such as at least about 7000 U/g, such as at least about 8000 U/g, such as at least about 8500 U/g, as measured by in the assay described in the examples.

**[0069]** The enzyme composition according to the invention may have cellulolytic activity. The systematic name of cellulose is 4-(1,3;1,4)- $\beta$ -D-glucan 4-glucanohydrolase and cellulolytic enzymes or cellulases are classified in EC 3.2.1.4. Cellulase endohydrolyse (1 $\rightarrow$ 4)- $\beta$ -D-glucosidic linkages in e.g. cellulose, lichenin and cereal  $\beta$ -D-glucans and will also hydrolyse 1,4-linkages in  $\beta$ -D-glucans also containing 1,3-linkages. Cellulase also have other names such as endo-1,4- $\beta$ -D-glucanase,  $\beta$ -1,4-glucanase,  $\beta$ -1,4-endoglucan hydrolase, cellulase A, cellosin AP, endoglucanase D, alkali cellulose, cellulase A 3, celludextrinase, 9.5 cellulase, avicelase, pancellase SS and 1,4-(1,3;1,4)- $\beta$ -D-glucan 4-glucano-

hydrolase.

**[0070]** In one aspect of the invention, the cellulase activity of the enzyme composition according to the invention is measured by the "Cellulase activity method" as described in the following under the heading "Assays".

**[0071]** Described herein are enzymes having endo-1,3(4)- $\beta$ -glucanase activity is determined by the assay described in the examples.

**[0072]** " $\beta$ -glucanase" or "beta-glucanase" as used herein refers to an endo-1,3(4)-beta-glucanase of EC 3.2.1.6. Catalyze the endohydrolysis of (1 $\rightarrow$ 3)- or (1 $\rightarrow$ 4)-linkages in beta-D-glucans when the glucose residue whose reducing group is involved in the linkage to be hydrolyzed is itself substituted at C-3. Suitable beta-glucanases to be used in combination with an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the invention includes any one beta-glucanase disclosed in WO2004087889, WO2005059084, WO9414953, WO2007056321, WO9531533, WO08023060, WO2005100582, WO9828410, WO9742301, WO2006066582, WO05118769, WO2005003319, and WO10059424.

**[0073]** The standard assay is carried out at pH 5.0, and it can be performed at different pH values for the additional characterisation and specification of enzymes.

**[0074]** One unit of endo-1,3(4)- $\beta$ -glucanase activity is defined as the amount of enzyme which produces 1  $\mu$ mole glucose equivalents per minute under the conditions of the assay (pH 5.0 (or as specified) and 50 °C).

**[0075]** In some embodiments the enzyme composition according to the invention comprises a  $\beta$ -glucanase activity of at least about 10000 U/g, such as at least about 12000 U/g, such as at least about 14000 U/g, such as at least about 15000 U/g, such as at least about 18000 U/g as measured by the assay described in the examples.

**[0076]** The enzyme composition according to the invention may have laminarinase activity or may comprise any one or more further enzyme having laminarinase activity. The laminarinase activity is determined as described in the laminarinase assay described in the Assay section.

**[0077]** Laminarinase may be an endo-1,3(4)-beta-glucanase classified in E.C. 3.2.1.6 or glucan endo-1,3-beta-D-glucosidase classified in E.C. 3.2.1.39. Endo-1,3(4)-beta-glucanase with the alternative names, laminarinase, endo-1,3-beta-glucanase, Endo-1,4-beta-glucanase is classified in E.C. 3.2.1.6. The substrates include laminarin, lichenin and cereal D-glucans and the enzyme catalyze endohydrolysis of (1 $\rightarrow$ 3)- or (1 $\rightarrow$ 4)-linkages in beta-D-glucans when the glucose residue whose reducing group is involved in the linkage to be hydrolyzed is itself substituted at C-3. Glucan endo-1,3-beta-D-glucosidase with the alternative names (1 $\rightarrow$ 3)-beta-glucan endohydrolase, Endo-1,3-beta-glucanase and laminarinase is classified in E.C. 3.2.1.39 and hydrolyse (1 $\rightarrow$ 3)-beta-D-glucosidic linkages in (1 $\rightarrow$ 3)-beta-D-glucans in substrates as eg. laminarin, paramylon and pachyman.

**[0078]** The enzyme composition according to the invention may have arabinanase activity or may comprise a further enzyme having arabinanase activity. Arabinanase is classified as EC 3.2.1.99. The systematic name is 5- $\alpha$ -L-arabinan 5- $\alpha$ -L-arabinanohydrolase but it has several other names such as arabinan endo-1,5- $\alpha$ -L-arabinosidase, and endo-1,5- $\alpha$ -L-arabinanase, endo- $\alpha$ -1,5-arabanase, endo-arabanase, 1,5- $\alpha$ -L-arabinan and 1,5- $\alpha$ -L-arabinanohydrolase. Arabinase endohydrolyses (1 $\rightarrow$ 5)- $\alpha$ -arabinofuranosidic linkages in (1 $\rightarrow$ 5)-arabinans. Arabinanase also acts on arabinan.

**[0079]** The arabinase activity of the enzyme composition according to the invention may be measured by arabinase assay as described in the following under the heading "Assays". The assay can be carried out at pH 3.5 and 50 °C using sugar beet arabinan as substrate, and it can be performed at different pH and temperature values for the additional characterisation and specification of enzymes. Enzyme activity is calculated from the increase in absorbance at 540 nm per unit time.

**[0080]** One unit of arabinase activity is defined as the amount of enzyme (normalised for total assay volume) that gives an increase in  $\Delta OD_{540nm} \cdot min^{-1}$  under the conditions of the assay (pH 3.5 and 50 °C).

**[0081]** The enzyme composition according to the invention may have beta-D-glucoside glucohydrolase activity or may comprise a further enzyme having beta-D-glucoside glucohydrolase activity. Beta-D-glucoside glucohydrolase refers to enzymes of E.C 3.2.1.21.

**[0082]** The enzyme composition according to the invention may have  $\beta$ -Xylosidase activity or may comprise a further enzyme having  $\beta$ -Xylosidase activity. " $\beta$ -Xylosidase" or "Xylan 1,4-beta-xylosidase" refers to enzymes of E.C 3.2.1.37.  $\beta$ -Xylosidase catalyze the hydrolysis of (1 $\rightarrow$ 4)-beta-D-xylans, to remove successive D-xylose residues from the non-reducing termini.

**[0083]** The enzyme composition according to the invention may have cellobiohydrolase activity or may comprise a further enzyme having cellobiohydrolase activity. "Cellobiohydrolase" or "Cellulose 1,4-beta-cellobiosidase" refers to enzymes of EC 3.2.1.91. Cellulose 1,4-beta-cellobiosidase catalyze hydrolysis of 1,4-beta-D-glucosidic linkages in cellulose and cellotetraose, releasing cellobiose from the non-reducing ends of the chains.

**[0084]** The cellobiohydrolase activity of the enzyme composition according to the invention may be measured by the cellobiohydrolase assay as described in the following under the heading "Assays". The standard assay is carried out at pH 5.0, and it can be performed at different pH values for the additional characterisation and specification of enzymes.

**[0085]** One unit of cellobiohydrolase activity is defined as the amount of enzyme which produces 1  $\mu$ mole p-nitrophenol from p-nitrophenyl  $\beta$ -D-cellobiopyranoside per minute under the conditions of the assay (pH 5.0 (or as specified) and 50 °C).

**[0086]** The enzyme composition according to the invention may have  $\alpha$ -N-arabinofuranosidase activity or may comprise a further enzyme having arabinofuranosidase activity. " $\alpha$ -N-arabinofuranosidase" or "Alpha-N-arabinofuranosidase" refers to enzymes of EC 3.2.1.55.  $\alpha$ N-arabinofuranosidase catalyze the hydrolysis of terminal non-reducing alpha-L-arabinofuranoside residues in alpha-L- arabinosides.

**[0087]** The arabinofuranosidase activity of the enzyme composition according to the invention may be measured by the arabinofuranosidase assay as described in the following under the heading "Assays". The standard assay can be carried out at pH 5.0 and 50 °C and it can be performed at different values of pH and temperature for the additional characterisation and specification of enzymes.

**[0088]** One unit of  $\alpha$ -N-arabinofuranosidase activity is defined as the amount of enzyme which produces 1  $\mu$ mole p-nitrophenol from p-nitrophenyl  $\alpha$ -L-arabinofuranoside per minute under the conditions of the assay (pH 5.0 and 50 °C (or as specified)).

**[0089]** The enzyme composition according to the invention may have glucan 1,4-beta-glucosidase activity or may comprise a further enzyme having glucan 1,4-beta-glucosidase activity. "Glucan 1,4-beta-glucosidase" or "glucan 1,4-beta-glucosidase" refers to enzymes of E.C3.2.1.74. Glucan 1,4-beta-glucosidase catalyze the hydrolysis of (1->4)-linkages in (1->4)-beta-D-glucans, to remove successive glucose units.

**[0090]** The enzyme composition according to the invention may have xyloglucan-specific exo-beta-1,4-glucanase activity or may comprise a further enzyme having xyloglucan-specific exo-beta-1,4-glucanase activity. "xyloglucan-specific exo-beta-1,4-glucanase" refers to enzymes of E.C3.2.1.155. Xyloglucan-specific exo-beta-1,4-glucanase catalyze the exohydrolysis of (1->4)-beta-D-glucosidic linkages in xyloglucan.

**[0091]** The enzymes and enzyme compositions as described herein may be used in a process comprising reducing the viscosity of an aqueous solution comprising a starch hydrolysate.

**[0092]** The enzymes and enzyme compositions may also be used in a process comprising filtering of an aqueous solution comprising a starch hydrolysate. In some embodiments the aqueous solution comprising a starch hydrolysate is a mash for beer making, and in other embodiments the aqueous solution comprising a starch hydrolysate is a food composition.

**[0093]** Alternatively, the enzyme composition according to the present invention may be used in the production of fruit juice, wine, grain processing, fuel alcohol, first - or second-generation biofuel, such as bioethanol, and potable alcohol.

**[0094]** In some embodiments the first - or second-generation biofuel, such as bioethanol is produced from agricultural feed stocks such as sugar cane, potato, corn, wheat sorghum etc. or from cellulosic material such as corn stover, switchgrass or other plant material. In both cases fermentable sugars are extracted from the raw material and fermented by microorganisms into alcohol, which is distilled and may be used as transportation fuel. The enzyme composition according to the present invention may be used in this production of biofuel. The enzymes complex may be added to enhance extraction of polysaccharides from the raw material, help degrade polysaccharides down into fermentable sugars and/or to enhance processing parameters such as separation of liquids from solids, flow characteristics and pumpability.

**[0095]** The process of the invention may be applied in the mashing of any grist. According to the invention the grist may comprise any starch and/or sugar containing plant material derivable from any plant and plant part, including tubers, roots, stems, leaves and seeds.

**[0096]** In some embodiments the grist comprises grain, such as grain from barley, wheat, rye, oat, corn, rice, milo, millet and sorghum, and more preferably, at least 10%, or more preferably at least 15%, even more preferably at least 25%, or most preferably at least 35%, such as at least 50%, at least 75%, at least 90% or even 100% (w/w) of the grist of the wort is derived from grain.

**[0097]** In some embodiments the grist comprises malted grain, such as barley malt. Preferably, at least 10%, or more preferably at least 15%, even more preferably at least 25%, or most preferably at least 35%, such as at least 50%, at least 75%, at least 90% or even 100% (w/w) of the grist of the wort is derived from malted grain.

**[0098]** The term "mash" is understood as aqueous starch slurry, e. g. comprising crushed barley malt, crushed barley, and/or other adjunct or a combination hereof, mixed with water later to be separated into wort + spent grains.

**[0099]** The term "mash separation" is understood as the separation of wort from spent grains, such as by lautering or mash filtration.

**[0100]** The term "beer filtration" is understood as a separation process in which the yeast cells and other turbidity-causing materials still present in the beer are removed, such as by microfiltration or membrane processes.

**[0101]** The enzyme preparation, such as in the form of a food ingredient may be in the form of a solution or as a solid - depending on the use and/or the mode of application and/or the mode of administration. The solid form can be either as a dried enzyme powder or as a granulated enzyme.

**[0102]** Accordingly, described herein is an enzyme composition preparation comprising the enzymes described herein or enzyme composition according to the invention, an enzyme carrier and optionally a stabilizer and/or a preservative.

**[0103]** The enzyme carrier may be selected from the group consisting of glycerol or water.

**[0104]** The preparation may comprise a stabilizer. The stabilizer may be selected from the group consisting of inorganic



salts, polyols, sugars and combinations thereof. The stabilizer may be an inorganic salt such as potassium chloride. The polyol may be glycerol, propylene glycol, or sorbitol. The sugar may be a small-molecule carbohydrate, in particular any of several sweet-tasting ones such as glucose, fructose and saccharose.

**[0105]** The preparation may comprise a preservative. The preservative may be methyl paraben, propyl paraben, benzoate, sorbate or other food approved preservatives or a mixture thereof.

**[0106]** The enzyme exhibiting endo-1,4- $\beta$ -xylanase activity, optionally in combination with any one or more  $\beta$ -glucanase according to the present disclosure provides for a significantly reduced viscosity in brewing applications facilitating improved mash and beer separation.

**[0107]** Desired xylanase characteristics for brewing applications may include one or more of the following aspects:

a) Enzyme substrate specificity

- WE-AX/WU-AX ratio has an impact on viscosity. In some embodiments this ratio is less than about 7.0, such as less than about 6.5, such as less than about 6.0, such as less than about 5.5, such as less than about 5.0, such as less than about 4.5.

b) Enzyme substrate selectivity

- How close to branch points the enzyme(s) cuts is believed to have an impact on the functionality.

c) Enzyme thermostability

- Continuous solubilisation of AX during mashing - thermostability a key feature. Accordingly, in some embodiments, the enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the present invention is thermostable within a temperature range of 65-78°C.

d) Enzyme pH optimum. Accordingly, in some embodiments, the enzyme exhibiting endo-1,4- $\beta$ -xylanase activity has a pH optimum in the range of pH 5.4 - 5.6.

e) Enzyme inhibition (e.g. known key factor for xylanases)

**[0108]** Said significantly reduced viscosity in brewing applications may be measured as a reduced viscosity in the brewing application as compared to a control with a known enzyme or combination of enzyme activities, such as Ultraflo® Max used under same conditions and amounts.

**[0109]** The enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the present disclosure, optionally in combination with any one or more  $\beta$ -glucanase according to the present disclosure provides for an improved mash and beer separation in brewing applications.

**[0110]** The enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the present disclosure, optionally in combination with any one or more  $\beta$ -glucanase according to the present disclosure provides for a low potential for off flavour formation, such as off flavour formation related to arabinoxylan breakdown.

**[0111]** The enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the present disclosure, optionally in combination with any one or more  $\beta$ -glucanase according to the present disclosure provides for a decreased risk of filter bed collapse, such as at lautering.

**[0112]** The enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the present disclosure, optionally in combination with any one or more  $\beta$ -glucanase according to the present disclosure provides for a reduction in off flavour potential and/or reduction in off flavor formation. Described herein is an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity, which enzyme comprises an amino acid sequence having at least 80% identity with any one selected from SEQ ID NO:1, SEQ ID NO:2, SEQ ID NO:3, SEQ ID NO:4, SEQ ID NO:5, SEQ ID NO:6, SEQ ID NO:17, and SEQ ID NO:18, or any functional fragment thereof.

**[0113]** Also described herein is an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity, which enzyme comprises an amino acid sequence having at least 80% identity with any one selected from SEQ ID NO:7, SEQ ID NO:8, SEQ ID NO:9, SEQ ID NO:10, and SEQ ID NO:11, SEQ ID NO:12, SEQ ID NO:13, SEQ ID NO:14, SEQ ID NO:15, SEQ ID NO:16, or any functional fragment thereof.

**[0114]** In some embodiments of the invention the enzyme exhibiting endo-1,4- $\beta$ -xylanase activity has a ratio in activity on soluble arabinoxylan substrate (WE-AX) to insoluble arabinoxylan substrate (WU-AX) arabinoxylan substrate of less than about 7.0, such as less than about 6.5, such as less than about 6.0, such as less than about 5.5, such as less than about 5.0, such as less than about 4.5.

**[0115]** In some embodiments the enzyme according to the invention has a temperature optimum in the range of 40-70

°C, such as in the range of 45-65 °C, such as in the range of 50-65 °C, such as in the range of 55-65 °C.

**[0116]** The enzyme according to the disclosure may have at least 81, 82, 83, 84, 85, 86, 87, 88, 89, 90, 91, 92, 93, 94, 95, 96, 97, 98 or 99% identity with any one amino acid sequence selected from SEQ ID NO: 1-18, or any functional fragment thereof.

**[0117]** In some embodiments the enzyme according to the invention has a total number of amino acids of less than 350, such as less than 340, such as less than 330, such as less than 320, such as less than 310, such as less than 300 amino acids, such as in the range of 200 to 350, such as in the range of 220 to 345 amino acids.

**[0118]** The amino acid sequence of said enzyme according to the disclosure may have at least one, two, three, four, five, six, seven, eight, nine or ten amino acid substitutions as compared to any one amino acid sequence selected from SEQ ID NO: 1-18, or any functional fragment thereof.

**[0119]** The amino acid sequence of said enzyme according to the disclosure may have a maximum of one, two, three, four, five, six, seven, eight, nine or ten amino acid substitutions compared to any one amino acid sequence selected from SEQ ID NO: 1-18, or any functional fragment thereof.

**[0120]** The enzyme according to the disclosure may comprise the amino acid sequence identified by any one of SEQ ID NO: 1-18, or any functional fragment thereof.

**[0121]** The enzyme according to the disclosure may consist of the amino acid sequence identified by any one of SEQ ID NO: 1-18, or any functional fragment thereof.

**[0122]** Also described herein is a composition comprising an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the disclosure in combination with any one or more  $\beta$ -glucanase. This one or more  $\beta$ -glucanase may be according to the disclosure.

**[0123]** Also described herein is a composition comprising an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity according to the disclosure in combination with any one or more xylanase. In some embodiments this one or more xylanase is an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to the disclosure. This one or more xylanase may be an enzyme according to SEQ ID NO:17 and/or SEQ ID NO:18, or any functional fragment thereof.

**[0124]** The combination of an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity with an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity may be any combination according to the following table:

1 <sup>st</sup> enzyme (Xylanase) 2 <sup>nd</sup> enzyme (Glucanase)	SEQ ID NO:1	SEQ ID NO:2	SEQ ID NO:3	SEQ ID NO:4	SEQ ID NO:5	SEQ ID NO:6	SEQ ID NO:17	SEQ ID NO:18
SEQ ID NO:7	X	X	X	X	X	X	X	X
SEQ ID NO:8	X	X	X	X	X	X	X	X
SEQ ID NO:9	X	X	X	X	X	X	X	X
SEQ ID NO:10	X	X	X	X	X	X	X	X
SEQ ID NO:11	X	X	X	X	X	X	X	X
SEQ ID NO:12	X	X	X	X	X	X	X	X
SEQ ID NO:13	X	X	X	X	X	X	X	X
SEQ ID NO:14	X	X	X	X	X	X	X	X
SEQ ID NO:15	X	X	X	X	X	X	X	X
SEQ ID NO:16	X	X	X	X	X	X	X	X

**[0125]** It is to be understood that any one of the above combination of a 1<sup>st</sup> enzyme being an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity may be combined with one one enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity with a ratio between the two enzymes of 1:10, 2:10, 3:10, 4:10, 5:10, 6:10, 7:10, 8:10, 9:10, 10:10, 10:9, 10:8, 10:7, 10:6, 10:5, 10:4, 10:3, 10:2, or 10:1, such as within a range of 1:10-10:1, such as 2:10-10:2, such as 3:10-10:3, such as 4:10-10:4, such as 5:10-10:5, such as 6:10-10:6, such as 7:10-10:7, such as 8:10-10:8, or within 9:10-10:9.

**[0126]** In some embodiments the composition according to the invention comprises a combination of at least two enzymes, said two enzymes, or two enzymes with an amino acid sequence having at least 90% sequence identity with the respective SEQ IDs, being selected from the list consisting of SEQ ID NO:1 and SEQ ID NO:7.

