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### (54) ELECTROCATALYTIC GENERATION OF IMINES FROM ALCOHOLS AND AMINES

(57) A use of an acceptor-less alcohol dehydrogenation catalyst for an electrocatalytic oxidation of an alcohol with an amine, to an imine by electrocatalytic synthesis under electrochemical conditions.

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### Description

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#### Field of the invention

[0001] The invention generally relates to a process of electrocatalytic generation of imines from alcohols and amines using Acceptor-less Alcohol Dehydrogenation (AAD) catalysts.

#### Background of the invention

[0002] Acceptor-less Alcohol Dehydrogenation (AAD) catalysts have become a powerful tool for green synthetic approaches and energy storage over recent years.

**[0003]** Acceptorless alcohol dehydrogenation catalyzed by transition metal complexes was first reported in 1987 by Murahashi et al. (Ruthenium-catalyzed oxidative transformation of alcohols and aldehydes to esters and lactones, J.Org. Chem. 52, 10.1021/jo00228a032).

[0004] In the acceptorless alcohols dehydrogenation reaction, alcohols are dehydrogenated in the presence of a transition metal complex to yield carbonyls compounds, such as aldehydes or ketones, together with molecular hydrogen. As the only byproduct, hydrogen gas is formed, making those systems extremely interesting in terms of atom efficiency and green synthesis.

**[0005]** In particular, AAD catalysts have been used extensively for the oxidation of alcohols to e.g. esters, amides, acids, thiosesters, under thermal conditions (high temperatures).

**[0006]** Various pincer complexes have been reported as AAD catalysts, the transition metal used being e.g. manganese, ruthenium, rhodium, osmium, platinum, cobalt, iridium. Various complexes are commercially available for the acceptorless alcohol oxidation, such as RuCl<sub>3</sub>·nH<sub>2</sub>O/phosphine/NaOH system and [RuCl<sub>2</sub>(p-Cymene)]<sub>2</sub>/diamine ligand, Grubb's catalyst in presence of KOH, base free Shvo di nuclear ruthenium complex, and Milstein complex and various Milstein pincer-ligands.

**[0007]** A recent review of manganese-based pincer complexes as AAD is presented by Chandra et al. (Recent advancement in oxidation or acceptorless dehydrogenation of alcohols to valorized products using manganese based catalysts, Coordination chemistry reviews, 411, 2020, 10.1016/j.ccr.2020.213241). A recent review of pincer transition metal catalysts used for AAD is presented by Piccirilli et al. (Catalysts, 10, 773, 2020, 10.3390/catal10070773). A recent review of homogeneously catalyzed acceptorless dehydrogenation of alcohols is presented by Trincado et al. (Coordination Chemistry Reviews 443, 2021, 10.1016/j.ccr.2021.213967).

**[0008]** Imines are compounds containing the N=C double bond. In other words, imines are related to ketones and aldehydes by replacement of the oxygen with an NR group. When R is H, the compound is a primary imine. When R is hydrocarbyl, the compound is a secondary imine. Various subclass of imines are known, e.g. aldimines having the structure RCH-NH or RCH-NR', ketimines have the structure R'2C=NR (where R' is not H). Imines are versatile functional groups used in pharmaceuticals or agrochemicals, imines being important intermediates in the formation of other organic compounds, e.g. products of reaction of azomethine includes derivatives of pyrazoles, triazoles, triazoles, triazoles.

**[0009]** Classical synthetic pathways to imines generally employ stoichiometric amounts of oxidants and/or high temperature. Recently, there has been growing interest in catalytic processes utilizing biomass-derived alcohols for sustainable production of imines.

**[0010]** Pincer complexes have been tested as catalysts for the dehydrogenation of alcohol and the production of imines. Examples can be found e.g. in Zhang et al. (Cobalt-catalyzed acceptorless alcohol dehydrogenation: synthesis of imines from alcohols and amines, Org. Lett. 15, 2013, 10.1021/0l303479f), Midya et al. (Direct access to N-alkylated amines and imines via acceptorless dehydrogenative coupling catalyzed by a cobalt (ii)-NNN pincer complex, Catal. Sci. Technol. 8, 2018, 10.1039/C8CY00859K), Bottaro et al. (In situ generated cobalt catalyst for the dehydrogenative coupling of alcohols and amines into imines, ChemCatChem, 11, 2019, 10.1002/cctc.201900392).

**[0011]** Higuchi et al. (Tunable ligand effects on ruthenium catalyst activity for selectively preparing imines or amides by dehydrogenative coupling reactions of alcohols and amines, Chem. Eur. J. 2017, 10.1002/chem.201701342) disclose the selective synthesis of imines using  $RuCl_2(dpea)_2$ , in the presence of catalytic amounts of  $Zn(OCOCF_3)_2$  and KOtBu, alcohol being preferably methoxy or methyl substituted benzyl alcohols.