**[0127]** Also described herein are the following compositions:

SEQ ID NO:2 and SEQ ID NO:7;  
SEQ ID NO:3 and SEQ ID NO:7;  
SEQ ID NO:4 and SEQ ID NO:7;

SEQ ID NO:5 and SEQ ID NO:7;  
 SEQ ID NO:6 and SEQ ID NO:7;  
 SEQ ID NO:17 and SEQ ID NO:7;  
 SEQ ID NO:18 and SEQ ID NO:7;  
 5 SEQ ID NO:1 and SEQ ID NO:8;  
 SEQ ID NO:2 and SEQ ID NO:8;  
 SEQ ID NO:3 and SEQ ID NO:8;  
 SEQ ID NO:4 and SEQ ID NO:8;  
 SEQ ID NO:5 and SEQ ID NO:8;  
 10 SEQ ID NO:6 and SEQ ID NO:8;  
 SEQ ID NO:17 and SEQ ID NO:8;  
 SEQ ID NO:18 and SEQ ID NO:8;  
 SEQ ID NO:1 and SEQ ID NO:9;  
 SEQ ID NO:2 and SEQ ID NO:9;  
 15 SEQ ID NO:3 and SEQ ID NO:9;  
 SEQ ID NO:4 and SEQ ID NO:9;  
 SEQ ID NO:5 and SEQ ID NO:9;  
 SEQ ID NO:6 and SEQ ID NO:9;  
 SEQ ID NO:17 and SEQ ID NO:9;  
 20 SEQ ID NO:18 and SEQ ID NO:9;  
 SEQ ID NO:1 and SEQ ID NO:10;  
 SEQ ID NO:2 and SEQ ID NO:10;  
 SEQ ID NO:3 and SEQ ID NO:10;  
 SEQ ID NO:4 and SEQ ID NO:10;  
 25 SEQ ID NO:5 and SEQ ID NO:10;  
 SEQ ID NO:6 and SEQ ID NO:10;  
 SEQ ID NO:17 and SEQ ID NO:10;  
 SEQ ID NO:18 and SEQ ID NO:10;  
 SEQ ID NO:1 and SEQ ID NO:11;  
 30 SEQ ID NO:2 and SEQ ID NO:11;  
 SEQ ID NO:3 and SEQ ID NO:11;  
 SEQ ID NO:4 and SEQ ID NO:11;  
 SEQ ID NO:5 and SEQ ID NO:11;  
 SEQ ID NO:6 and SEQ ID NO:11;  
 35 SEQ ID NO:17 and SEQ ID NO:11;  
 SEQ ID NO:18 and SEQ ID NO:11;  
 SEQ ID NO:1 and SEQ ID NO:12;  
 SEQ ID NO:2 and SEQ ID NO:12;  
 SEQ ID NO:3 and SEQ ID NO:12;  
 40 SEQ ID NO:4 and SEQ ID NO:12;  
 SEQ ID NO:5 and SEQ ID NO:12;  
 SEQ ID NO:6 and SEQ ID NO:12;  
 SEQ ID NO:17 and SEQ ID NO:12;  
 SEQ ID NO:18 and SEQ ID NO:12;  
 45 SEQ ID NO:1 and SEQ ID NO:13;  
 SEQ ID NO:2 and SEQ ID NO:13;  
 SEQ ID NO:3 and SEQ ID NO:13;  
 SEQ ID NO:4 and SEQ ID NO:13;  
 SEQ ID NO:5 and SEQ ID NO:13;  
 50 SEQ ID NO:6 and SEQ ID NO:13;  
 SEQ ID NO:17 and SEQ ID NO:13;  
 SEQ ID NO:18 and SEQ ID NO:13;  
 SEQ ID NO:1 and SEQ ID NO:14;  
 SEQ ID NO:2 and SEQ ID NO:14;  
 55 SEQ ID NO:3 and SEQ ID NO:14;  
 SEQ ID NO:4 and SEQ ID NO:14;  
 SEQ ID NO:5 and SEQ ID NO:14;  
 SEQ ID NO:6 and SEQ ID NO:14;

SEQ ID NO:17 and SEQ ID NO:14;  
 SEQ ID NO:18 and SEQ ID NO:14;  
 SEQ ID NO:1 and SEQ ID NO:15;  
 SEQ ID NO:2 and SEQ ID NO:15;  
 5 SEQ ID NO:3 and SEQ ID NO:15;  
 SEQ ID NO:4 and SEQ ID NO:15;  
 SEQ ID NO:5 and SEQ ID NO:15;  
 SEQ ID NO:6 and SEQ ID NO:15;  
 SEQ ID NO:17 and SEQ ID NO:15;  
 10 SEQ ID NO:18 and SEQ ID NO:15;  
 SEQ ID NO:1 and SEQ ID NO:16;  
 SEQ ID NO:2 and SEQ ID NO:16;  
 SEQ ID NO:3 and SEQ ID NO:16;  
 SEQ ID NO:4 and SEQ ID NO:16;  
 15 SEQ ID NO:5 and SEQ ID NO:16;  
 SEQ ID NO:6 and SEQ ID NO:16;  
 SEQ ID NO:17 and SEQ ID NO:16; and  
 SEQ ID NO:18 and SEQ ID NO:16.

20 **[0128]** In some embodiments the endo-1,3(4)- $\beta$ -glucanase activity and the endo-1,4- $\beta$ -xylanase activity are derived from at least two different enzymes, such as at least two different enzymes from two different species.

**[0129]** In some embodiments the total pressure built up is reduced to a value of less than 470 mm WC, such as less than 450 mm WC, such as less than 430 mm WC, such as less than 410 mm WC, such as less than 390 mm WC, such as less than 370 mm WC, such as less than 350 mm WC, such as less than 330 mm WC, such as less than 310 mm  
 25 WC, such as less than 300 mm WC, such as less than 290 mm WC, when the composition according to the present invention is used prior to the lautering in a brewing application.

**[0130]** In some embodiments the total pressure built up is reduced by at least 5, 7, 9, 11, 13, 15, 17, 19, 21, 23, 25, 27, 29, 31, 33, 35, 37, 39, 41, 43, 45, 47, 49, 51, 53, 55, 57, 59, 61, 63, 65, 67, 69, 71, 73, 75, 77, 79, 81, 83, 85, 87, 89, 91, 93 or 95 % compared to the use of a negative control without said composition; when used prior to the lautering  
 30 in a brewing application.

**[0131]** In some embodiments the wort filterability as measured by volume wort collected after 5 min of filtration relative to a control without enzymes is increased to above 1.5, such as above 1.6, such as above 1.7, such as above 1.8, such as above 1.9, such as above 2.0, such as above 2.1, such as above 2.2, such as above 2.3, such as above 2.4, such as above 2.5, when the composition according to invention is used in a brewing application prior to the wort separation.

35 **[0132]** In some embodiments the wort filterability as measured by volume wort collected after 5 min of filtration is increased at least 5, 7, 9, 11, 13, 15, 17, 19, 21, 23, 25, 27, 29, 31, 33, 35, 37, 39, 41, 43, 45, 47, 49, 51, 53, 55, 57, 59, 61, 63, 65, 67, 69, 71, 73, 75, 77, 79, 81, 83, 85, 87, 89, 91, 93, 95, 97, 99, 110, 120, 130, 140, 150, 160, 170, 180, 190, 200, 210, 220, 230, 240, 250, 260, 270, 280, 290, or 300 % as compared to the use of a negative control without said composition.

40 **[0133]** In some embodiments the composition according to the invention comprises any one or more further enzyme. In some embodiments the one or more further enzyme is selected from list consisting of a xylanase classified in EC 3.2.1.32, EC 3.2.1.136, or EC 3.2.1.156, a cellulase, a laminarinase, an endo-1,5- $\alpha$ -L-arabinanase, a beta-D-glucoside glucosidase, a  $\beta$ -Xylosidase, a cellobiohydrolase, a glucan 1,4-beta-glucosidase, a xyloglucan-specific exo-beta-1,4-glucanase and an  $\alpha$ -N-Arabinofuranosidase.

45 **[0134]** Sequences and enzymes identified by a sequence as mentioned herein and used according to the present invention alone or in combinations with other enzymes or compounds may be with or without signal peptide.

## Assays

### 50 DNS Cellulase activity method (DNS CMC method)

#### **[0135]**

55 Systematic Name: 1,4-(1,3;1,4)- $\beta$ -D-glucan 4-glucanohydrolase  
 IUB Number: EC 3.2.1.4

## Principle

[0136] The assay of cellulase is based on the enzymatic endo-hydrolysis of the 1,4-β-D-glucosidic bonds in carboxymethylcellulose (CMC), a β-1,4-glucan. The products of the reaction (β-1,4 glucan oligosaccharides) was determined colorimetrically by measuring the resulting increase in reducing groups using a 3,5-dinitrosalicylic acid reagent. Enzyme activity was calculated from the relationship between the concentration of reducing groups, as glucose equivalents, and absorbance at 540nm.

[0137] The assay was carried out at pH 5.0, but it can be performed at different pH values for the additional characterisation and specification of enzymes.

## Unit definition

[0138] One unit of cellulase activity is defined as the amount of enzyme which produces 1 μmole glucose equivalents per minute under the conditions of the assay (pH 5.0 (or as specified) and 50 °C).

## Materials

### [0139]

Carboxymethylcellulose. Supplier: Megazyme Ltd. Product no.: CM-Cellulose 4M  
 D-Glucose 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10117. M.W.: 180.16  
 Sodium acetate *anhydrous* 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10236. M.W.: 82.03  
 Acetic acid ("*glacial*") 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10001. M.W.: 60.05  
 3,5-Dinitrosalicylic acid GPR (3,5-dinitro-2-hydroxybenzoic acid). Supplier: Merck Ltd (BDH). Product no.: 28235  
 Sodium hydroxide *pellets* 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10252. M.W.: 40.00  
 Potassium sodium (+)-tartrate 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10219. M.W.: 282.22  
 1.5 % (w/v solution) Carboxymethylcellulose (CMC) solution in 0.1M sodium acetate buffer, pH 5.0 (substrate solution).  
 3,5-Dinitrosalicylic acid (DNS) solution. 20g/L of DNS in buffer containing 32g/L sodium hydroxide pellets, and 600 g/L potassium sodium (+)-tartrate.  
 Glucose standard solution (0.50 mg/ml)

## Procedure

[0140] The enzyme composition was diluted into samples and a glucose standard curve as shown in fig. 2 was made using glucose concentrations of 0, 0.125, 0.25, 0.375, and 0.5 mg/ml.

[0141] 0.25 ml of enzyme solution was mixed with 1.75 ml of the substrate solution (1.5% w/v) at 50 °C and the reaction was stopped after 10 min by addition of DNS solution. This is followed by heating to 95 °C for 5 minutes.

[0142] The optical density was measured at 540 nm ( $OD_{540nm}$ ) of the different samples.

## Calculation

[0143] The enzyme activity is determined from the standard curve as shown in fig. 2.

[0144] The activity is calculated as follows:

$$\text{Activity (u.ml}^{-1} \text{ or u.g}^{-1}\text{)} = \frac{T - c}{m} \times A \times \frac{1}{180.16} \times 10^3 \times \frac{1}{V} \times \frac{1}{t} \times D$$

where:

$T = \Delta OD_{540nm} \text{ TEST}$

$= OD_{540nm} \text{ TEST} - OD_{540nm} \text{ BLANK}$

$m = \text{gradient of the standard curve (approximately 1.0)}$

$c = \text{y axis intercept of the standard curve (always negative and approximately -0.02)}$

$180.16 \equiv \text{molecular weight of glucose}$

$10^3 \equiv \text{to convert to } \mu\text{moles}$

$A \equiv \text{assay volume in ml}$

$V$  = enzymes volume in ml

$t$  = assay time in minutes

$D$  = actual enzyme dilution factor (e.g. for 1.000g diluted to 1 litre  $D = 1000$ )

## 5 Laminarinase (DNS laminarin method)

### Principle

10 [0145] The reaction, catalysed by laminarinase, involves the endohydrolysis of 1,3- glucosidic bonds in 1,3-β-D-glucans. Substrates include laminarin, paramylon and pachyman. The products of the reaction (β-1,3-glucan oligosaccharides) are determined colourimetrically by measuring the resulting increase in reducing groups using a 3,5-dinitrosalicylic acid reagent. Enzyme activity is calculated from the relationship between the concentration of reducing groups, as glucose equivalents, and absorbance at 540nm.

15 [0146] The assay was carried out at pH 5.0 and 50 °C, but it can be performed at different values of pH and temperature for the additional characterisation and specification of enzymes.

### Unit definition

20 [0147] One unit of laminarinase activity is defined as the amount of enzyme which produces 1 μmole glucose equivalents per minute under the conditions of the assay (pH 5.0 and 50 °C (or as specified)).

### Materials

[0148] See materials given above for the Cellulase activity assay.

25 [0149] Laminarin (from *Laminaria digitata*). Supplier: Sigma-Aldrich Co. Ltd. Product no.: L 9634  
1.00 % (w/v solution) Laminarin solution (substrate solution 0.1M sodium acetate buffer, pH 5.0)  
1.75 ml laminarin solution is mixed with 0.25 ml diluted enzyme solution at 50 °C for 10 minutes and the reaction stopped by addition of 2 ml DNS solution.

[0150] Standard curve was made using 0, 0.125, 0.25, 0.5 and 0.75 mg/ml glucose solution.

30 [0151] Optical density was measured at 540 nm ( $OD_{540nm}$ ).

### Calculation

[0152] The activity is calculated as follows:

35

$$\text{Activity (u.ml}^{-1} \text{ or u.g}^{-1}) = \frac{T - c}{m} \times A \times \frac{1}{180.16} \times 10^3 \times \frac{1}{V} \times \frac{1}{t} \times D$$

40 where:

$T = \Delta OD_{540nm} \text{ TEST}$

$= OD_{540nm} \text{ TEST} - OD_{540nm} \text{ BLANK}$

$m$  = gradient of the standard curve (approximately 1.0)

45  $c$  = y axis intercept of the standard curve (always negative and approximately -0.03)

180.16 = molecular weight of glucose

$10^3$  = to convert to μmoles

$A$  = assay volume in ml

$V$  = enzyme volume in ml

50  $t$  = assay time in minutes

$D$  = enzyme dilution factor (e.g. for 1g diluted to 1 litre  $D = 1000$ )

## Arabinase assay.

### 55 Principle

[0153] The assay of Arabinase activity is based on colorimetrically determination by measuring the resulting increase in reducing groups using a 3,5-dinitrosalicylic acid reagent. Enzyme activity was calculated from the relationship between

the concentration of reducing groups, as arabinose equivalents, and absorbance at 540nm.

[0154] The assay was carried out at pH 3.5, but it can be performed at different pH values for the additional characterisation and specification of enzymes.

## Unit definition

[0155] One unit of arabinase (Arabinanase (endo-1,5- $\alpha$ -L-arabinanase)) activity is defined as the amount of enzyme which produces 1  $\mu$ mole arabinose equivalents per minute under the conditions of the assay (pH 3.5 (or as specified) and 50 °C).

## Materials

### [0156]

Megazyme Sugar Beet Arabinan

Arabinose Sigma A3131 M.W.: 150.1

Sodium acetate *anhydrous* 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10236. M.W.: 82.03

Acetic acid ("*glacial*") 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10001. M.W.: 60.05 3,5-Dinitrosalicylic acid

GPR (3,5-dinitro-2-hydroxybenzoic acid). Supplier: Merck Ltd (BDH). Product no.: 28235

Sodium hydroxide *pellets* 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10252. M.W.: 40.00

Potassium sodium (+)-tartrate 'AnalaR'. Supplier: Merck Ltd (BDH). Product no.: 10219. M.W.: 282.22

1.5 % (w/v solution) Arabinan solution in 0.1M sodium acetate buffer, pH 3.5 (substrate solution).

3,5-Dinitrosalicylic acid (DNS) solution. 20g/L of DNS in buffer containing 32g/L sodium hydroxide pellets, and 600 g/L potassium sodium (+)-tartrate.

Arabinase standard solution (0.50 mg/ml)

## Procedure

[0157] The enzyme composition was diluted into samples and a glucose standard curve was made using arabinase concentrations of 0, 0.125, 0.25, 0.375, and 0.5 mg/ml.

[0158] 0.25 ml of enzyme solution was mixed with 1.75 ml of the substrate solution (1.5% w/v) at 50 °C and the reaction was stopped after 10 min by addition of DNS solution. Followed by heating to 95 °C for 5 minutes.

[0159] The optical density was measured at 540 nm ( $OD_{540nm}$ ) of the different samples.

## Calculation

[0160] The enzyme activity is determined from the standard curve.

[0161] The activity is calculated as follows:

$$\text{Activity (u.ml}^{-1} \text{ or u.g}^{-1}) = \frac{T - c}{m} \times A \times \frac{1}{150.13} \times 10^3 \times \frac{1}{V} \times \frac{1}{t} \times D$$

where:

$T = \Delta OD_{540nm} \text{ TEST}$

$= OD_{540nm} \text{ TEST} - OD_{540nm} \text{ BLANK}$

$m$  = gradient of the standard curve (approximately 1.0)

$c$  = y axis intercept of the standard curve (always negative and approximately -0.02)

150.13  $\equiv$  molecular weight of arabinase

$10^3 \equiv$  to convert to  $\mu$ moles

$A \equiv$  assay volume in ml

$V \equiv$  enzymes volume in ml

$t \equiv$  assay time in minutes

$D$  = actual enzyme dilution factor (e.g. for 1.000g diluted to 1 litre  $D = 1000$ )

**Arabinofuranosidase assay.**

**[0162]** The reaction, catalysed by  $\alpha$ -N-arabinofuranosidase, involves the hydrolysis of the terminal bond, at the non-reducing  $\alpha$ -L-arabinofuranoside residue, of  $\alpha$ -L-arabinosides. The enzyme acts on  $\alpha$ -L-arabinofuranosides,  $\alpha$ -L-arabinans containing (1,3)- and/or (1,5)-linkages, arabinoxylans and arabinogalactans.

**[0163]** The assay of  $\alpha$ -N-arabinofuranosidase is based upon the enzymatic hydrolysis of p-nitrophenyl  $\alpha$ -L-arabinofuranoside. The assay is a "two-point", rather than a "continuous monitoring", method. The calculation of enzyme activity is based on measurements taken only at the beginning and end of the incubation period. A product of the reaction, p-nitrophenol is determined colourimetrically (after pH adjustment). Enzyme activity is calculated from the relationship between the concentration of p-nitrophenol and absorbance at 400nm.

Preparation of diluted enzyme solution:

**[0164]** Prepare all enzyme solutions, from powder or liquid enzyme preparations, with glass distilled water. Minimise assay dilution errors by avoiding large dilution steps involving small volumes or weights. In making enzyme dilutions it is more accurate, even for a liquid sample, to weigh out the initial enzyme sample. If this is done, in the case of liquid samples it is therefore necessary to measure the specific gravity of the liquid at 20 °C

**[0165]** As the assay is a "two-point", rather than a "continuous monitoring", method it is important to ensure the linearity within the incubation period with different enzyme systems and conditions. Under the standard assay conditions of substrate concentration, pH, temperature and assay time the assay has been demonstrated to be linear in the range  $\Delta OD_{540nm}$  TEST (T) = 0.20 - 1.50. However, for good practice, the assay is operated within a defined range of  $\Delta OD_{540nm}$  TEST (T) = 0.400 - 0.800.

Procedure

**[0166]** Each enzyme sample assay involves three analyses: duplicate test (TEST) analyses and a blank (BLANK) analysis. The procedure given describes the analysis of a single enzyme sample.

	TEST	BLANK
0.2M Sodium acetate buffer, pH 5.0	1.00 ml	1.00 ml
Glass distilled water	1.00 ml	1.00 ml
p-Nitrophenyl- $\alpha$ -L-arabinofuranoside solution	1.00 ml	1.00 ml

**[0167]** 0.25 ml diluted enzyme solution was added to the solutions at 50 °C, the reaction was stopped after 10 minutes by addition of 4 ml of 0.4M glycine solution, pH 10.8 (stop reagent).

**[0168]** Absorbance was measured at 400 nm at 25 °C against a water blank.

- determine  $OD_{400nm}$  TEST for the duplicate TESTS measured;
- determine  $OD_{400nm}$  BLANK.

Calculation

**[0169]**

$$\Delta OD_{400nm} \text{ TEST (T)} = OD_{400nm} \text{ TEST} - OD_{400nm} \text{ BLANK}$$

$$\text{Units } (\mu\text{mol} \cdot \text{min}^{-1}) = \frac{T}{18300} \times \frac{V}{1000} \times 10^6 \times \frac{1}{t}$$

$$\text{Activity } (\text{u} \cdot \text{ml}^{-1} \text{ or } \text{u} \cdot \text{g}^{-1}) = \text{Units} \times \frac{1}{E} \times D$$

where: T =  $OD_{400nm}$  TEST -  $OD_{400nm}$  BLANK



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18300 = Molar extinction coefficient for p-nitrophenol (1 cm path length)

V = 7.25 (total liquid volume in test in ml)

t = 10 (minutes)

1 u = 1  $\mu\text{mol}\cdot\text{min}^{-1}$

E = 0.25 (volume of diluted enzyme sample in ml)

D = Enzyme dilution factor e.g. for 1 ml diluted to 1 litre D = 1000

### Cellobiohydrolase assay.

#### Principle

**[0170]** The reaction, catalysed by cellobiohydrolase, involves the hydrolysis of 1,4- $\beta$ -D-glucosidic linkages in cellulose and cellotetraose, releasing cellobiose from the non-reducing ends of the chains.

**[0171]** The assay of cellobiohydrolase is based on the enzymatic hydrolysis of p-nitrophenyl (3-D-cellobiopyranoside). The product of the reaction, p-nitrophenol is determined colorimetrically (after pH adjustment). Enzyme activity is calculated from the relationship between the concentration of p-nitrophenol and absorbance at 400nm.

**[0172]** The assay is operated within the linear defined range of  $\Delta\text{OD}_{540\text{nm}}$  **TEST (T)** = 0.400 - 0.800.

#### Procedure

**[0173]** Each enzyme sample assay involves three analyses: duplicate test (**TEST**) analyses and a blank (**BLANK**) analysis. The procedure given describes the analysis of a single enzyme sample.

	TEST	BLANK
0.2M Sodium acetate buffer, pH 5.0	1.00 ml	1.00 ml
Glass distilled water	1.00 ml	1.00 ml
p-Nitrophenyl $\beta$ -D-cellobiopyranoside solution	1.00 ml	1.00 ml

**[0174]** 0.25 ml diluted enzyme solution was added to the test solution at 50 °C, after 30 minutes 4 ml of 0.4M glycine solution, pH 10.8 (stop reagent) was added to each tube.

**[0175]** Absorbance was measured at 20°C at 400 nm in a 1cm glass cuvette against a water blank.

- determine  $\text{OD}_{400\text{nm}}$  **TEST** for the duplicate **TESTS** measured;
- determine  $\text{OD}_{400\text{nm}}$  **BLANK**.

#### Calculation

**[0176]**

$$\Delta\text{OD}_{400\text{nm}} \text{TEST (T)} = \text{OD}_{400\text{nm}} \text{TEST} - \text{OD}_{400\text{nm}} \text{BLANK}$$

$$\text{Units } (\mu\text{mol}\cdot\text{min}^{-1}) = \frac{T}{18300} \times \frac{V}{1000} \times 10^6 \times \frac{1}{t}$$

$$\text{Activity (u.ml}^{-1} \text{ or u.g}^{-1}) = \text{Units} \times \frac{1}{E} \times D$$

where: T =  $\text{OD}_{400\text{nm}} \text{TEST} - \text{OD}_{400\text{nm}} \text{BLANK}$

18300 = Molar extinction coefficient for p-nitrophenol (1 cm path length)

V = 7.25 (total liquid volume in test in ml)

1000 = to convert to litres

$10^6$  = to convert to  $\mu\text{moles}$

t = 30 (minutes)

1 u = 1  $\mu\text{mol}\cdot\text{min}^{-1}$

E = 0.25 (volume of diluted enzyme sample in ml)

D = Enzyme dilution factor e.g. for 1 ml diluted to 1 litre D = 1000)

5 [0177] The present disclosure also relates to the following numbered paragraphs:

1. An enzyme exhibiting endo-1,4- $\beta$ -xylanase activity, which enzyme comprises an amino acid sequence having at least 80% identity with any one selected from SEQ ID NO:1, SEQ ID NO:2, SEQ ID NO:3, SEQ ID NO:4, SEQ ID NO:5, SEQ ID NO:6, SEQ ID NO:17, and SEQ ID NO:18, or any functional fragment thereof.
2. The enzyme according to paragraph 1, which enzyme has a ratio in activity on soluble arabinoxylan substrate (WE-AX) to insoluble arabinoxylan substrate (WU-AX) arabinoxylan substrate of less than about 7.0, such as less than about 6.5, such as less than about 6.0, such as less than about 5.5, such as less than about 5.0, such as less than about 4.5.
3. An enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity, which enzyme comprises an amino acid sequence having at least 80% identity with any one selected from SEQ ID NO:7, SEQ ID NO:8, SEQ ID NO:9, SEQ ID NO:10, and SEQ ID NO:11, SEQ ID NO:12, SEQ ID NO:13, SEQ ID NO:14, SEQ ID NO:15, SEQ ID NO:16, or any functional fragment thereof.
4. The enzyme according to any one of paragraph 1-3, which enzyme has a temperature optimum in the range of 40-70 °C, such as in the range of 45-65 °C, such as in the range of 50-65 °C, such as in the range of 55-65 °C.
5. The enzyme according to any one of paragraphs 1-4, wherein said enzyme has at least 81, 82, 83, 84, 85, 86, 87, 88, 89, 90, 91, 92, 93, 94, 95, 96, 97, 98 or 99% identity with any one amino acid sequence selected from SEQ ID NO: 1-18, or any functional fragment thereof.
6. The enzyme according to any one of paragraphs 1-5 having a total number of amino acids of less than 350, such as less than 340, such as less than 330, such as less than 320, such as less than 310, such as less than 300 amino acids, such as in the range of 200 to 350, such as in the range of 220 to 345 amino acids.
7. The enzyme according to any one of paragraphs 1-6, wherein the amino acid sequence of said enzyme has at least one, two, three, four, five, six, seven, eight, nine or ten amino acid substitutions as compared to any one amino acid sequence selected from SEQ ID NO: 1-18, or any functional fragment thereof.
8. The enzyme according to any one of paragraphs 1-7, wherein the amino acid sequence of said enzyme has a maximum of one, two, three, four, five, six, seven, eight, nine or ten amino acid substitutions compared to any one amino acid sequence selected from SEQ ID NO: 1-18, or any functional fragment thereof.
9. The enzyme according to any one of paragraphs 1-8, which enzyme comprises the amino acid sequence identified by any one of SEQ ID NO: 1-18, or any functional fragment thereof.
10. The enzyme according to any one of paragraphs 1 or 3, which enzyme consists of the amino acid sequence identified by any one of SEQ ID NO: 1-18, or any functional fragment thereof.
11. A DNA construct comprising a DNA sequence encoding an enzyme according to any of paragraphs 1-10.
12. A recombinant expression vector comprising a DNA construct according to paragraph 11.
13. A cell that has been transformed with a DNA construct of paragraph 11 or the vector of paragraph 12.
14. A preparation comprising an enzyme according to any one of paragraphs 1-10, or a DNA construct according to paragraph 11, or a vector according to paragraph 12, or a cell according to paragraph 13.
15. A composition comprising an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to any one of paragraphs 1, 2, 4-10 in combination with any one or more  $\beta$ -glucanase.
16. The composition according to paragraph 15, wherein said one or more  $\beta$ -glucanase is an enzyme exhibiting

endo-1,3(4)- $\beta$ -glucanase activity according to any one of paragraphs 3-10.

17. A composition comprising an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity according to any one of paragraphs 3-10 in combination with any one or more xylanase.

18. The composition according to paragraph 17, wherein said one or more xylanase is an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity according to any one of paragraphs 1, 2, 4-10.

19. The composition according to any one of paragraphs 15-18, wherein said endo-1,3(4)- $\beta$ -glucanase activity and said endo-1,4- $\beta$ -xylanase activity are derived from at least two different enzymes, such as at least two different enzymes from two different species.

20. The composition according to any one of paragraphs 15-19, comprising a combination of at least two enzymes, said two enzymes, or two enzymes with an amino acid sequence having at least 80% sequence identity with the respective SEQ ID, or any functional fragment thereof, being selected from the list consisting of

SEQ ID NO:1 and SEQ ID NO:7;  
 SEQ ID NO:2 and SEQ ID NO:7;  
 SEQ ID NO:3 and SEQ ID NO:7;  
 SEQ ID NO:4 and SEQ ID NO:7;  
 SEQ ID NO:5 and SEQ ID NO:7;  
 SEQ ID NO:6 and SEQ ID NO:7;  
 SEQ ID NO:17 and SEQ ID NO:7;  
 SEQ ID NO:18 and SEQ ID NO:7;  
 SEQ ID NO:1 and SEQ ID NO:8;  
 SEQ ID NO:2 and SEQ ID NO:8;  
 SEQ ID NO:3 and SEQ ID NO:8;  
 SEQ ID NO:4 and SEQ ID NO:8;  
 SEQ ID NO:5 and SEQ ID NO:8;  
 SEQ ID NO:6 and SEQ ID NO:8;  
 SEQ ID NO:17 and SEQ ID NO:8;  
 SEQ ID NO:18 and SEQ ID NO:8;  
 SEQ ID NO:1 and SEQ ID NO:9;  
 SEQ ID NO:2 and SEQ ID NO:9;  
 SEQ ID NO:3 and SEQ ID NO:9;  
 SEQ ID NO:4 and SEQ ID NO:9;  
 SEQ ID NO:5 and SEQ ID NO:9;  
 SEQ ID NO:6 and SEQ ID NO:9;  
 SEQ ID NO:17 and SEQ ID NO:9;  
 SEQ ID NO:18 and SEQ ID NO:9;  
 SEQ ID NO:1 and SEQ ID NO:10;  
 SEQ ID NO:2 and SEQ ID NO:10;  
 SEQ ID NO:3 and SEQ ID NO:10;  
 SEQ ID NO:4 and SEQ ID NO:10;  
 SEQ ID NO:5 and SEQ ID NO:10;  
 SEQ ID NO:6 and SEQ ID NO:10;  
 SEQ ID NO:17 and SEQ ID NO:10;  
 SEQ ID NO:18 and SEQ ID NO:10;  
 SEQ ID NO:1 and SEQ ID NO:11;  
 SEQ ID NO:2 and SEQ ID NO:11;  
 SEQ ID NO:3 and SEQ ID NO:11;  
 SEQ ID NO:4 and SEQ ID NO:11;  
 SEQ ID NO:5 and SEQ ID NO:11;  
 SEQ ID NO:6 and SEQ ID NO:11;  
 SEQ ID NO:17 and SEQ ID NO:11;  
 SEQ ID NO:18 and SEQ ID NO:11;  
 SEQ ID NO:1 and SEQ ID NO:12;  
 SEQ ID NO:2 and SEQ ID NO:12;

SEQ ID NO:3 and SEQ ID NO:12;  
 SEQ ID NO:4 and SEQ ID NO:12;  
 SEQ ID NO:5 and SEQ ID NO:12;  
 SEQ ID NO:6 and SEQ ID NO:12;  
 SEQ ID NO:17 and SEQ ID NO:12;  
 SEQ ID NO:18 and SEQ ID NO:12;  
 SEQ ID NO:1 and SEQ ID NO:13;  
 SEQ ID NO:2 and SEQ ID NO:13;  
 SEQ ID NO:3 and SEQ ID NO:13;  
 SEQ ID NO:4 and SEQ ID NO:13;  
 SEQ ID NO:5 and SEQ ID NO:13;  
 SEQ ID NO:6 and SEQ ID NO:13;  
 SEQ ID NO:17 and SEQ ID NO:13;  
 SEQ ID NO:18 and SEQ ID NO:13;  
 SEQ ID NO:1 and SEQ ID NO:14;  
 SEQ ID NO:2 and SEQ ID NO:14;  
 SEQ ID NO:3 and SEQ ID NO:14;  
 SEQ ID NO:4 and SEQ ID NO:14;  
 SEQ ID NO:5 and SEQ ID NO:14;  
 SEQ ID NO:6 and SEQ ID NO:14;  
 SEQ ID NO:17 and SEQ ID NO:14;  
 SEQ ID NO:18 and SEQ ID NO:14;  
 SEQ ID NO:1 and SEQ ID NO:15;  
 SEQ ID NO:2 and SEQ ID NO:15;  
 SEQ ID NO:3 and SEQ ID NO:15;  
 SEQ ID NO:4 and SEQ ID NO:15;  
 SEQ ID NO:5 and SEQ ID NO:15;  
 SEQ ID NO:6 and SEQ ID NO:15;  
 SEQ ID NO:17 and SEQ ID NO:15;  
 SEQ ID NO:18 and SEQ ID NO:15;  
 SEQ ID NO:1 and SEQ ID NO:16;  
 SEQ ID NO:2 and SEQ ID NO:16;  
 SEQ ID NO:3 and SEQ ID NO:16;  
 SEQ ID NO:4 and SEQ ID NO:16;  
 SEQ ID NO:5 and SEQ ID NO:16;  
 SEQ ID NO:6 and SEQ ID NO:16;  
 SEQ ID NO:17 and SEQ ID NO:16; and  
 SEQ ID NO:18 and SEQ ID NO:16.

21. The composition according to any one of paragraphs 15-20, wherein when used prior to the lautering in a brewing application the total pressure built up is reduced to a value of less than 470 mm WC, such as less than 450 mm WC, such as less than 430 mm WC, such as less than 410 mm WC, such as less than 390 mm WC, such as less than 370 mm WC, such as less than 350 mm WC, such as less than 330 mm WC, such as less than 310 mm WC, such as less than 300 mm WC, such as less than 290 mm WC.

22. The composition according to any one of paragraphs 15-21, wherein when used prior to the lautering in a brewing application the total pressure built up is reduced by at least 5, 7, 9, 11, 13, 15, 17, 19, 21, 23, 25, 27, 29, 31, 33, 35, 37, 39, 41, 43, 45, 47, 49, 51, 53, 55, 57, 59, 61, 63, 65, 67, 69, 71, 73, 75, 77, 79, 81, 83, 85, 87, 89, 91, 93 or 95 % compared to the use of a negative control without said composition.

23. The composition according to any one of paragraphs 15-22, wherein when used in a brewing application prior to the wort separation, the wort filterability as measured by volume wort collected after 5 min of filtration relative to a control without enzymes is increased to above 1.5, such as above 1.6, such as above 1.7, such as above 1.8, such as above 1.9, such as above 2.0, such as above 2.1, such as above 2.2, such as above 2.3, such as above 2.4, such as above 2.5.

24. The composition according to any one of paragraphs 15-23, when used in a brewing application prior to the wort separation, the wort filterability as measured by volume wort collected after 5 min of filtration is increased by at least

5, 7, 9, 11, 13, 15, 17, 19, 21, 23, 25, 27, 29, 31, 33, 35, 37, 39, 41, 43, 45, 47, 49, 51, 53, 55, 57, 59, 61, 63, 65, 67, 69, 71, 73, 75, 77, 79, 81, 83, 85, 87, 89, 91, 93, 95, 97, 99, 110, 120, 130, 140, 150, 160, 170, 180, 190, 200, 210, 220, 230, 240, 250, 260, 270, 280, 290, or 300 % as compared to the use of a negative control without said composition.

25. The composition according to any one of paragraphs 15-24, comprising any one or more further enzyme.

26. The composition according to paragraph 25, wherein said one or more further enzyme is selected from list consisting of a xylanase classified in EC 3.2.1.32, EC 3.2.1.136, or EC 3.2.1.156, a cellulase, a laminarinase, an endo-1,5- $\alpha$ -L-arabinanase, a beta-D-glucoside glucohydrolase, a  $\beta$ -Xylosidase, a cellobiohydrolase, a glucan 1,4-beta-glucosidase, a xyloglucan-specific exo-beta-1,4-glucanase and an  $\alpha$ -N-Arabinofuranosidase.

27. Use of an enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26 in the production of a food, feed, or malt beverage product.

28. Use of an enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26, in the production of dough or baked products.

29. Use of an enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26, in the preparation of pulp or paper.

30. Use of an enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26, for the preparation of cereal components.

31. The use according to paragraph 29, in which the cereal is rye, wheat, or barley.

32. Use of enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26, in the production of beer or modification of by-products from a brewing process.

33. Use of enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26, in the production of wine or juice.

34. Use of enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26, in the production of a first - or second-generation biofuel, such as bioethanol .

35. Method of altering filterability of a starch comprising material, said method comprising the step of treating said starch comprising material with enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26.

36. Method of reducing pressure built up during lautering in a brewing application, said method comprising the step of treating a brewing mash with enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26.

37. Method for the production of a food, feed, or beverage product, such as an alcoholic or non-alcoholic beverage, such as a cereal- or malt-based beverage like beer or whiskey, said method comprising the step of treating a starch comprising material with enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26.

38. Method for the production of a brewing mash, said method comprising the step of treating a starch comprising material with enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26.

39. Method for the production of a first - or second-generation biofuel, such as bioethanol, said method comprising the step of treating a starch comprising material with an enzyme according to paragraphs 1-10, or a preparation according to paragraph 14, or a composition according to any one of paragraphs 15-26.

40. Product obtained by the method according to any one of paragraphs 38-39.

41. A composition comprising the product according to paragraph 40, such as wherein the product is in a range of 0.1%-99.9%.

## EXAMPLES

### Example 1

**[0178]** Methods and results in relation to xylanases/glucanase filing for brew application.

**[0179]** The below methods have been used to screen for xylanases and glucanases with application in brewing:

Methods:

#### Water extractable arabinoxylan (WE-AX) xylanase method:

**[0180]** Samples, to obtain approx. OD540 = 0.25 - 0.30 in this assay and xylose standards (0, 0.125, 0.250, 0.375 and 0.500 mg/ml distilled water) are prepared in distilled water. At time t=0 minutes, 1.75 ml soluble wheat arabinoxylan (0.5% wheat arabinoxylan (PWAXYH, Megazyme, Bray, Ireland)) in 0.1M sodium acetate/acetic acid, pH 5) is placed in a test tube at 50°C. At time t=5 minutes, 250µl enzyme solution is added to the substrate at 50°C followed by mixing. Distilled water is used as blank. At time t=15 minutes, 2ml DNS solution (1% 3,5-Dinitrosalicylic acid (DNS), 1.6% sodium hydroxide, 30% potassium sodium tartrate in distilled water) is added to the enzyme-substrate solution and 2.0 ml standard solution. Samples, blanks and standards added DNS are placed in a boiling water bath (95°C) for 5 minutes. Hereafter samples, blanks and standards are cooled by placing them in a 25°C water bath for 20 minutes. The Optical density of all samples are read at OD540 using a spectrophotometer. Based on the dilution of the samples, the amount of sample taking into work and the standards, the xylanases activity of the sample can be calculated.

**[0181]** One Unit of endo-1,4-beta-xylanase WE-AX activity is defined as the amount of enzyme which produces 1 µmole xylose equivalents per minute under the conditions mentioned above (Water extractable arabinoxylan (WE-AX) xylanase method).

#### Water un-extractable arabinoxylan (WU-AX) xylanase method:

**[0182]** Samples are prepared in distilled water. At time t=0 minutes, 1.75 ml Insoluble wheat (0.5% wheat arabinoxylan (PWAXYI, Megazyme, Bray, Ireland)) in 0.1M sodium acetate/acetic acid, pH 5) is placed in a test tube at 50°C. At time t=5 minutes, 250µl enzyme solution is added to the substrate at 50°C followed by mixing. Distilled water is used as blank. At time t=15 minutes, samples and blanks are placed in a boiling water bath (95°C) for 5 minutes.

**[0183]** Hereafter samples and blanks are centrifuged to precipitate residual insoluble substrate. The amount of arabinoxylan brought into solution is determined using the method described by Rouau, X. and Surget, A. (1994), Carbohydrate Polymers, 24, 123-132.

**[0184]** WU-AX endo-1,4-beta-xylanase activity is defined as the amount of pentoses solubilised (µg pentoses) under the conditions described above giving a unit definition of µg pentose/gram of xylanase sample.

#### Xylanase activity assay

**[0185]** Samples, to obtain approx. OD540 = 0.25 - 0.30 in this assay and xylose standards (0, 0.125, 0.250, 0.375 and 0.500 mg/ml distilled water) are prepared in distilled water. At time t=0 minutes, 1.75 ml soluble wheat arabinoxylan (0.5% wheat arabinoxylan (PWAXYH, Megazyme, Bray, Ireland)) in 0.1M sodium acetate/acetic acid, pH 5) is placed in a test tube at 50°C. At time t=5 minutes, 250µl enzyme solution is added to the substrate at 50°C followed by mixing. Distilled water is used as blank. At time t=15 minutes, 2ml DNS solution (1% 3,5-Dinitrosalicylic acid (DNS), 1.6% sodium hydroxide, 30% potassium sodium tartrate in distilled water) is added to the enzyme-substrate solution and 2.0 ml standard solution. Samples, blanks and standards added DNS are placed in a boiling water bath (95°C) for 5 minutes. Hereafter samples, blanks and standards are cooled by placing them in a 25°C water bath for 20 minutes. The Optical density of all samples are read at OD540 using a spectrophotometer. Based on the dilution of the samples, the amount of sample taking into work and the standards, the xylanases activity of the sample can be calculated.