**[0012]** Sindhuja et al. (Direct synthesis of imines from primary alcohols and amines using an active ruthenium pincer complex, Tetrahedron Letters 55, 2014) disclose the use of a ruthenium pincer metal complex, containing bis(benzimidazole)pyridine ligand, for the coupling reaction between benzylalcohol and benzylamine, the temperature being between 30°C and 189°C.

[0013] AAD systems of the prior art have some limitations.

[0014] These systems often work under refluxing conditions to eliminate evolving H<sub>2</sub> gas, thus relying on elevated temperatures.

[0015] When it comes to specific molecular motifs, in particular imines, additional problems arise from difficulties in

selectively oxidizing primary alcohols to the two-electron imine product, without over-oxidation to possible four electron products.

**[0016]** In principal, electrochemistry allows to control the energy input directly via the applied potentials and makes the coupling of chemical reactions to renewable energy resources feasible. In combination with catalysts that allow to follow reaction pathways with minimal thermal dissipation, electrochemistry can thus help to overcome the limitations of thermal chemistry outlined above.

**[0017]** Over recent years, electrochemical processes for the homogeneous electrocatalytic oxidation of alcohols have emerged, using a variety of well-defined catalysts or electro-transfer mediators.

**[0018]** In 2010, Grützmacher et al. have described a fuel cell operating in a strongly basic media (2M KOH) for the oxidation of ethanol to acetate (CH3COO-), using as the anode catalyst a molecular [Rh(OTf)(trop2NH)(PPh3)] complex, deposited on a conductive carbon support (Angewandte Chemie International Edition 2010, 49 (40), 7229-7233, 10.1002/anie.201002234).

**[0019]** In a 2020 review paper, *Cook et al.* have presented the current state-of-the-art for molecular electrocatalysis capable of alcohol oxidation, illustrated by three case studies; namely a copper/nitroxyl radical cooperative catalyst system, noble metal-hydrides with proximal amine group for transfer hydrogenation, nickel hydrides with  $P_2N_2$  ligands (Molecular Electrocatalysts for Alcohol Oxidation: Insights and Challenges for Catalyst Design, ACS Appl. Energy Mater. 2020, 3 (1), 38-46, 10.1021/acsaem.9b01820).

**[0020]** WO2022136475 disclose the use of acceptor-less dehydrogenation catalyst for an electrocatalytic oxidation of an alcohol to an ester or/and an acid.

**[0021]** Although prior art systems demonstrate that electrocatalytic oxidation is possible, they often operate at high potentials (many Tempo-based mediators, Ru=O species), with low turnover number TON for most transition metal-based systems, and limited access to functionalized products involving C-N bonds.

**[0022]** No reports on such systems for the synthesis of imines (or other C-N functionalized alcohol oxidation products) exist to the best of the knowledge of the inventors.

**[0023]** In contrast, classical methodologies to access imines from alcohols and amines due to their thermal nature, do not offer the advantages of electrochemical approaches.

**[0024]** The invention provides AAD catalysts that can be used under electrochemical conditions to conduct the selective oxidation of alcohols in the presence of amines to the corresponding imines.

### 30 Summary of the invention

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**[0025]** Various embodiments are directed to address the effects of one or more of the problems set forth above. The following presents a simplified summary of embodiments in order to provide a basic understanding of some aspects of the various embodiments. This summary is not an exhaustive overview of these various embodiments. It is not intended to identify key/critical elements or to delineate the scope of these various embodiments. Its sole purpose is to present some concepts in a simplified form as a prelude to the more detailed description that is discussed later. The invention provides use of an acceptor-less alcohol dehydrogenation (AAD) catalyst for an electrocatalytic oxidation of an alcohol with an amine, to an imine, by electrocatalytic synthesis,

the acceptor-less dehydrogenation catalyst used under electrochemical conditions being represented by the structure of any one of the formulae F1 or F2:

F1

$$L_{1}$$
 $R_{1}$ 
 $L_{2}$ 
 $R_{2}$ 
 $R_{3}$ 
 $R_{45}$ 
 $R_{1}$ 
 $R_{2}$ 
 $R_{3}$ 
 $R_{45}$ 
 $R_{1}$ 
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L and  $L^*$  being tridentate aliphatic or aromatic pincer ligands, with  $L^*$  being the deprotonated or dearomatized anionic form of the pincer ligand L,

D being a donor group chosen from: a phosphine PR2, tertiary amine NR2, secondary amine NHR, thiol SR, or an N-heterocyclic carbene derived from imidazole, imidazoline, thiazole or triazole units,