**[0186]** One Unit of endo-1,4-beta-xylanase WE-AX activity is defined as the amount of enzyme which produces 1 µmole xylose equivalents per minute under the conditions mentioned above

Glucanase activity assay

**[0187]** Samples, to obtain OD<sub>540</sub> within the standard curve in this assay and glucose standards (0; 0.125; 0.250; 0.500; and 0.750 mg/ml distilled water) are prepared in distilled water. At time t=0 minutes, 1,75 ml barley beta-glucan (1.5% barley beta-glucan (P-BGBM, Megazyme, Bray, Ireland)) in 1M sodium acetate/acetic acid, pH 5) is placed in a test tube at 50°C. At time t=5 minutes, 250 µl enzyme solution is added to the substrate at 50°C followed by mixing. Distilled water is used as blank. At time t=15 minutes, 2ml DNS solution (1% 3,5-Dinitrosalicylic acid (DNS), 1,6% sodium hydroxide, 30% potassium sodium tartrate in distilled water) is added to the enzyme-substrate solution and 2.0 ml standard solution. Samples, blanks and standards added DNS are placed in a boiling water bath (95°C) for 15 minutes. Hereafter samples, blanks and standards are cooled by placing them in a 25°C water bath for 20 minutes. The Optical density of all samples are read at OD<sub>540</sub> using a spectrophotometer. Based on the dilution of the samples, the amount of sample taking into work and the standards, the glucanase activity of the sample can be calculated.

**[0188]** One unit of endo-1,3(4)-β-glucanase activity is defined as the amount of enzyme which produces 1 µmole glucose equivalents per minute under the conditions of the assay (pH 5.0 (or as specified) and 50 °C).

Lab scale brewing application method:

**[0189]** Lab scale brewing application studies were conducted using Pilsner malt:Barley in a 75:25 ratio at a water:grist ratio of 3:1 (150ml:50g grist). Initially water was preheated to 53 °C before mashing in and pH adjustment (5.4, 2 M H<sub>2</sub>SO<sub>4</sub>). After regaining initial temperature (10 min period) the mashing profile (see figur 1) is initiated and enzymes are added. After mashing off wort separation is conducted using a conventional plastic funnel and filter paper (paper filter No 1, 24 cm diameter, Whatman, England ). Filtration performance was evaluated as well as several other wort parameters, such as i.e. viscosity, β-glucan and pentosan.

**[0190]** Wort filtration was measured for 30 min after which filtration was terminated. Collected wort was cooled before any further analysis.

Filtration

**[0191]** Filtration data are presented as volume wort collected after 5, 10, 15 and 30 minutes relative to a blank (brewing without added exogenous enzymes).

Pilot scale brewing

**[0192]** Trials were conducted in a pilot scale brewing facility (2 HL capacity). Wort separation was conducted by lautering and beer filtration by horizontal kiselguhr filtration.

**[0193]** To elucidate filtration optimization by combination of glucanase and xylanase under "challenging" brewing conditions, pilot scale brewing trials were conducted using a mixed grist comprising of 75 % malt and 25 % barley. Initially, the water:grist ratio was set at 2.8:1 (mash start) increasing to 3.1:1 at the start of lautering. In comparison water:grist ratios around 3.2-3.8 are typical in full scale brew house lautering. Thus the current pilot trial settings of a 3.1:1 water:grist ratio are believed to be in the challenging end of the scale.

**[0194]** Malt and barley was ground dry using a two-roller mill. Both barley and malt was milled twice using a roller distance of ~0.7 mm.

**[0195]** Mashing-in was conducted aiming at an initial mash temperature of 53 °C. After mashing-in small adjustments were conducted such as: mash volume adjustment for water:grist ratio of 2.8:1 and pH adjustment to ~5.56 (Lactic acid). After fine tuning the mash, enzyme was added and the mashing profile given in figure 1 was followed. Saccharification rest at 70 °C was programmed to 15 min, however rest period was extended by 5 min until an iodine test showed that no starch was present. (Ludwig Narziss and Werner Back, Technische Universitaet Muenchen (Fakultaet fuer Brauwesen, Weihenstephan), Abriss der Bierbrauerei. WILEY-VCH Verlags GmbH Weinheim Germany, 2005).

**[0196]** Mashing-off was initiated after a 5 min rest at 78 °C. Mash was transferred to the Lauter Tun, which was beforehand prefilled with water to a height just below the "false bottom". The mash was left to rest for 5 min for settling of filter cake. This was followed by a 15 min recirculation (140 L/h) ensuring filter cake settling and wort clarification. Typically in full scale brewing, filtration will be initiated when a given wort turbidity is obtained, however in the current trials recirculation was kept constant at 15 min enabling comparison of trials. During lautering the following data were collected, including time (min), wort volume collected (L), filtration pressure difference across filter cake (mmWC, mm Water Column), pump capacity (%), wort turbidity (EBC) and mash temperature (°C).

**[0197]** The pressure build up across the filter cake during filtration is believed to be a factor contributing to setting the standard of the wort lautering performance. Reaching very high pressure differences - e.g. 250 mmWC during first wort collection and e.g. 450 mmWC for the remainder of the lautering - a filter cake racking (also known as deep cut) is induced.

Racking is a process where a filter cake collapses or a filtration channel formation is relieved by slowing cutting the filter cake with special designed knives. Following filter cake racking a 6 min wort recirculation (flow rate: 120 l/h) was introduced priming the filter cake for continued filtration. Filter cake racking relieves an otherwise compromised filtration performance which would otherwise also result in poor wort quality. If no pressure induced racking has been introduced by the beginning of the 3rd sparging, automatic rackings were conducted at the beginning of the 3rd and 4th spargings to ensure that no full filtration block would occur just before finishing wort separation.

**[0198]** Lautering was conducted with the settings illustrated in table 1.

Table 1. Lautering settings. Volumes collected (L), filtration flow (L/h) and Sparging volumes (L).

Wort	Volume collected, L	Filtration flow, L/h	Sparging volume, L
First wort	0 - 60	130	
1 st sparging	60 - 78	140	18
2nd sparging	78 - 96	160	18
3rd sparging	96 - 114	180	18
4th sparging	114 - 140	180	26

**[0199]** After end lautering, sweet wort was returned to the Mash Tun, heated to boiling and hops were added. Hopping was continued for 80 min and at the end of hopping pH is adjusting to  $5.10 \pm 0.05$ . Hops were cleared from the bitter wort by use of whirlpool and following wort was cooled to  $\sim 8^\circ\text{C}$ . For fermentation, a bottom fermenting dried yeast (*Saccharomyces cerevisiae*) W34/70 from Fermentis was chosen. Yeast was rehydrated for 30 min and pitched at 100 g/HL. Main fermentation was hold for 5-6 days at  $10^\circ\text{C}$ , followed by maturation at  $15^\circ\text{C}$  until attenuated and Diacetyl below 80 ppb. Beer was stored for another 2-3 weeks at  $1^\circ\text{C}$  and 0.7 bar before filtering.

**[0200]** Beer was filtered horizontally by use of  $1.2\ \mu\text{m}$  PP-candle plates and kieselguhr. Up to 8 plates could be included in the filtration unit, resulting in a total filtration area of  $\sim 0.5\ \text{m}^2$ . In the current studies 3 plates were included and filtration was conducted at a flow rate of 130 L/h, resulting in a speed of filtration of  $6.9\ \text{HL}/(\text{h}\cdot\text{m}^2)$ . In full scale breweries, speed of filtration is usually set between  $5\text{--}7\ \text{HL}/(\text{h}\cdot\text{m}^2)$ . It is thus obvious that the current settings are in the high end - a deliberate choice challenging the beer filtration conditions to verify potential benefits from the choice of using an enzyme in the brewing process. During beer filtration, flow rates (L/h) as well as pressure values (P-in and P-out) were monitored to verify beer filtration performance. Also a number of beer analyses, such as Original Gravity (OG), Apparent Extract (AE), Alcohol By Volume (ABV), Apparent Degree of Fermentation (ADF), Reel Degree of Fermentation (RDF), pH, colour and bitterness were conducted for evaluation of beer quality.

Results:

Xylanases:

**[0201]** Xylanases were screened for their activity on soluble substrate and insoluble substrate, their pH and temperature characteristics.

**[0202]** Results are shown in table 2.

Table 2. Xylanases screened, their activity on soluble (WE-AX) and insoluble (WU-AX) arabinoxylan substrate and their biochemical characteristics in regard to temp and pH.

Name	Origin	GH	WE-AX	WU-AX	WU-AX/WE-AX	Temp opt, $^\circ\text{C}$	T $\frac{1}{2}$ temp, $^\circ\text{C}$	pH opt.
<b>AfuXyn2</b>	<i>Aspergillus fumigatus</i>	11	7798	68790526	8822	65	59	5.5
<b>AfuXyn3</b>	<i>Aspergillus fumigatus</i>	11	26283	99716865	3794	60	62	5
<b>AfuXyn5</b>	<i>Aspergillus fumigatus</i>	11	90005	714363158	7937	60	50	4



(continued)

Name	Origin	GH	WE-AX	WU-AX	WU-AX/WE-AX	Temp opt, °C	T½ temp, °C	pH opt.
<b>BsuXyn3</b>	<i>Bacillus subtilis</i> , BS3	11	82	1095357	13388	50	<i>n. d.</i>	6
<b>BsuXyn4</b>	<i>subtilis</i> , BS4 #160	11	54	1005400	18619	50	<i>n. d.</i>	6
<b>TerXyn1</b>	<i>Geosmithia emersonii</i>	10	1467	6208786	4232	78	>78	3
<b>AtuXyn3</b>	<i>Aspergillus tubigensis</i>	10	1220	7760982	6361	65	67	4.5
<b>AtuXyn4</b>	<i>Aspergillus tubigensis</i>	11	1600	12934971	8084	45	58	5
<b>AacXyn2</b>	<i>Aspergillus aculeatus</i>	10	777	3880491	4994	70	73	4
<b>TreXyn2</b>	<i>Trichoderma reesei</i>	11	2244	16015846	7137	55	<i>n. d.</i>	5
<b>TreXyn3</b>	<i>Trichoderma reesei</i>	10	21487	141108772	6567	60	64	5.5
<b>TreXyn5</b>	<i>Trichoderma reesei</i>	11	1410	8842816	6272	70	68	5
<i>n.d.</i> = Not determined								

**[0203]** WE-AX and WU-AX enzyme activities (U) were measured as described in sections "water extractable arabinoxylan (WE-AX) xylanase method" and "water un-extractable arabinoxylan (WU-AX) xylanase method".

**[0204]** Based on the results from the biochemical screening, xylanases having an appropriate activity ratio on soluble vs. insoluble arabinoxylan were chosen for further testing in application trials. The results are shown in table 3.

Table 3. Xylanases screened and the relative extract yield obtained using the xylanases versus a blank (without xylanases). Finally the xylanases substrate specificity is illustrated as a ration of their activity on insoluble vs. soluble arabinoxylan (WU-AX/WE-AX).

Name	Origin	Filtration Performance				WU-AX/WE-AX
		5 min	10 min	15 min	30 min	
<b>Blank</b>		1.00	1.00	1.00	1.00	
<b>BsuXyn3</b>	<i>Bacillus subtilis</i> , BS3	0.93	0.95	0.96	0.95	13388
<b>BsuXyn4</b>	<i>Bacillus subtilis</i> , BS4 # 160	<i>n. d.</i>	<i>n. d.</i>	<i>n. d.</i>	<i>n. d.</i>	18619
<b>TerXyn1</b>	<i>Geosmithia emersonii</i> ( <i>Taleromyces emersonii</i> )	2.19	1.92	1.70	1.44	4232
<b>AtuXyn3</b>	<i>Aspergillus tubigensis</i>	2.06	1.75	1.59	1.37	6361
<b>AtuXyn4</b>	<i>Aspergillus tubigensis</i>	1.02	1.01	1.01	1.01	8084
<b>AacXyn2</b>	<i>Aspergillus aculeatus</i>	2.07	1.86	1.67	1.43	4994
<b>TreXyn3</b>	<i>Trichoderma reesei</i>	2.41	2.02	1.81	1.55	6567
<b>TreXyn5</b>	<i>Trichoderma reesei</i>	2.06	1.75	1.59	1.37	6272

**[0205]** Filtration performance was measured as described earlier ("filtration"), and is presented as volume filtrate at the different time points relative to the negative control (blank).

[0206] WE-AX and WU-AX enzyme activities (U) were measured as described in sections "water extractable arabinoxylan (WE-AX) xylanase method" and "water un-extractable arabinoxylan (WU-AX) xylanase method".

Glucanases:

[0207] Glucanases were screened for their activity and temperature characteristics, and the results are shown in table 4.

Table 4. Glucanases screened, their activity and their biochemical characteristics in regard to temperature

Name	Origin	U/ml	Temp opt, °C	T½ temp _buffer, °C	T½ temp _wort, °C	pH opt.
TerGlu1	Talaromyces emersonii/ Geosmithia emersonii	7338	70	78	78	3
BsuGluS	Bacillus subtilis	208	55-65	60	68	5-6
BsuGlu103FULL	Bacillus subtilis	391	50-60	53	58	5-6
TreGlu2	Trichoderma reesei	13	40-50	70	74	4.5-6
TreGlu3	Trichoderma reesei	9215	40-51	58	62	4.5-6
TreGlu4	Trichoderma reesei	n.d.	40-52	62	62	4.5-6
TreGlu6	Trichoderma reesei	n.d.	40-53	62	64	4.5-6
TreGlu7	Trichoderma reesei	n.d.	40-54	62	62	4.5-6
TreGlu8	Trichoderma reesei	n.d.	40-55	61	63	4.5-6
BsuGluC CBD	Bacillus subtilis	10	50-60	60	67	5-6
n.d. = Not determined						

[0208] Glucanase activity/units was/were determined as described in the glucanase activity assay as described above.

[0209] Based on the results from the biochemical screening, glucanases having suitable characteristics were chosen for further testing in application trials. The results are shown in table 5.

Table 5. Name and origin of glucanases screened and the relative extract yield obtained using the glucanases versus a blank (without enzyme).

Name	Origin	Filtration performance			
		5 min	10 min	15 min	30 min
Blank	Neg control	1.00	1.00	1.00	1.00
TerGlu1	<i>Geosmithia emersonii</i>	1.36	1.43	1.46	1.36
BsuGluS	<i>Bacillus subtilis</i>	1.48	1.49	1.48	1.35
BsuGlu103FULL	<i>Bacillus subtilis</i>	1.29	1.28	1.30	1.22
TreGlu2	<i>Trichoderma reesei</i>	1.15	1.18	1.20	1.15
TreGlu3	<i>Trichoderma reesei</i>	1.29	1.32	1.30	1.22
TreGlu4	<i>Trichoderma reesei</i>	1.11	1.11	1.11	1.09
TreGlu6	<i>Trichoderma reesei</i>	1.13	1.15	1.13	1.10
TreGlu7	<i>Trichoderma reesei</i>	1.06	n.d.	1.01	1.02
TreGlu8	<i>Trichoderma reesei</i>	1.12	1.11	1.13	1.09
BsuGluC CBD	<i>Bacillus subtilis</i>	1.33	1.37	1.37	1.32

**[0210]** Filtration performance was measured as described earlier ("filtration"), and is presented as volume filtrate at the different time points relative to the negative control (blank).

**[0211]** Based on the individual screening of xylanases and glucanases, combinatorial experiments were conducted, and results are illustrated in table 6.

Table 6. Brewing application results from combinatorial experiments of xylanases and glucanases versus a blank and versus UltraFlo® Max. 250 Fungal Xylanase Units FXU-S/g; 700 Cellulase Units EGU/g (Novozymes, Denmark) results are illustrated as relative extract yield obtained.

Name	Origin	Filtration performance			
		5 min	10 min	15 min	30 min
Control		1.00	1.00	1.00	1.00
UFmax 0.1	<i>A. aculeatus</i>	2.29	2.13	2.00	1.77
BsuGluS/TauXyn1	<i>B. sub/T. aurantiacus</i>	1.70	1.69	1.60	1.47
BsuGluS/AtuXyn3	<i>B. sub/A. tubingensis</i>	2.57	2.14	1.96	1.75

(Origin of UltraFlo® Max may include other microorganisms than *A. aculeatus*, such as described in WO05059084)

**[0212]** Filtration performance was measured as described earlier ("filtration"), and is presented as volume filtrate at the different time points relative to the negative control (blank).

**[0213]** Suitable combinations were further tested in a 2HL pilot scale facility for verification, and results are shown in table 7 and figure 3.

Table 7. Pilot scale Brewing application results from verification of the glucanase and xylanases screening. The B. sub glucanase S combined with the A. tub xylanases were tested against a blank and UltraFlo® Max. Data collected was the average flow (L/h), the total pressure build up over the lautering (mm WC) and the max pressure recorded during the lautering (mm WC).

ID	Avg Flow (L/h)	Total pressure build up (mm WC)	Max pressure (mm WC)
Blank	148	556	356
UltraFlo max	149	478	280
BsuGluS/AtuXyn3	147	263	163

#### Example 2

**[0214]** In this example it was attempted to show that xylanases for brewing applications may have a very high selectivity for High Molecular Weight Soluble-arabinoxylan (HMWS-AX) and water extractable arabinoxylan (WE-AX). It is believed that hereby only limited amounts of arabinoxylan need to be solubilised. Consequently, the related off flavour potential is highly reduced.

**[0215]** A significantly reduced viscosity is facilitating mash and beer separation. Desired xylanase characteristics for brewing applications may include one or more of the following aspects of table 8:

<b>Table 8:</b>	
<b>Screening criterias for xylanase selection</b>	
Enzyme <b>substrate specificity</b>	WE-AX/WU-AX ratio has an impact on viscosity
Enzyme <b>substrate selectivity</b>	How close to branch points the enzyme will cut has an impact on the functionality
Enzyme <b>thermostability</b>	Continuous solubilisation of AX during mashing - <b>thermostability</b> is a key feature
Enzyme <b>pH optimum</b> (pH 5.4 - 5.6)	

(continued)

<b>Table 8:</b>
<b>Screening criterias for xylanase selection</b>
Enzyme <b>inhibition</b> (e.g. known key factor for xylanases)

**Table 9: Xylanases - biochem characteristics Inhibition by endogenous cereal xylanase inhibitors occur in both xylanase GH's**

Xylanase GH	GH10	GH11
Mw	+ 30 kDa	20 kDa
Substrate specificity	Hydrolyse close to Arabinose substitutions	Need more unsubstituted Xylose to hydrolyse AX
Substrate selectivity	WE-AX/WU-AX typically > 1	WE-AX/WU-AX typically < 1
SBD	Often separate SBD	No classical SBD, but secondary BD on surface
Technological effect	Viscosity reducers	Solubilizer/ viscosity reducers

**[0216]** Water-Unsoluble ArabinoXylan (WU-AX) in cereals as shown in figure 3 is linked to filter cake stability in the brew house.

The concentration of ferulic acid (FA) in cereals very much depends on the tissue. The highest concentration is found in the pericarp material, whereas the concentration in the endosperm is much lower. Different concentrations are reported. A concentration of 2700 µg/g insoluble fiber, 185 µg/g soluble fiber is likely (Bunzel et al. 2001, Journal of Sc. of food and agriculture, vol. 81, p. 653-60).

**[0217]** To put this into perspective it means that FA is only found for every 200th xylose molecules in arabinoxylan in insoluble fiber (WU-AX) and for every 2500 xylose in soluble fiber (WE-AX).

**[0218]** It is a well-known fact that xylanases may lead to off-flavor formation in beer such as free ferulic acid and 4-VG.

Methods:

**[0219]** Based on the criteria mentioned in table 8+9 more than 15 xylanases from DuPont Industrial Biosciences were found as potential candidates. The xylanases were screened in laboratory mashing application applying up to 30% barley in combination with malt. Among others, mash separation speed, pentosan/arabinoxylan level and wort viscosities were monitored. Top candidates were tested at several pilot brewery plant studies to test our hypothesis and link xylanase characteristics to functionality in brewing. The optimal dosage of the selected xylanase candidate was tested in combination with a β-glucanase.

Results and discussion:

**[0220]**

Table 10: Sample ID	Control	Ref (X+B).	X1	X2	X3
Dyn. Viscosity (12 °Plato) mPa.s	1.798	1.670	1.801	1.746	1.794
Extract (°Plato)	15.1	15,7	15.6	15.2	15.1
<b>Total pentosan (mg/l)</b>	<b>1610</b>	<b>1910</b>	<b>2440</b>	<b>2020</b>	<b>1710</b>

**[0221]** Pilot plant brews where enzyme dosage is the only variable. Applying a WU-AX selective xylanase (X1) results in filter bed collapse. WE-AX selective xylanase candidates (reference, X2, X3) results in low pressure buildup. The reference is a blend of xylanase + beta-glucanase.