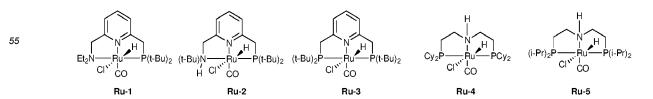
R being a substituent selected from the group of: i-Pr, t-Bu, Cyclohexyl, Bn, Ph, Me, Et, Pr, Bu, H,

X being an anionic ligand, selected from the group of:  $H^-$ ,  $BH_4^-$ ,  $OH^-$ ,  $CI^-$ ,  $Br^-$ ,  $F^-$ ,  $PF_6^-$ ,  $NH_2^-$ ,  $NHR^-$ ,  $NR_2^-$ ,  $OR^-$ , with R as defined above,

L' being a mono-dentate strong field ligand selected from the group of: CO, a phosphine PR3, NO, a nitrile RCN, an isonitrile RNC or an N-heterocyclic carbene, derived from imidazole, imidazoline, thiazole or triazole units, with R as defined above,

L" and L"\* being bidentate ligands with 1 to 4  $\rm CH_2$  units and with R and D as defined above and L"\* being the deprotonated anionic form of the ligand L".

- [0026] Phosphine PR2 are for example monodentate phosphine of the type PR2, R being Ph, Me, Et, i-Pr, t-Bu, Cy.
- [0027] Phosphine PR3 are for example tertiary phosphine PR3, where R is alkyl, aryl, alkoxyl.
- [0028] Advantageously, the electrocatalytic oxidation is carried out in a homogeneous phase.
- [0029] Advantageously, the alcohol oxidation is carried out under neat conditions without added solvent.
- [0030] In some embodiments, the alcohol oxidation is carried out in the presence of a solvent or binary solvent mixtures.
- **[0031]** In other embodiments, the alcohol oxidation is carried out in heterogeneous phase, the acceptor-less dehydrogenation catalyst being immobilized on a conductive support.
  - [0032] Advantageously water is used as solvent and the pH is between 7 and 14.
  - **[0033]** Advantageously, the alcohol oxidation is carried out under potential control, with an applied potential in the range of -0.5-0.5 V vs Ag/AgCl. Advantageously, the alcohol oxidation is carried out under current control, with an applied current between 0.2 and 50 mA.
- **[0034]** In some embodiments, the alcohol oxidation is carried out in a divided electrochemical cell with ratio working electrode surface/cell volume between 0.5 and 10 cm<sup>-1</sup>.
- **[0035]** Advantageously, the alcohol oxidation is carried at a temperature below 60°C. In some embodiments the alcohol oxidation is carried at room temperature without heating.
- **[0036]** In some embodiments, the organometallic catalyst is in contact with a working solution comprising the alcohol, the amine and a base chosen in the group comprising: LiOH, NaOH, KOH, CsOH, tetramethylammonium hydroxide, tetrabutylammonium hydroxide, trimethylbenzylammonium hydroxide, Cs<sub>2</sub>CO<sub>3</sub>, Li<sub>2</sub>CO<sub>3</sub>, NaOPiv, KOPiv, LiOPiv, CsOPiv, tetrabutylammonium dihydrogen phosphate, Na<sup>t</sup>Bu, K<sup>t</sup>Bu, Li<sup>t</sup>Bu, Cs<sup>t</sup>Bu, NaOEt, KOEt, LiOEt, CsOEt, NaOBn, KOBn, LiOBn, CsOBn, or a tertiary amine NR<sub>3</sub>, with R being a substituent selected from the group of: *i*-Pr, t-Bu, Cyclohexyl, Bn, Ph, Me, Et, Pr, Bu, H.
  - **[0037]** In some embodiments, the alcohol is a primary or secondary alcohol of the form HOR' and the amine is a primary amine of the form  $H_2NR'$ , with R' being an alkyl or benzyl group bearing substituents from the group of H, Me, Et, Pr, i-Pr, Bu, n-Bu, cyclopropyl, vinyl, allyl, fluoro, chloro, bromo, iodo, nitro, phenyl, alkoxo, borane, a borate, silyl, siloxyl, vinyl, allyl, furanyl, thiophenyl, a thiolate, an ester, a ketone, a sulfoxide.
- 50 [0038] Advantageously, the amine presents a center of chirality which is maintained in the imine product.
  - [0039] Advantageously, the organometallic catalyst is chosen among the following structures



$$Ph_{2}P \xrightarrow{Ru} PPh_{2} \qquad Ph_{2}P \xrightarrow{Ru} PPh_{2} \qquad EtS \xrightarrow{Ru} SEt \qquad Ph_{2}P \xrightarrow{Ru} PPh_{2} \qquad Ph_{2}P \xrightarrow{Ru} PPh_{2}$$

$$Ru-6 \qquad Ru-7 \qquad Ru-8 \qquad Ru-9 \qquad Ru-10$$

$$(t-Bu)N \xrightarrow{Mn} P(t-Bu)_{2} \qquad (t-Bu)_{2}P \xrightarrow{Nn} P(t-Bu)_{2} \qquad Mn-2$$

**[0040]** In some embodiments, an anodic half-cell reaction is coupled with a cathodic half-cell reaction, the cathodic half-cell reaction being an electrochemical reduction of CO<sub>2</sub> to CO, H<sub>2</sub> production or O<sub>2</sub> reduction and the reaction being carried out in a flow-cell.

[0041] In some embodiments, the alcohol is oxidized with at least 50-100 FE% (Faradaic efficiency), 50-100% amine conversion and 50-100% selectivity (from amine) to an imine, in the presence of 0.1-2 M base, 0.1-3 M alcohol, 0.05-1.5 M amine 0.01-10 mM catalysts, at a potential between -0.5-0.5 V vs Ag/AgCI, using a carbon-based working electrode, in a divided cell with cell dimensions (working electrode surface-to-cell volume) comprised between 0.1 - 10 cm<sup>-1</sup>, the temperature being below 60°C, for instance under argon atmosphere.

**[0042]** In some embodiments, the alcohol is oxidized with at least 50-100 FE% (Faradaic efficiency), 50-100% amine conversion and 50-100% selectivity (from amine) to an imine in the presence of 0.1-2 M Base, at an alcohol to amine ratio between 20:1-200:1, an amine to catalyst ratio of 20:1-200:1 and an alcohol to catalyst ratio of 50:1-5000:1, at a potential between -0.5-0.5 V vs Ag/AgCl, using a carbon-based working electrode, in a divided cell with working electrode surface-to-cell volume comprised between 0.1-10 cm<sup>-1</sup>, at a temperature below 60°C.

[0043] Detailed description

**[0044]** Examples presented below concerns the synthesis of imines from amines and alcohols. The amine can be an aliphatic amine, or a benzylic amine. The reaction scheme and conditions for the selective electrocatalytic synthesis of imines from alcohol and amines, together with possible other side-products is presented below:

**[0045]** Possible side-products are an aldehyde, ester, secondary amine. Advantageously, the synthesis is conducted at room temperature (25°C), and ambient pressure.

**[0046]** Advantageously, the synthesis is conducted without the use of solvent. In the presented scheme, the working electrode (WE) is a carbon cloth and the counter electrode (CE) is Pt-mesh, the cell being a divided cell. The use of carbon cloth ensures the effective penetration of electrolyte into the electrode surface.

**[0047]** The reference electrode is an Ag/AgCl electrode, and the working electrode is maintained at a constant potential of 0.3V (controlled potential electrolysis CPE).

**[0048]** The process is demonstrated in a home-made 8 mL working compartment H-Cell, using a simple carbon cloth as the working electrode (3x 1\*1\*0.5 cm carbon felt connected to 2.0\*0.6 cm graphite rod) under controlled potential (CPE, vs. Ag/AgCl) with shut-off after 2F electrons corresponding to reaction times generally between 4-6 hours.

**[0049]** In the examples given below, the following range of catalysts were successfully tested for the reaction presented in the above scheme.

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**[0050]** Elevated conversion of amine and high imine selectivity is obtained using the above-mentioned catalysts Ru1-Ru10 or Mn-1 for the reaction presented in the above scheme. Results are given below, in standard condition: neat 0.2M LiOH/BnOH (6mL), 50  $\mu$ L hexylamine, 1.3 mM catalyst, CPE 0.3 V vs Ag/AgCl, 25°C, 2F mol amine.

**[0051]** For Ru-1, Ru-2, Ru5, Ru-10 and Mn-1, imine selectivity is higher than 99%. For Ru-3, Ru6, Ru7 and Ru8, imine selectivity is 99%. The reaction scheme and conditions for the electrocatalytic synthesis of imines from alcohol and amines enable the production of imines nearly without any other side-products such as aldehyde, ester or secondary amine.