Table 11: Wort analyses - pilot plant studies

Sample ID	Ref.	X+B	Xh+B
Extract (°Plato)	15.70	16.00	15.95
Betaglucan in wort (mg/l)	44	35	25
Dyn. Viscosity at 12 °Plato (mPa.s)	1.65	1.68	1.68
Total pentosan (mg/l)	3540	2970	3010

Table 12: Strecker Aldehyd analysis of aged beer

Aging markers (forced aged beer)	Unit	Ref.	X+B	Xh+B
2-Me-Pr	ppb	25	24	22
2-Me-Bu	ppb	3	2	3
3-Me-Bu	ppb	9	7	8
<b>Furfural</b>	<b>ppb</b>	<b>113</b>	<b>85</b>	<b>93</b>
Methional	ppb	6	5	6
PheAcal	ppb	10	9	10
T2N	ppb	0.022	0.022	0.022

**[0222]** Optimized blends of a WE-AX selective xylanase applied at a medium (X) and a high dosage (Xh) in combination with  $\beta$ -glucanase (B) on 20% barley/80% malt. The results indicate a good mash and beer separation performance with a low risk of off-flavor formation and filter bed collapse.

Conclusion

**[0223]** The study has proven the importance of applying xylanases for brewing which are highly selective for the WE-AX during mashing. The following benefits are achieved:

- Good mash separation and beer filtration performance
- Minimized risk of filter bed collapse at lautering
- Reduced potential for off-flavor formation related to arabinoxylan breakdown
- Tolerance towards xylanase overdose

**[0224]** Xylanases can often be applied with a high beneficial effect in combination with beta-glucanases for separation control.

Example 3:

**[0225]** Evaluation of X3/BglS (also referred to as AtuXyn3/BsuGluS) combinations in 2 HL Pilot brewing trials

MATERIAL AND METHODS:

Experiments: Enzymes:

**[0226]** AtuXyn3 (X3)/ BsuGluS (Bgls) (a): Combination of BglS (Bacillus glucanase) and X3 (Aspergillus xylanase; BgLS: 0.50 mg protein/kg grist and X3: 1.50 mg protein/kg grist).

**[0227]** AtuXyn3 (X3)/ BsuGluS (Bgls) (b): As AtuXyn3 (X3)/ BsuGluS (Bgls) (a), but with 20% increase X3 dose to test robustness.

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Reference: Benchmark enzyme product (Ultraflo® Max) dosed at 0.20 kg/T grist.

Raw material:

- 5    **[0228]** Adjunct material: barley 22% w/w.  
     **[0229]** Malt: Pilsner malt Chiraz 42,6% w/w, Pilsner malt Quench DMG 35,4% weight pr. weight (ww).  
     **[0230]** All material used for acid adjustment of pH, Calcium, Zink and bitterness levels are food grade and considered as standard brewing materials.  
10    **[0231]** The recipe for the brew was aiming at a beer style as an international lager beer.

Milling:

- [0232]** Künzel 2 roller pilot mill. The milled material was passing the rollers twice simulating a 4 roller mill.  
     **[0233]** Malt grist: the mill was running at 1.5 mm at the first pass and 0.7mm at the second pass of the rollers.  
15    **[0234]** Barley grist: the mill was running at 1.5 mm at the first pass and 0.4mm at the second pass of the rollers.

Brewhouse 2 HL:

- 20    **[0235]** All brews were based on HGB (High Gravity Brewing) infusion mashing and standard lautering of 190 L wort aiming at 16 °Plato. During lautering which was performed at fixed flow, the differential pressure was recorded (used as parameter for evaluating lautering performance). All brew materials were milled ahead of time (24 h) and kept in closed buckets prior to water contact. All material was dumped in the mash kettle within the first 3 minutes after start of mashing. Calcium and pH adjustment were done prior to enzyme addition. pH (20 °C) was rechecked at the 52 °C break. Iodine normality was confirmed after 10 minutes at 72 °C. Lautering was performed at 78°C  
25    **[0236]** Lautering performance was evaluated on fixed flow at 90 l/h during first wort collection. Flow was increased to 110 L/hour and 130 L/hour during sparging and weak wort collection. Chemical analysis was performed on cold wort.

Wort boiling:

- 30    **[0237]** Boiling was performed using an external boiler with 4-5% evaporation. Hop extracts were added from the beginning of the wort boiling aiming at 20 BU in the final beer.

Fermentation 50L:

- 35    **[0238]** All fermentations were performed in 50L cylindric tanks. Fermentation was made according to standard operation procedures. Pitching was done with  $15 \times 10^6$  live yeast cells / ml. Yeast counts and viability was calculated using a Nucleo counter.

Beer processing:

- 40    **[0239]** Plate and frame filter operated at constant pressure. Flow evaluation was done by weight.  
     **[0240]** Data was collected from 1 and 3 filter plates.

Debrewing:

- 45    **[0241]** All beers were de-brewed to 5.0% ABV (Alcohol By Volume), considered as international lager beer standard.

Bottling:

- 50    **[0242]** CO<sub>2</sub> was adjusted to 5.0g / L. All beer samples were bottled in 33 cl standard bottles on a McLennon automatic filling machine using single evacuation.

Beer analysis:

- 55    **[0243]** Fresh beers were analysed using GC-MS  
     **[0244]** Chemical aging profile was determined using GC-MS.  
     **[0245]** Results and observations: Mashing.  
     **[0246]** Mashing was performed with the following condition:

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52 °C for 10 minutes simulating a 15 -20 minutes mashing using a running mill.

65 °C for 40 minutes.

72 °C for 30 minutes.

78 °C for 10 minutes.

**[0247]** All ramping steps were executed at 1 °C. A graphic representation is given in figure 7.

**[0248]** All trials were made with this mashing regime aiming at a 16 °Plato brew. There were no remarks to this process step.

**[0249]** Results and observations: Lautering.

**[0250]** The lautering was performed in the 2hl brewery with a load of 150 kg / m<sup>2</sup>. This is representative for a standard brew house operation. Control of the lautering process was made as a fixed flow at an average of 100 litre / hour. Initial flow rate is 90 litre / hour, increasing to 130 litre / hour during weak wort collection. Differential pressure and in-line measurement of haze was recorded for the four brews. Total lautering and wort collection was done over approximately 2 hours.

**[0251]** Trial X3/BglS (b) and X3/BglS (a) are suggested to be the trials that had the best lautering performance followed by trial X3/BglS (a) and trial UF max with the worst performance.

Table 13: Data collected during lautering of the mash from the four trials.

	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
Lauter tun load (kg/m <sup>3</sup> )	153	153	153	153
Lauter tun time (min)	154	164	170	154
Diff. Pressure (cm)	40	30	30	30
Racking (# deep cuts)	1	1	1	1
Haze (EBC)	10	15	10	10
First wort pressure build up (cm/h)	40	33	31	30
Time to first deep cut (min)	45	60	120	115

**[0252]** "Diff. Pressure" and "First wort pressure build up" in the table was measured as cmWC (cm Water column) and not as (cm) and (cm/h) respectively.

**[0253]** Results and observations: Wort analysis after boiling.

**[0254]** Analysis of the cold wort shows similar results. The beta-glucan analysis indicates a slight difference between the samples.

Table 14: Chemical analysis of the cold wort.

Wort	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
Extract (% plato)	16.09	16.05	15.99	16.1
Color (EBC)	9.7	9.3	9.3	9.3
pH	5	5.2	5.2	5.2
Iodine (Y/N)	N	N	N	N
Bitterness (BU, EBC)	52	51	46	50

Table 15: Analytical data on cold wort.

	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
Beta-glucan in wort (mg/L)	49	40	25	30
Dyn. Viscosity at 12°C (mPa.s)	1,888	1,685	1,679	1,686

(continued)

	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
Pentosan (mg/l)	3365	2975	3014	2964
Ferulic acid (ug/ml)	4,3	3,9	3,8	3,9
4-VG (ug/ml)	<0,49	<0,49	<0,49	<0,49
(12 °C is 12 °Plato); (%Plato may be used interchangeably with °Plato)				

**[0255]** Results and observations: Fermentation.

**[0256]** Analysis of the green beer is given in table 16.

Table 16: Green beer analysis.

Green beer	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
Alcohol (% vol)	6.79	6.79	6.7	6.86
Real extract (% P)	6.28	6	6	6
RDF (%)	63.5	63.7	63.5	64.4
Original extract (% P)	16.29	16.25	16.09	16.24
Color (EBC)	8.3	8.5	-	-
pH	4.4	4.4	4.4	4.4
SO <sub>2</sub> (ppm)	7	9	11	10
Bitterness (BU, EBC)	29	28	27	27

**[0257]** The green beer analysis shows a high degree of similarity between the trials. All trials have relative low RDF, but this is normally seen with the inclusion of 22% barley calculated on the basis of weight per weight (ww).

**[0258]** Results and observations: Beer filtration.

**[0259]** Beer samples were filtered using a plate and frame filter using a fixed pressure. Two kegs of approximately 15 kg were filtered and the individual keg filtration data are presented in table 17. The first keg was filtered using 1 filter sheet and the second keg was filtered using 3 filter sheets. The differential pressure was always 0.5 bar. The filter plates are KD7 (20cmx20cm) from Begerow.

**[0260]** The overall picture of the filtrations curves from either 1 or 3 filter plate filtrations is the same. We believe that the 1 filter plate record may be too sensitive to show the real ratio difference.

Table 17: Keg filtration data from the four trials

Filtration	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
Filtration speed - 1 filter sheet (L/h)	4.8	5.6	9.9	11.8
Filtration speed - 3 filter sheet (L/h)	77.2	59.6	70.6	105.4

**[0261]** Results and observations: Final beer analysis.

**[0262]** Trial beers were analysed according to standard operation procedures (EBC) and presented in table 18.

Table 18: Final beer analysis.

Finished beer	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
alcohol (%)	4.82	4.89	5.01	4.92
Real extract (% P)	4.5	4.6	4.6	4.4
RDF (%)	63.2	63.4	63.8	64.3
Original extract (% P)	11.85	11.99	12.19	11.89
Color(EBC)	4.8	4.9	5	5



(continued)

Finished beer	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
pH	4.4	4.4	4.4	4.4
SO <sub>2</sub> (ppm)	13	13	10	6
Bitterness (BU, EBC)	22	22	20	18
Haze(EBC)	0.43	0.4	0.38	0.4
Total haze - 5d-60 dg C (EBC)	8.6	12.9	7.3	6.2
CO <sub>2</sub> (g/L)	4.9	5.3	5.1	5.2
Diacetyl (ppb)	12	11	8	10
Head retention (S)	107	111	119	108
Foam volume (ml)	452	476	460	470

**[0263]** Results and observations: Strecker aldehydes and "age markers" in final beer.

**[0264]** Analysis was performed both on fresh and aged beer. Strecker aldehydes and the "age and heat markers" (2-Me-Pr (2-methyl Propanal), 2-Me-Bu (2-methyl Butanal), 3-Me-Bu (3-methyl Butanal), Furfural, Methional, PheAcal (phenyl Acetaldehyde) and T2N (trans-2-nonenal)) were analysed by GC-MS on both fresh and aged beer. The data from analysis of fresh beer is presented in table 19.

Table 19: Strecker aldehyde analysis of fresh beer. Markers for heat and aging (Furfural and trans-2-Nonenal) are used as sample control.

Aging markers (fresh beer)	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
2-ME-Pr (ppb)	5	5	5	6
2-ME-Bu (ppb)	2	2	2	2
3-ME-Bu (ppb)	6	6	6	6
Furfural (ppb)	10	11	11	10
Methional (ppb)	4	4	4	4
PheAcal (ppb)	6	6	6	7
T2N (ppb)	0.0011	0.005	0.004	0.006

**[0265]** The trial beers were incubated at 37 °C for 2 weeks prior to the Strecker aldehyde analysis.

**[0266]** The data for aged beer samples are presented in table 20.

Table 20: Strecker aldehyde analysis of aged beer. Markers for heat and aging (furfural and trans-2-Nonenal) is used as a sample control.

Aging markers (forced aged beer)	UF max	X3/BglS (a)	X3/BglS (b)	X3/BglS (a)
2-ME-Pr (ppb)	25	23	22	26
2-ME-Bu (ppb)	3	3	3	2
3-ME-Bu (ppb)	9	7	7	8
Furfural (ppb)	111	92	93	78
Methional (ppb)	6	5	6	6
PheAcal (ppb)	10	9	9	10
T2N (ppb)	0.017	0.022	0.022	0.022

**[0267]** The data presented in table 20 show an expected increase in Strecker aldehyde level. The increase in furfural and trans-2-Nonenal reach an expected level.

Conclusion:

**[0268]** Based on the pilot scale experiments, we can conclude that the ratios of the BglS and X3 tested in this Experiment performs as good or even better than the reference UltraFlo Max in pilot scale brewing.

**[0269]** The results are surprising, seen in the light of the challenging rawmaterial used, 22% barley inclusion in combination with the 300 mg/l  $\beta$ -glucan containing malt. The performance is not only seen in the mash separation results, also in the beer filtration. Due to the low solubilisation of cell wall material when using the BREW2 (pentosan data), a lower degree of cell wall material that might cause quality issues in relation to off-taste and stability, can be recorded.

**[0270]** Finally it can be concluded that a 20% increase in the dose of the xylanase component in X3/BglS (b) appears not to have any impact on any of the evaluated parameters, indicating that X3/BglS (a) is a robust enzyme combination.

Sequences:

**[0271]**

AtuXyn3, *Aspergillus tubingensis* (SEQ ID NO:1), 302 aa

QASVSIDTKFKAHGKKYLGNI GDQYTLTKNSKTPAIKADFGALTPENSMKWDATEPSRGQFSFSGSDYL  
VNFAQSNNKLIRGHTLVWHSQ LPSWVQAITDKNTLIEVMKNHITTVMQHYKGKIYAWDVVNEIFNEDGS  
LRDSVIFYQVIGEDYVRIAFETARAADPNKLYINDYNLDSASYPKLTGMVSHVKKWIEAGIPIDGIGSQTH  
LSAGGGAGISGALNALAGAGTKEIAVTELDIAGASSTDYVEVVEACLDQPKCIGITVWGVADPDSWRSSS  
TPLLFD SNYNPKPAYTAI ANAL

TerXyn1, *Geosmithia emersonii* (*Taleromyces emersonii*) (SEQ ID NO:2)

AGLNTAAKAIGLKYFGTATDNPELSDTAYETQLNNTQDFGQLTPANSMKWDATEPEQNVFTFSAGDQIAN  
LAKANGQMLRCHNLVWYNQLPSWVTSGSWTNETLLAAMKNHITNVVTHYKGQCYAWDVVNEALNDDG  
TYRSNVFYQYIGEAYIPIAFATAAAADPNKLYINDYNIEYPGAKATAAQNLVKLVQSYGARIDGVGLQSH  
FIVGETPSTSSQQQNMAAFTALGVEVAITELDIRMQLPETEALLTQQATDYQSTVQACANTKGCVGITVW  
DWTDKYSWVPSTFSGYG DACPWDANYQKKPAYEGILTGLGQTVTSTTYIISPTTSVGTGTTTSSGGSGG  
TTGVAQHWEQCGGLGWTGPTVCASGYTCTVINEYYSQCL

AtuXyn4, *Aspergillus tubingensis* (SEQ ID NO:3)

EPIEPRQASVSIDTKFKAHGKKYLGNI GDQYTLTKNSKTPAIKADFGALTPENSMKWDATEPSRGQFSFS  
GSDYLVNFAQSNNKLIRGHTLVWHSQ LPSWVQSIDTKNTLIEVMKNHITTVMQHYKGKIYAWDVVNEIF  
NEDGSLRDSVIFYK VIGEDYVRIAFETARAADPNKLYINDYNLDSASYPKLTGMVSHVKKWIAAGIPIDGI  
GSQTHLSAGGGAGISGALNALAGAGTKEIAVTELDIAGASSTDYVEVVEACLNQPKCIGITVWGVADPDS  
WRSSSTPLLFD SNYNPKPAYTAI ANAL

AacXyn2, *Aspergillus aculeatus* (SEQ ID NO:4)

MVGLLSITAALAATVLPNIVSAVGLDQAAVAKGLQYFGTATDNPELTDIPYVTQLNNTADFGQITPGNSMK  
 WDATEPSQGTFTFTKGDVIADLAEGNGQYLRCHTLVWYNQLPSWVTSGTWTNATLTAALKNHI TNVVS  
 5 YKGKCLHWDVVNEALNDGTYRTNIFYTTIGEAYIPIAFAAAAAADPDAKLFYNDYNLEYGGAKAASARAI  
 VQLVKNAGAKIDGVGLQAHFSVGTVPSTSSLVSVLQSFTALGVEVAYTEADVRIILLPTTATTLAQQSSDFQ  
 ALVQSCVQTTGCVGFTIWDWTDKYSWVPSTFSGYGAALPWDENLVKKPAYNGLLAGMGVTVTTTTTTTT  
 10 ATATGKTTTTTTGATSTGTAAHWGQCGGLNWSGPTACATGYTCTYVNDYYSQCL

TreXyn3, *Trichoderma reesei* (SEQ ID NO:5)

MKANVILCLLAPLVAALPTETIHLDPELAALRANLTERTADLWDRQASQSIDQLIKRKGLYFGTATDRGLL  
 15 QREKNAAIIQADLGQVTPENSMKWQSLENNQGQLNWGDADYLVNFAQQNGKSIRGHTLIWHSQLP  
 VNNINNADTLRQVIRTHVSTVVGRYKGKIRAWDVVNEIFNEDGTLRSSVFSRLLGEEFVSIAFRAARDADP  
 SARLYINDYNLDRANYGKVNGLKTYVSKWISQGVPIDGIGSQSHLSGGGGSGTLGALQQLATVPVTELA  
 20 TELDIQGAPTTDYTVVQACLSVSKCVGITVWGISDKDSWRASTNPLLFDFANFNPKPAYNSIVGILQ

TreXyn5, *Trichoderma reesei* (SEQ ID NO:6)

QCIQPGTGYNNGYFYSYWNDGHGGVTYCNGPGGQFSVNWSNSGNFVGGKGWQPGTKNRVINFSGSY  
 25 NPNGNSYLSVYGWSRNPLIEYYIVENFGTYNPSTGATKLGEVTS DGSVYDIYRTQRVNQPSII GTATFYQY  
 WSVRRNHRSSGSVNTANHFNAWAQQGLTLGTMDYQIVAVEGYFSSGSASITVSD

BsuGluS, *Bacillus subtilis* (SEQ ID NO:7), 214 aa

QTGGSFFDPFNGYNSGFQWQADGYSNGNMFNCTWRANNVSMTSLGEMRLALTSPAYNKFDCGENRSV  
 35 QTYGYGLYEVRMKPAKNTGIVSSFFTYTGPTDGTWPDEIDIEFLGKDTTKVQFNYYTNGAGNHEKIVDLGF  
 DAANAYHTYAFDWQPNSIKWYVDGQLKHTATNQIPTTPGKIMMNLWNGTGVDEWLGSYNGVNPLYAHY  
 DWVRYTKK

TerGlu1, *Geosmithia emersonii* (*Taleromyces emersonii*) (SEQ ID NO:8)

APVKEKGIIKRASPFQWFGSNESGAIEFGNNNIPGVEGTDYTFPNTSAIQILIDQGMNIFRVPFLMERMVP  
 45 NQMTGPVDSAYFQGYQVINYITSHGASAVIDPHNFGRYNNIISSPSDFQTFWHTIASNFADNDNVIFD  
 TNNEYHDMDESLVVQLNQAAIDGIRAAGATSQYIFVEGNSWTGAWTWTQVNDAMANLTD PQNKIVYEM  
 HQYLDSDGSGTSDQCVNSTIGQDRVESATAWLKQNGKKAILGEYAGGANSVCETAVTGMLDYLANNTD  
 50 VWTGAIWWAAGPWWGDYIFSMEPPSGIAYEQVLPPLQPYL

BsuGlu103FULL, *Bacillus subtilis* (SEQ ID NO:9)

DDYSVVEEHGQLSISNGELVNERGEQVQLKGMSSHGLQWYGQFVNYESMKWLRDDWGITVFRAAMYT  
 SSGGYIDDPVSVKEKVKETVEAAIDLGIYVIDWHILSDNDPNIIYKEEAKDFFDEMESELYGDYPNVIYEIANE  
 5 PNGSDVTWDNQIKPYAEEVIPVIRDNDPNINIVIGTGTWSQDVHHAADNQLADPNVMYAFHFYAGTHG  
 QNLRDQVDYALDQGAAIFVSEWGTSAAATGDGGVFLDEAQVWIDFMDERNLSWANWSLTHKDESSAAL  
 MPGANPTGGWTEAELSPSGTFVREKIREASIPPSDPTPPSDPGEPDPPSDPGEPDTPPSDPGEYPAWDSNQI  
 10 YTNEIVYHNGQLWQAKWWTQNQEPGDPYGPWEPLKSDPDSGEPDTPPSDPGEYPAWDSNQIYTNEIV  
 YHNGQLWQAKWWTQNQEPGDPYGPWEPLN