Entry	Catalyst	Con	version	Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1	Ru-1	>99	0.40	>99	102
2	Ru-2	>99	0.34	>99	85
3	Ru-3	>99	0.33	99	85
4	Ru-4	62	0.22	65	55
5	Ru-5	90	0.26	>99	66
6	Ru-6	93	0.25	99	65
7	Ru-7	97	0.27	99	69
8	Ru-8	91	0.27	99	70
9	Ru-9	72	0.25	65	63
10	Ru-10	93	0.36	>99	66
11	Mn-1	>99	0.38	>99	98

**[0052]** In standard condition (neat 0.2M LiOH/BnOH (6mL), 0.38 mmol amine, 1.3 mM catalyst, CPE 0.3 V vs Ag/AgCl, 25°C, 2F mol per amine), elevated conversion of various amines and high imine selectivity is obtained using the abovementioned catalysts Ru1-Ru10 or Mn-1 for the reaction presented in the above scheme. Results are presented below for various amines (aliphatic or aromatic).

Entry	Amine	Conversion		Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1	NH <sub>2</sub>	>99	0.40	>99	102
2	NH <sub>2</sub>	>99	0.41	>99	105
3	NH <sub>2</sub>	85	0.43	76	99
4	NH <sub>2</sub>	22	0.14	77	35
5	NH <sub>2</sub>	>99	0.42	>99	107
6	>···NH <sub>2</sub>	>99	0.38	>99	98
7	NH <sub>2</sub>	>99	0.44	99	110
8	NH <sub>2</sub>	75	0.31	>99	80
9	Br NH <sub>2</sub>	>99	0.46	>99	110
10	Br—NH <sub>2</sub>	98	0.41	>99	103
12	F <sub>3</sub> C—NH <sub>2</sub>	99	0.34	>99	88
12	CF <sub>3</sub> NH <sub>2</sub>	88	0.39	99	101
13	NH <sub>2</sub>	>99	0.43	>99	110
14	NH <sub>2</sub>	>99	0.41	>99	106
15	MeO NH <sub>2</sub>	>99	0.43	>99	108

(continued)

Entry	Amine	Con	Conversion		F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
16	OMe NH <sub>2</sub>	84	0.34	>99	88
17	$H_2N$ $NH_2$	69	0.29	>99 (diamine)	75

**[0053]** Results of different alcohol derivatives screened in the study in standard condition (3 M alcohol, 0.2 M Li-OH/(THF/H2O - 7:1 v/v) (6 mL), 0.38 mmol n-hexylamine, 1.3 mM catalyst, CPE 0.3 V vs Ag/AgCl, 25oC, 2F mol amine) are presented below:

Entry	Alcohol	Con	version	Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1*	ОН	>99	0.40	>99	102
2	ОН	52	0.18	93	47
3	,o-(OH	86	0.31	95	79
4	Me OH	60	0.22	72	68
5	Me—OH	90	0.36	98	94
6	F <sub>3</sub> C OH	90	0.34	73	104
7	BrOH	42	0.16	91	42
8	Br—OH	53	0.22	90	56
9	CF <sub>3</sub> OH	82	0.28	91	75
10	NO <sub>2</sub> OH	52	0.21	>99	53

(continued)

Entry	Alcohol	Conversion		Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
11	O <sub>2</sub> N—OH	26	0.06	80	17
12	—о ОН — ОН	72	0.39	>99	100

[0054] A variety of amine nucleophiles can be used for the generation of the corresponding imines, including aliphatic, benzylic and aromatics.

**[0055]** A variety of functional groups can be tolerated such as, bromo, trifluromethyl, nitro, methyl, thiophenyl, furanyl and methoxy substituents.

[0056] A number of different parameters were optimized in order to obtain the desirable results.

**[0057]** These parameters include the concentration of the alcohol, the nature of co-solvents, the alcohol to amine ratio, the nature and concentration of the supporting electrolyte/base, water content, working potential, as well as cell/electrode dimensions.

[0058] Some results are presented below.

**[0059]** By finely tuning the reaction conditions, such as concentration ranges, electrolyte composition, electrochemical cell dimensions, applied potential, it is possible to selectively carry out the two-electron oxidation of alcohols in the presence of amines to the imine product with negligible amount of 4-electron overoxidation products and complete conversion of the limiting amine reagent.

### Effect of the electrolyte composition

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[0060] Results of different electrolyte (base) screened in the study in standard condition (neat 0.1M BnOH (6 mL),  $100 \mu L$  hexylamine (130 mM), 1.3 mM Ru-1, CPE 0.3 V vs Ag/AgCl, 25°C, 6 hours) are presented below:

Entry	Electrolyte (0.1 M)	Con	version	Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1	LiOH	43	0.31	96	90
2	NaOH	41	0.31	95	98
3	КОН	28	0.20	96	102
4	CsOH	34	0.26	95	108
5	Cs <sub>2</sub> CO <sub>3</sub>	13	0.11	90	135
6	Li <sub>2</sub> CO <sub>3</sub>	4	0.04	78	373
7	(CH <sub>3</sub> ) <sub>3</sub> CCOOK	0	0	0	0
8	(C <sub>4</sub> H <sub>9</sub> ) <sub>4</sub> NH <sub>2</sub> PO <sub>4</sub>	15	0.14	86	158
9	(CH <sub>3</sub> ) <sub>4</sub> NOH *10% of water presence	49	0.34	95	62

### Effect of electrolyte concentration

[0061] Results of different electrolyte (base) concentration screened in the study in standard condition (neat 0.1M BnOH (6 mL),  $100 \mu L$  hexylamine (130 mM),  $1.3 \mu L$  nexylamine (130

Ī	Entry	[LiOH] (M)	Con	version	Selectivity (%)	F.E. (%)
			Amine (%)	BnOH (mmol)	Imine	
	1	0.1	43	0.31	96	90
	2	0.2	62	0.49	92	77
	3	0.5	32	0.24	97	99
	4	1.0	29	0.21	98	101

### Effect of alcohol concentration

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[0062] Results of different benzyl alcohol (BnOH) concentration screened in the study in standard condition (0.1M LiOH 1:7 v/v  $H_2O/THF^*$ , 100  $\mu$ L hexylamine (130 mM), 1.3 mM Ru-1, CPE 0.3 V vs Ag/AgCl, 25°C, 6 hours) are presented below.

\*(the amount of BnOH was replaced by for retaining the total amount of working solution at 6 mL)

Entry	[BnOH] (M)	Conversion		Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1	Neat	43	0.31	96	90
2	3.0	32	0.20	88	70
3	1.6	30	0.20	84	55
4	0.6	46	0.29	73	29

### Effect of amine concentration

**[0063]** Results of different amine concentration screened in the study in standard condition (0.1M LiOH/BnOH, x mM hexylamine, 1.3 mM Ru-1, CPE 0.3 V vs Ag/AgCl, 25oC, 6 hours) are presented below:

Entry	[Hexylamine] (mM)	Conversion		Selectivity (%)	F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1	1,500	0.01	0.06	96	28
2	130	62	0.49	92	77
3	63	100	0.39	85	84

# Effect of solvent

**[0064]** Results of different solvent screened in the study in standard condition (0.1M LiOH/solvent, 0.6 M BnOH, 130 mM hexylamine, 1.3 mM Ru-1, CPE 0.3 V vs Ag/AgCl, 25oC, 6 hours) are presented below:

Entry	Solvent (0.1 M LiOH)	Con	Conversion		F.E. (%)
		Amine (%)	BnOH (mmol)	Imine	
1	Neat	43	0.31	96	90
2	CH <sub>2</sub> Cl <sub>2</sub> /water (7:1)	20	0.15	84	78
3	PhCF <sub>3</sub> /water (7:1)	4	0.087	94	980
4	THF/water (7:1)	46	0.29	73	29
5	1,4-Dioxane/water (7:1)	22	0.23	96	32

## Effect of applied potential

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[0065] Table below allows comparison of blank experiments to standard conditions in terms of amine conversion, as well as product selectivity. (neat 0.2 M LiOH/BnOH (6 mL), 50  $\mu$ L hexylamine, 25 °C, 6 hours, 1.3 mM catalyst, CPE 0.3 V vs Ag/AgCl; the presence of two latter conditions is indicated in the table):

Entry	Catalyst	Applied potential	Conversion		Selectivity (%)	F.E.
			Amine (%)	BnOH (mmol)	Imine	(%)
1	•	•	43	0.31	96	90
2	•	-	11	0.03	100	-
3	-	•	4	0.02	50	4
4	-	-	0	0	0	-
5	As entry 4, the 1.2 mL of 1 M (CH <sub>3</sub> ) <sub>4</sub> NOH/H <sub>2</sub> O solution was replaced LiOH and BnOH		6	0.03	79	-

**[0066]** In the absence of applied potential, or catalysts, or both, conversions under otherwise identical conditions are negligible (<15%), demonstrating the electrification of the AAD systems.

### Possible industrial applications

[0067] Possible applications of the invention are anyone or a combination of the following:

- safe, room temperature and energy efficient (as controlled) synthesis of imines from renewable feedstock (alcohol),
- use as a anode reaction for electrolyzers (H<sub>2</sub> or CO<sub>2</sub>) for the co-generation of imines from renewable feedstock (alcohols) with small molecule transformation (CO<sub>2</sub> reduction, H<sub>2</sub> production, O<sub>2</sub> reduction),
- value-added co-generation of oxidized products in low-voltage (compared to oxygen evolution) electrolyzers (e.g. in water reduction, CO<sub>2</sub> reduction etc.),
- association with other electrochemical set-ups, such as convergent synthetic routes, e.g. with concomitant reduction of nitro-compounds to amines on the cathode and utilization of the so-formed amines in the anodic coupling reactions;
- hydrogen release from small amino-alcohols (equally via intermolecular coupling) to form possible cyclic iminehydrogen storage molecules.