TreGlu2, *Trichoderma reesei* (SEQ ID NO:10)

15 QQTVMWGQCGGIGWSGPTNCAPGSACSTLNPYYAQCIPTATTITSTRPPSGPTTTTTRATSTSSSTPPTSS  
 GVRFAGVNIAGFDGCTTDGTCVTSKVYPPLKNFTGSNNYPDGIGQMQLHFVNDDGMTIFRLPVGWQYLV  
 NNNLGGNLDSTSISKYDQLVQGCLSLGAYCIVDIHNYARWNGGIIGQGGPTNAQFTSLWSQLASKYASQ  
 20 SRVWFGIMNEPHDVNINTWAATVQEVVTAIRNAGATSQFISLPGNDWQSAGAFISDGSAAALSQVTNPD  
 GSTTNLIFDVHXYLSDNSGTHAECTTNIDGAFSPLATWLRQNNRQAILTETGGGNVQSCIQDMCQOI  
 QYLNQNSDVYLGYPVWGAGSFDSTVLTETPTGSGNSWTDTSLVSSCLARK

25 TreGlu3, *Trichoderma reesei* (SEQ ID NO:11)

30 QTSCDQWATFTGNGYTVSNNLWGASAGSGFGCVTAVSLSGGASWHADWQWSGGQNNVKSYSQNSQI  
 AIPQKRTVNSISSMPTTASWSYSGSNIRANVAYDLFTAANPNHVTYSGDYELMIWLKGYGDIGPIGSSQG  
 TVNVGGQSWTLYYGYNGAMQVYSFVAQTNTTNYSGDVKNFFNYLRDNKGYNAAAGQYVLSYQFGTEPFT  
 GSGTLNVASWTASIN

35 TreGlu4, *Trichoderma reesei* (SEQ ID NO:12)

40 HGHINDIVINGVWYQAYDPTTFPYESNPPIVVGWTAADLDNGFVSPDAYQNPDIICHKNATNAKGHASVK  
 AGDTILFQWVPVPWPHPGPIVDYLANCNGDCETVDKTTLEFFKIDGVLLSGGDPGTWASDVLISNNNT  
 WVVKIPDNLAPGNYVLRHEIALHSAGQANGAQNYPQCFNIAVSGSGSLQPSGVLGTDLYHATDPGVLIN  
 IYTSPLNYIIPGPTVVSGLPTSVAQGSAAATATASATVPGGGSGPTSRTTTTARTTQASSRPSSTPPATTS  
 PAGGPTQTLYGQCGSGSGYSGPTRCAPPATCSTNPYYAQCLN

45 TreGlu6, *Trichoderma reesei* (SEQ ID NO:13)

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AFSWKNVKLGGGGGFVPGIIFHPKTKGVAYARTDIGGLYRLNADDSWTAVTDGIADNAGWHNWGIDAV  
 ALDPQDDQKVYAAVGMYTNSWDPSNGAIIRSSDRGATWSFTNLPFKVGGNMPGRGAGERLAVDPANSN  
 IIYFGARSGNGLWKSTDGGVTFSKVSSFTATGTYPDPSDSNGYNSDKQGLMWVTFDSTSSTTGATSR  
 IFVGTADNITASVYVSTNAGSTWSAVPGQPGKYFPHKAKLQPAEKALYLTYSWWPDAQLFRSTDSGTTW  
 SPIWAWASYPTETYYYYSISTPKAPWIKNNFIDVTSESPSDGLIKRLGWMIESLEIDPTDSNHWLYGTGMTI  
 FGGHDLTNWDTRHNVSISQSLADGIEEFSVQDLASAPGGSELLAAVGDDNGFTFASRNDLGTSPQTVWAT  
 PTWATSTSVDYAGNSVKSVMVRVGN TAGTQQVAISSDGGATWSIDYAADTSMNGGTVAYSADGDTILWS  
 TASSGVQRSQFQGSFASVSSLPAGAVIASDKKTNSVFYAGSGSTFYVSKDTGSSFTRGPKLGSAGTIRDI  
 AAHPTTAGTLYVSTDVGIFRSTDSGTTFGQVSTALTNTYQIALGVGSGSNWNLYAFGTGPSGARLYASGD  
 SGASWTDIQGSQGFSGSIDSTKVAGSGSTAGQVYVGTNNGRVFYAQGTVGGGTGGTSSSTKQSSSTS  
 SASSSTTLRSSVSTTRASTVTSSRTSSAAGPTGSGVAGHYACGGIGWTGPTQCVPAPYVCQKQNDYYY  
 QCV

TreGlu7, *Trichoderma reesei* (SEQ ID NO:14)

HGQVQNFTINGQYNQGFILDYYYQKQNTGHFPNVAGWYAEDLDLGFISPDQYTPDIVCHKNAAPGAISA  
 TAAAGSNIVFQWGPVWPHYPYGPVITYVVECSGSCCTTVNKNLNRVWKIQEAGINYNTQVWAQQDLINQ  
 GNKWTVKIPSSLRPGNYVFRHELLAAHGASSANGMQNYPQCVNIAVTGSGTKALPAGTPATQLYKPTDP  
 GILFNPYTTITSYTIPGPALWQG

TreGlu8, *Trichoderma reesei* (SEQ ID NO:15)

GKIKYLGVAIPIGIDFGCDIDGSCPTDTSSVPLLSYKGGDGAGQMKHFAEDDGLNVFRISATWQFVLNNTV  
 DGKLDDELNWGSYNKVVNACLETGAYCMIDMHNFAFYNGGIIIGQGGVSDDIFVDLWVQIAKYEDNDKII  
 FGLMNEPHDLIDIEIWAQTCQKVVTAIRKAGATSQMILLPGTNFASVETYVSTGSAEALGKITNPDGSTDLL  
 YFDVHKYLDINNSGSHAECTTDNVDAFNDFADWLRQNKRAISETGASMEPSCMTAFCAQNKAISENS  
 DVYIGFVGWAGSFDTSYILTTLPLGKPGNYTDNKLMECILDQFTLDEKYRPTPTSISTAAEETATATATS  
 DGDAPSTTKPIFREETASPTPNAVTKPSPTSDSSDDDKDSAASMSAQGLTGTVLFTVAALGYMLVAF

BsuGluC CBD, *Bacillus subtilis* (SEQ ID NO:16)

MKRSISIFITCLLITLLTMGGMIASPASAAGTKTPVAKNGQLSIKGTQLVNRDQKAVQLKGISSHGLQWYG  
 EYVNKDSLKLWRDDWGIVFRAAMYADGGYIDNPSVKNKVKEAVEAAKELGIYVIIDWHILNDGNPNQ  
 NKEKAKEFFKEMSSLYGNTPNVIYEIANEPNGDVNWKRDIPYAEVSVIRKNDPDNIIIVGTGTWSQDV  
 NDAADDQLKDANVMYALHFYAGTHGQFLRDKANYALSKGAPIFVTEWGTSDASGNGGVFLDQSREWLG  
 YLDSKTISWVNWNLSDKQESSSALKPGASKTGGWRLSDLSASGTFVRENILGTDSTKDIPETPSKDKPT  
 QENGISVQYRAGDGSMSNSQIRPQLQIKNNGNTTVDLKDV TARYWYKAKNKGQNFDCDYAQIGCGNVT  
 HKFVTLHKPKQGADTYLELGFKNGLAPGASTGNIQLRLHNDWSNYAQSGDYSFFKSNTFKTKKITLY  
 DQGKLIWGTEPN

BsuXyn3, *Bacillus subtilis* xylanase variant (SEQ ID NO:17)

ASTDYWQNWTFGGGIVNAVNGSGGNYSVNWSNTGNFVVGKGWTTGSPFRTINYNAGVWAPNGNGYL  
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BsuXyn4, *Bacillus subtilis* xylanase variant (SEQ ID NO:18)

ASTDYWQNWTDGYGIVNAVNGSGGNYSVNWSNTGNFVVGKGWTTGSPFRTINYNAGVWAPNGNGYL  
 10 TLYGWTRSPLIEYYVVDSWGTYRPTGTYKGTVYSDGGWYDIYTATRDNAPSIDGDFTTFTQYWSVRQSK  
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Thr Pro Gly Asn Ser Met Lys Trp Asp Ala Thr Glu Pro Ser Gln Gly  
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35	Asp	Gly	Gln	Leu	Lys	His	Thr	Ala	Thr	Asn	Gln	Ile	Pro	Thr	Thr	Pro
					165					170					175	
40	Gly	Lys	Ile	Met	Met	Asn	Leu	Trp	Asn	Gly	Thr	Gly	Val	Asp	Glu	Trp
				180					185					190		
45	Leu	Gly	Ser	Tyr	Asn	Gly	Val	Asn	Pro	Leu	Tyr	Ala	His	Tyr	Asp	Trp
			195					200					205			
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	1				5					10					15	
65	Trp	Phe	Gly	Ser	Asn	Glu	Ser	Gly	Ala	Glu	Phe	Gly	Asn	Asn	Asn	Ile
				20					25				30			
70	Pro	Gly	Val	Glu	Gly	Thr	Asp	Tyr	Thr	Phe	Pro	Asn	Thr	Ser	Ala	Ile
			35					40					45			

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	Gln	Ile	Leu	Ile	Asp	Gln	Gly	Met	Asn	Ile	Phe	Arg	Val	Pro	Phe	Leu	
	50						55					60					
5	Met	Glu	Arg	Met	Val	Pro	Asn	Gln	Met	Thr	Gly	Pro	Val	Asp	Ser	Ala	
	65					70					75					80	
10	Tyr	Phe	Gln	Gly	Tyr	Ser	Gln	Val	Ile	Asn	Tyr	Ile	Thr	Ser	His	Gly	
					85					90					95		
15	Ala	Ser	Ala	Val	Ile	Asp	Pro	His	Asn	Phe	Gly	Arg	Tyr	Tyr	Asn	Asn	
				100					105					110			
20	Ile	Ile	Ser	Ser	Pro	Ser	Asp	Phe	Gln	Thr	Phe	Trp	His	Thr	Ile	Ala	
			115					120					125				
25	Ser	Asn	Phe	Ala	Asp	Asn	Asp	Asn	Val	Ile	Phe	Asp	Thr	Asn	Asn	Glu	
	130						135					140					
30	Tyr	His	Asp	Met	Asp	Glu	Ser	Leu	Val	Val	Gln	Leu	Asn	Gln	Ala	Ala	
	145					150					155					160	
35	Ile	Asp	Gly	Ile	Arg	Ala	Ala	Gly	Ala	Thr	Ser	Gln	Tyr	Ile	Phe	Val	
					165					170					175		
40	Glu	Gly	Asn	Ser	Trp	Thr	Gly	Ala	Trp	Thr	Trp	Thr	Gln	Val	Asn	Asp	
				180					185					190			
45	Ala	Met	Ala	Asn	Leu	Thr	Asp	Pro	Gln	Asn	Lys	Ile	Val	Tyr	Glu	Met	
			195					200					205				
50	His	Gln	Tyr	Leu	Asp	Ser	Asp	Gly	Ser	Gly	Thr	Ser	Asp	Gln	Cys	Val	
	210						215					220					
55	Asn	Ser	Thr	Ile	Gly	Gln	Asp	Arg	Val	Glu	Ser	Ala	Thr	Ala	Trp	Leu	
	225					230					235					240	
60	Lys	Gln	Asn	Gly	Lys	Lys	Ala	Ile	Leu	Gly	Glu	Tyr	Ala	Gly	Gly	Ala	
				245						250					255		
65	Asn	Ser	Val	Cys	Glu	Thr	Ala	Val	Thr	Gly	Met	Leu	Asp	Tyr	Leu	Ala	
				260					265					270			
70	Asn	Asn	Thr	Asp	Val	Trp	Thr	Gly	Ala	Ile	Trp	Trp	Ala	Ala	Gly	Pro	
			275					280					285				
75	Trp	Trp	Gly	Asp	Tyr	Ile	Phe	Ser	Met	Glu	Pro	Pro	Ser	Gly	Ile	Ala	

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5 Tyr Glu Gln Val Leu Pro Leu Leu Gln Pro Tyr Leu  
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<213> Bacillus subtilis

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	Asp	Asp	Tyr	Ser	Val	Val	Glu	Glu	His	Gly	Gln	Leu	Ser	Ile	Ser	Asn
	1				5					10					15	
5	Gly	Glu	Leu	Val	Asn	Glu	Arg	Gly	Glu	Gln	Val	Gln	Leu	Lys	Gly	Met
				20					25					30		
10	Ser	Ser	His	Gly	Leu	Gln	Trp	Tyr	Gly	Gln	Phe	Val	Asn	Tyr	Glu	Ser
			35					40					45			
15	Met	Lys	Trp	Leu	Arg	Asp	Asp	Trp	Gly	Ile	Thr	Val	Phe	Arg	Ala	Ala
		50					55					60				
20	Met	Tyr	Thr	Ser	Ser	Gly	Gly	Tyr	Ile	Asp	Asp	Pro	Ser	Val	Lys	Glu
	65					70				75						80
25	Lys	Val	Lys	Glu	Thr	Val	Glu	Ala	Ala	Ile	Asp	Leu	Gly	Ile	Tyr	Val
					85					90					95	
30	Ile	Ile	Asp	Trp	His	Ile	Leu	Ser	Asp	Asn	Asp	Pro	Asn	Ile	Tyr	Lys
				100					105					110		
35	Glu	Glu	Ala	Lys	Asp	Phe	Phe	Asp	Glu	Met	Ser	Glu	Leu	Tyr	Gly	Asp
			115					120					125			
40	Tyr	Pro	Asn	Val	Ile	Tyr	Glu	Ile	Ala	Asn	Glu	Pro	Asn	Gly	Ser	Asp
		130					135					140				
45	Val	Thr	Trp	Asp	Asn	Gln	Ile	Lys	Pro	Tyr	Ala	Glu	Glu	Val	Ile	Pro
	145					150					155					160
50	Val	Ile	Arg	Asp	Asn	Asp	Pro	Asn	Asn	Ile	Val	Ile	Val	Gly	Thr	Gly
				165						170					175	
55	Thr	Trp	Ser	Gln	Asp	Val	His	His	Ala	Ala	Asp	Asn	Gln	Leu	Ala	Asp
				180					185					190		
	Pro	Asn	Val	Met	Tyr	Ala	Phe	His	Phe	Tyr	Ala	Gly	Thr	His	Gly	Gln

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	195	200	205
5	Asn Leu Arg Asp Gln Val Asp Tyr Ala Leu Asp Gln Gly Ala Ala Ile 210 215 220		
10	Phe Val Ser Glu Trp Gly Thr Ser Ala Ala Thr Gly Asp Gly Gly Val 225 230 235 240		
15	Phe Leu Asp Glu Ala Gln Val Trp Ile Asp Phe Met Asp Glu Arg Asn 245 250 255		
20	Leu Ser Trp Ala Asn Trp Ser Leu Thr His Lys Asp Glu Ser Ser Ala 260 265 270		
25	Ala Leu Met Pro Gly Ala Asn Pro Thr Gly Gly Trp Thr Glu Ala Glu 275 280 285		
30	Leu Ser Pro Ser Gly Thr Phe Val Arg Glu Lys Ile Arg Glu Ser Ala 290 295 300		
35	Ser Ile Pro Pro Ser Asp Pro Thr Pro Pro Ser Asp Pro Gly Glu Pro 305 310 315 320		
40	Asp Pro Gly Glu Pro Asp Pro Thr Pro Pro Ser Asp Pro Gly Glu Tyr 325 330 335		
45	Pro Ala Trp Asp Ser Asn Gln Ile Tyr Thr Asn Glu Ile Val Tyr His 340 345 350		
50	Asn Gly Gln Leu Trp Gln Ala Lys Trp Trp Thr Gln Asn Gln Glu Pro 355 360 365		
55	Gly Asp Pro Tyr Gly Pro Trp Glu Pro Leu Lys Ser Asp Pro Asp Ser 370 375 380		
	Gly Glu Pro Asp Pro Thr Pro Pro Ser Asp Pro Gly Glu Tyr Pro Ala 385 390 395 400		
	Trp Asp Ser Asn Gln Ile Tyr Thr Asn Glu Ile Val Tyr His Asn Gly 405 410 415		
	Gln Leu Trp Gln Ala Lys Trp Trp Thr Gln Asn Gln Glu Pro Gly Asp 420 425 430		
	Pro Tyr Gly Pro Trp Glu Pro Leu Asn 435 440		

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Thr	Asn	Cys	Ala	Pro	Gly	Ser	Ala	Cys	Ser	Thr	Leu	Asn	Pro	Tyr	Tyr	20	25	30	
Ala	Gln	Cys	Ile	Pro	Gly	Ala	Thr	Thr	Ile	Thr	Thr	Ser	Thr	Arg	Pro	35	40	45	
Pro	Ser	Gly	Pro	Thr	Thr	Thr	Thr	Arg	Ala	Thr	Ser	Thr	Ser	Ser	Ser	50	55	60	
Thr	Pro	Pro	Thr	Ser	Ser	Gly	Val	Arg	Phe	Ala	Gly	Val	Asn	Ile	Ala	65	70	75	80
Gly	Phe	Asp	Phe	Gly	Cys	Thr	Thr	Asp	Gly	Thr	Cys	Val	Thr	Ser	Lys	85	90	95	
Val	Tyr	Pro	Pro	Leu	Lys	Asn	Phe	Thr	Gly	Ser	Asn	Asn	Tyr	Pro	Asp	100	105	110	
Gly	Ile	Gly	Gln	Met	Gln	His	Phe	Val	Asn	Asp	Asp	Gly	Met	Thr	Ile	115	120	125	
Phe	Arg	Leu	Pro	Val	Gly	Trp	Gln	Tyr	Leu	Val	Asn	Asn	Asn	Leu	Gly	130	135	140	
Gly	Asn	Leu	Asp	Ser	Thr	Ser	Ile	Ser	Lys	Tyr	Asp	Gln	Leu	Val	Gln	145	150	155	160
Gly	Cys	Leu	Ser	Leu	Gly	Ala	Tyr	Cys	Ile	Val	Asp	Ile	His	Asn	Tyr	165	170	175	
Ala	Arg	Trp	Asn	Gly	Gly	Ile	Ile	Gly	Gln	Gly	Gly	Pro	Thr	Asn	Ala	180	185	190	
Gln	Phe	Thr	Ser	Leu	Trp	Ser	Gln	Leu	Ala	Ser	Lys	Tyr	Ala	Ser	Gln	195	200	205	
Ser	Arg	Val	Trp	Phe	Gly	Ile	Met	Asn	Glu	Pro	His	Asp	Val	Asn	Ile	210	215	220	

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	Asn	Thr	Trp	Ala	Ala	Thr	Val	Gln	Glu	Val	Val	Thr	Ala	Ile	Arg	Asn	
	225						230					235				240	
5	Ala	Gly	Ala	Thr	Ser	Gln	Phe	Ile	Ser	Leu	Pro	Gly	Asn	Asp	Trp	Gln	
					245					250					255		
10	Ser	Ala	Gly	Ala	Phe	Ile	Ser	Asp	Gly	Ser	Ala	Ala	Ala	Leu	Ser	Gln	
				260					265					270			
15	Val	Thr	Asn	Pro	Asp	Gly	Ser	Thr	Thr	Asn	Leu	Ile	Phe	Asp	Val	His	
			275					280					285				
20	Lys	Tyr	Leu	Asp	Ser	Asp	Asn	Ser	Gly	Thr	His	Ala	Glu	Cys	Thr	Thr	
	290						295					300					
25	Asn	Asn	Ile	Asp	Gly	Ala	Phe	Ser	Pro	Leu	Ala	Thr	Trp	Leu	Arg	Gln	
	305					310					315					320	
30	Asn	Asn	Arg	Gln	Ala	Ile	Leu	Thr	Glu	Thr	Gly	Gly	Gly	Asn	Val	Gln	
				325						330					335		
35	Ser	Cys	Ile	Gln	Asp	Met	Cys	Gln	Gln	Ile	Gln	Tyr	Leu	Asn	Gln	Asn	
				340					345					350			
40	Ser	Asp	Val	Tyr	Leu	Gly	Tyr	Val	Gly	Trp	Gly	Ala	Gly	Ser	Phe	Asp	
			355					360					365				
45	Ser	Thr	Tyr	Val	Leu	Thr	Glu	Thr	Pro	Thr	Gly	Ser	Gly	Asn	Ser	Trp	
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	1				5					10					15		
55	Val	Ser	Asn	Asn	Leu	Trp	Gly	Ala	Ser	Ala	Gly	Ser	Gly	Phe	Gly	Cys	
				20					25					30			
60	Val	Thr	Ala	Val	Ser	Leu	Ser	Gly	Gly	Ala	Ser	Trp	His	Ala	Asp	Trp	
			35					40					45				