### Advantages of the invention

**[0068]** The invention combines the advantages of homogeneous electrocatalysis with the selectivities and products so-far only observed under thermal conditions, opening the way towards more sustainable synthetic procedures. Using thermal AAD catalysts in an electrochemical set-up that produces imines is an important step beyond the current state-of-the-art in homogeneous electrocatalysis.

[0069] The technology can be used to generate amount of imine on a reasonable time scale (roughly 6 h) at room temperature.

**[0070]** An alcohol (preferentially under neat conditions) can be oxidized in the presence of an amine as the limiting agent to the corresponding imine with the help of an Acceptor-less Alcohol Dehydrogenation catalysts and an applied potential. Some of the AAD are commercially available.

**[0071]** The invention allows to form the corresponding imine with excellent conversions (generally above >95%), selectivities (around 80%) and faradaic efficiency (up to 100%) at catalyst loading of 1 mM, low working potential of 0.3 V vs Ag/AgCl and at room temperature (25°C).

**[0072]** A large range of ruthenium pincer complexes can be employed successfully. Under the employed conditions, catalytic turnover is generally in the order of 30-50 TONs.

**[0073]** The process allows to retain chiral centers, making it possibly attractive for pathways towards chiral (pharmaceutical) molecular targets.

**[0074]** An electrochemical approach benefits from the advantages of electrochemistry, such as safety, scalability, cheapest redox agent (electron), possibility to couple to other redox processes, direct usage of renewable energy for chemical synthesis and importantly direct control of the energy input.

**[0075]** The use of potentially renewable feedstocks, such as alcohols, for the production of imines under energy efficient conditions (energy input controlled) is a key development towards more sustainable processes for fine chemistry.

#### 5 Claims

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- 1. A use of an acceptor-less alcohol dehydrogenation catalyst for an electrocatalytic oxidation of an alcohol with an amine, to an imine by electrocatalytic synthesis under electrochemical conditions,
- the acceptor-less dehydrogenation catalyst used under electrochemical conditions being represented by the structure of any one of the formulae F1 or F2:

F1

$$L_{m,N} = L_{m,N} =$$

F2

$$L^{"n} = \frac{X}{X} \quad \text{or} \quad L^{"*n} = \frac{X}{X} \quad \text{or} \quad L^{"n} = \frac{L}{X} \quad \text{or} \quad L^{"*n} = \frac{L}{X} \quad \text{or}$$

L and L\* being tridentate aliphatic or aromatic pincer ligands of the type shown-above, with L\* being the deprotonated or dearomatized anionic form of the pincer ligand L,

D being a donor group chosen from: a phosphine PR2, tertiary amine NR2, secondary amine NHR, thiol SR, or an N-heterocyclic carbene derived from imidazole, imidazoline, thiazole or triazole units,

with R being a substituent selected from the group of: i-Pr, t-Bu, Cyclohexyl, Bn, Ph, Me, Et, Pr, Bu, H,

X being an anionic ligand, selected from the group of:  $H^-$ ,  $BH_4^-$ ,  $OH^-$ ,  $CI^-$ ,  $Br^-$ ,  $F^-$ ,  $PF_6^-$ ,  $NH_2^-$ ,  $NHR^-$ ,  $NR_2^-$ ,  $OR^-$ , with R as defined above,

L' being a mono-dentate strong field ligand selected from the group of: CO, a phosphine PR3, NO, a nitrile RCN, an isonitrile RNC or an N-heterocyclic carbene, derived from imidazole, imidazoline, thiazole or triazole units, with R as defined above,

L" and L"\* being bidentate ligands as shown above with 1 to 4 CH<sub>2</sub> units and with R and D as defined above and L"\* being the deprotonated anionic form of the ligand L".

- 2. The use according to claim 1, wherein in that the electrocatalytic alcohol oxidation is carried out in a homogeneous phase.
- 3. The use according to claim 2, wherein the electrocatalytic alcohol oxidation is carried out under neat conditions without added solvent.

- **4.** The use according to claim 2, wherein that the electrocatalytic alcohol oxidation is carried out in the presence of a solvent or binary solvent mixtures.
- **5.** The use according to claim 1, wherein in that the electrocatalytic alcohol oxidation is carried out in heterogeneous phase, and in that the acceptor-less dehydrogenation catalyst is immobilized on a conductive support.
  - 6. The use according to anyone of claims 1, 2, 4 or 5, wherein solvent is water and the pH is between 7 and 14.

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- 7. The use according to anyone of claims 1 to 6, wherein the electrocatalytic alcohol oxidation is carried out under potential control, with an applied potential in the range of -0.5-0.5 V vs Ag/AgCl.
  - **8.** The use according to anyone of claims 1 to 6, wherein the electrocatalytic alcohol oxidation is carried out under current control, with an applied current between 0.2 and 50 mA.
- **9.** The use according to anyone of claims 1 to 8, wherein the electrocatalytic alcohol oxidation is carried out in a divided electrochemical cell with a ratio of working electrode surface to cell volume between 0.5 and 10 cm<sup>-1</sup>.
  - **10.** The use according to anyone of claims 1 to 9, wherein the electrocatalytic alcohol oxidation is carried at a temperature below 60°C.
  - **11.** The use according to anyone of claims 1 to 10, wherein the electrocatalytic alcohol oxidation is carried at room temperature without heating.
  - 12. The use according to anyone of claims 1 to 11, wherein in that the organometallic catalyst is in contact with a working solution comprising the alcohol, the amine and a base chosen in the group comprising: LiOH, NaOH, KOH, CsOH, tetramethylammonium hydroxide, tetrabutylammonium hydroxide, trimethylbenzylammonium hydroxide, Cs<sub>2</sub>CO<sub>3</sub>, Li<sub>2</sub>CO<sub>3</sub>, NaOPiv, KOPiv, LiOPiv, CsOPiv, tetrabutylammonium dihydrogen phosphate, Na¹Bu, K¹Bu, Li¹Bu, Cs¹Bu, NaOEt, KOEt, LiOEt, CsOEt, NaOBn, KOBn, LiOBn, CsOBn, or a tertiary amine NR<sub>3</sub>, with R being a substituent selected from the group of: *i*-Pr, *t*-Bu, Cyclohexyl, Bn, Ph, Me, Et, Pr, Bu, H.
  - **13.** The use according to anyone of claims 1 to 12, wherein in that the alcohol oxidized is a primary or secondary alcohol of the form HOR' and the amine is a primary amine of the form H<sub>2</sub>NR', with R' being an alkyl or benzyl group bearing substituents from the group of: H, Me, Et, Pr, *i*-Pr, Bu, n-Bu, cyclopropyl, vinyl, allyl, fluoro, chloro, bromo, iodo, nitro, phenyl, alkoxo, borane, a borate, silyl, siloxyl, vinyl, allyl, furanyl, thiophenyl, a thiolate, an ester, a ketone, a sulfoxide.
  - **14.** The use according to anyone of claims 1 to 13, wherein the amine presents a center of chirality which is maintained in the imine product.
- **15.** The use according to anyone of claims 1 to 14, wherein in that the organometallic catalyst is chosen among the following structures

$$(t-Bu)N \xrightarrow{N} Mn \xrightarrow{Br} P(t-Bu)_2$$

$$(t-Bu)_2P \xrightarrow{N} CO \xrightarrow{N} P(t-Bu)_2$$

$$Mn-1 \qquad Mn-2$$

- 16. The use according to anyone of claim 1 to 15, wherein in that an anodic half-cell reaction is coupled with a cathodic half-cell reaction, the cathodic half-cell reaction being an electrochemical reduction of CO<sub>2</sub> to CO, H<sub>2</sub> production or O<sub>2</sub> reduction and the reaction being carried out in a flow-cell.
- 17. The use according to anyone of claims 1 to 16, wherein in that the alcohol is oxidized with at least 50-100 FE% (Faradaic efficiency), 50-100% amine conversion and 50-100% selectivity (from amine) to an imine in the presence of 0.1-2 M Base, 0.1-3 M alcohol, 0.05-1.5 M amine 0.01-10 mM catalysts, at a potential between -0.5-0.5 V vs Ag/AgCl, using a carbon-based working electrode, in a divided cell with working electrode surface-to-cell volume comprised between 0.1 10 cm<sup>-1</sup>, at a temperature below 60°C.
- **18.** The use according to anyone of claims 1 to 17, wherein in that the alcohol is oxidized with at least 50-100 FE% (Faradaic efficiency), 50-100% amine conversion and 50-100% selectivity (from amine) to an imine in the presence of 0.1-2 M Base, at an alcohol to amine ratio between 20:1-200:1, an amine to catalyst ratio of 20:1-200:1 and an alcohol to catalyst ratio of 50:1-5000:1, at a potential between -0.5-0.5 V vs Ag/AgCl, using a carbon-based working electrode, in a divided cell with working electrode surface-to-cell volume comprised between 0.1-10 cm<sup>-1</sup>, at a temperature below 60°C.



# **EUROPEAN SEARCH REPORT**

**Application Number** 

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