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	Gln	Trp	Ser	Gly	Gly	Gln	Asn	Asn	Val	Lys	Ser	Tyr	Gln	Asn	Ser	Gln
	50						55					60				
5	Ile	Ala	Ile	Pro	Gln	Lys	Arg	Thr	Val	Asn	Ser	Ile	Ser	Ser	Met	Pro
	65					70					75					80
10	Thr	Thr	Ala	Ser	Trp	Ser	Tyr	Ser	Gly	Ser	Asn	Ile	Arg	Ala	Asn	Val
					85					90					95	
15	Ala	Tyr	Asp	Leu	Phe	Thr	Ala	Ala	Asn	Pro	Asn	His	Val	Thr	Tyr	Ser
				100					105					110		
20	Gly	Asp	Tyr	Glu	Leu	Met	Ile	Trp	Leu	Gly	Lys	Tyr	Gly	Asp	Ile	Gly
			115					120					125			
25	Pro	Ile	Gly	Ser	Ser	Gln	Gly	Thr	Val	Asn	Val	Gly	Gly	Gln	Ser	Trp
	130						135					140				
30	Thr	Leu	Tyr	Tyr	Gly	Tyr	Asn	Gly	Ala	Met	Gln	Val	Tyr	Ser	Phe	Val
	145					150					155					160
35	Ala	Gln	Thr	Asn	Thr	Thr	Asn	Tyr	Ser	Gly	Asp	Val	Lys	Asn	Phe	Phe
					165					170					175	
40	Asn	Tyr	Leu	Arg	Asp	Asn	Lys	Gly	Tyr	Asn	Ala	Ala	Gly	Gln	Tyr	Val
				180					185					190		
45	Leu	Ser	Tyr	Gln	Phe	Gly	Thr	Glu	Pro	Phe	Thr	Gly	Ser	Gly	Thr	Leu
			195					200					205			
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	1				5					10					15	
65	Tyr	Asp	Pro	Thr	Thr	Phe	Pro	Tyr	Glu	Ser	Asn	Pro	Pro	Ile	Val	Val
				20					25					30		
70	Gly	Trp	Thr	Ala	Ala	Asp	Leu	Asp	Asn	Gly	Phe	Val	Ser	Pro	Asp	Ala
			35					40					45			

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	Tyr	Gln	Asn	Pro	Asp	Ile	Ile	Cys	His	Lys	Asn	Ala	Thr	Asn	Ala	Lys	
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5	Gly	His	Ala	Ser	Val	Lys	Ala	Gly	Asp	Thr	Ile	Leu	Phe	Gln	Trp	Val	
	65					70					75					80	
	Pro	Val	Pro	Trp	Pro	His	Pro	Gly	Pro	Ile	Val	Asp	Tyr	Leu	Ala	Asn	
10					85					90					95		
	Cys	Asn	Gly	Asp	Cys	Glu	Thr	Val	Asp	Lys	Thr	Thr	Leu	Glu	Phe	Phe	
				100					105					110			
15	Lys	Ile	Asp	Gly	Val	Gly	Leu	Leu	Ser	Gly	Gly	Asp	Pro	Gly	Thr	Trp	
			115				120						125				
	Ala	Ser	Asp	Val	Leu	Ile	Ser	Asn	Asn	Asn	Thr	Trp	Val	Val	Lys	Ile	
20			130				135					140					
	Pro	Asp	Asn	Leu	Ala	Pro	Gly	Asn	Tyr	Val	Leu	Arg	His	Glu	Ile	Ile	
25						150					155					160	
	Ala	Leu	His	Ser	Ala	Gly	Gln	Ala	Asn	Gly	Ala	Gln	Asn	Tyr	Pro	Gln	
					165					170					175		
30	Cys	Phe	Asn	Ile	Ala	Val	Ser	Gly	Ser	Gly	Ser	Leu	Gln	Pro	Ser	Gly	
				180					185					190			
	Val	Leu	Gly	Thr	Asp	Leu	Tyr	His	Ala	Thr	Asp	Pro	Gly	Val	Leu	Ile	
35			195					200					205				
	Asn	Ile	Tyr	Thr	Ser	Pro	Leu	Asn	Tyr	Ile	Ile	Pro	Gly	Pro	Thr	Val	
			210				215					220					
40	Val	Ser	Gly	Leu	Pro	Thr	Ser	Val	Ala	Gln	Gly	Ser	Ser	Ala	Ala	Thr	
	225					230					235					240	
	Ala	Thr	Ala	Ser	Ala	Thr	Val	Pro	Gly	Gly	Gly	Ser	Gly	Pro	Thr	Ser	
45					245					250					255		
	Arg	Thr	Thr	Thr	Thr	Ala	Arg	Thr	Thr	Gln	Ala	Ser	Ser	Arg	Pro	Ser	
50				260					265					270			
	Ser	Thr	Pro	Pro	Ala	Thr	Thr	Ser	Ala	Pro	Ala	Gly	Gly	Pro	Thr	Gln	
			275					280					285				
55	Thr	Leu	Tyr	Gly	Gln	Cys	Gly	Gly	Ser	Gly	Tyr	Ser	Gly	Pro	Thr	Arg	
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Cys Ala Pro Pro Ala Thr Cys Ser Thr Asn Pro Tyr Tyr Ala Gln Cys  
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5 Leu Asn

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10 <213> Trichoderma reesei

<400> 13

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Pro Gly Ile Ile Phe His Pro Lys Thr Lys Gly Val Ala Tyr Ala Arg  
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Thr Asp Ile Gly Gly Leu Tyr Arg Leu Asn Ala Asp Asp Ser Trp Thr  
35 40 45

25 Ala Val Thr Asp Gly Ile Ala Asp Asn Ala Gly Trp His Asn Trp Gly  
50 55 60

30 Ile Asp Ala Val Ala Leu Asp Pro Gln Asp Asp Gln Lys Val Tyr Ala  
65 70 75 80

Ala Val Gly Met Tyr Thr Asn Ser Trp Asp Pro Ser Asn Gly Ala Ile  
85 90 95

Ile Arg Ser Ser Asp Arg Gly Ala Thr Trp Ser Phe Thr Asn Leu Pro  
100 105 110

40 Phe Lys Val Gly Gly Asn Met Pro Gly Arg Gly Ala Gly Glu Arg Leu  
115 120 125

45 Ala Val Asp Pro Ala Asn Ser Asn Ile Ile Tyr Phe Gly Ala Arg Ser  
130 135 140

Gly Asn Gly Leu Trp Lys Ser Thr Asp Gly Gly Val Thr Phe Ser Lys  
145 150 155 160

Val Ser Ser Phe Thr Ala Thr Gly Thr Tyr Ile Pro Asp Pro Ser Asp  
165 170 175

55 Ser Asn Gly Tyr Asn Ser Asp Lys Gln Gly Leu Met Trp Val Thr Phe  
180 185 190

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	Asp	Ser	Thr	Ser	Ser	Thr	Thr	Gly	Gly	Ala	Thr	Ser	Arg	Ile	Phe	Val
			195					200					205			
5	Gly	Thr	Ala	Asp	Asn	Ile	Thr	Ala	Ser	Val	Tyr	Val	Ser	Thr	Asn	Ala
		210					215					220				
10	Gly	Ser	Thr	Trp	Ser	Ala	Val	Pro	Gly	Gln	Pro	Gly	Lys	Tyr	Phe	Pro
	225					230					235					240
15	His	Lys	Ala	Lys	Leu	Gln	Pro	Ala	Glu	Lys	Ala	Leu	Tyr	Leu	Thr	Tyr
				245						250					255	
20	Ser	Trp	Trp	Pro	Asp	Ala	Gln	Leu	Phe	Arg	Ser	Thr	Asp	Ser	Gly	Thr
				260					265					270		
25	Thr	Trp	Ser	Pro	Ile	Trp	Ala	Trp	Ala	Ser	Tyr	Pro	Thr	Glu	Thr	Tyr
			275					280						285		
30	Tyr	Tyr	Ser	Ile	Ser	Thr	Pro	Lys	Ala	Pro	Trp	Ile	Lys	Asn	Asn	Phe
	290						295					300				
35	Ile	Asp	Val	Thr	Ser	Glu	Ser	Pro	Ser	Asp	Gly	Leu	Ile	Lys	Arg	Leu
	305					310					315					320
40	Gly	Trp	Met	Ile	Glu	Ser	Leu	Glu	Ile	Asp	Pro	Thr	Asp	Ser	Asn	His
				325						330					335	
45	Trp	Leu	Tyr	Gly	Thr	Gly	Met	Thr	Ile	Phe	Gly	Gly	His	Asp	Leu	Thr
				340					345					350		
50	Asn	Trp	Asp	Thr	Arg	His	Asn	Val	Ser	Ile	Gln	Ser	Leu	Ala	Asp	Gly
			355					360					365			
55	Ile	Glu	Glu	Phe	Ser	Val	Gln	Asp	Leu	Ala	Ser	Ala	Pro	Gly	Gly	Ser
	370						375					380				
60	Glu	Leu	Leu	Ala	Ala	Val	Gly	Asp	Asp	Asn	Gly	Phe	Thr	Phe	Ala	Ser
	385					390					395					400
65	Arg	Asn	Asp	Leu	Gly	Thr	Ser	Pro	Gln	Thr	Val	Trp	Ala	Thr	Pro	Thr
				405						410					415	
70	Trp	Ala	Thr	Ser	Thr	Ser	Val	Asp	Tyr	Ala	Gly	Asn	Ser	Val	Lys	Ser
				420					425					430		
75	Val	Val	Arg	Val	Gly	Asn	Thr	Ala	Gly	Thr	Gln	Gln	Val	Ala	Ile	Ser
			435					440					445			

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	Ser	Asp	Gly	Gly	Ala	Thr	Trp	Ser	Ile	Asp	Tyr	Ala	Ala	Asp	Thr	Ser	
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5	Met	Asn	Gly	Gly	Thr	Val	Ala	Tyr	Ser	Ala	Asp	Gly	Asp	Thr	Ile	Leu	
	465					470					475					480	
10	Trp	Ser	Thr	Ala	Ser	Ser	Gly	Val	Gln	Arg	Ser	Gln	Phe	Gln	Gly	Ser	
					485					490					495		
15	Phe	Ala	Ser	Val	Ser	Ser	Leu	Pro	Ala	Gly	Ala	Val	Ile	Ala	Ser	Asp	
				500					505					510			
20	Lys	Lys	Thr	Asn	Ser	Val	Phe	Tyr	Ala	Gly	Ser	Gly	Ser	Thr	Phe	Tyr	
			515				520						525				
25	Val	Ser	Lys	Asp	Thr	Gly	Ser	Ser	Phe	Thr	Arg	Gly	Pro	Lys	Leu	Gly	
		530					535					540					
30	Ser	Ala	Gly	Thr	Ile	Arg	Asp	Ile	Ala	Ala	His	Pro	Thr	Thr	Ala	Gly	
	545				550						555					560	
35	Thr	Leu	Tyr	Val	Ser	Thr	Asp	Val	Gly	Ile	Phe	Arg	Ser	Thr	Asp	Ser	
				565					570						575		
40	Gly	Thr	Thr	Phe	Gly	Gln	Val	Ser	Thr	Ala	Leu	Thr	Asn	Thr	Tyr	Gln	
				580					585					590			
45	Ile	Ala	Leu	Gly	Val	Gly	Ser	Gly	Ser	Asn	Trp	Asn	Leu	Tyr	Ala	Phe	
			595				600						605				
50	Gly	Thr	Gly	Pro	Ser	Gly	Ala	Arg	Leu	Tyr	Ala	Ser	Gly	Asp	Ser	Gly	
		610					615					620					
55	Ala	Ser	Trp	Thr	Asp	Ile	Gln	Gly	Ser	Gln	Gly	Phe	Gly	Ser	Ile	Asp	
	625				630				635					640			
60	Ser	Thr	Lys	Val	Ala	Gly	Ser	Gly	Ser	Thr	Ala	Gly	Gln	Val	Tyr	Val	
				645					650					655			
65	Gly	Thr	Asn	Gly	Arg	Gly	Val	Phe	Tyr	Ala	Gln	Gly	Thr	Val	Gly	Gly	
			660				665						670				
70	Gly	Thr	Gly	Gly	Thr	Ser	Ser	Ser	Thr	Lys	Gln	Ser	Ser	Ser	Ser	Thr	
			675				680					685					
75	Ser	Ser	Ala	Ser	Ser	Ser	Thr	Thr	Leu	Arg	Ser	Ser	Val	Val	Ser	Thr	

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690

695

700

5 Thr Arg Ala Ser Thr Val Thr Ser Ser Arg Thr Ser Ser Ala Ala Gly  
705 710 715 720

10 Pro Thr Gly Ser Gly Val Ala Gly His Tyr Ala Gln Cys Gly Gly Ile  
725 730 735

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## Claims

- 50 1. A composition comprising an enzyme exhibiting endo-1,4- $\beta$ -xylanase activity, which enzyme comprises an amino acid sequence having at least 90 % identity with SEQ ID NO: 1; in combination with an enzyme exhibiting endo-1,3(4)- $\beta$ -glucanase activity which enzyme comprises an amino acid sequence having at least 90% identity with SEQ ID NO:7.
- 55 2. The composition according to claim 1, wherein said enzyme exhibiting endo-1,4- $\beta$ -xylanase activity has at least 91, 92, 93, 94, 95, 96, 97, 98 or 99% identity with the amino acid sequence selected of SEQ ID NO: 1.
3. Use of a composition according to any one of claims 1-2 in the production of a food, feed, or malt beverage product,

in the production of dough or baked products, in the preparation of pulp or paper, for the preparation of cereal components, such as in which the cereal is rye, wheat, or barley, in the production of beer or modification of byproducts from a brewing process, in the production of wine or juice, or in the production of a first- or second-generation biofuel, such as bioethanol.

4. Method of altering filterability of a starch comprising material, said method comprising the step of treating said starch comprising material with a composition according to any one of claims 1-2.
5. Method of reducing pressure built up during lautering in a brewing application, said method comprising the step of treating a brewing mash with a composition according to any one of claims 1-2.
6. Method for the production of a food, feed, or beverage product, such as an alcoholic or non-alcoholic beverage, such as a cereal- or malt-based beverage like beer or whiskey, said method comprising the step of treating a starch comprising material with a composition according to any one of claims 1-2.
7. Method for the production of a brewing mash, said method comprising the step of treating a starch comprising material with a composition according to any one of claims 1-2.
8. Method for the production of a first- or second-generation biofuel, such as bioethanol, said method comprising the step of treating a starch comprising material with a composition according to any one of claims 1-2.

#### Patentansprüche

1. Zusammensetzung, umfassend ein Enzym, das Endo-1,4-Beta-Xylanaseaktivität zeigt, wobei das Enzym eine Aminosäuresequenz aufweist, die mindestens eine Identität von 90% mit SEQ ID NO: 1 hat; in Kombination mit einem Enzym, das Endo-1,3(4)-Beta-Xylanaseaktivität zeigt, wobei das Enzym eine Aminosäuresequenz aufweist, die mindestens eine Identität von 90% mit SEQ ID NO: 7 hat.
2. Enzym nach Anspruch 1, wobei das Enzym, das Endo-1,4-Beta-Xylanaseaktivität zeigt, mindestens eine Identität von 91%, 92%, 93%, 94%, 95%, 96%, 97%, 98% oder 99% mit der Aminosäuresequenz SEQ ID NO: 1 hat.
3. Verwendung einer Zusammensetzung nach einem der Ansprüche 1 bis 2 in der Herstellung eines Lebensmittels, Futtermittels oder Produkt eines Malzgetränks, in der Herstellung von Teig- oder Backwaren, in der Herstellung von Pulpe oder Papier, für die Herstellung von Komponenten von Cerealien, wo beispielsweise das Getreide Roggen, Weizen oder Gerste ist, in der Herstellung von Bier oder der Modifizierung von Nebenprodukten eines Brauprozesses, in der Herstellung von Wein oder Saft oder in der Herstellung eines Biokraftstoffes der ersten oder zweiten Generation, wie beispielsweise Bioethanol.
4. Verfahren zur Veränderung der Filtrationsfähigkeit eines Stärke aufweisenden Materials, wobei das Verfahren den Schritt der Behandlung des Stärke aufweisenden Materials mit einer Zusammensetzung nach einem der Ansprüche 1 bis 2 umfasst.
5. Verfahren zum Verringern des Druckaufbaus während des Läuterns in einer Brau-Anwendung, wobei das Verfahren den Schritt der Behandlung einer Brauereimaische mit einer Zusammensetzung nach einem der Ansprüche 1 bis 2 umfasst.
6. Verfahren für die Herstellung eines Lebensmittels, Futtermittels oder Getränkeprodukts, wie beispielsweise eines alkoholischen oder alkoholfreien Getränks, wie beispielsweise eines Getränks auf Basis eines Getreides oder Malz, wie beispielsweise Bier oder Whisky, wobei das Verfahren den Schritt der Behandlung eines Stärke aufweisenden Materials mit einer Zusammensetzung nach einem der Ansprüche 1 bis 2 umfasst.
7. Verfahren für die Herstellung einer Brauereimaische, wobei das Verfahren den Schritt der Behandlung eines Stärke aufweisenden Materials mit einer Zusammensetzung nach einem der Ansprüche 1 bis 2 umfasst.
8. Verfahren für die Herstellung eines Biokraftstoffes der ersten oder zweiten Generation, beispielsweise Bioethanol, wobei das Verfahren den Schritt der Behandlung eines Stärke aufweisenden Materials mit einer Zusammensetzung nach einem der Ansprüche 1 bis 2 umfasst.

**Revendications**

1. Composition comprenant une enzyme présentant une activité d'endo-1,4- $\beta$ -xylanase, laquelle enzyme comprend une séquence d'acides aminés ayant au moins 90% d'identité avec la SEQ ID NO: 1; en combinaison avec une enzyme présentant une activité d'endo-1,3(4)- $\beta$ -glucanase, laquelle enzyme comprend une séquence d'acides aminés ayant au moins 90% d'identité avec la SEQ ID NO: 7.
2. Composition selon la revendication 1, dans laquelle ladite enzyme présentant une activité d'endo-1,4- $\beta$ -xylanase a au moins 91, 92, 93, 94, 95, 96, 97, 98 ou 99% d'identité avec la séquence d'acides aminés choisie de la SEQ ID NO: 1.
3. Utilisation d'une composition selon l'une quelconque des revendications 1-2 dans la production d'un aliment, d'un aliment pour animaux ou d'un produit de boisson maltée, dans la production de produits de pâte ou cuits, dans la préparation d'une pâte à papier ou d'un papier, pour la préparation de composants de céréales, comme ceux dans lesquels la céréale est le seigle, le blé ou l'orge, dans la production de bière ou la modification de sous-produits d'un procédé de brassage, dans la production de vin ou de jus, ou dans la production d'un biocarburant de première ou deuxième génération, comme le bioéthanol.
4. Procédé de modification de la filtrabilité d'une matière comprenant un amidon, ledit procédé comprenant l'étape consistant à traiter ladite matière comprenant un amidon avec une composition selon l'une quelconque des revendications 1-2.
5. Procédé de réduction de la pression accumulée pendant le filtrage dans une application de brassage, ledit procédé comprenant l'étape consistant à traiter une suspension de brassage avec une composition selon l'une quelconque des revendications 1-2.
6. Procédé pour la production d'un aliment, d'un aliment pour animaux ou d'un produit de boisson, tel qu'une boisson alcoolique ou non alcoolique, telle qu'une boisson à base de céréale ou de malt comme la bière ou le whisky, ledit procédé comprenant l'étape consistant à traiter une matière comprenant un amidon avec une composition selon l'une quelconque des revendications 1-2.
7. Procédé pour la production d'une suspension de brassage, ledit procédé comprenant l'étape consistant à traiter une matière comprenant un amidon avec une composition selon l'une quelconque des revendications 1-2.
8. Procédé pour la production d'un biocarburant de première ou deuxième génération, tel que le bioéthanol, ledit procédé comprenant l'étape consistant à traiter une matière comprenant un amidon avec une composition selon l'une quelconque des revendications 1-2.



Figure 1

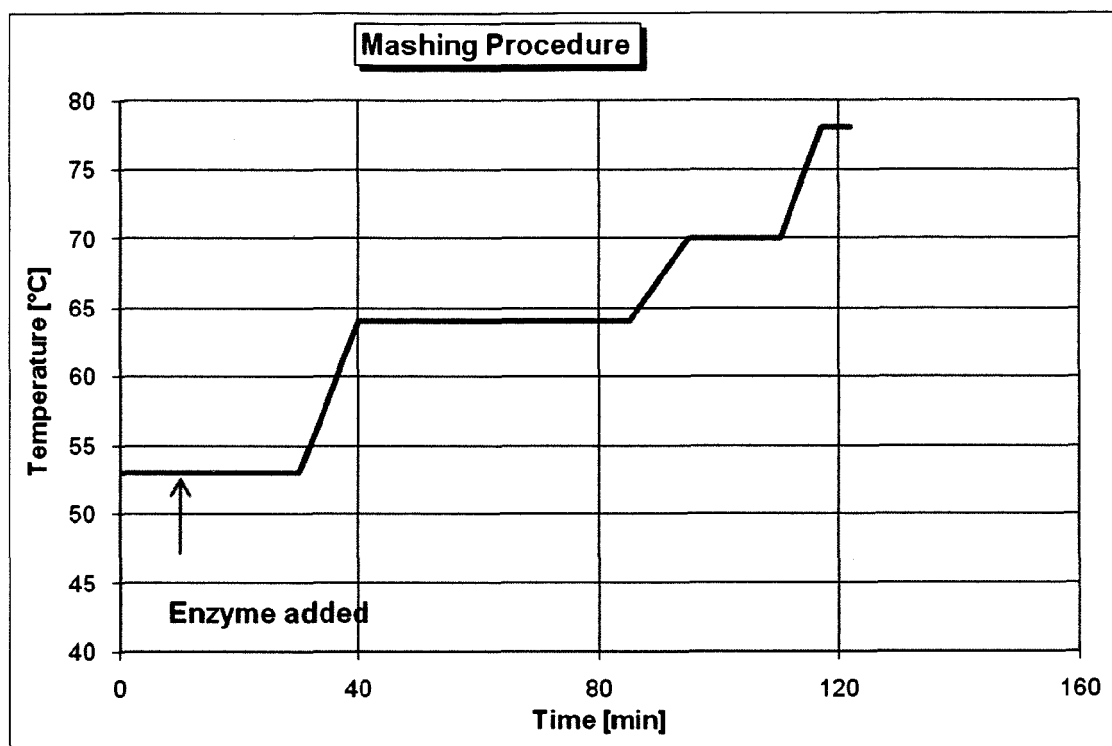


Figure 2

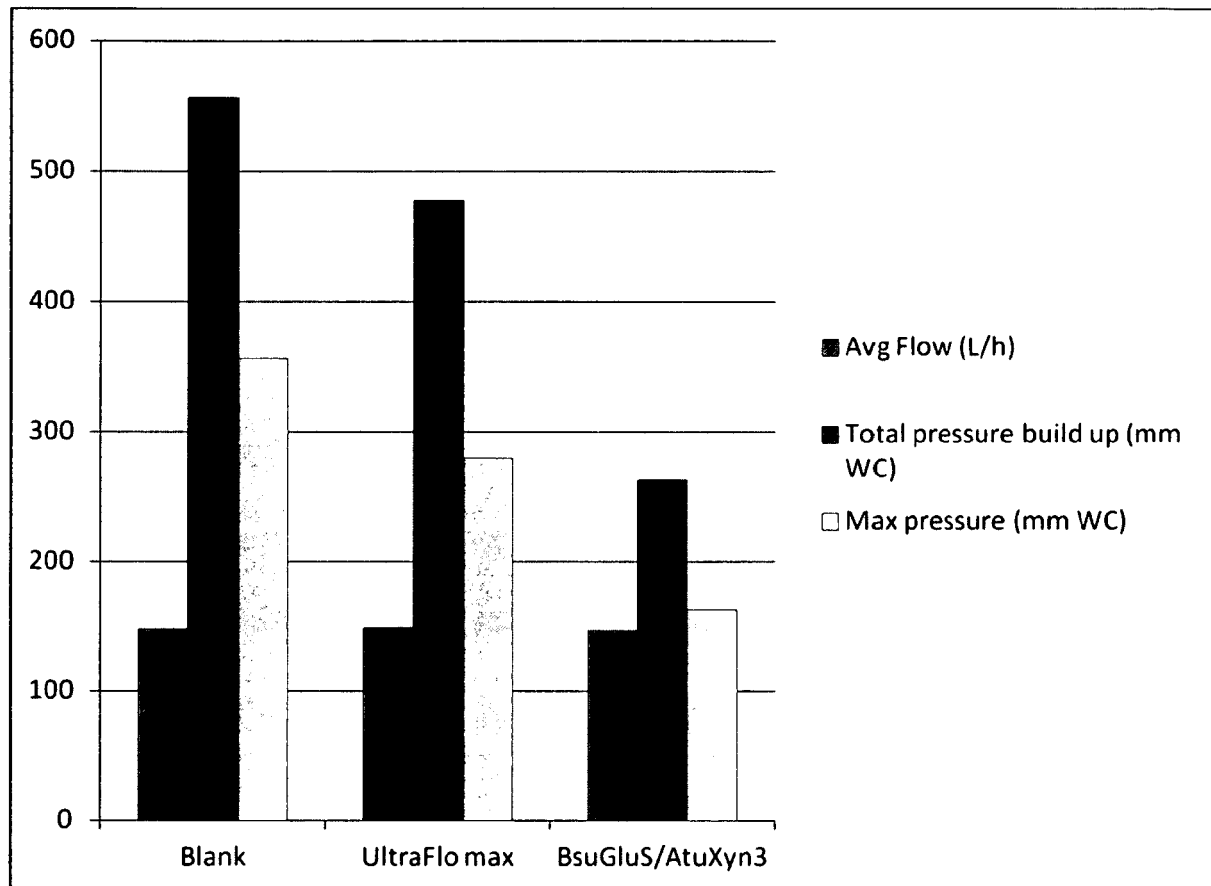


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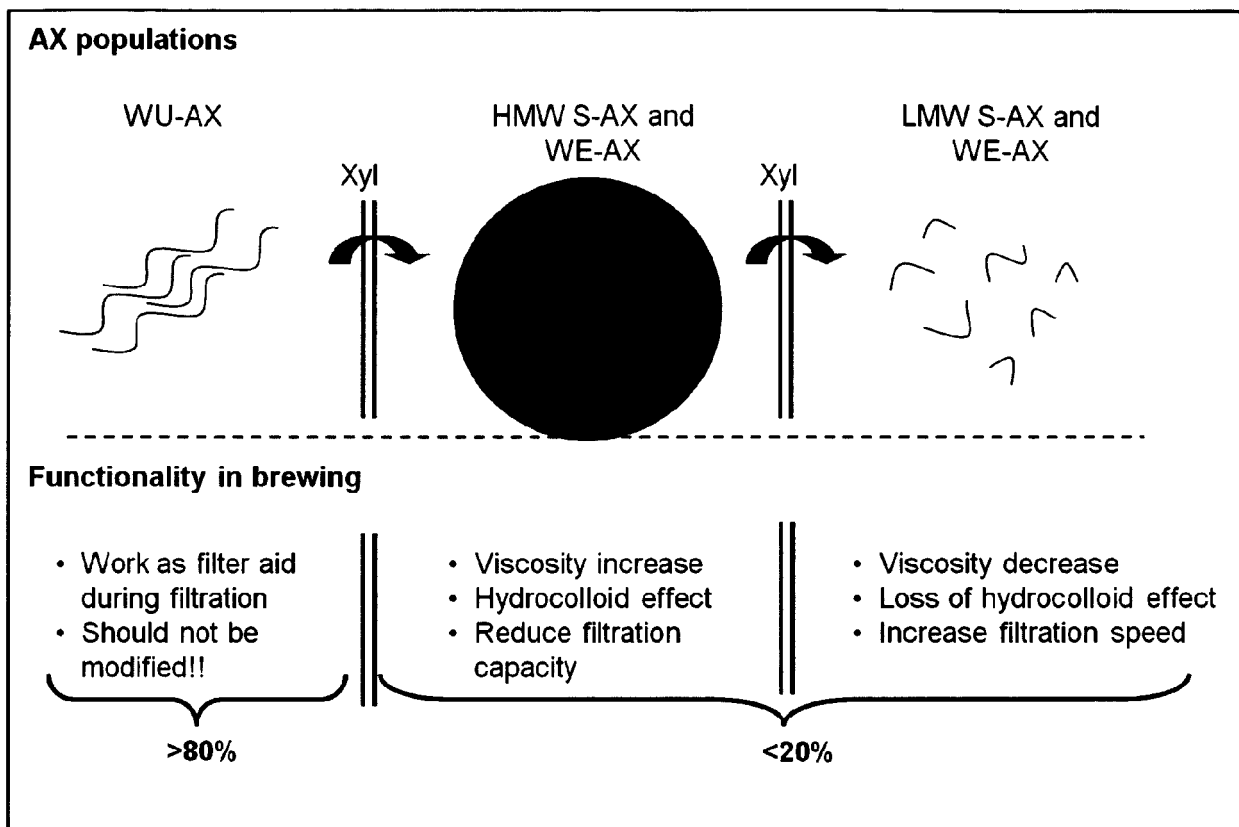


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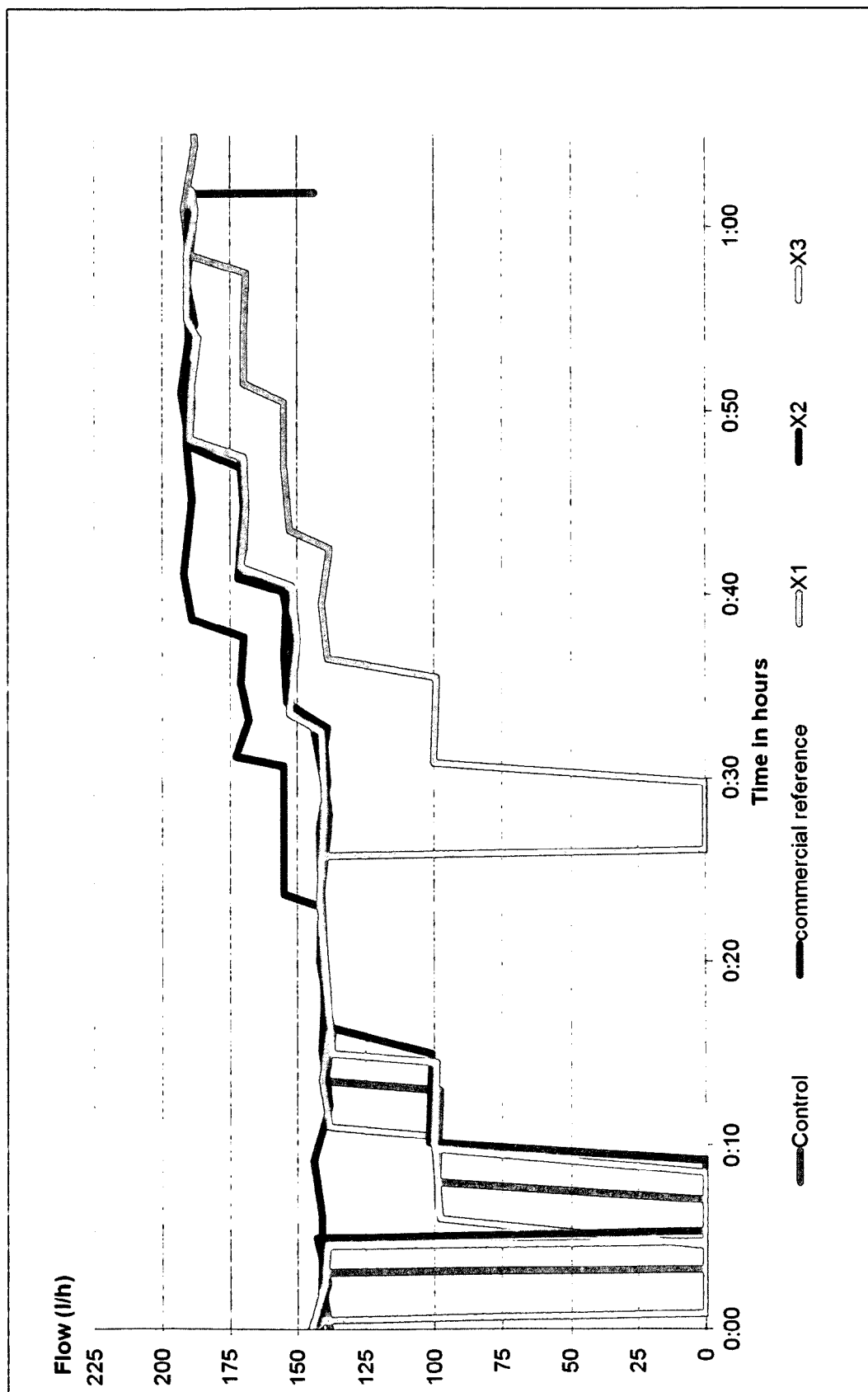


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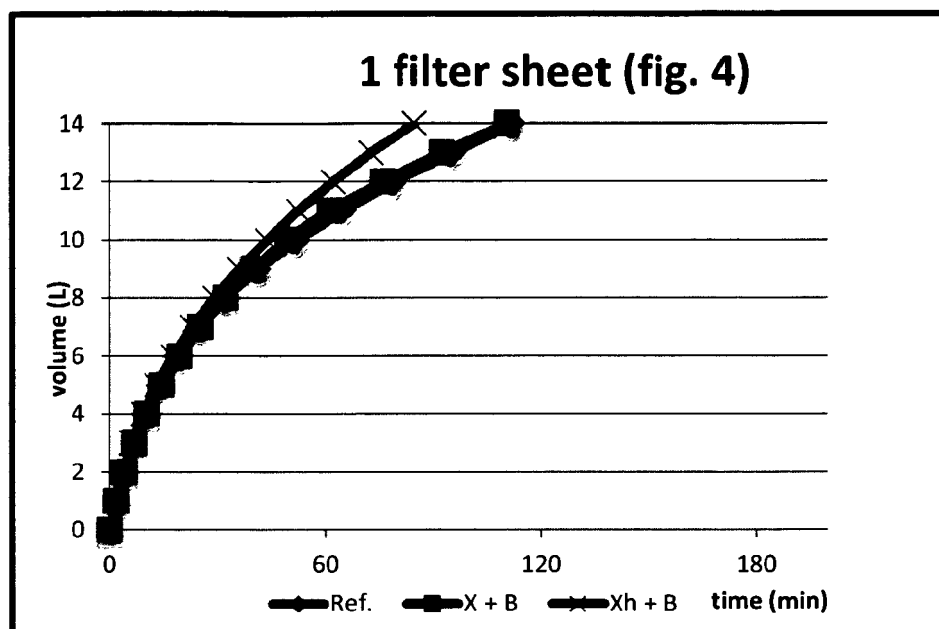


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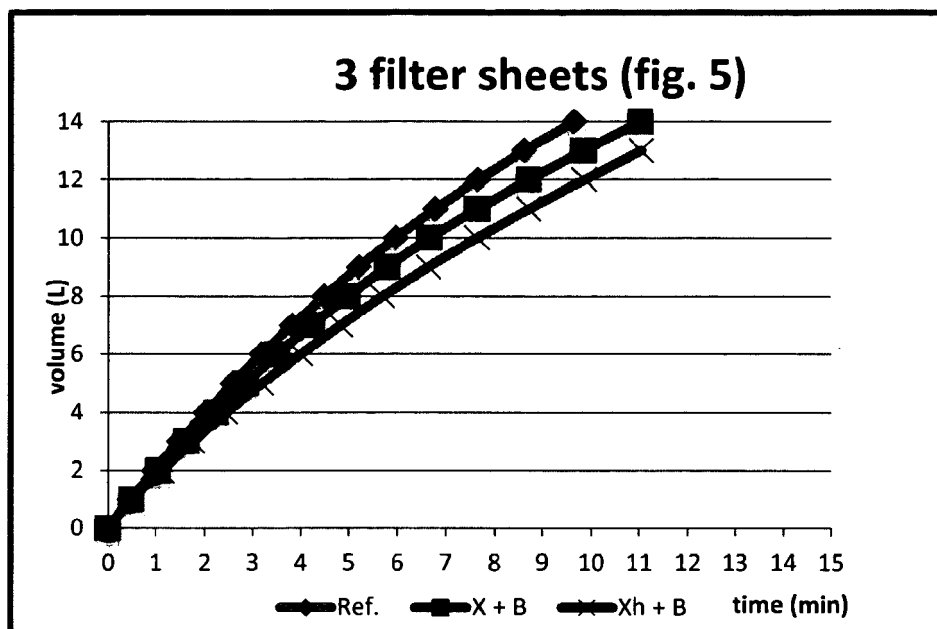
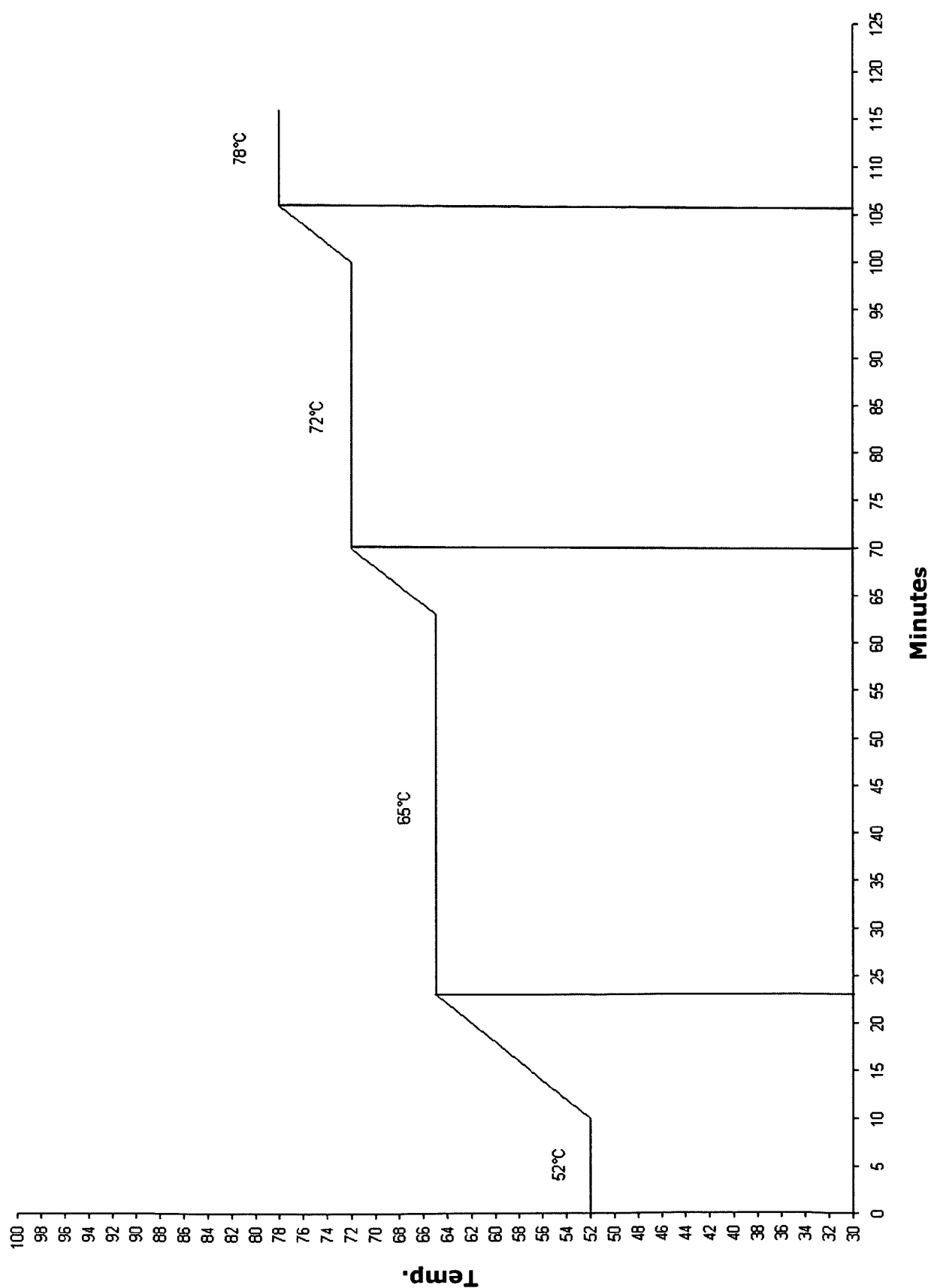


Figure 7



## REFERENCES CITED IN THE DESCRIPTION

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